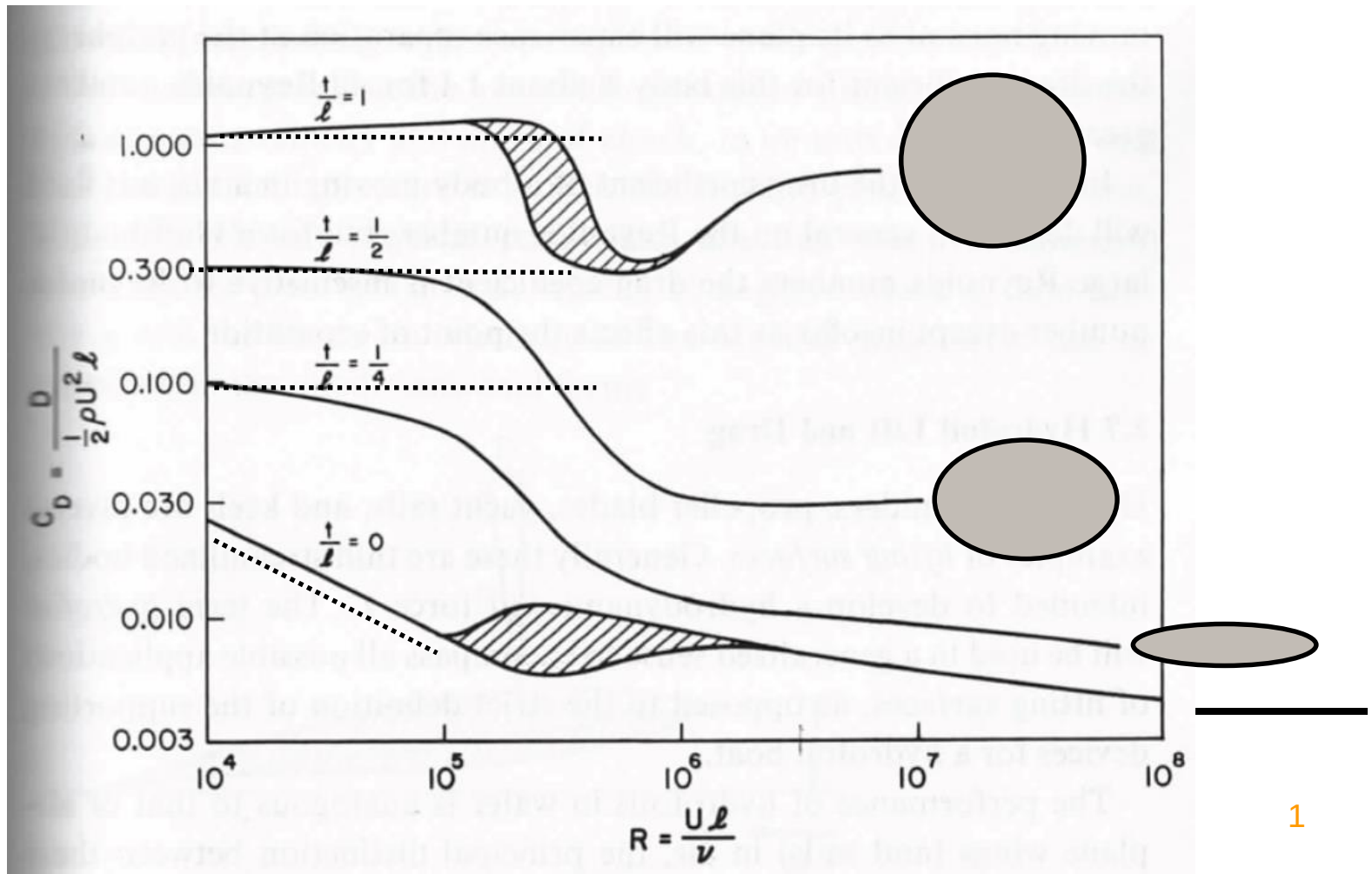


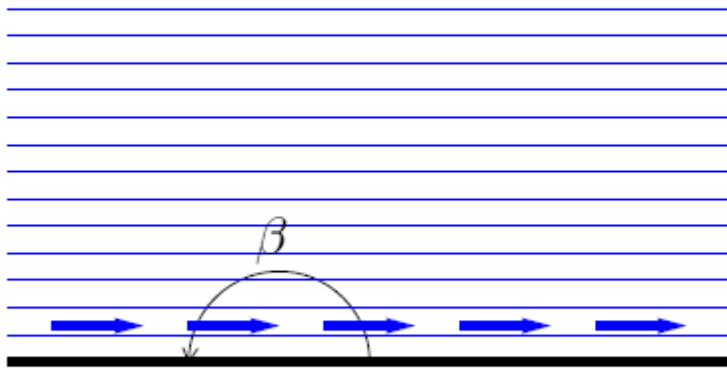
But this does still not explain the aerodynamic drag scaling:

$$\frac{1}{2} \rho_{\infty} U_{\infty}^2 S$$



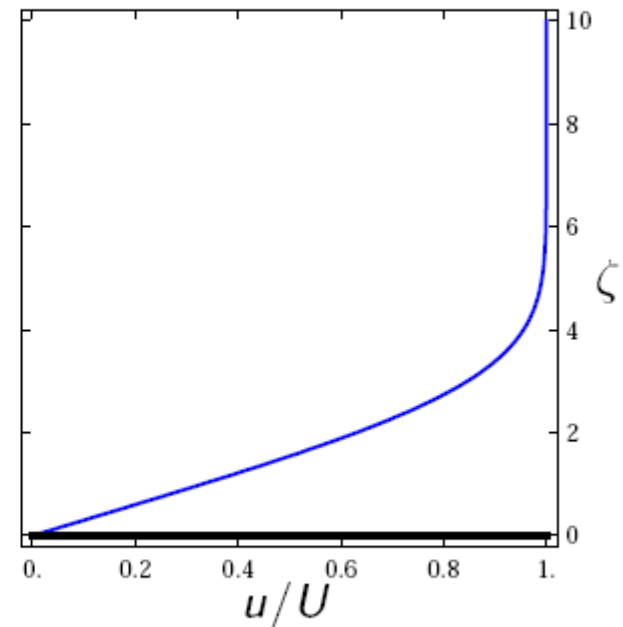
Pressure gradient effect

Le cas de référence est le cas $m = 0$ i.e. $\beta = \pi/(m + 1) = \pi$ correspondant à l'écoulement au dessus d'une plaque plane :



écoulement uniforme

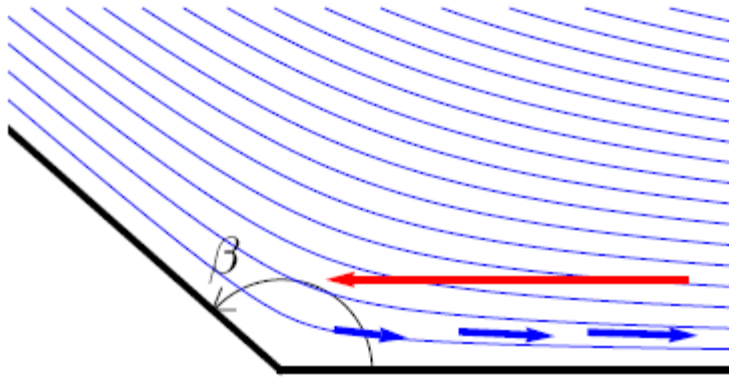
∇p nul



→ couche limite de Blasius

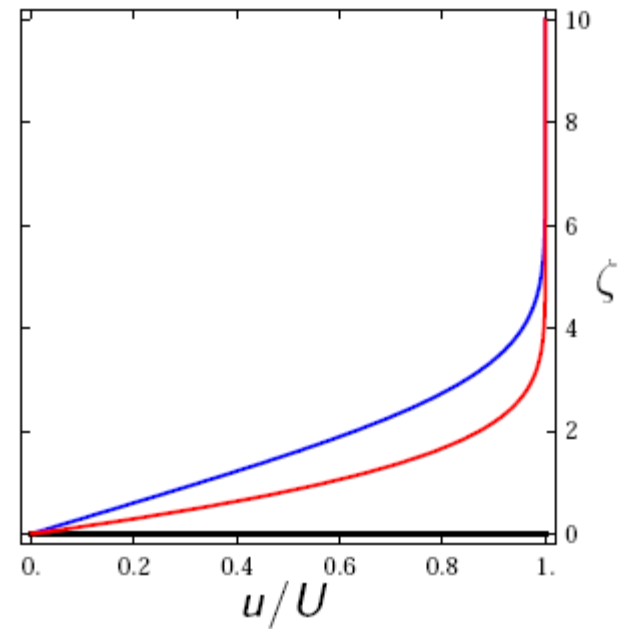
Pressure gradient effect

Si $m > 0$ on a $\beta = \pi/(m+1) < \pi$ correspondant à l'écoulement au dessus d'un dièdre rentrant :



écoulement accéléré

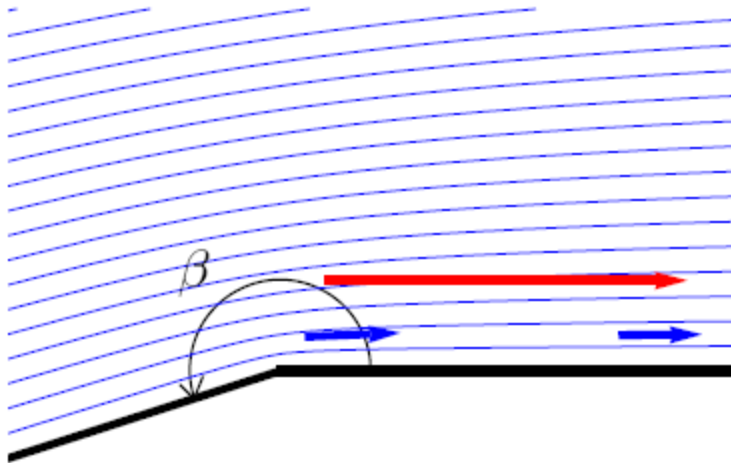
∇p accélérateur



→ couche limite + collée

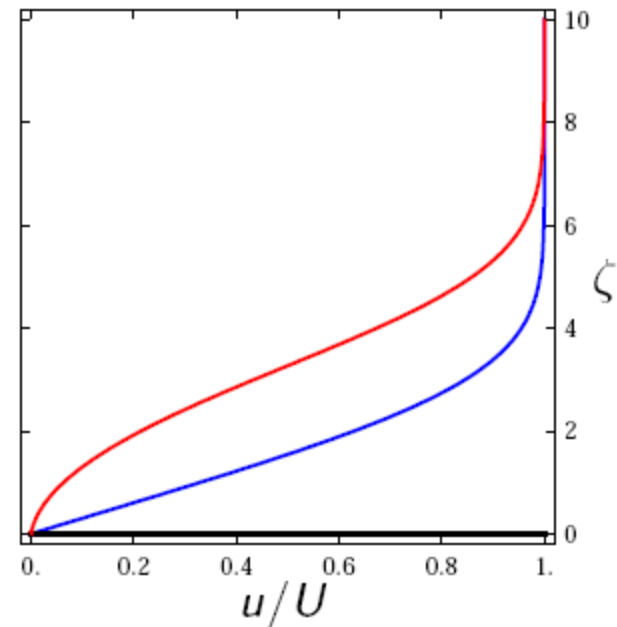
Pressure gradient effect

Si $m < 0$ on a $\beta = \pi/(m+1) > \pi$ correspondant à l'écoulement au dessus d'un dièdre saillant :



