

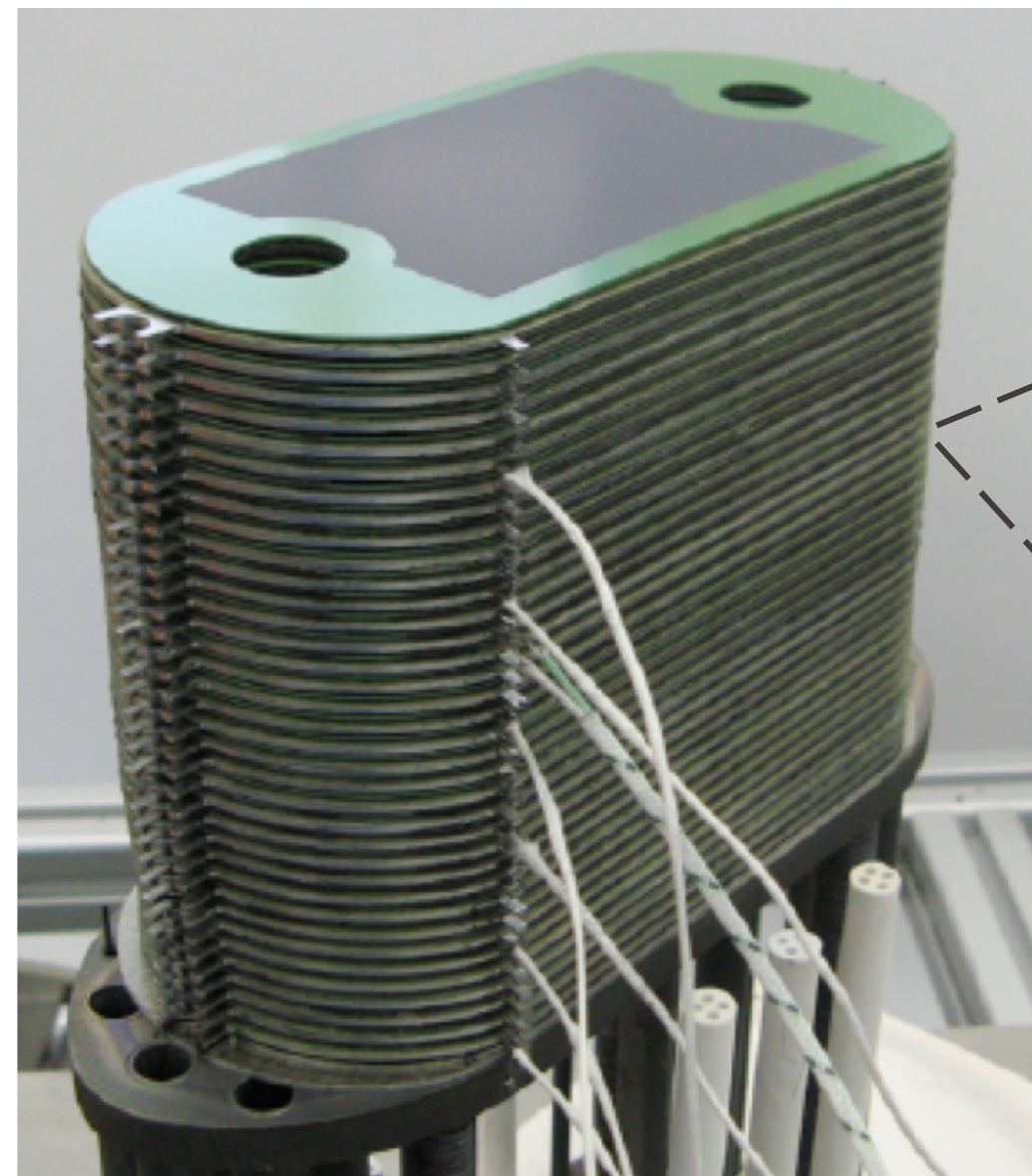
# Flow case 3: Fuel cell

## Numerical Flow Simulation

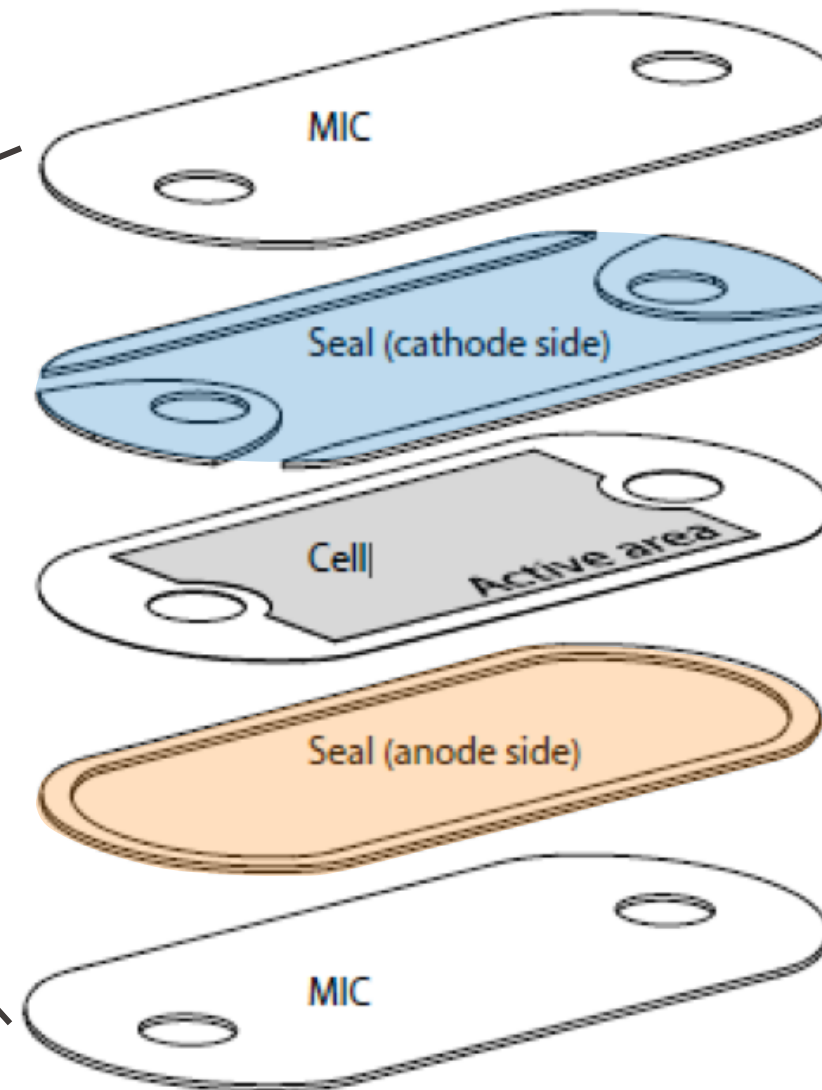
# Physical problem

- A solid-oxide fuel cell is used to generate electrical power through the reaction of fuel (containing  $\text{H}_2$ ) and air (containing  $\text{O}_2$ )
- Air is circulated across the cell to:
  - provide oxygen for the electrochemical reaction
  - dissipate the heat generated

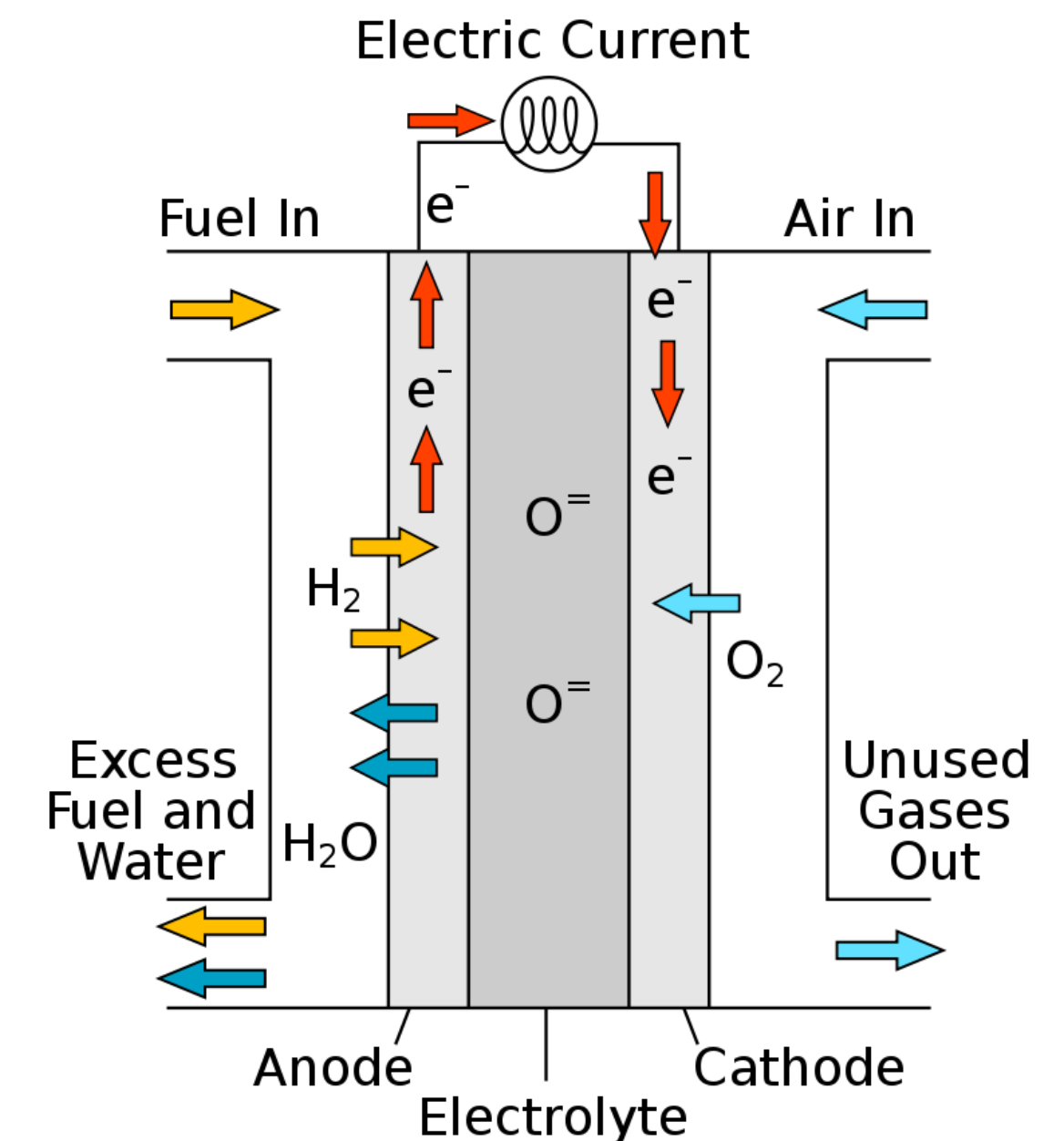
Numerical Flow Simulation



Fuel cell stack



One cell module

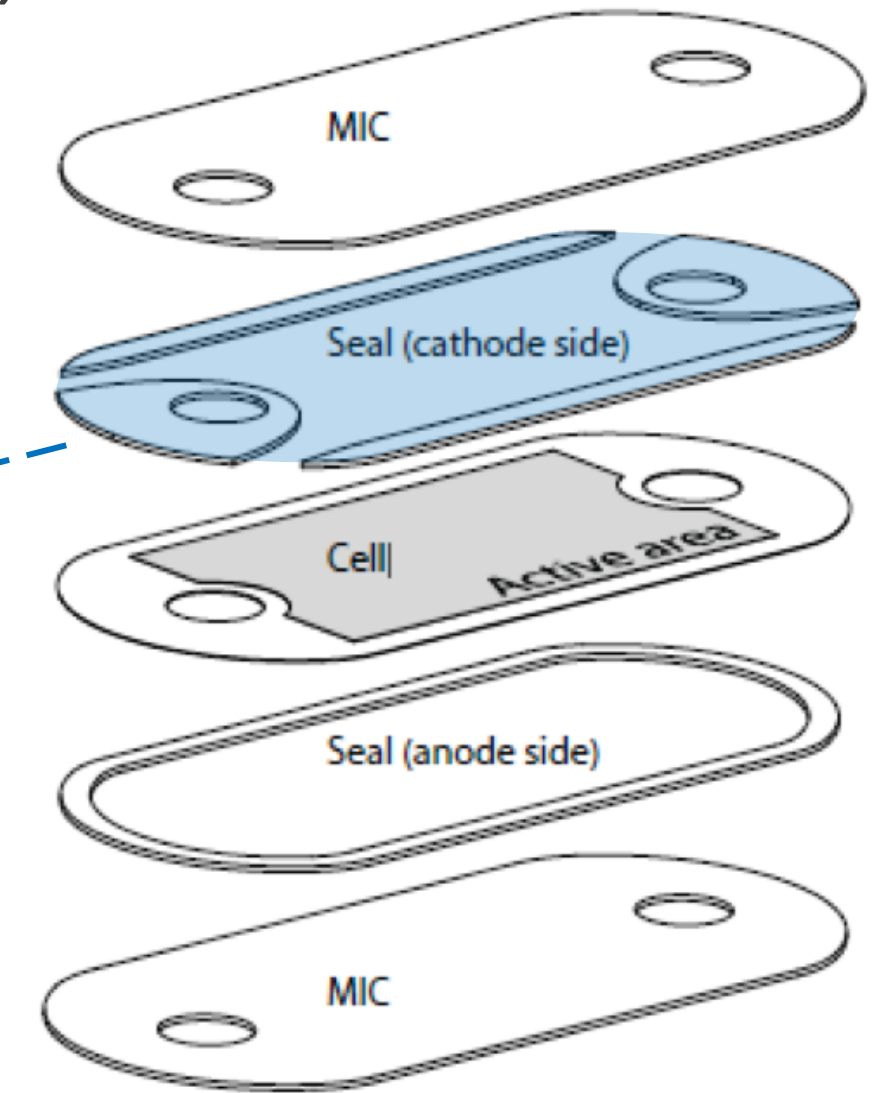
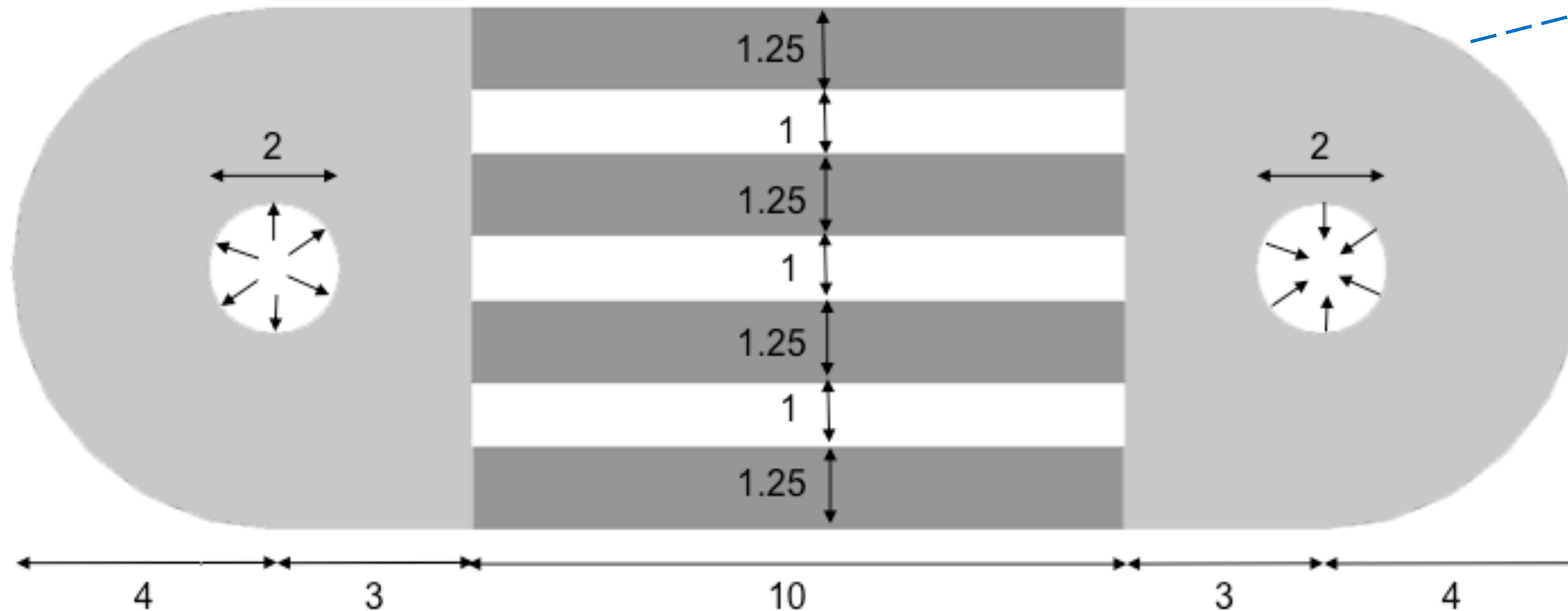