écoulement ralenti

∇p décélérateur

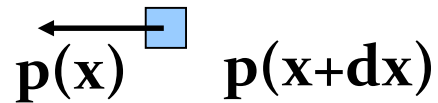
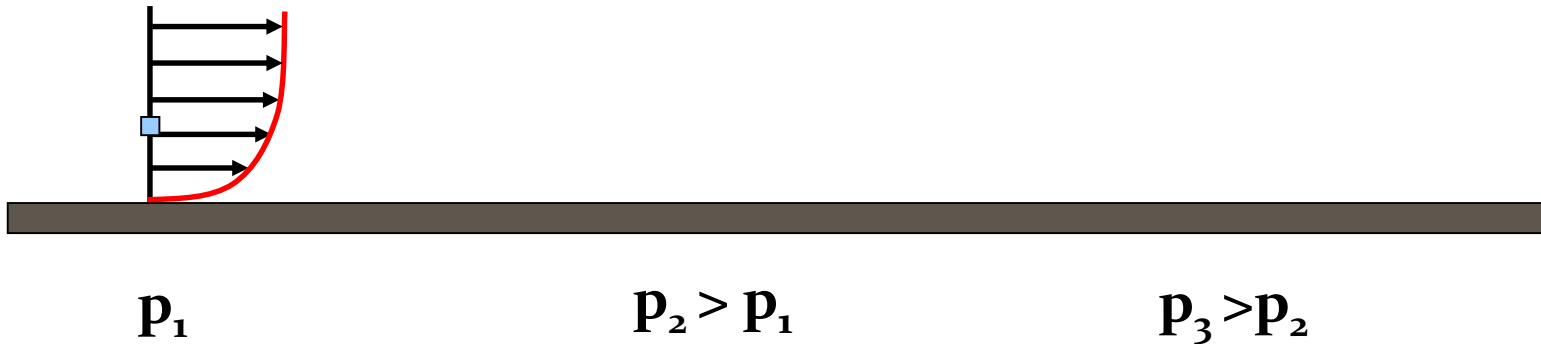


→ couche limite + épaisse

Pressure gradient effect

Adverse pressure gradient :

$$\frac{\partial p}{\partial x} > 0$$

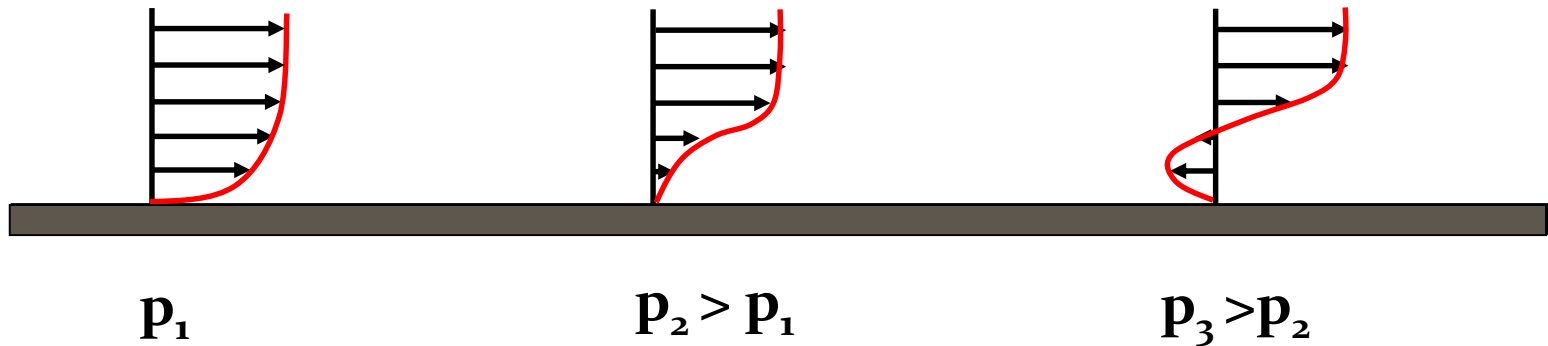


Resulting pressure force

Pressure gradient effect

Adverse pressure gradient :

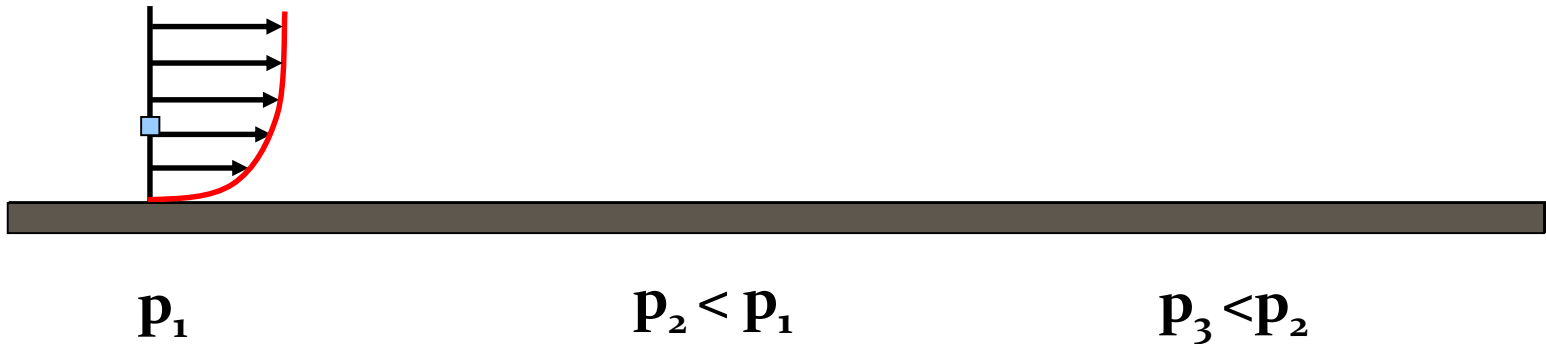
$$\frac{\partial p}{\partial x} > 0$$



Close to the wall, the viscous effects dominate
The pressure gradient further decreases the velocity
⇒ Detachment

Pressure gradient effect

Favorable pressure gradient: $\frac{\partial p}{\partial x} < 0$

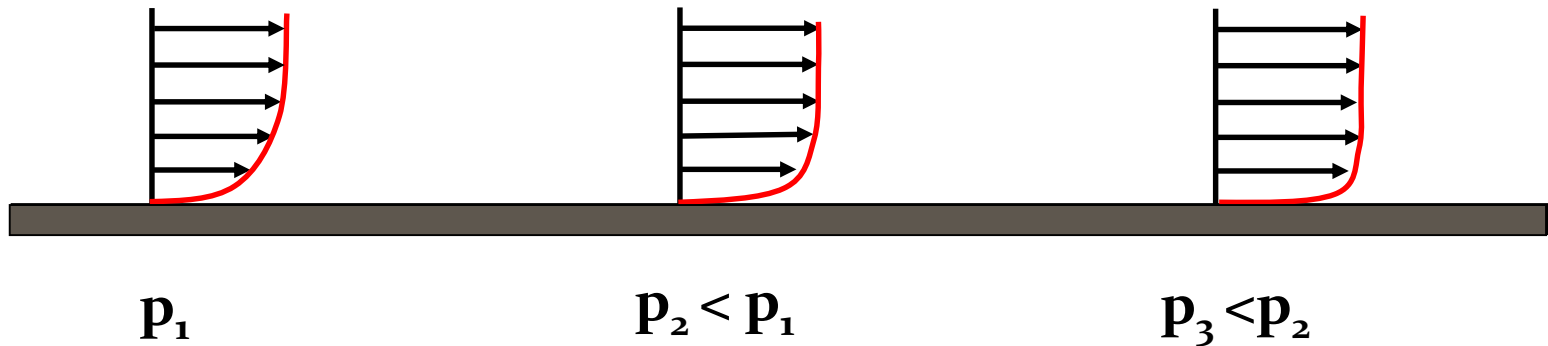


$$p(x) \quad \boxed{\text{blue square}} \quad \rightarrow \quad p(x+dx)$$

Resulting pressure force

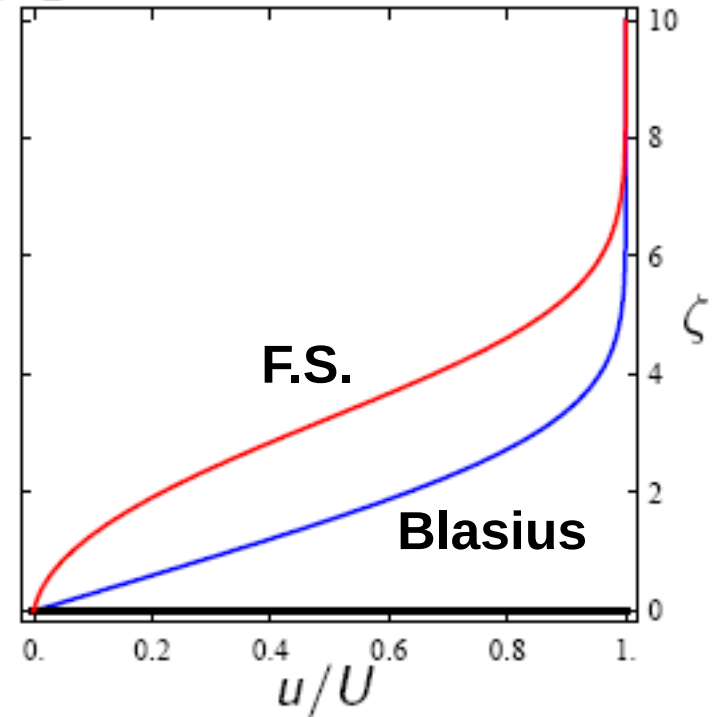
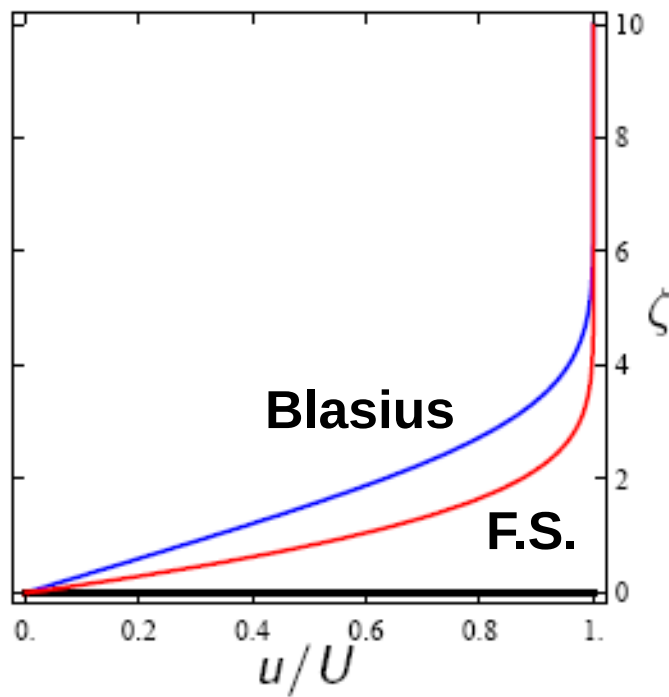
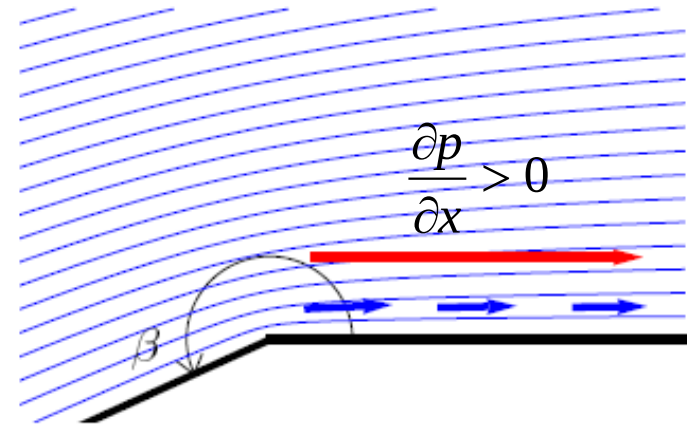
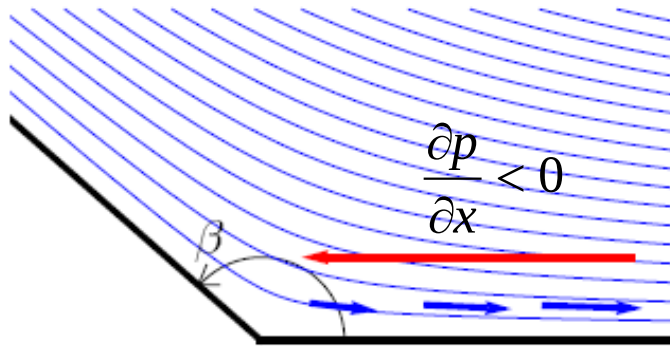
Pressure gradient effect

Favorable pressure gradient: $\frac{\partial p}{\partial x} < 0$



Close to the wall, the pressure gradient further increases the velocity of the flow $\Rightarrow$ no detachment

Pressure gradient effect



Falkner-Skan solutions

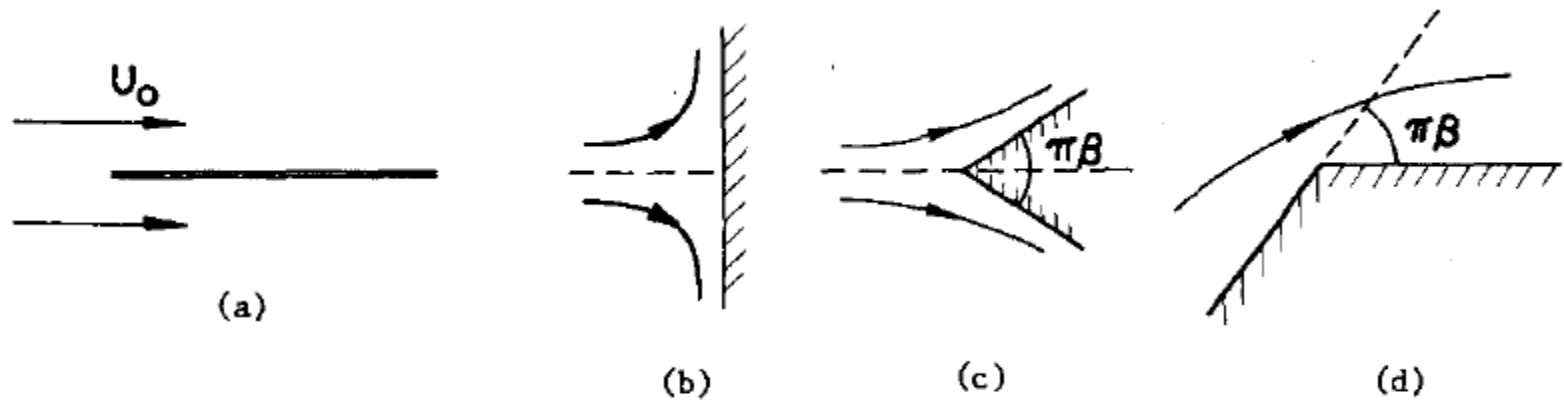
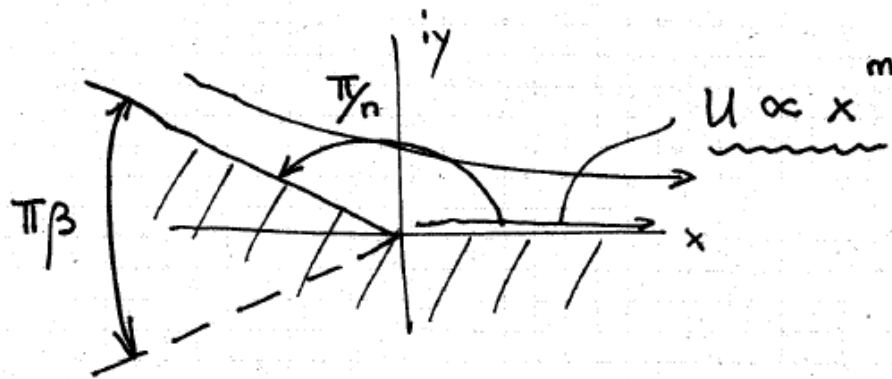


Figure 5.2 Boundary layer flows represented by solutions of the Falkner-Skan equation for different values of the parameter m : (a) $m = 0$; (b) $m = 1$; (c) $0 < m < 1$; (d) $-1/2 < m < 0$

Falkner-Skan far field solutions

pot. complexe

$$F(z) = C z^n$$



$$\frac{dF}{dz} = C n z^{n-1} = v_x - i v_y \rightarrow \boxed{n = 1 + m}$$

$$\frac{\pi}{n} + \frac{\pi\beta}{2} = \pi \rightarrow \frac{1}{1+m} + \frac{\beta}{2} = 1$$

$$\boxed{\beta = \frac{2m}{1+m}}$$

Falkner-Skan boundary layer equations

1. Prandtl equations

$$\hat{\psi}_{\hat{y}} \hat{\psi}_{x\hat{y}} - \hat{\psi}_x \hat{\psi}_{\hat{y}\hat{y}} = U \frac{dU}{dx} + \hat{\psi}_{\hat{y}\hat{y}\hat{y}},$$

$$\hat{\psi} = \hat{\psi}_{\hat{y}} = 0 \text{ on } \hat{y} = 0, \quad \hat{\psi}_{\hat{y}} \rightarrow U(x) \text{ as } \hat{y} \rightarrow \infty.$$

Falkner-Skan boundary layer equations

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2. Self-similar solution

$$\hat{\psi}(x, \hat{y}) = (Ax^{m+1})^{1/2} f(\eta) \text{ where } \eta = \hat{y}(Ax^{m-1})^{1/2}.$$

Falkner-Skan boundary layer equations

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$$\hat{\psi}_{\hat{y}} \hat{\psi}_{x\hat{y}} - \hat{\psi}_x \hat{\psi}_{\hat{y}\hat{y}} = U \frac{dU}{dx} + \hat{\psi}_{\hat{y}\hat{y}\hat{y}},$$

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2. Self-similar solution

$$\hat{\psi}(x, \hat{y}) = (Ax^{m+1})^{1/2} f(\eta) \text{ where } \eta = \hat{y}(Ax^{m-1})^{1/2}.$$

3. Falkner-Skan equation

$$f''' + \frac{1}{2}(m+1)ff'' + m(1-f'^2) = 0$$

$$f(0) = f'(0) = 0, \quad f'(\infty) = 1$$

Falkner-Skan boundary layer solutions

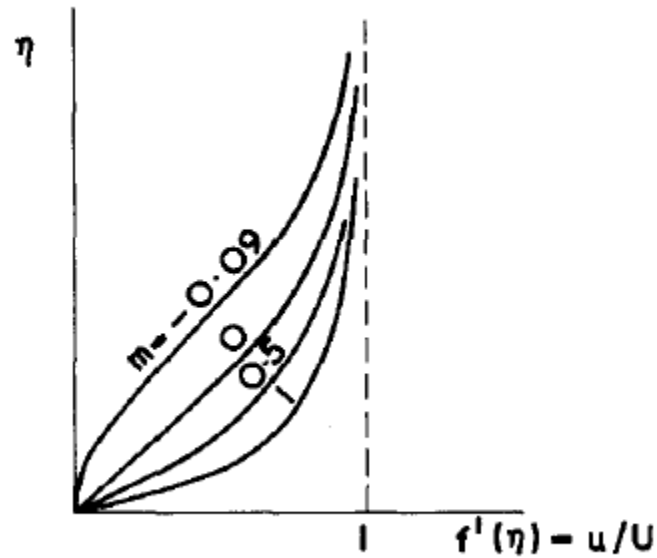
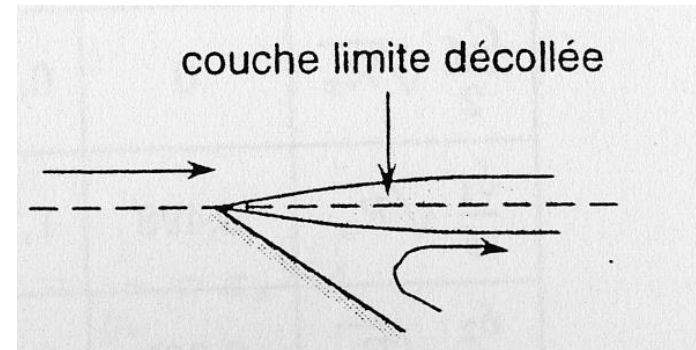
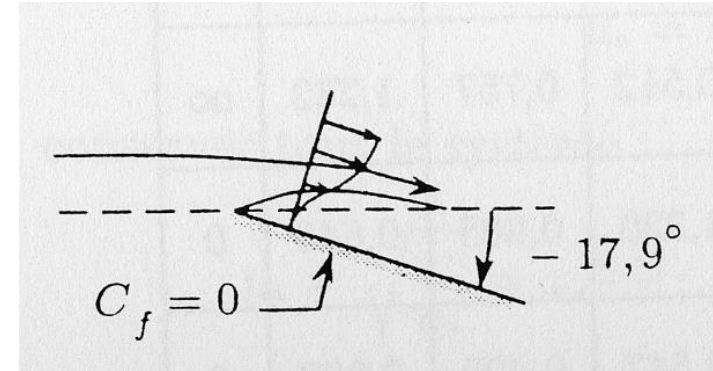
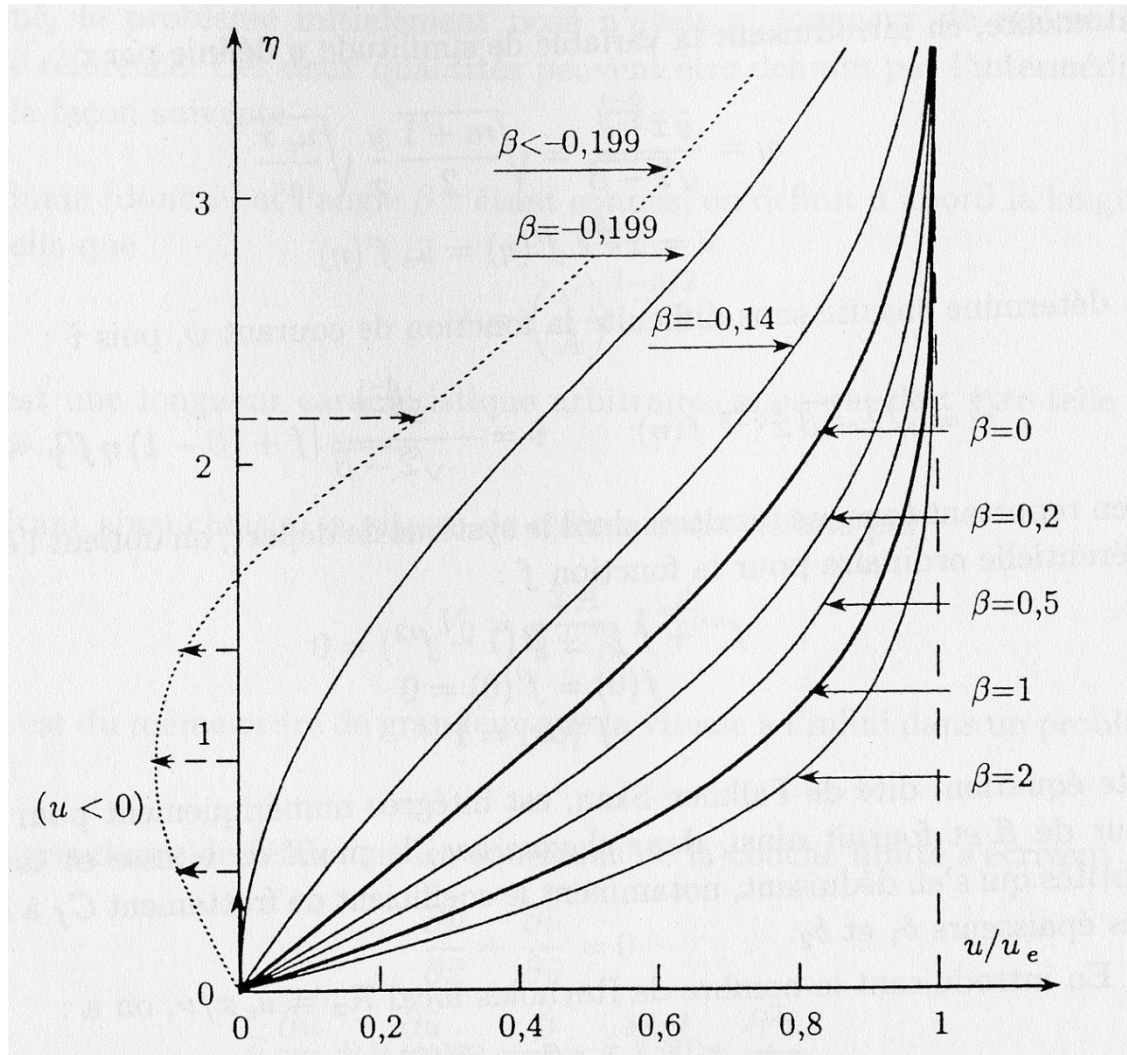