# Physical problem

- Goals of present numerical simulation study:
  1. Compute 2D solution for a simplified version of the problem
    - Neglect details of electrical power generation process
    - Simplify heat generation by imposing fixed surface heating rate
    - Simplify geometry by considering 2D problem
  2. Questions to resolve:
    - Are these approximations valid? Do they influence the flow?
    - How can they be improved to make the simulation results more realistic?

# Fuel cell geometry

- Simplified geometry:
  - 2D horizontal cross-section through one cell module (ignore vertical flow)
  - Oblong section with circular end sections (total length  $L = 24$  cm)
  - Circular inflow & outflow sections (diameter 2 cm)
  - 3 inserts (each of width 1 cm)
  - 4 flow channels (each of width 1.25 cm)





# Flow conditions

## ■ Flow and thermal conditions:

- uniform inflow velocity  $V = 4 \text{ m/s}$
- inflow turbulence intensity 10%
- inflow temperature  $T = 1000 \text{ K}$
- uniform heat generation rate in 4 flow channels  $Q = 10 \text{ MW/m}^3$
- outer cell wall and sidewalls of 3 rectangular inserts assumed adiabatic

## ■ Material properties (high-temperature air):

- air density,  $\rho = 0.34 \text{ kg/m}^3$
- dynamic viscosity,  $\mu = 4.30 \times 10^{-5} \text{ Pa s}$
- specific heat capacity at constant pressure,  $C_p = 1145 \text{ J/kg K}$
- thermal conductivity,  $k = 0.068 \text{ W/m K}$

Gravitation and associated buoyancy effects, as well as radiation, are to be neglected.

# Flow conditions

- Dimensionless numbers

- Reynolds number

- $Re = \rho VL/\mu = 7'600$
    - Slightly turbulent flow
    - Relatively thick velocity boundary layer (thickness  $\delta \sim x/Re^{1/2}$ )  
→ choice of boundary-layer mesh, and wall treatment for turbulence model

- Mach number

- $M_\infty = V/c = V/(\gamma RT/M_{\text{air}})^{1/2} = 0.006 \ll 1$  ( $\gamma = 1.4$ ,  $R = 8.314 \text{ J/(mol.K)}$ ,  $M_{\text{air}} = 0.029 \text{ kg/mol}$ )
    - Flow can be considered as incompressible  
→ choice of physical model for fluid, and numerical method

# Flow conditions

- Dimensionless numbers

- Prandtl number (depends only on material)

- $Pr = \text{momentum diffusivity} / \text{thermal diffusivity} = \mu / (k / C_p) = 0.74$

- Thermal boundary layer,  $\delta_t \sim \delta / Pr^{-1/3} \sim 1.1 \delta$

- thermal boundary layer as thin as velocity boundary layer

- Brinkman number

- $Br = \text{heat produced by viscous dissipation} / \text{heat transported by conduction}$   
 $= \mu V^2 / k (T_w - T_f) \ll 1$  for air in general

- viscous heating effects can be neglected (in turbulence model)

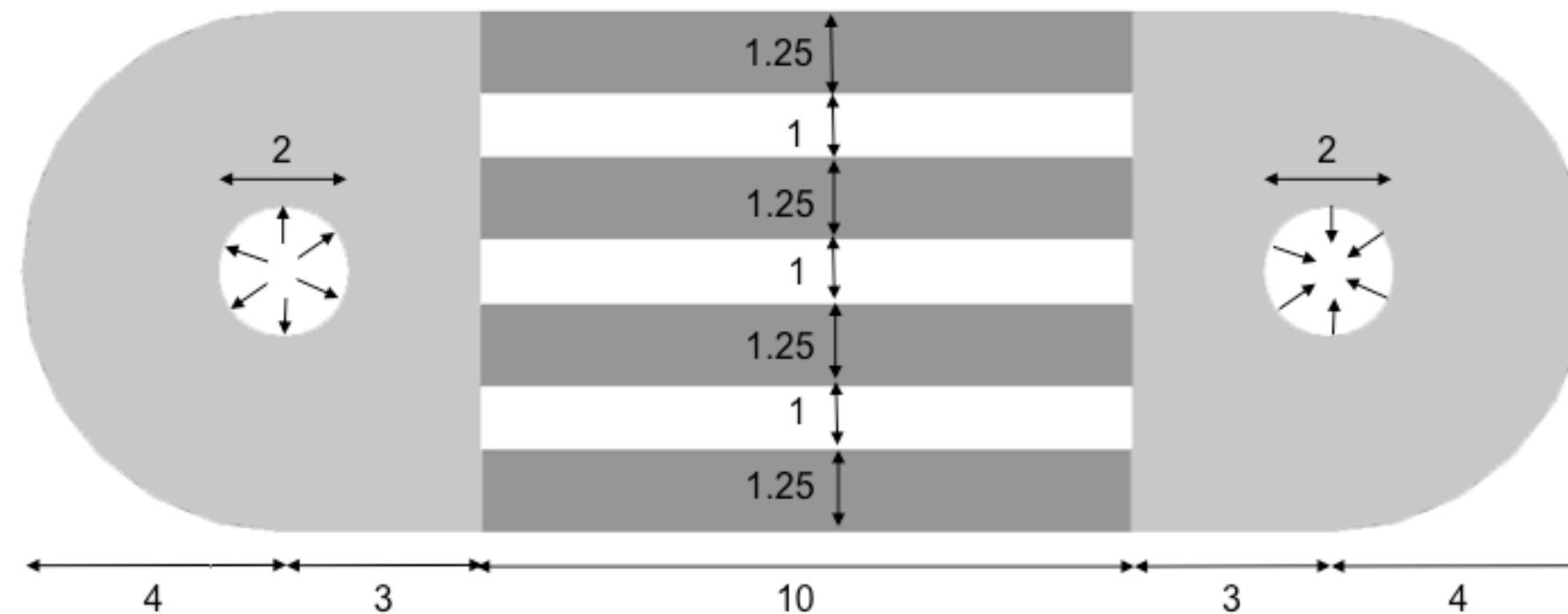
- Nusselt number

- $Nu = \text{convective heat transfer} / \text{conductive heat transfer}$   
 $= h / (k / L)$  (with  $h = Q / \Delta T$  the heat transfer coefficient)  $\gg 1$

- heat produced will be much more transported than conducted

# Flow conditions

- Other geometrical / physical considerations
  - Flow in 4 channels:
    - Decide which boundary layers are important
    - Heat generation in channels
  - Flow around 3 inserts:
    - Possible boundary-layer separation and recirculation  
→ choice of mesh and turbulence model



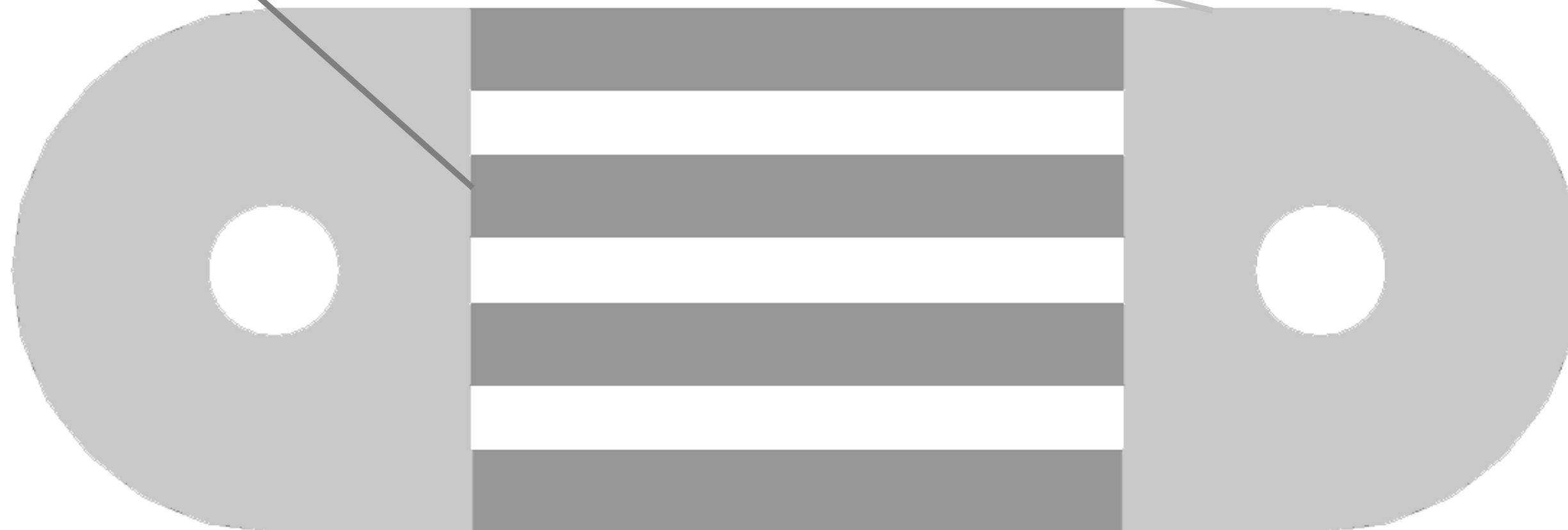


# Pre-processing

- Mesh

- Two main regions:

- Inflow and outflow regions
    - 4 channels

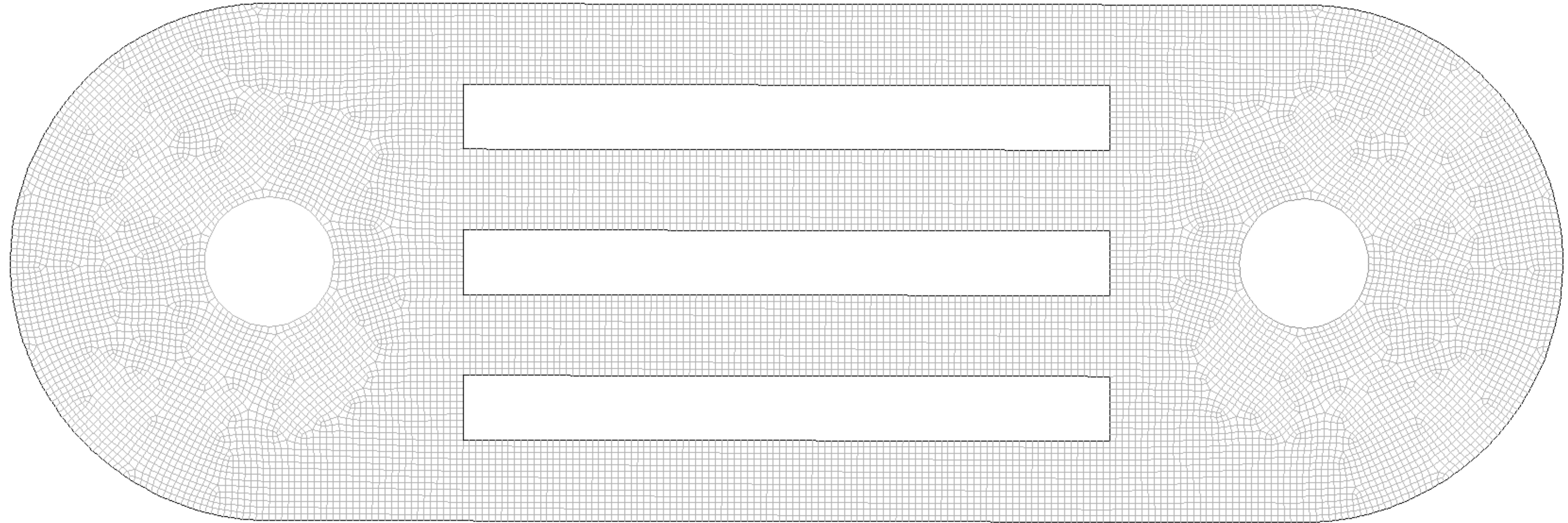


- Type of mesh?