Figure 5.3 Sketch of velocity profiles given by solutions of the Falkner-Skan equation

Falkner-Skan boundary layer solutions

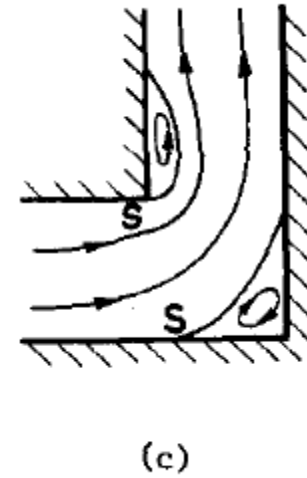
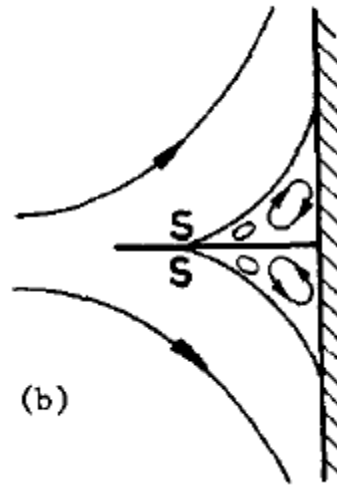
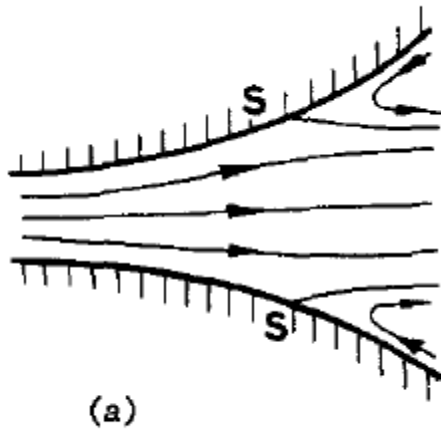


Boundary layer separation



$$\hat{\psi} \sim (x - x_s)^{1/2}, \quad \text{so that } \frac{\partial \hat{\psi}}{\partial x} \sim (x - x_s)^{-1/2} \text{ as } x \rightarrow x_s.$$

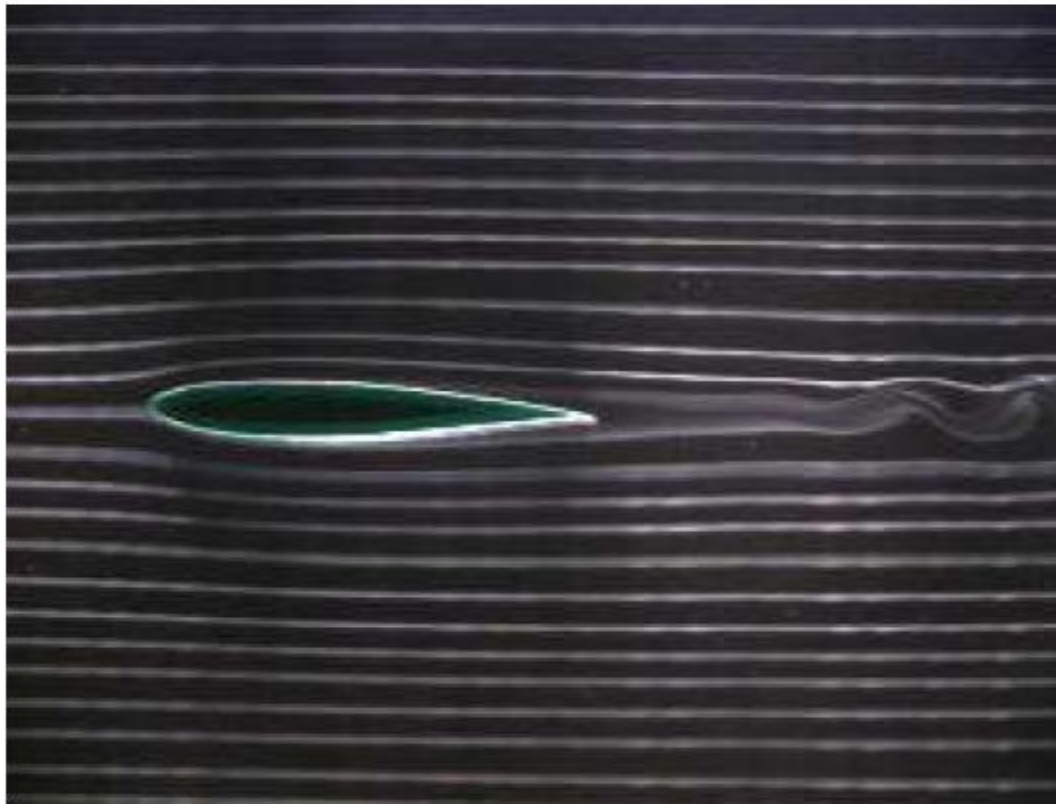
Boundary layer separation



Decollement sur un profil d'aile

Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 0^\circ$:

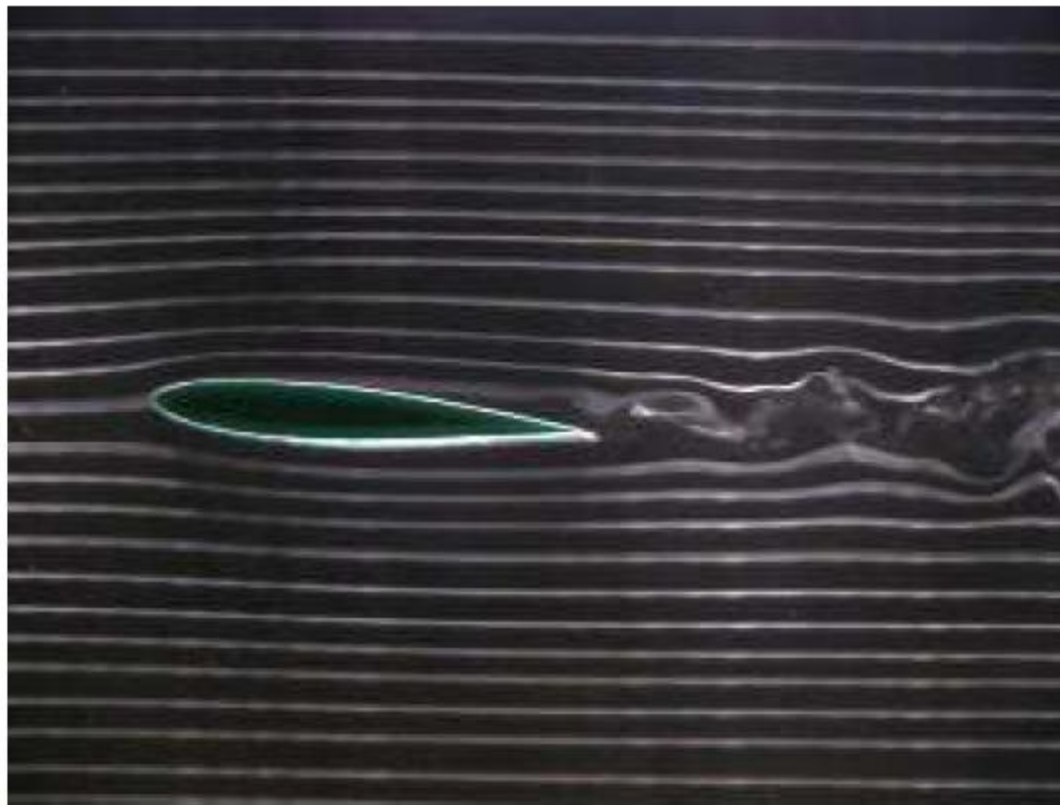


[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

Décollement sur un profil d'aile

Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 5^\circ$:

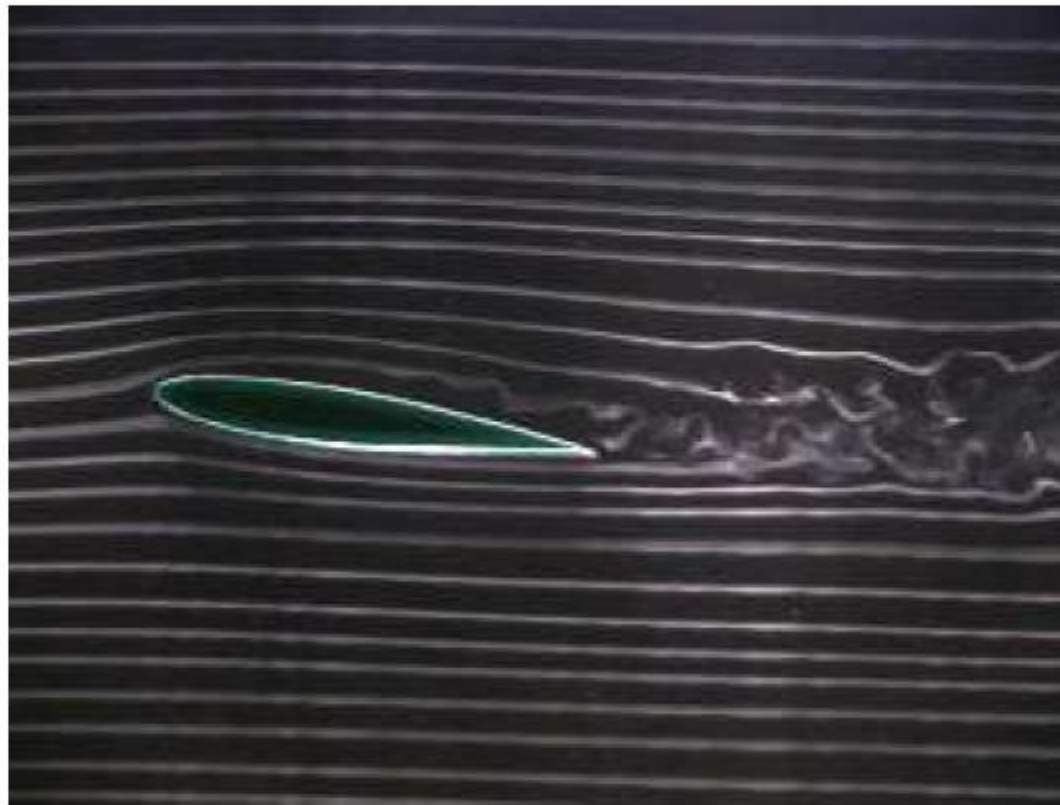


[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

Décollement sur un profil d'aile

Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 10^\circ$:

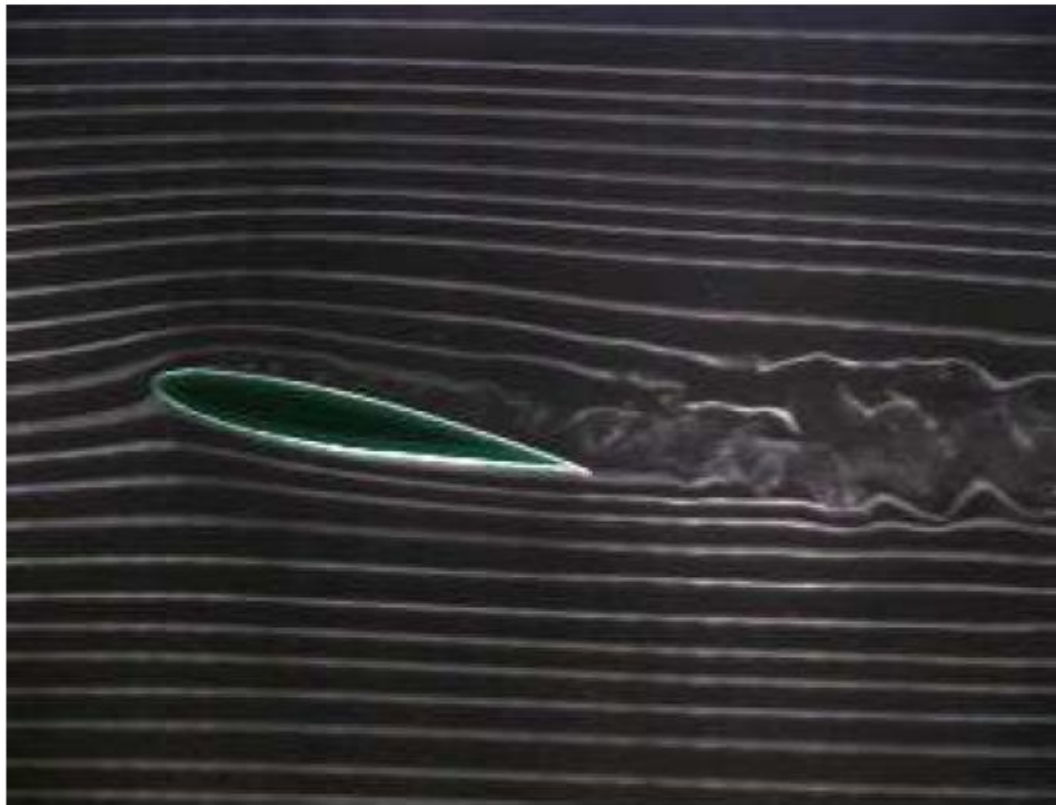


[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

Décollement sur un profil d'aile

Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 15^\circ$:

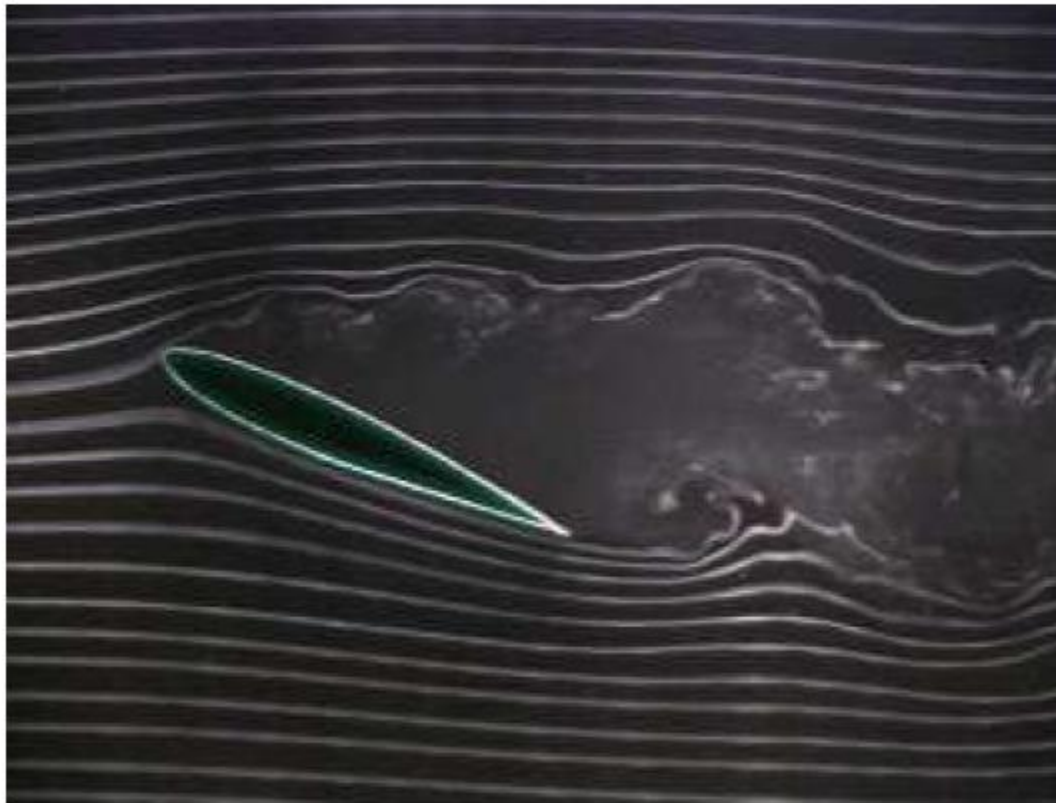


[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

Décollement sur un profil d'aile

Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 25^\circ$:



Décollement sur un profil d'aile

Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 30^\circ$:

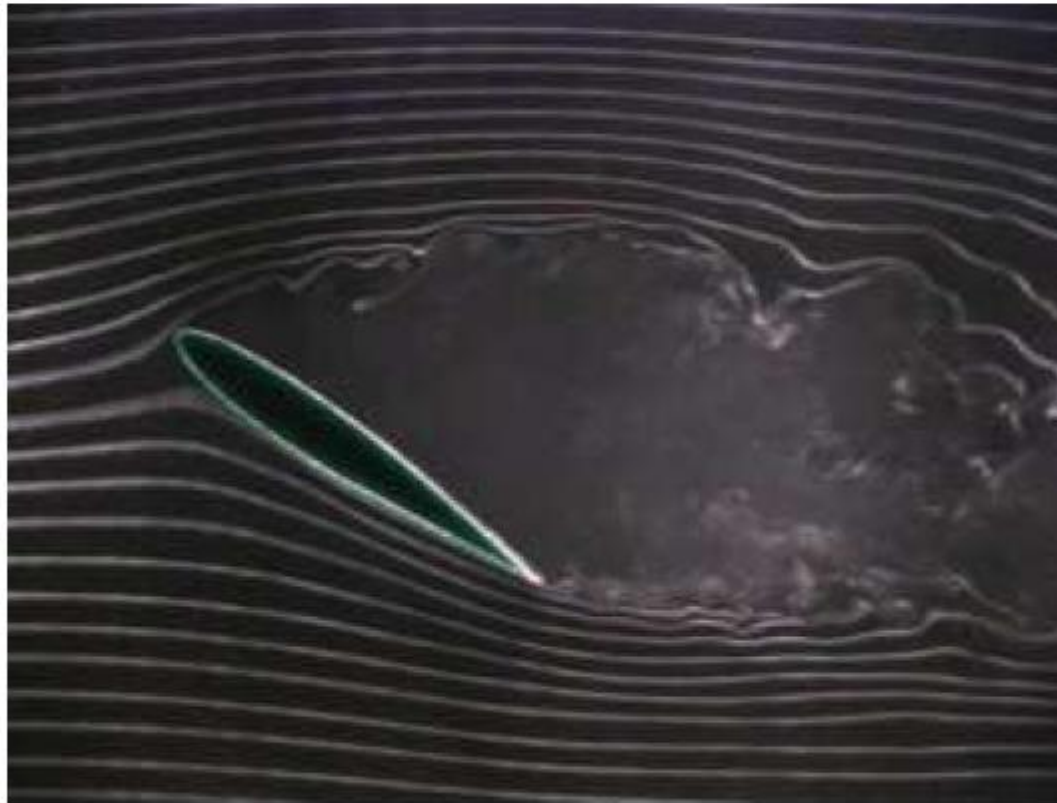


[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

Décollement sur un profil d'aile

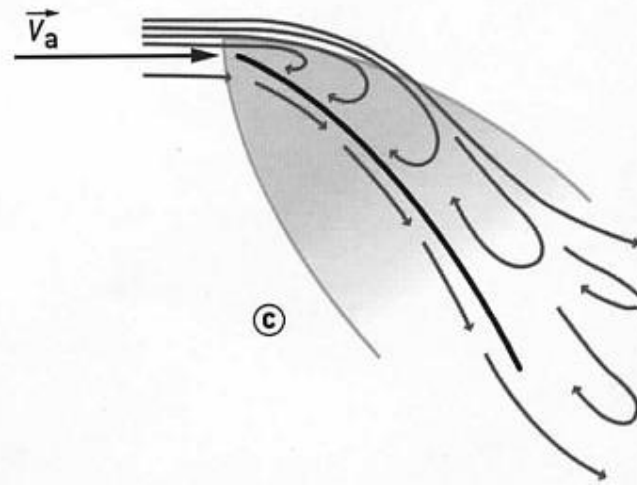
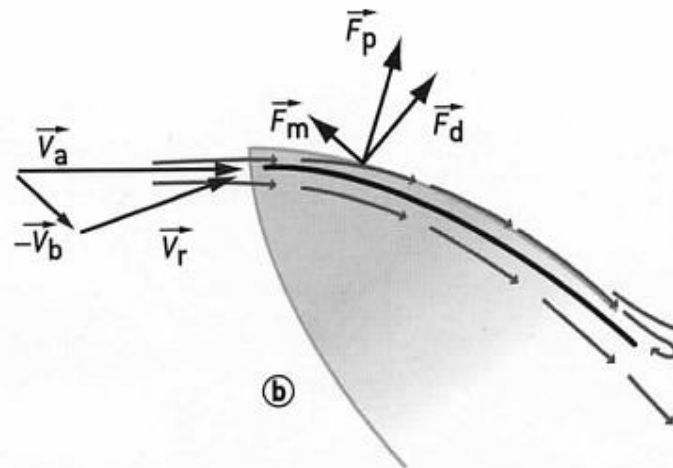
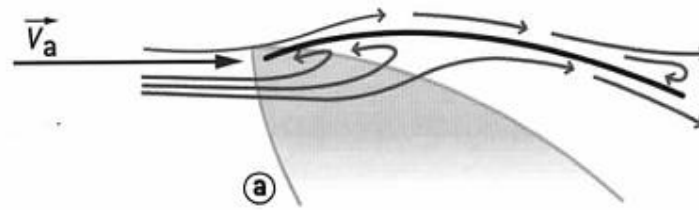
Expériences en soufflerie menées à l'université de Stanford, l'écoulement est visualisé grâce à des fumées :

angle d'incidence $\gamma = 35^\circ$:



[DVD 'Multimedia Fluid Mechanics', Homsy et al. 2004, Cambridge University Press]

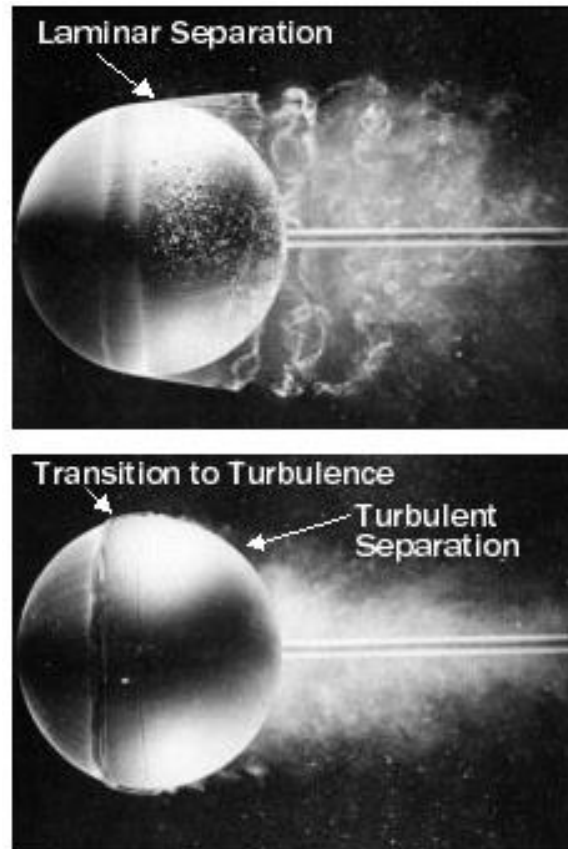
Application to sailing



Application to sailing



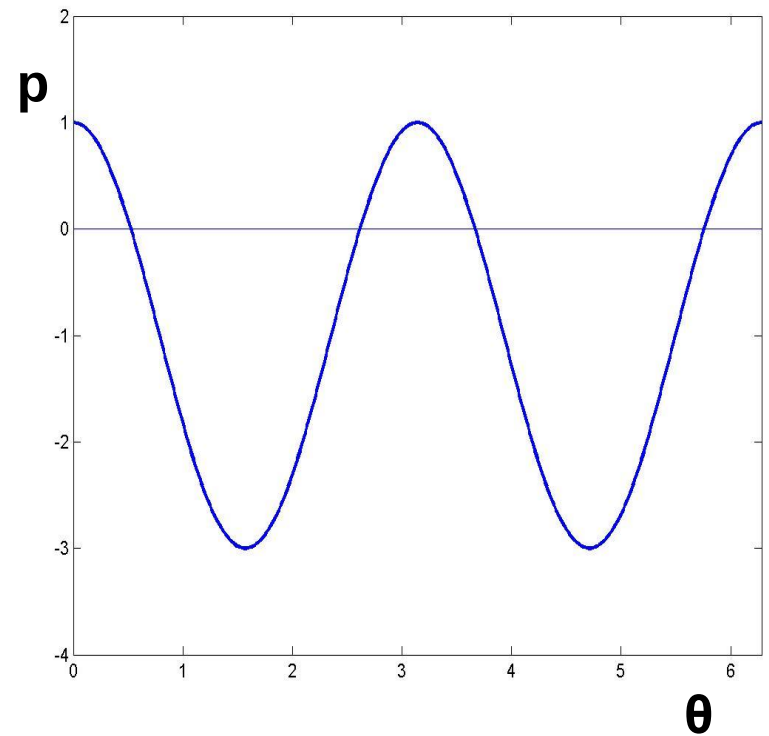
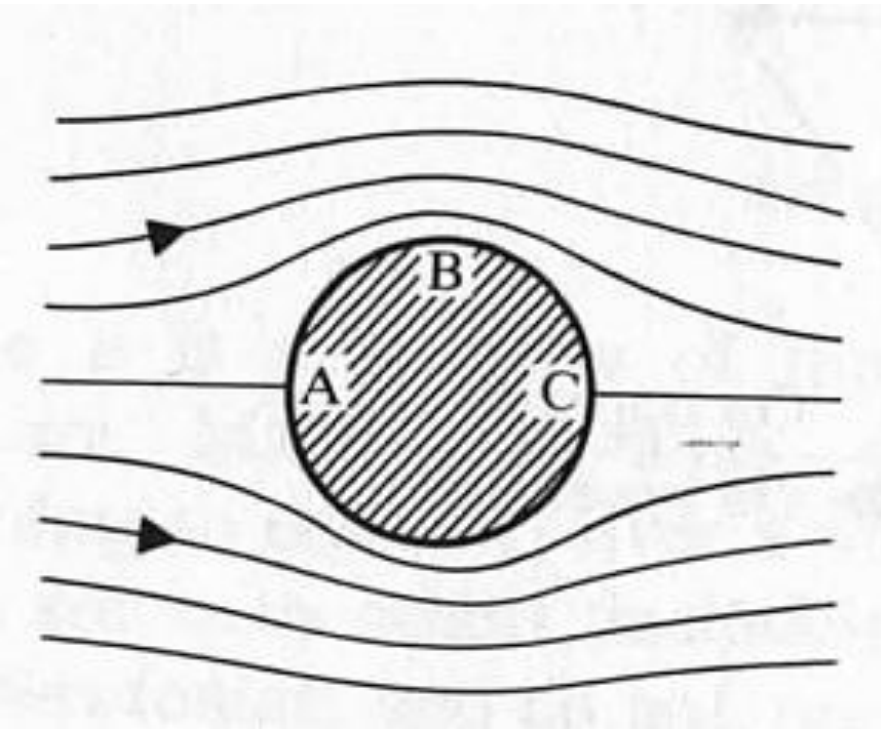
Example: Flow around a sphere



© ONERA

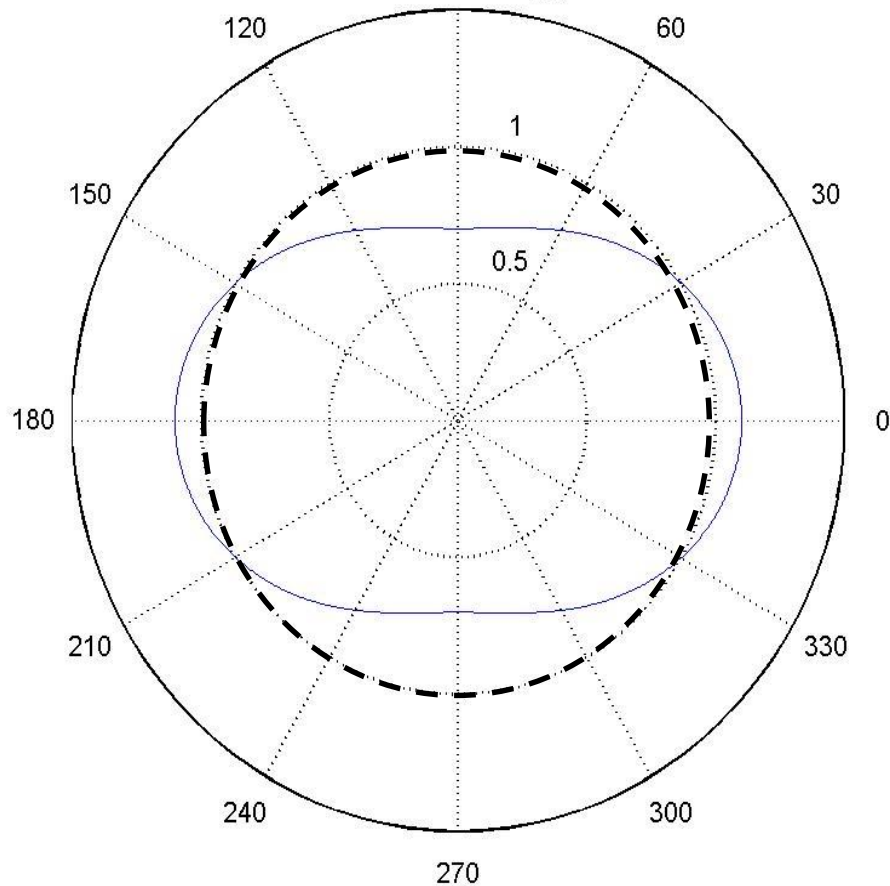
Flow around a cylinder

$$p(a, \theta) = \frac{1}{2} \rho U_{\infty}^2 (1 - 4 \sin^2 \theta)$$

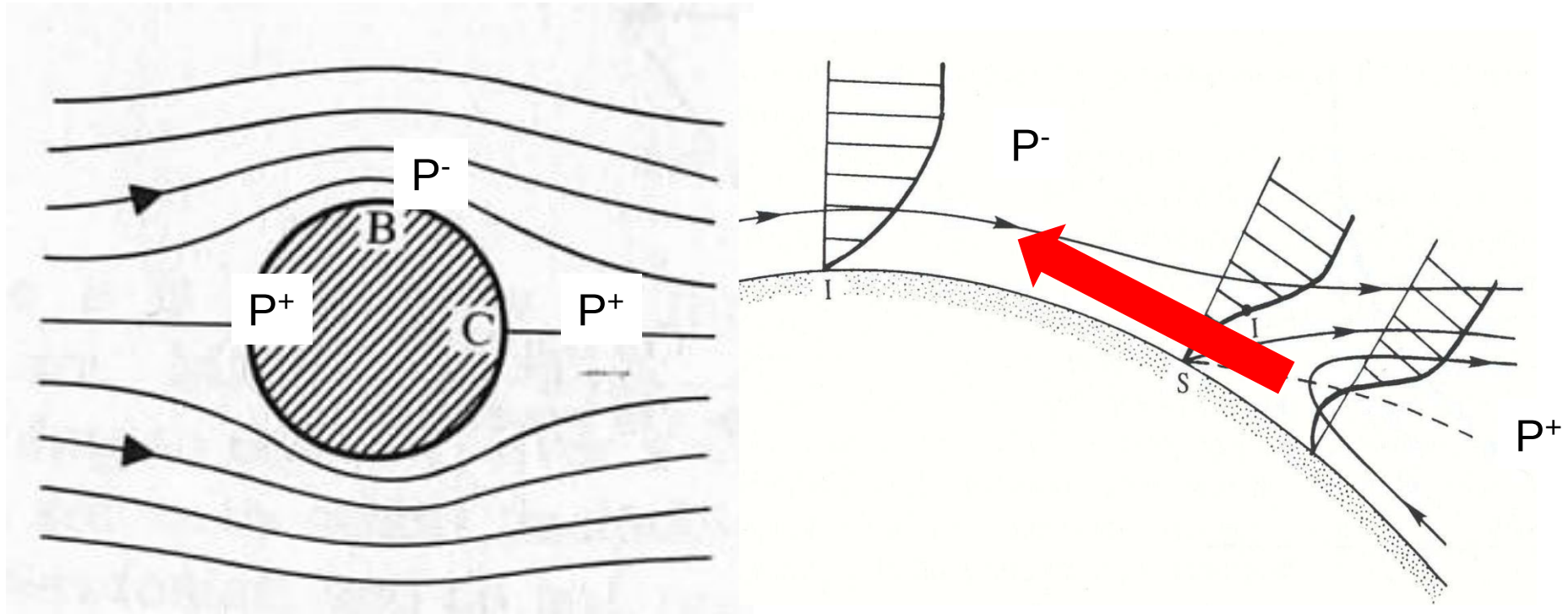


Flow around a cylinder

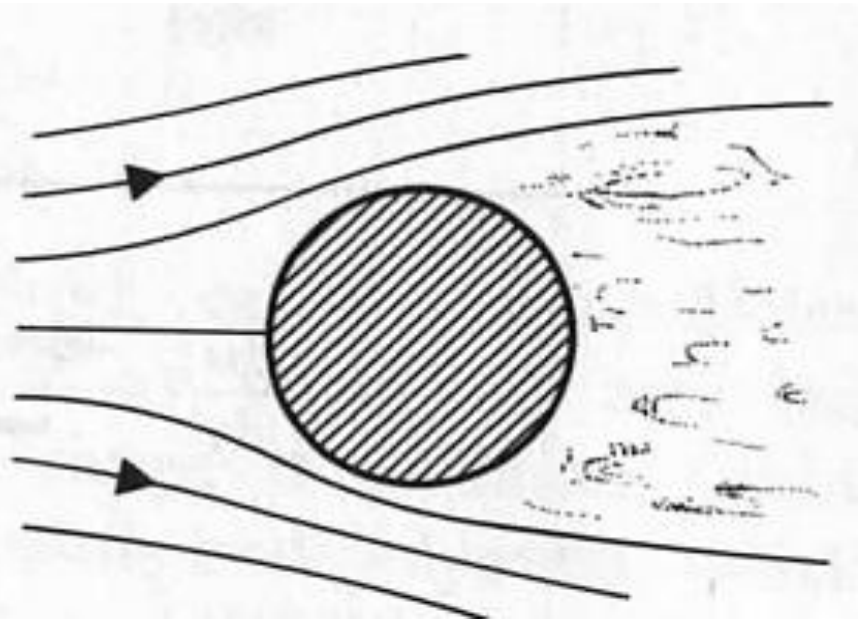
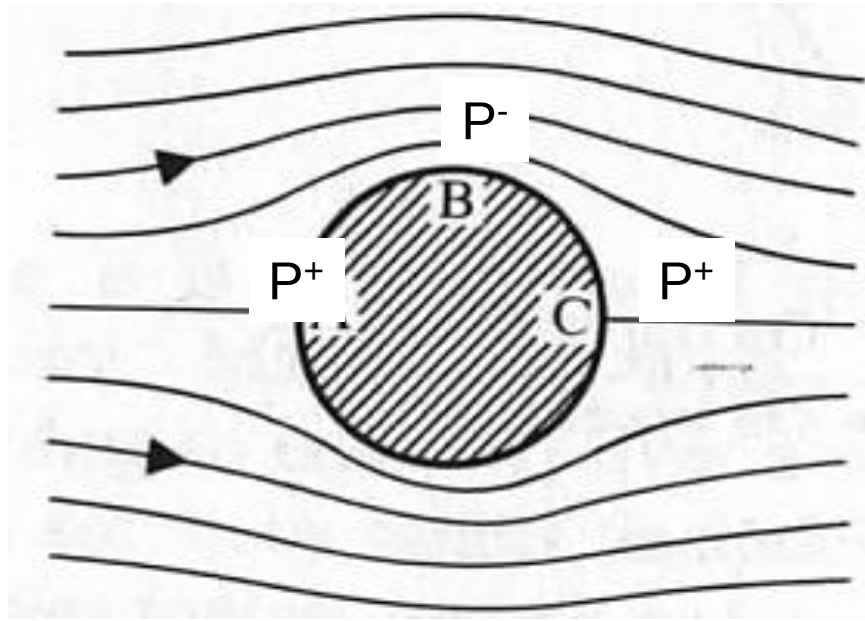
$$p(a, \theta) = \frac{1}{2} \rho U_{\infty}^2 (1 - 4 \sin^2 \theta)$$