- structured / unstructured / block-structured / hybrid
    - triangular / quadrilateral / mixed

# Pre-processing

- Mesh:



- Properties:

- Hybrid: unstructured (quad) + structured (quad) in 4 channels
- 14'561 cells
- Minimum orthogonal quality = 0.87 (1 represents high quality cells)
- Maximum orthogonal skew = 0.13 (0 represents high quality cells)
- Other suitable types exist

# Solver set-up

- Physical models
  - Ideal gas law, high-temperature air properties
  - $k$ - $\varepsilon$  turbulence model
    - RNG  $k$ - $\varepsilon$  (realizable also possible; RNG may be suitable)
    - Enhanced wall treatment (two-layer model) (thick boundary layer  $\rightarrow$  can afford  $y^+=O(1)$ )
    - Neglect viscous heating (Brinkman number  $\ll 1$ )
    - $k$ - $\omega$  models are also appropriate
- Numerical methods
  - Pressure-based segregated solver, SIMPLE scheme, 2<sup>nd</sup>-order discretization
  - Default under-relaxation factors
  - Monitor average temperature on channel walls

# Solver set-up

- Boundary conditions (flow + thermal):

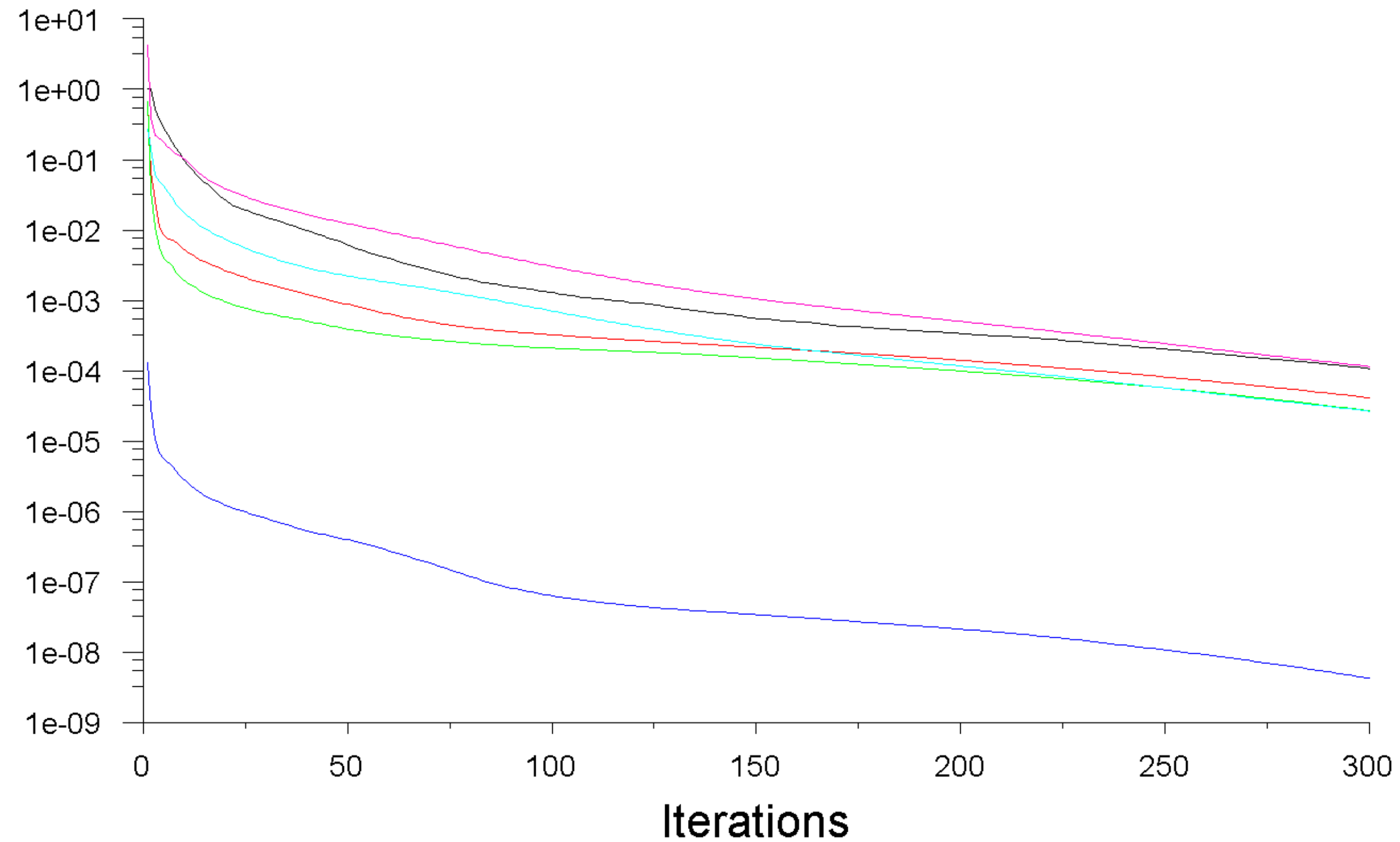
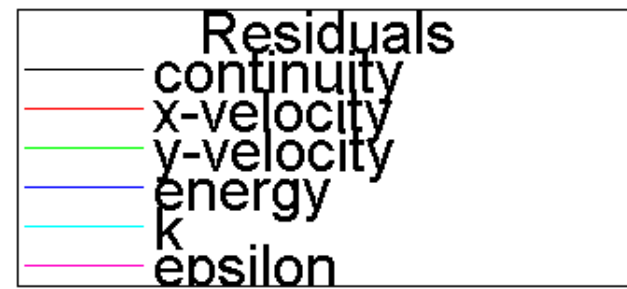
Outer wall and channel walls: no-slip  $V_w = 0$ , adiabatic



Volumic heat flux  $Q$  in 4 channels

# Solver procedure

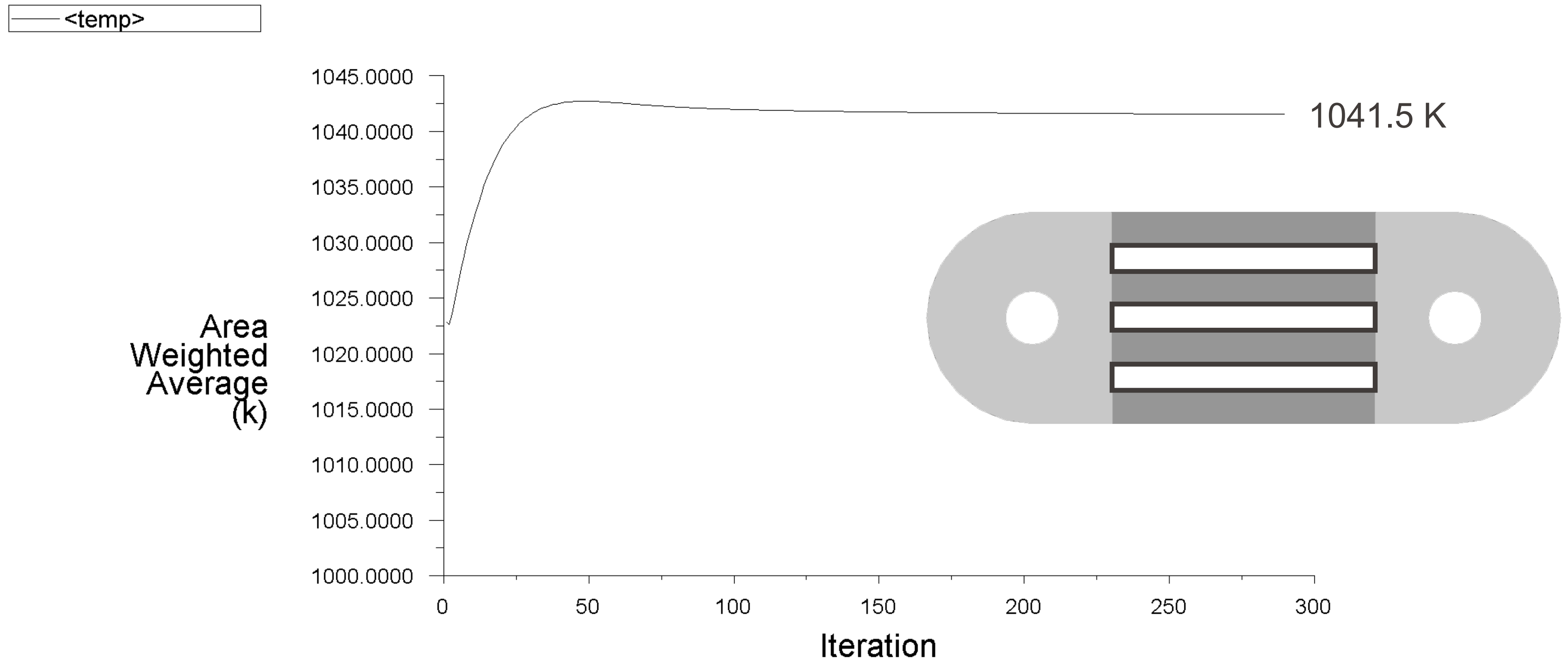
## ■ Convergence: residuals





# Solver procedure

- Convergence: average temperature on channel walls



# Solver procedure

- Convergence: mass conservation
  - Require net mass flux between inlet and outlet to be conserved to  $< 0.2 \%$

Mass flow rate [kg/s]	
Inlet	0.0854170
Outlet	-0.0854169
Net imbalance	$5.2 \times 10^{-8}$ ( $6 \times 10^{-5} \%$ )

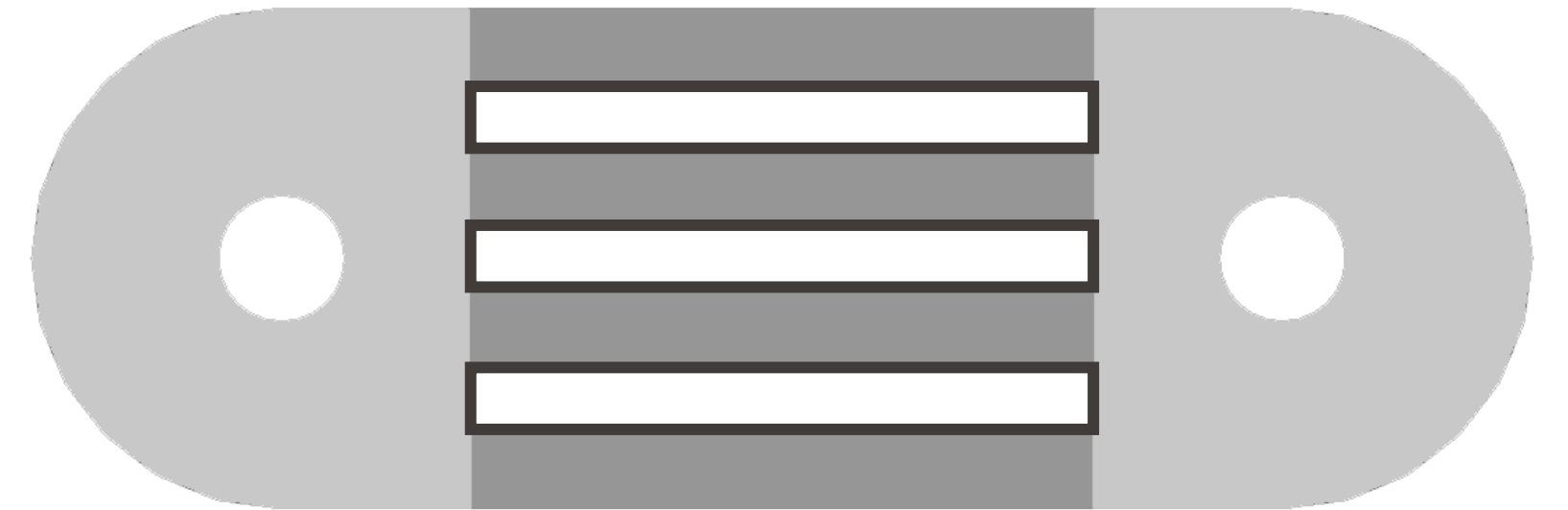
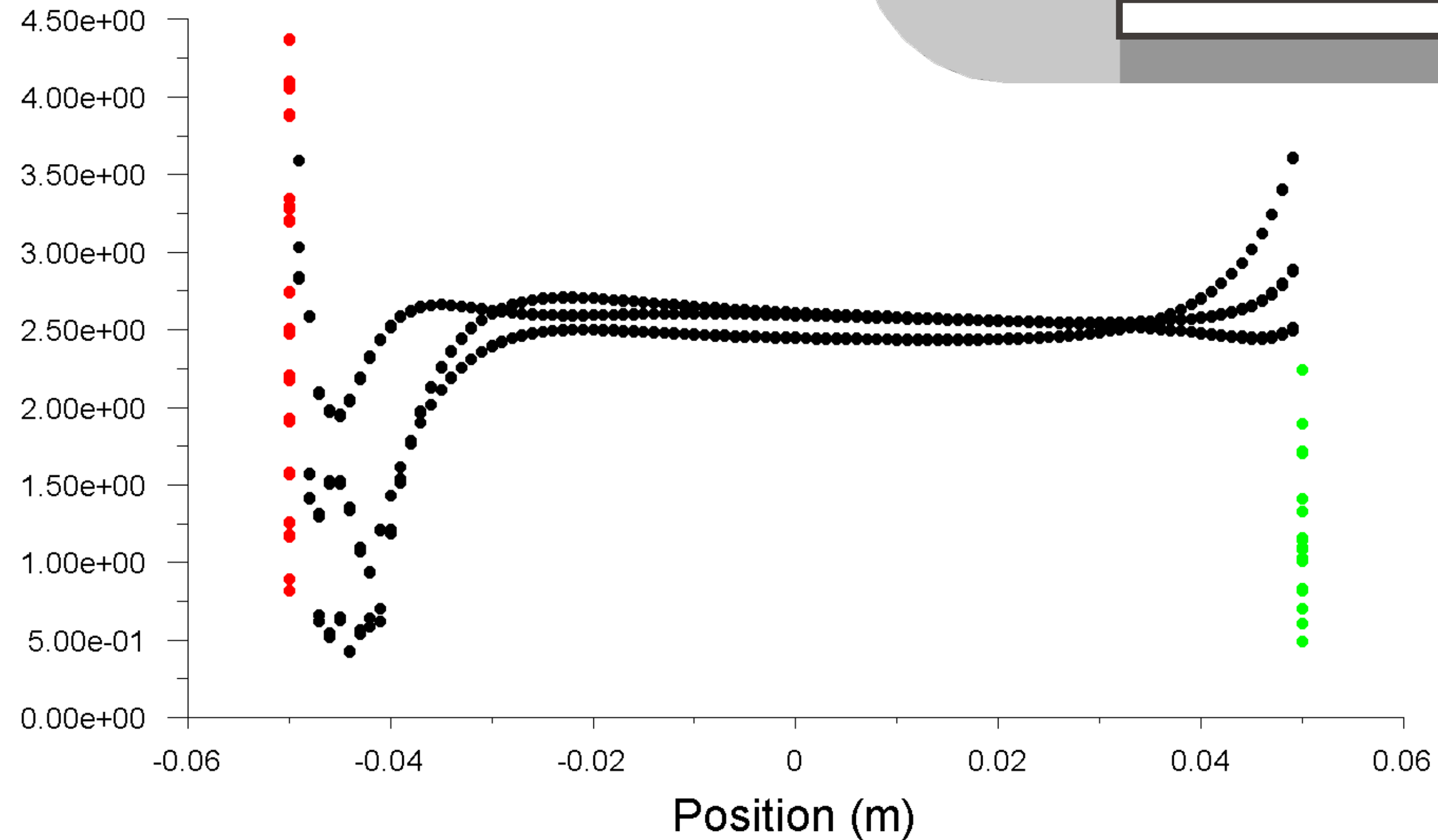
- Mass conservation satisfied for this solution.

# Post-processing

- Control: first-cell  $y^+$  along channels



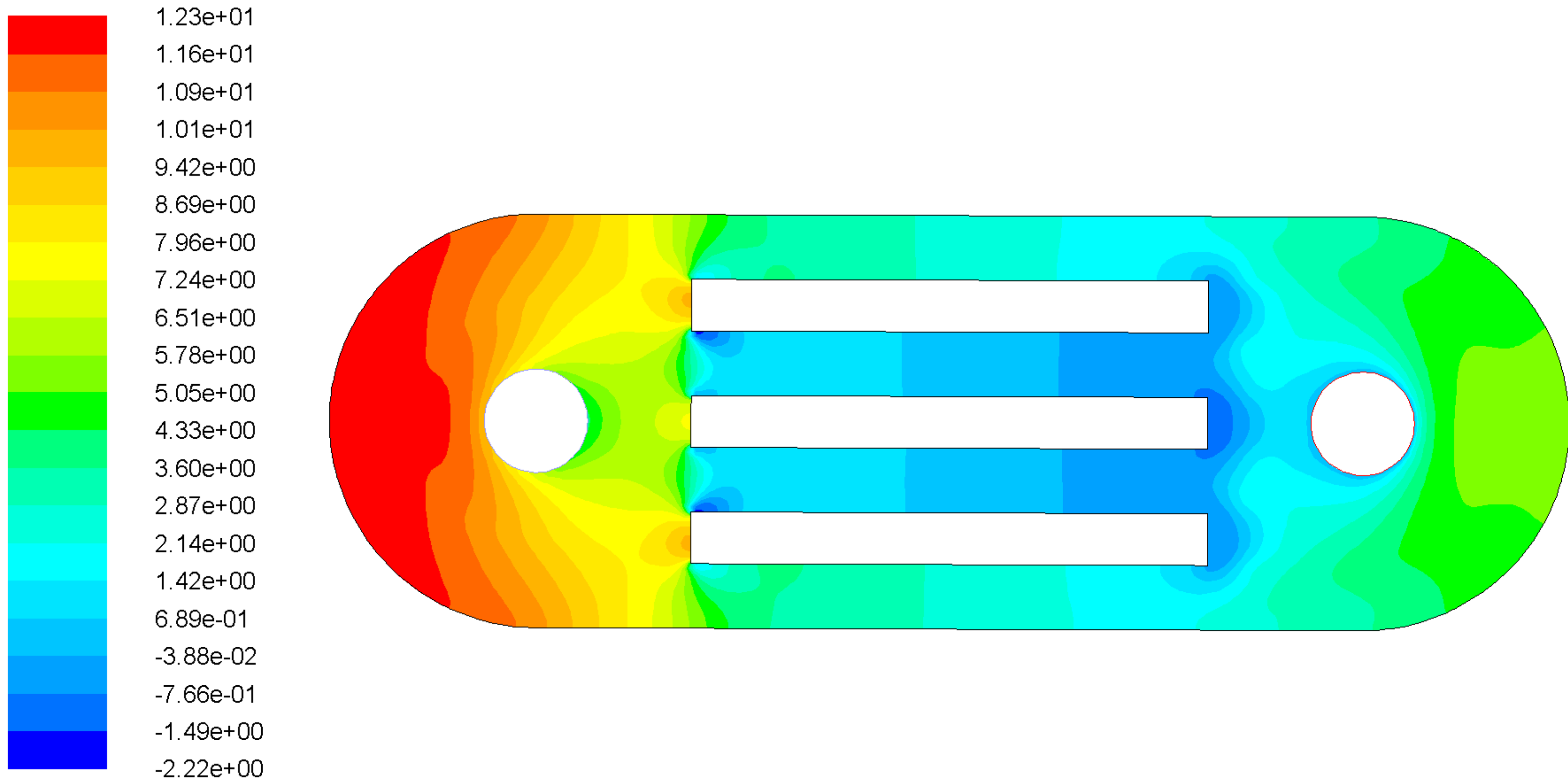
Wall  
 $Y_{plus}$



# Post-processing

- Contours: pressure

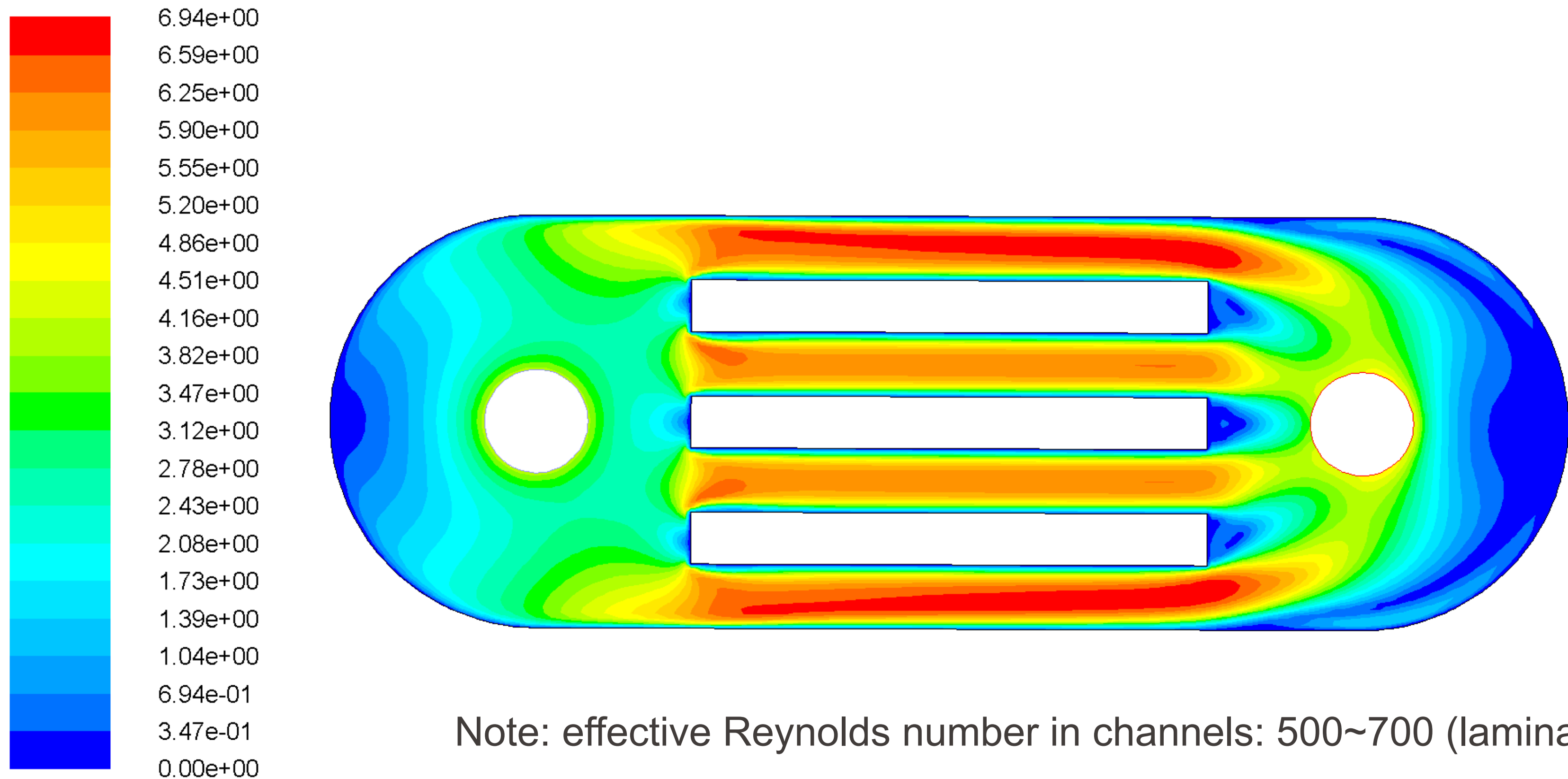
Numerical Flow Simulation



# Post-processing

- Contours: velocity magnitude

Numerical Flow Simulation



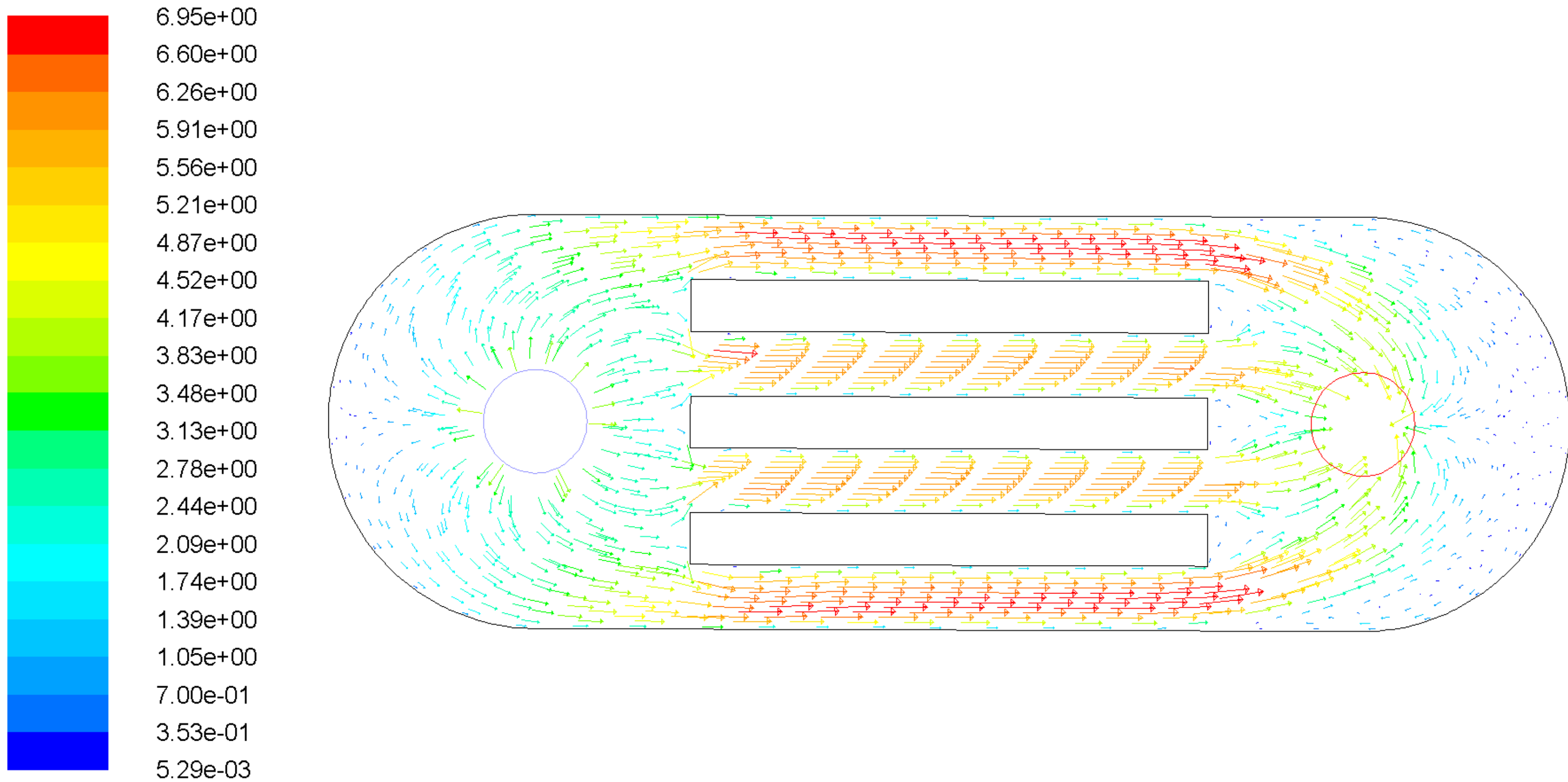
Note: effective Reynolds number in channels: 500~700 (laminar)