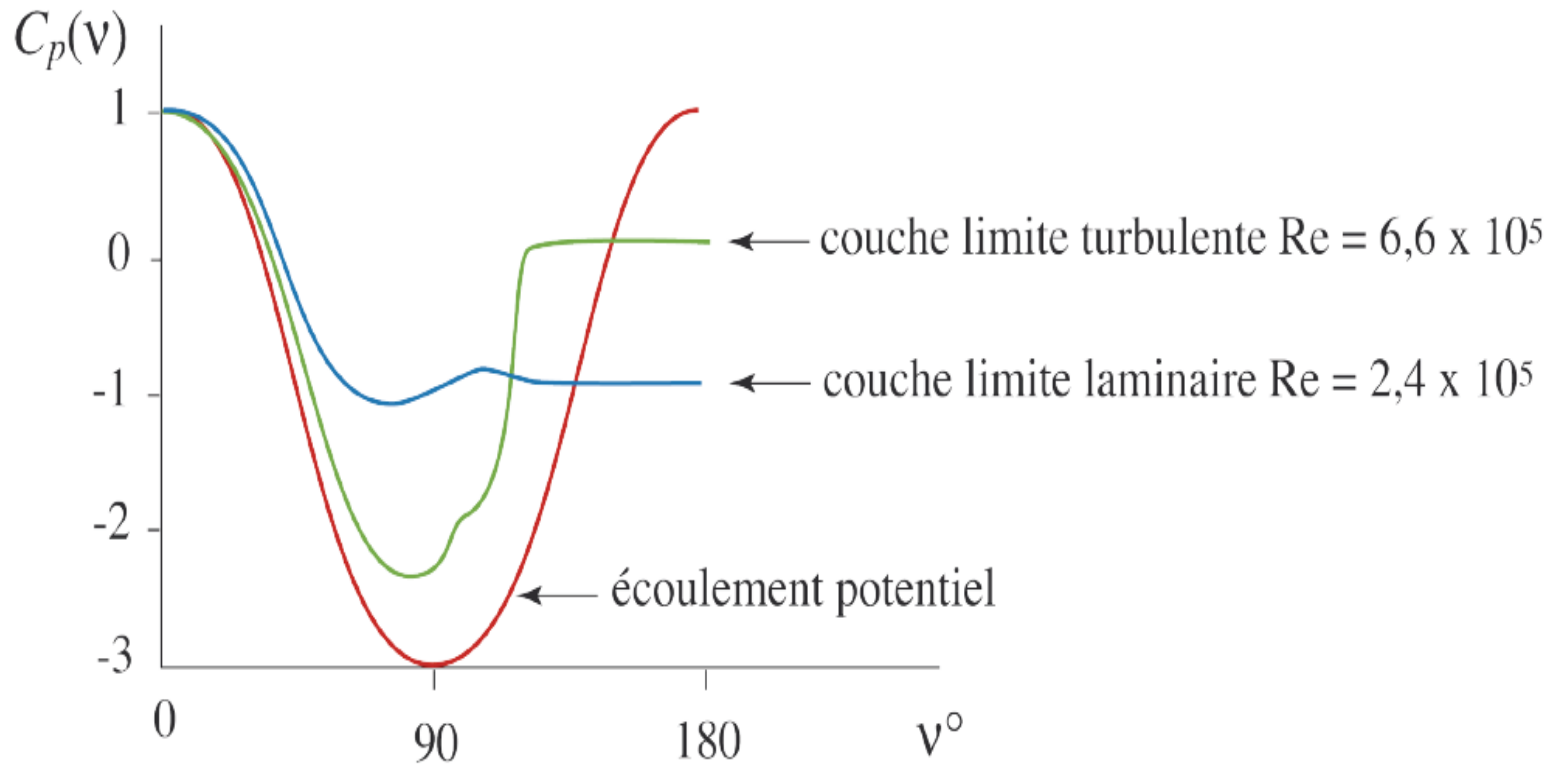
Origin of detachment: pressure gradient



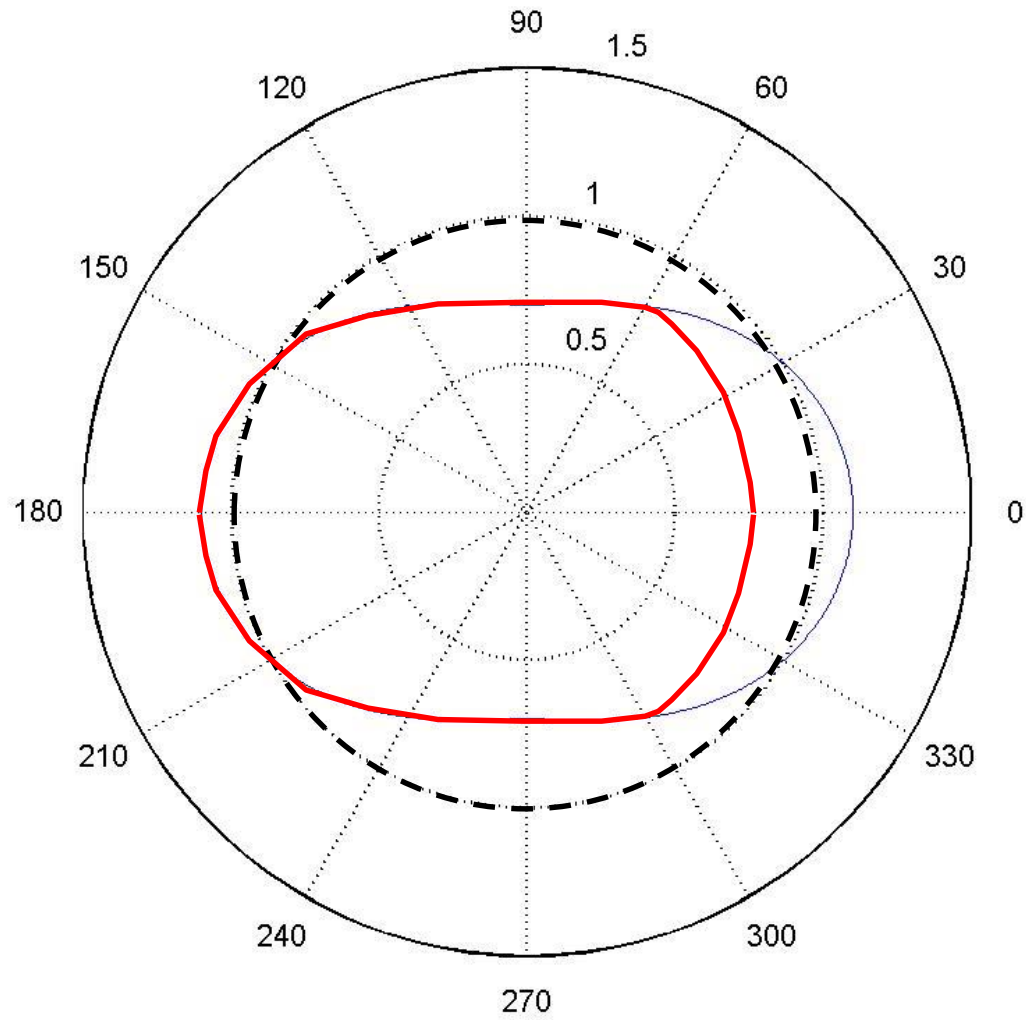
A viscous flow close to the wall opposes the free-stream



Pressure coefficient



Form drag



Drag coefficient

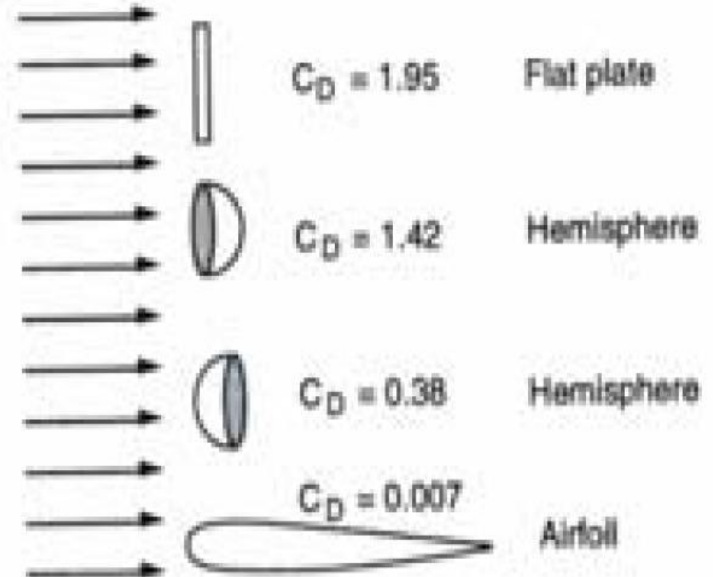
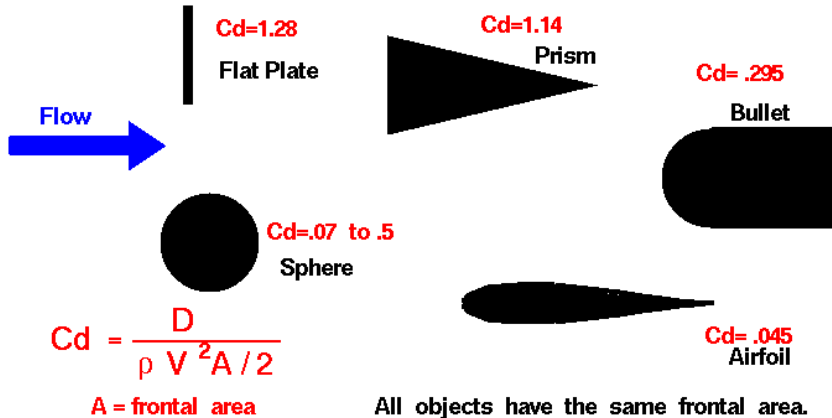
$$C_X = \frac{\text{trainée}}{\frac{1}{2} \rho U^2 A}$$



Shape Effects on Drag

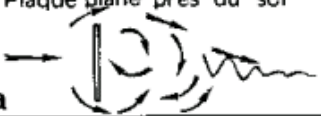
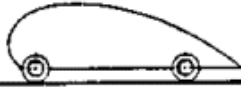
Glenn
Research
Center

The shape of an object has a very great effect on the amount of drag.