# Post-processing

- Velocity vectors

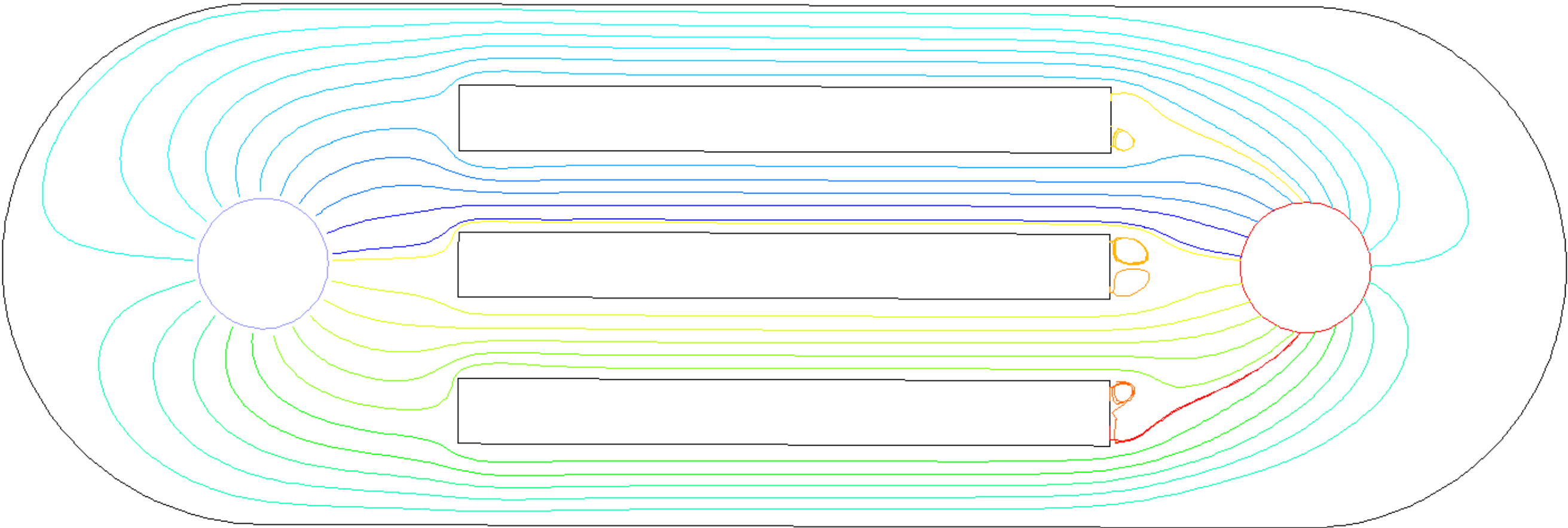
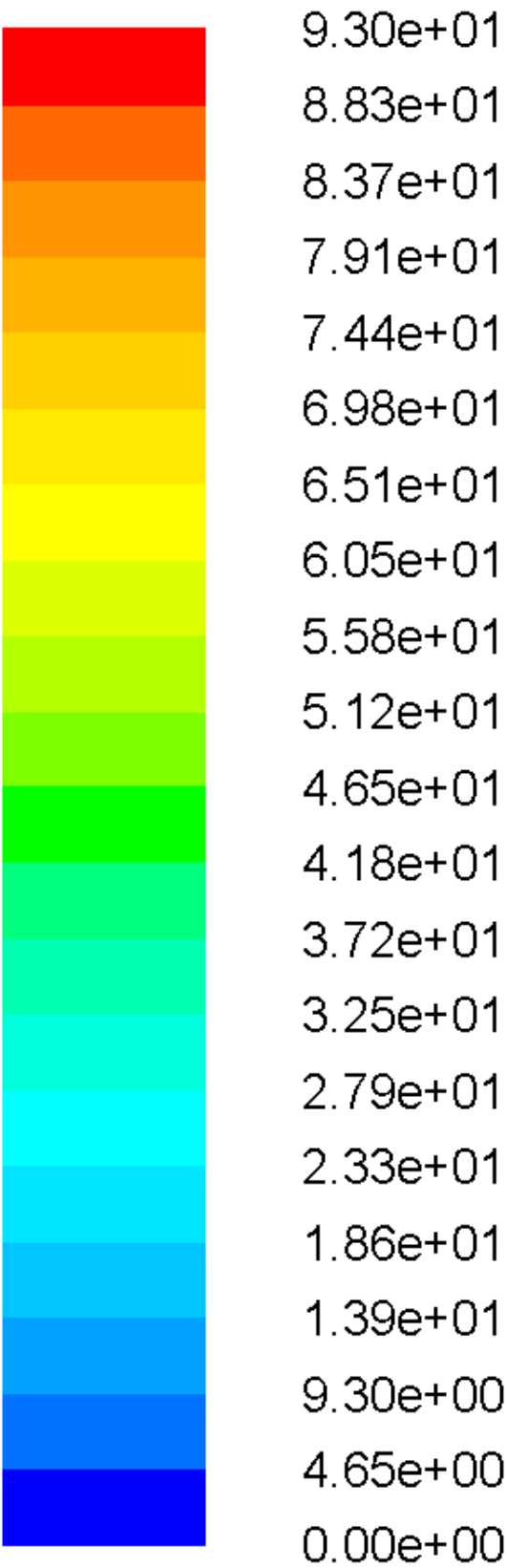
Numerical Flow Simulation



# Post-processing

- Streamlines

Numerical Flow Simulation

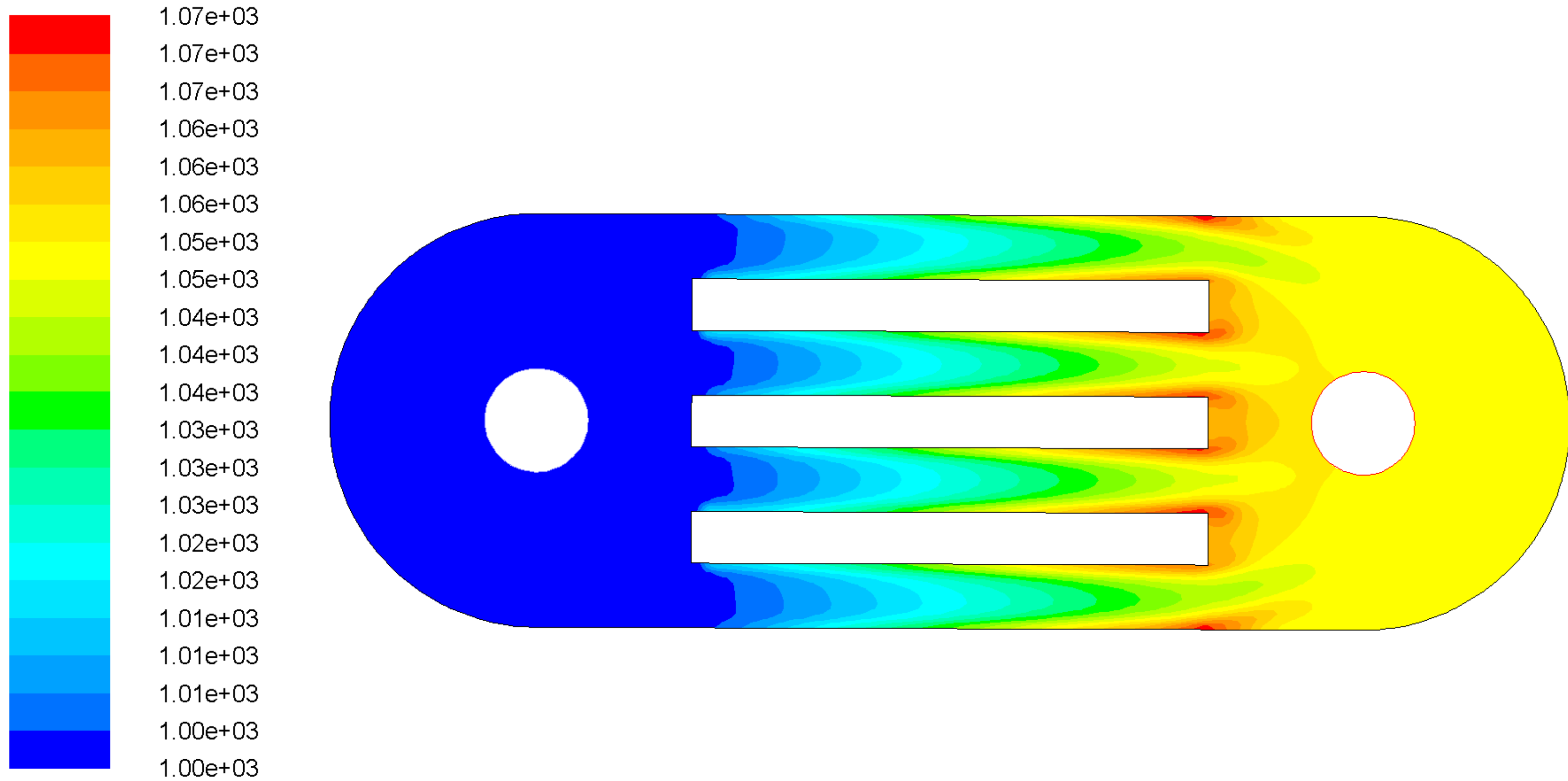


Flow attached in channels; separation at sharp edge downstream

# Post-processing

- Contours: temperature

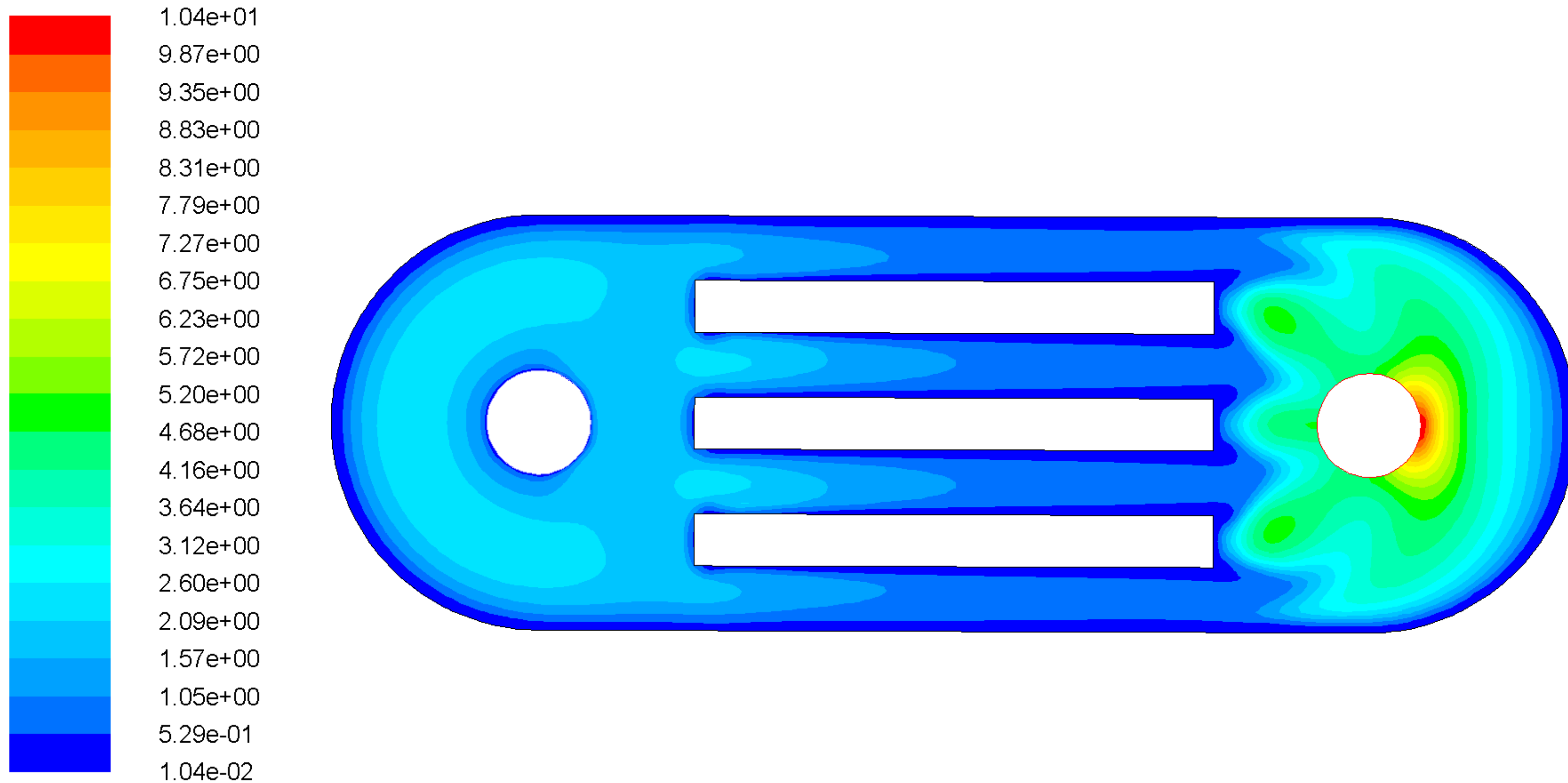
Numerical Flow Simulation



# Post-processing

- Contours: turbulent kinetic energy  $k$

Numerical Flow Simulation

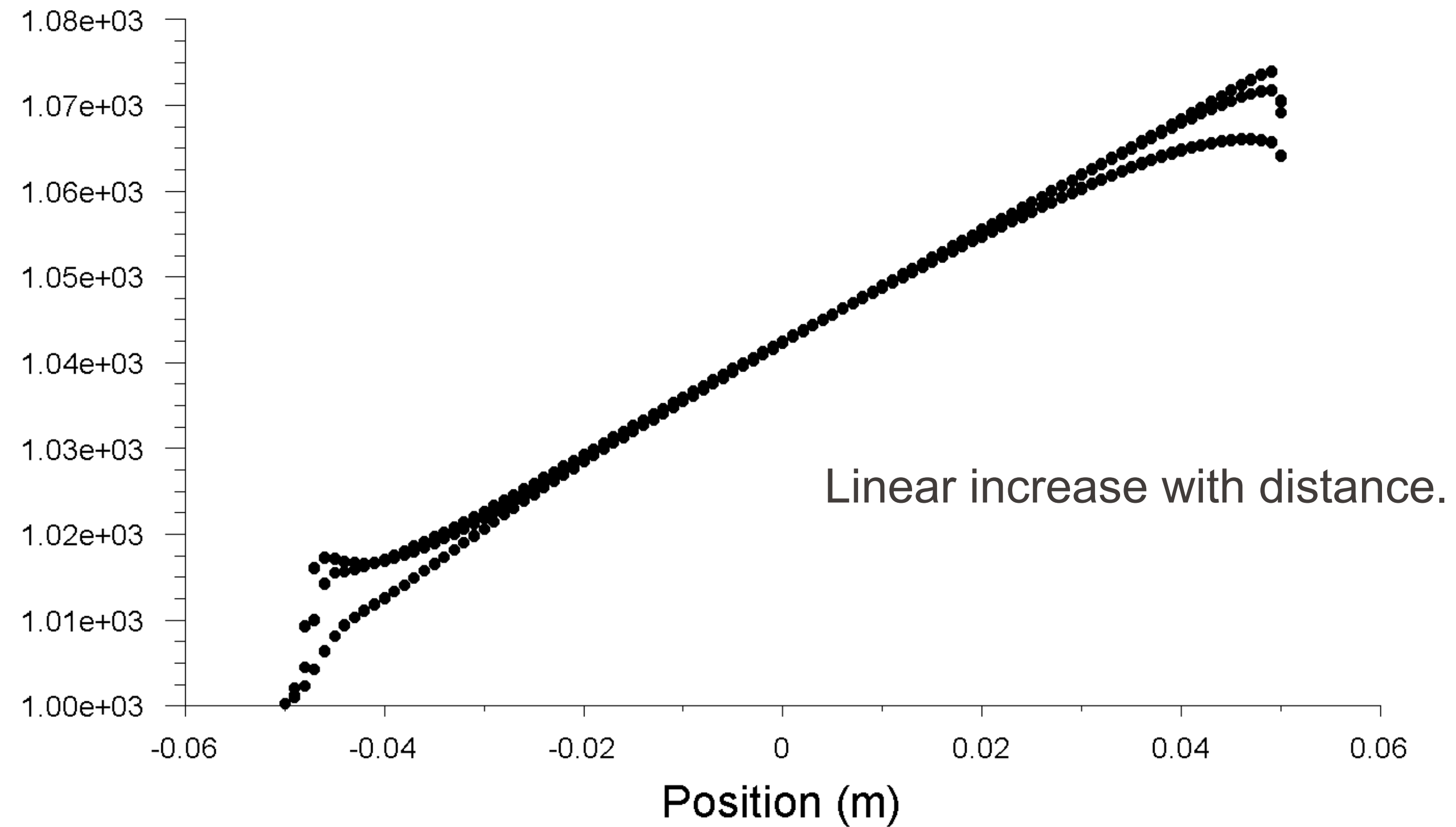


# Post-processing

## ■ Temperature on channel surfaces

• wall-channels-cent

Static  
Temperature  
(k)



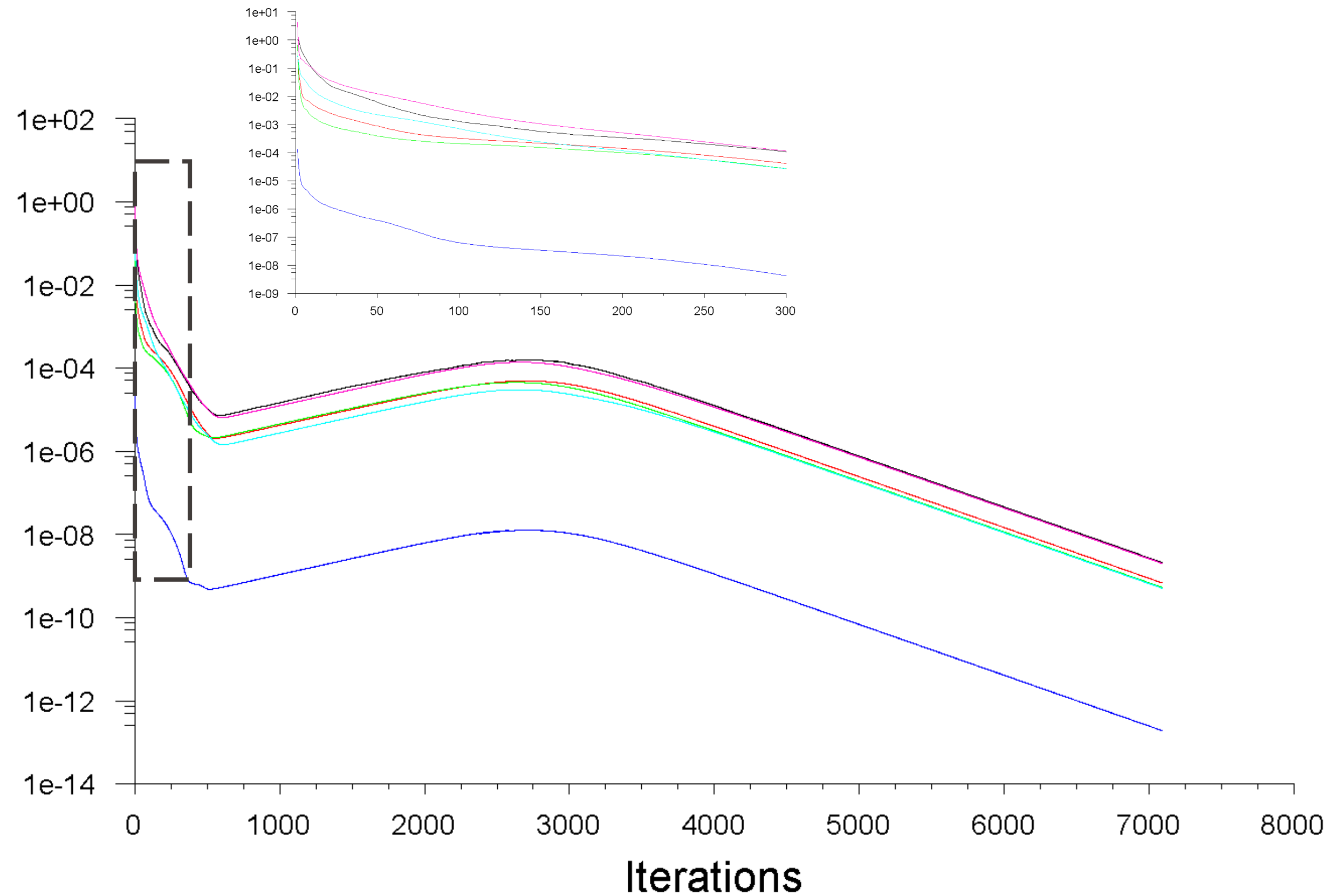
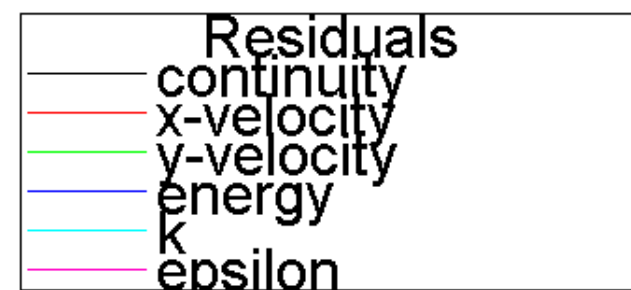


# Global observations (1/2)

- Physical analysis of the numerical solution:
  - The flow field has the same top-bottom symmetry as the geometry and boundary conditions.
  - Within the channels, flow aligned with geometry (and mesh).
  - Flow attached in channels; separation at the sharp edge downstream.
  - Turbulence generation highest in outflow region (recirculation, large gradients of mean velocity).
  - Relatively thick boundary layer, justifying the use of a near wall (two-layer) treatment of the turbulence (with  $y^+$  confirmed to be  $O(1)$ ).
  - Air temperature increases linearly in the channels; same temperature in the central region of all channels.
- However...

# Solver procedure

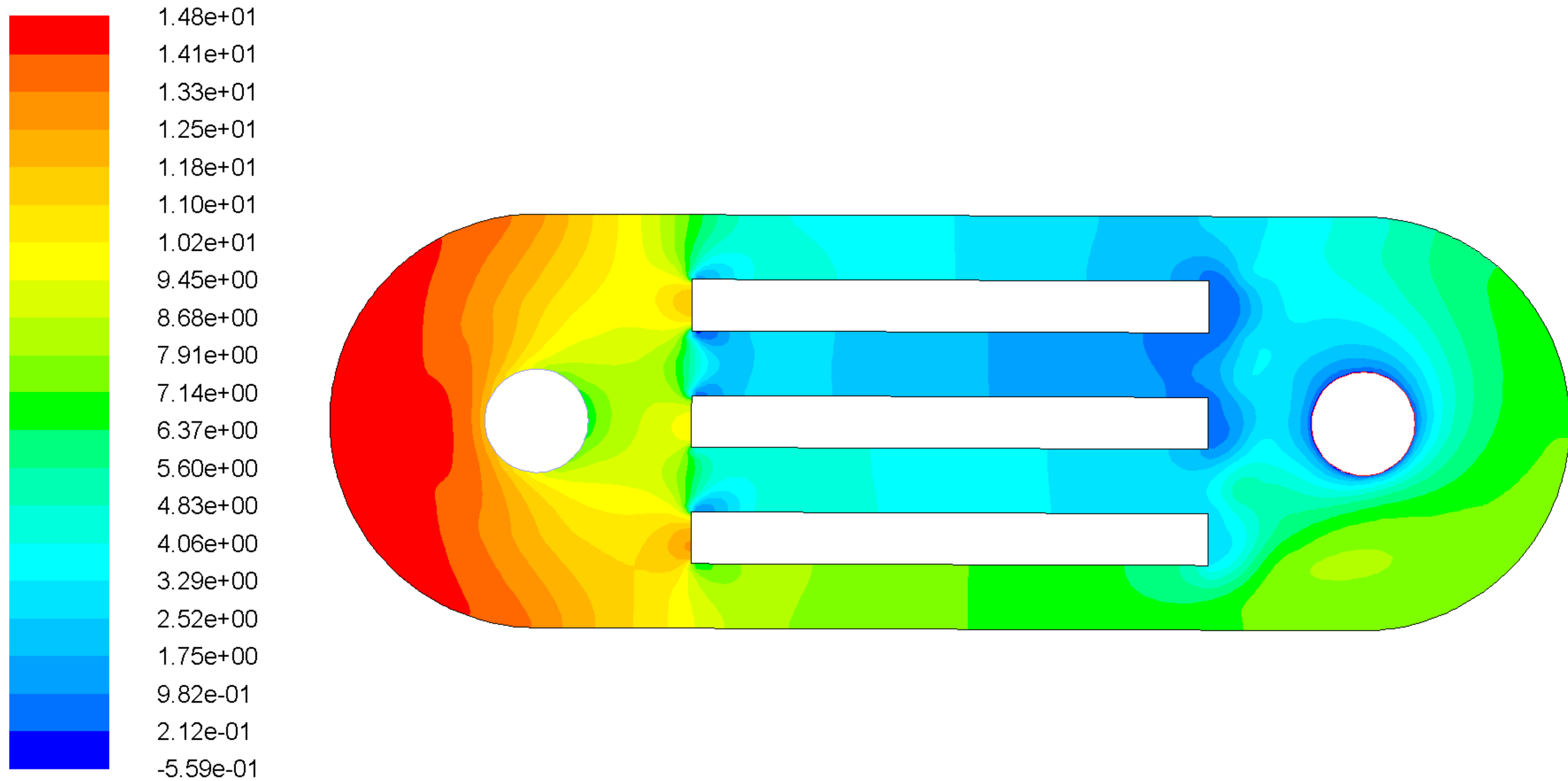
- Convergence: further iterations reveal a second solution



# Post-processing

- Contours: pressure

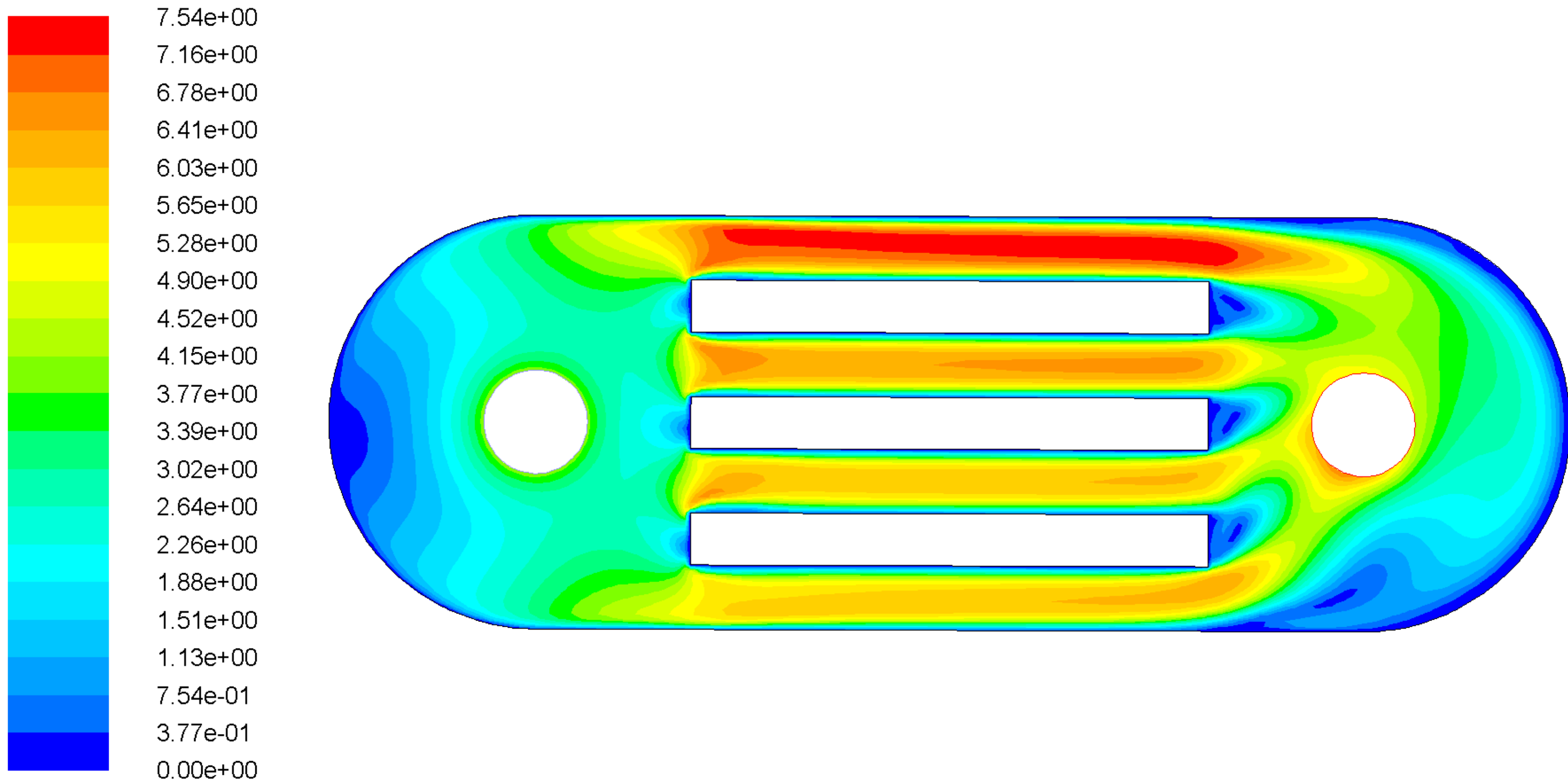
Numerical Flow Simulation



# Post-processing

- Contours: velocity magnitude

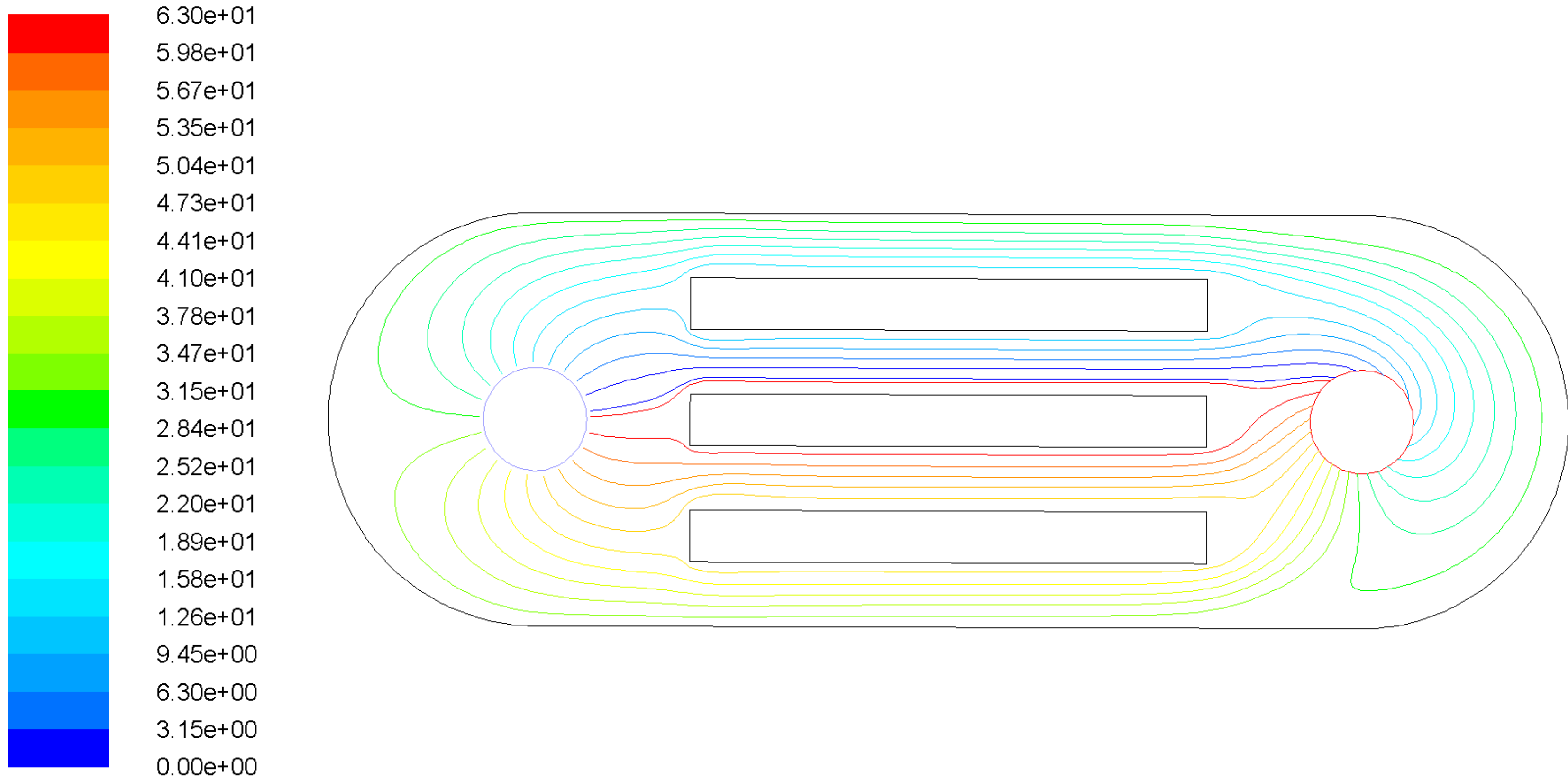
Numerical Flow Simulation



# Post-processing

## ■ Streamlines

Numerical Flow Simulation

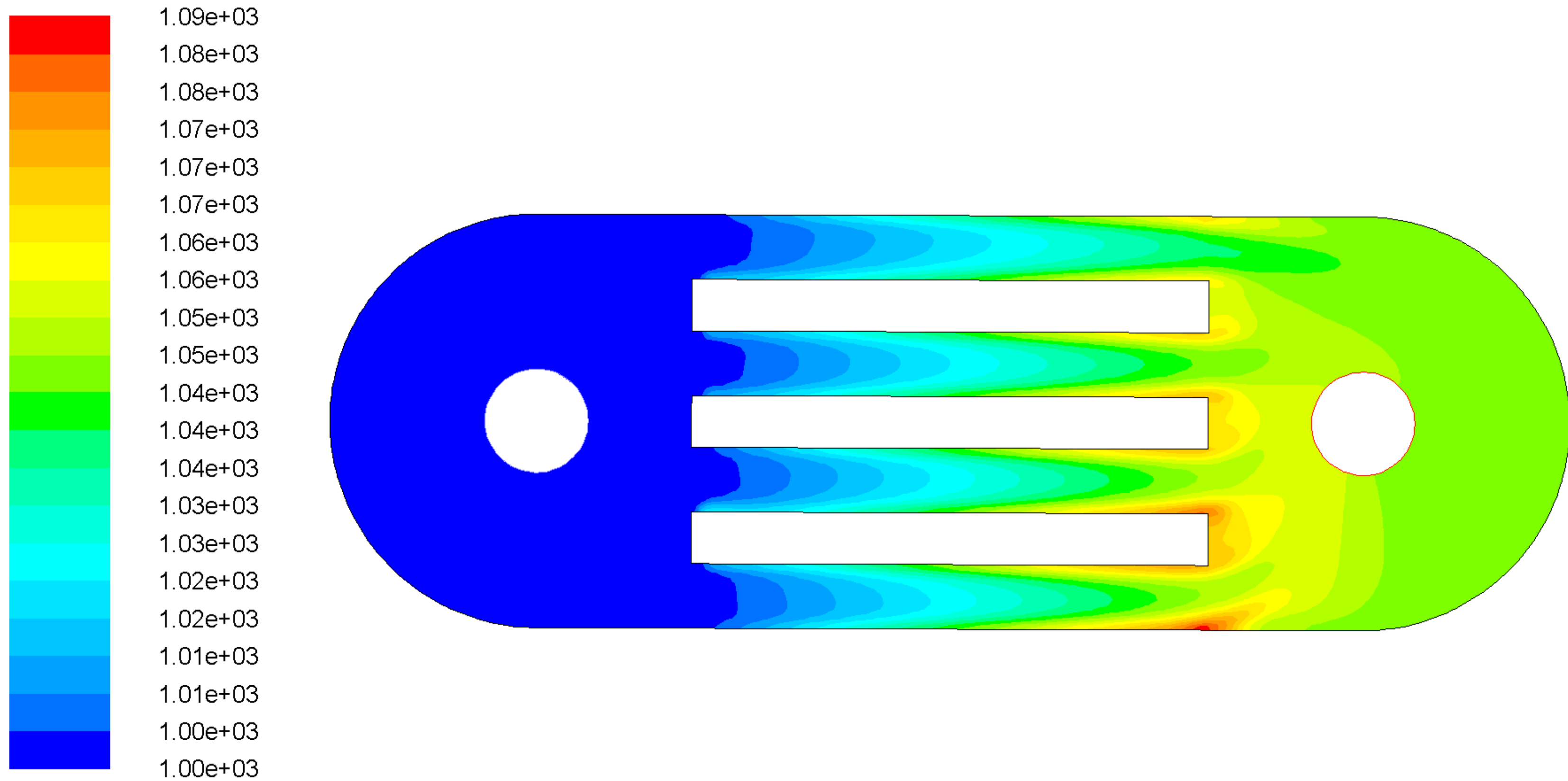




# Post-processing

- Contours: temperature

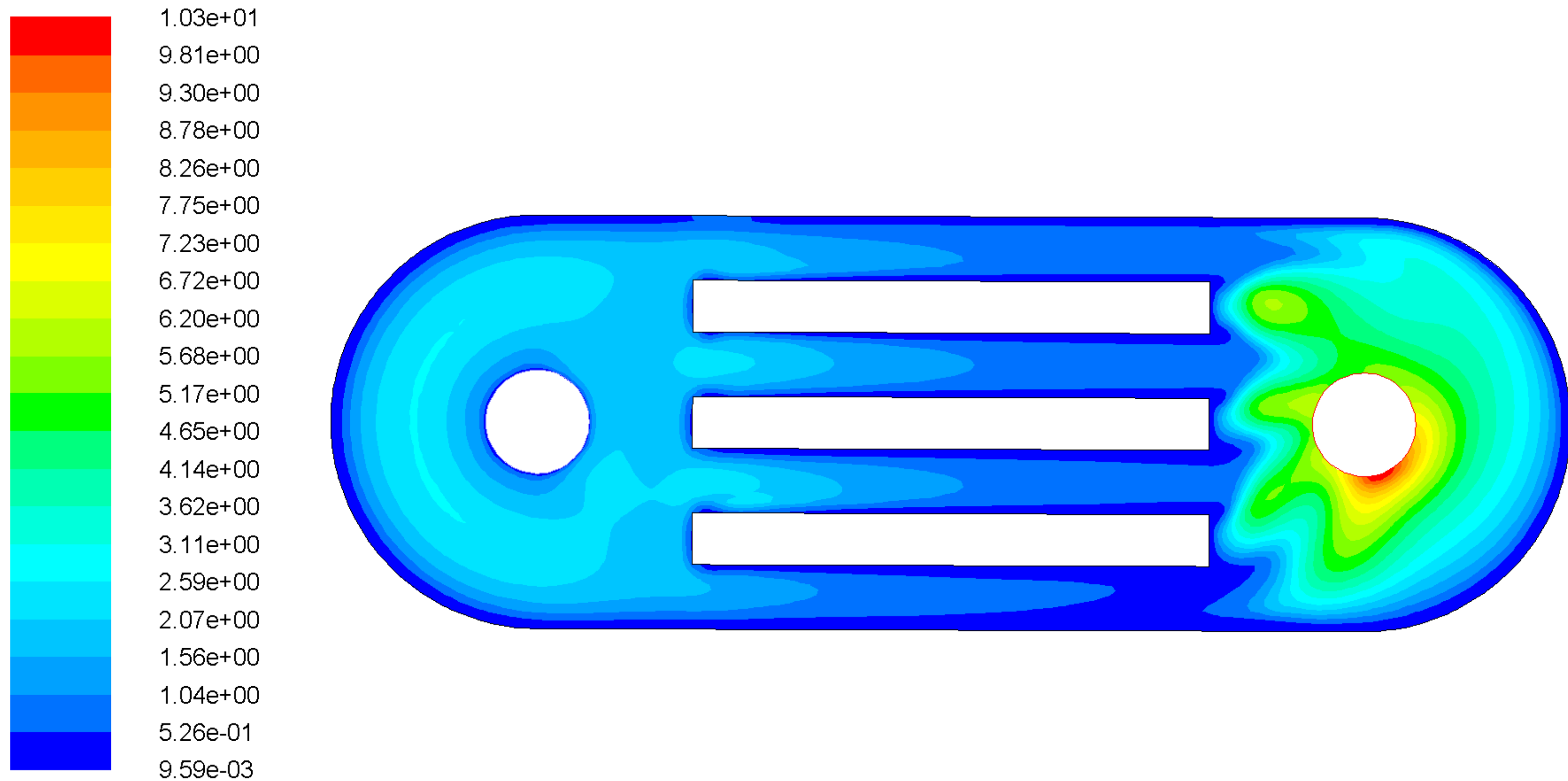
Numerical Flow Simulation



# Post-processing

- Contours: turbulent kinetic energy  $k$

Numerical Flow Simulation

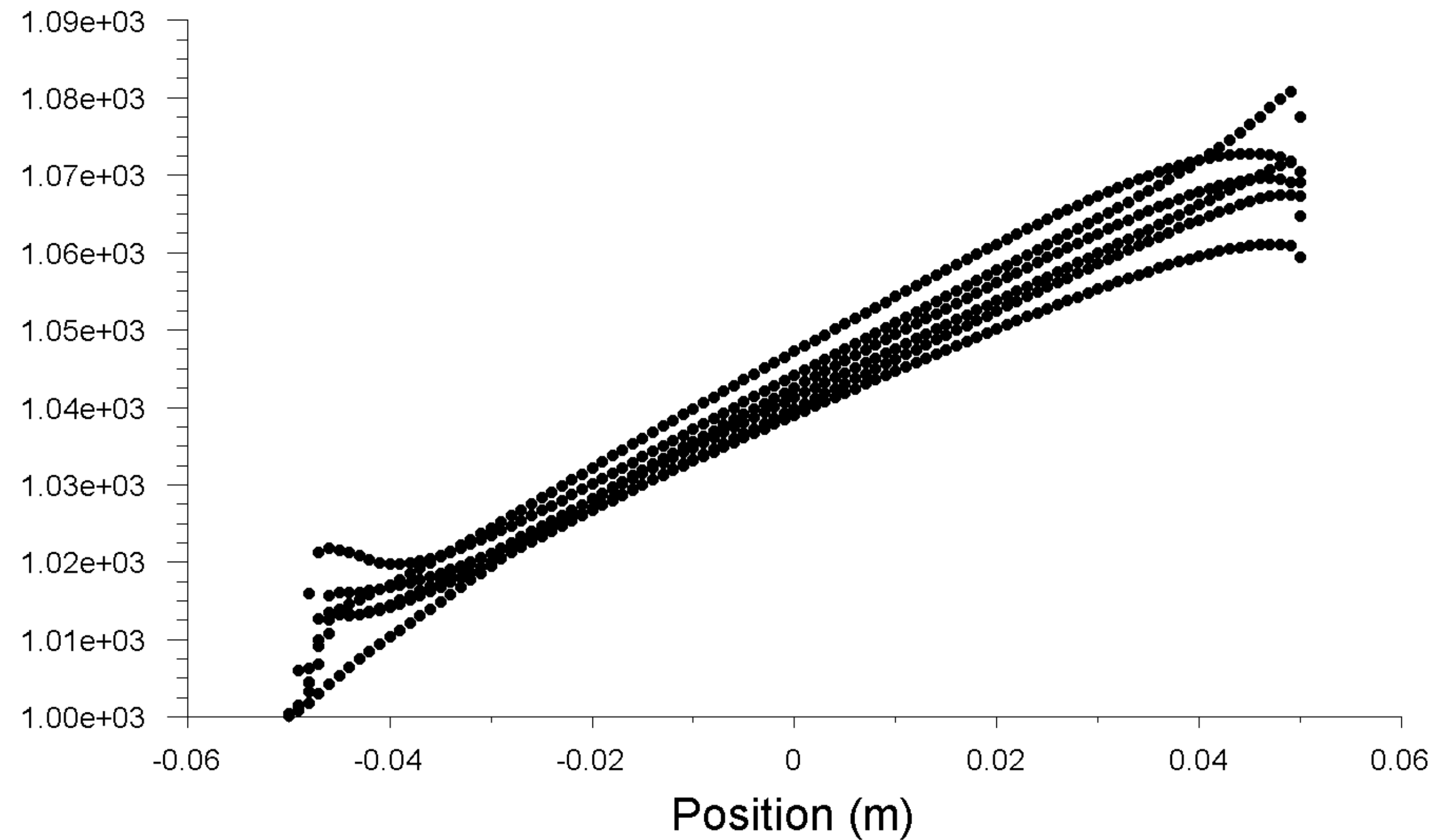


# Post-processing

## ■ Temperature on channel surfaces

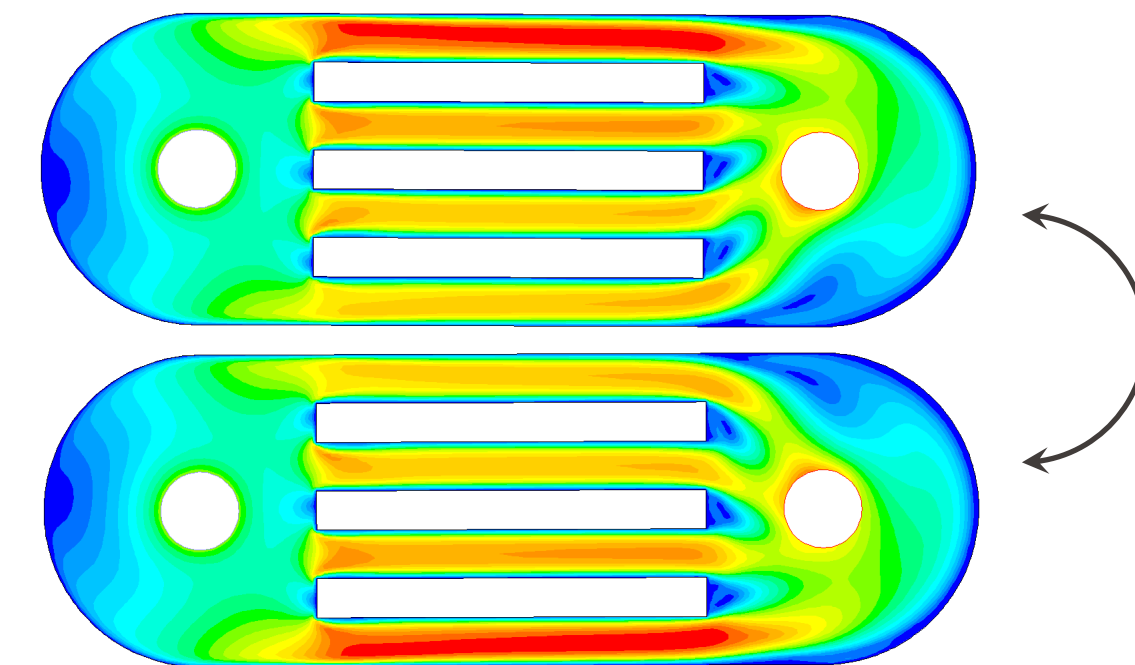
• wall-channels-cent

Static  
Temperature  
(k)



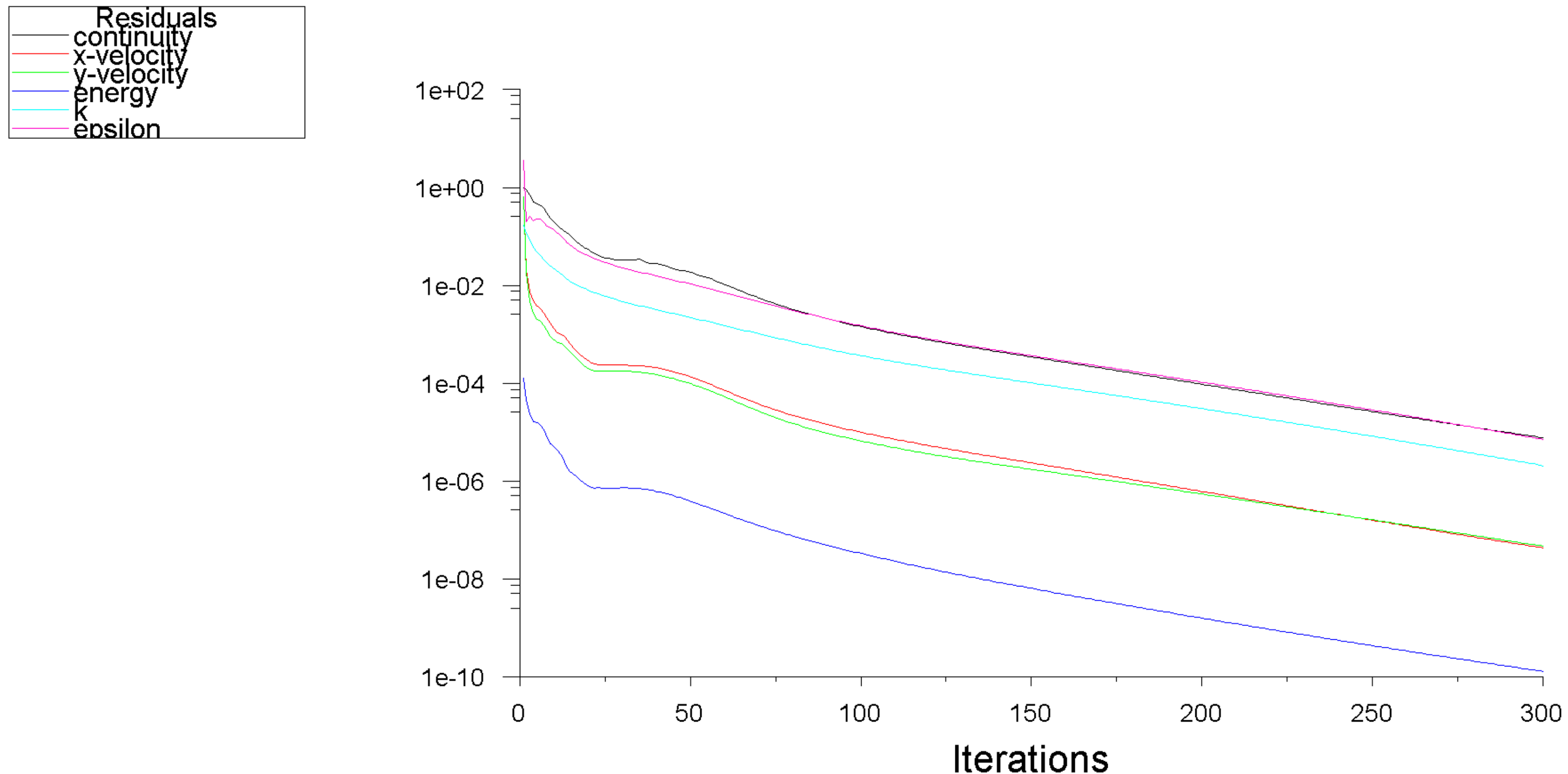
# Global observations (2/2)

- Physical analysis of the numerical solution:
  - Residuals increase and then decrease until they reach machine precision.
  - The 2<sup>nd</sup> solution breaks the top-bottom symmetry.
  - Within the channels, flow still aligned with geometry (and mesh), and still attached; separation at the sharp edge downstream.
  - Temperature still increases linearly, but different value in each channel.
  - 1<sup>st</sup> (symmetric) solution not stable, therefore not physically observable. Obtained solution depends on initialization, numerical method, physical model...
  - Due to turbulence, actual physical flow may switch between the two symmetry-breaking solutions, and restore symmetry on average. Need experiments or long time-dependent simulations to investigate this point.



# Solver procedure

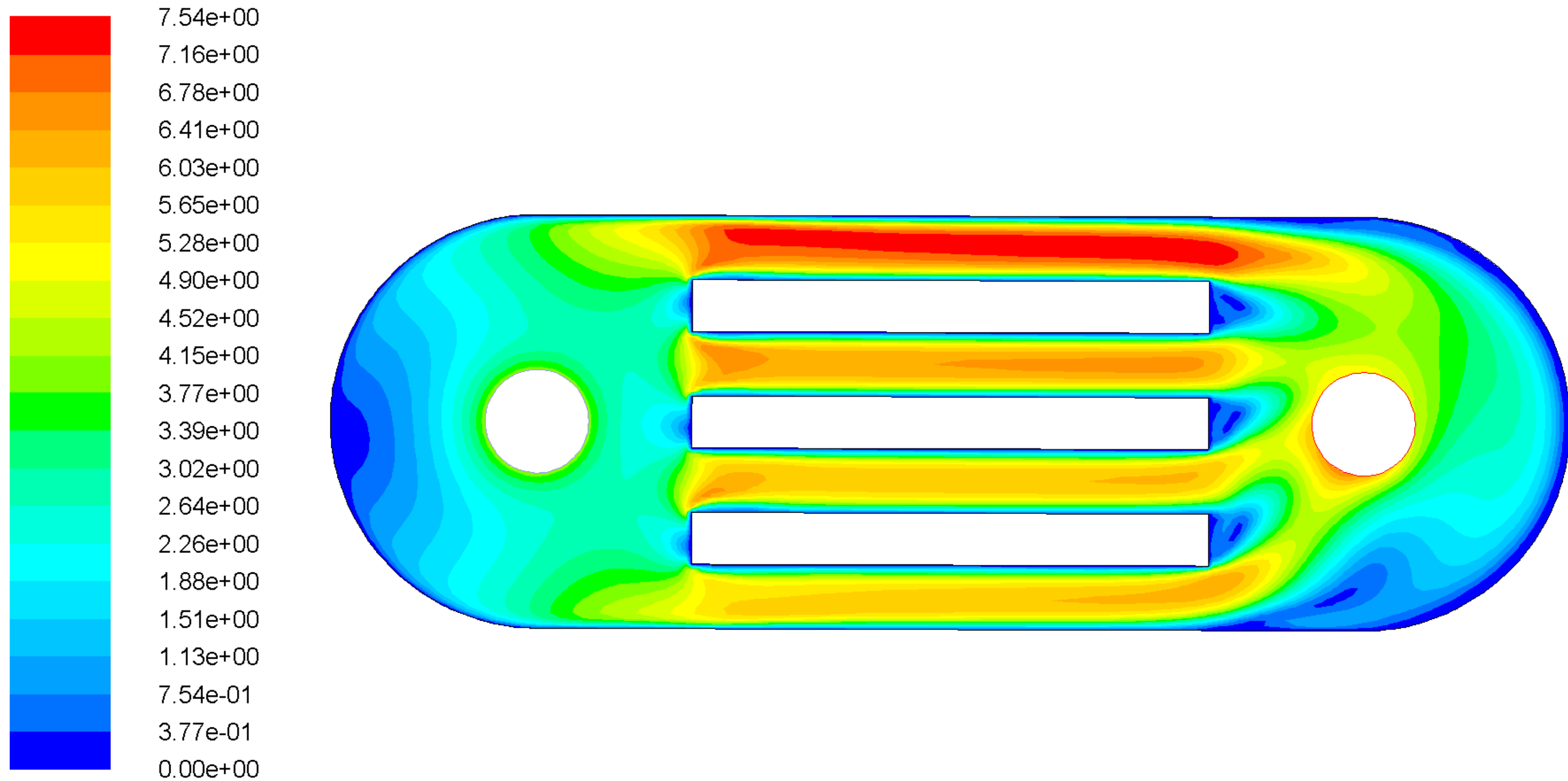
- Convergence: same computation with coupled solver. Obtain the same asymmetric solution much faster.



# Post-processing

- Contours: velocity magnitude

Numerical Flow Simulation



# Your work (optional):

- Perform the flow simulation using Fluent, varying the numerical method, physical model etc.
- Perform a detailed post-processing analysis of the solution.
- Analyze whether the initial assumptions are justified.
- Suggest improvements in fuel cell design.