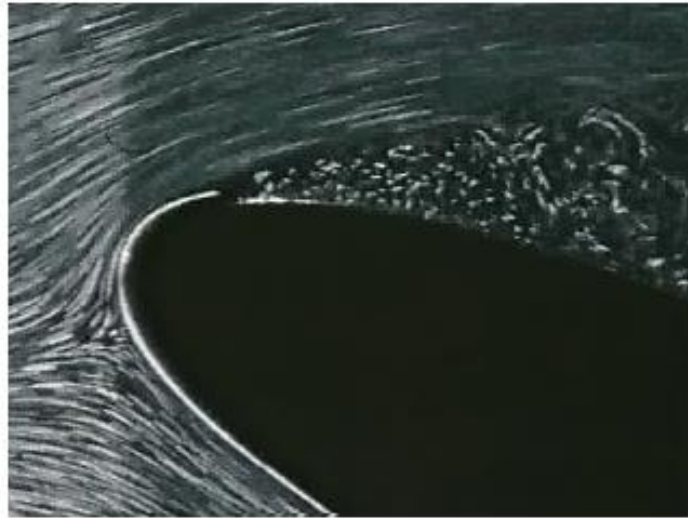


$$C_x = \frac{\text{drag}}{\frac{1}{2}\rho U^2 A}$$

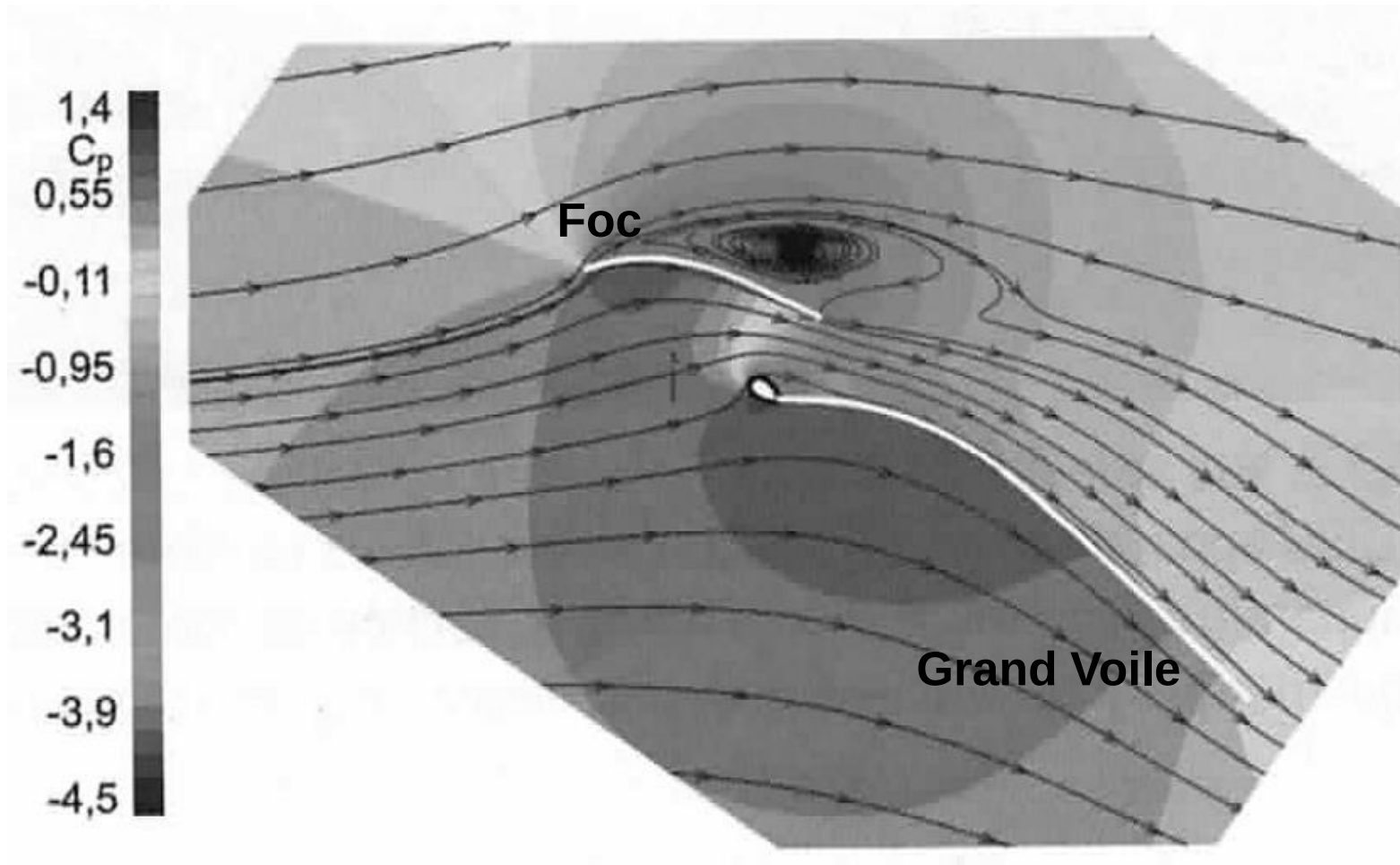
section, somewhat arbitrary...

Plaque plane près du sol		C_{xp}
a		1,27
b		0,9
c		0,52
d		0,34
e		0,2
f		0,43
g		0,75 à 0,9

Separation control



Application to sailing



Thickness effect

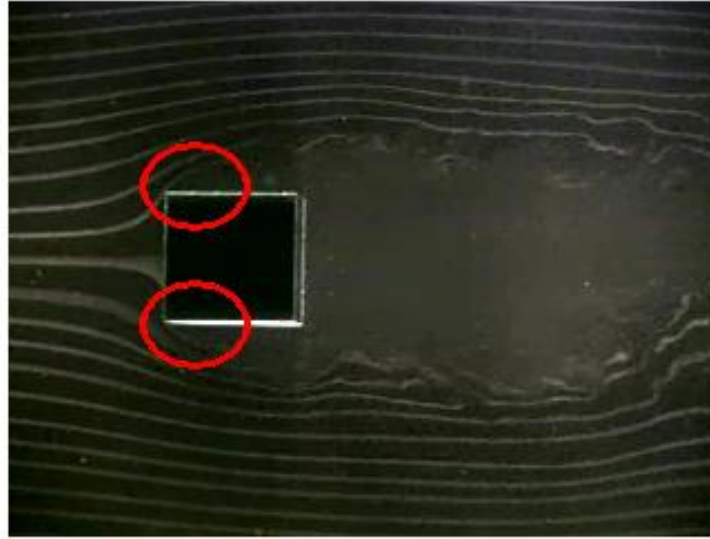


Attached

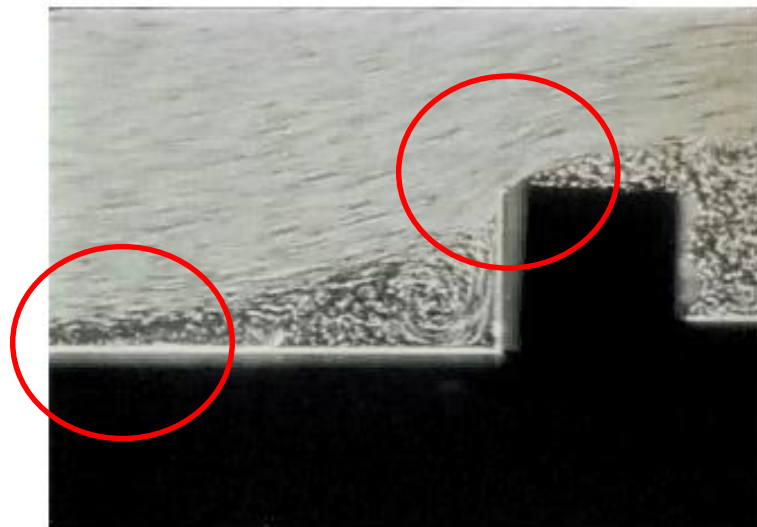
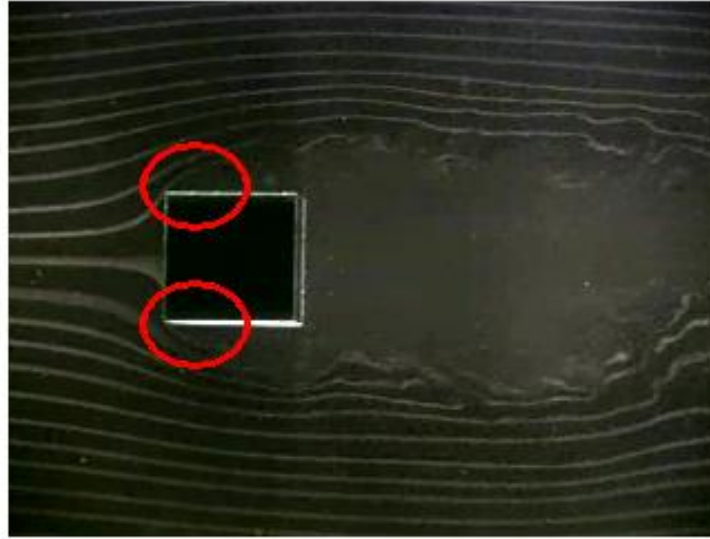


Detached

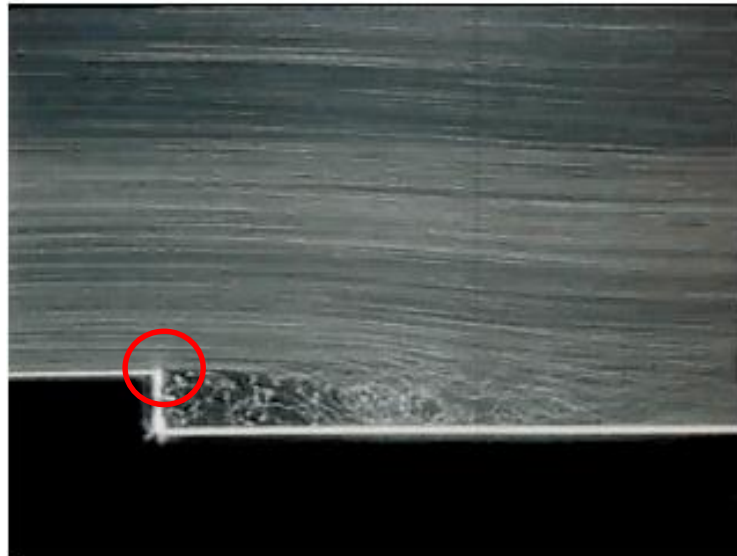
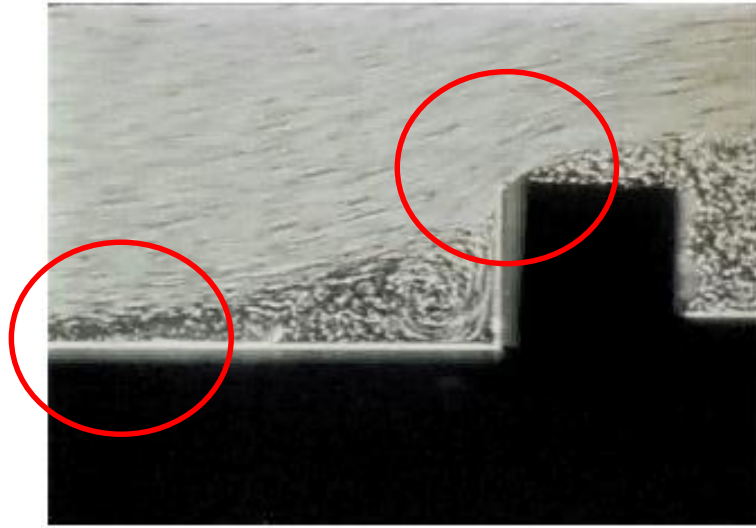
A gallery of detached flows



A gallery of detached flows

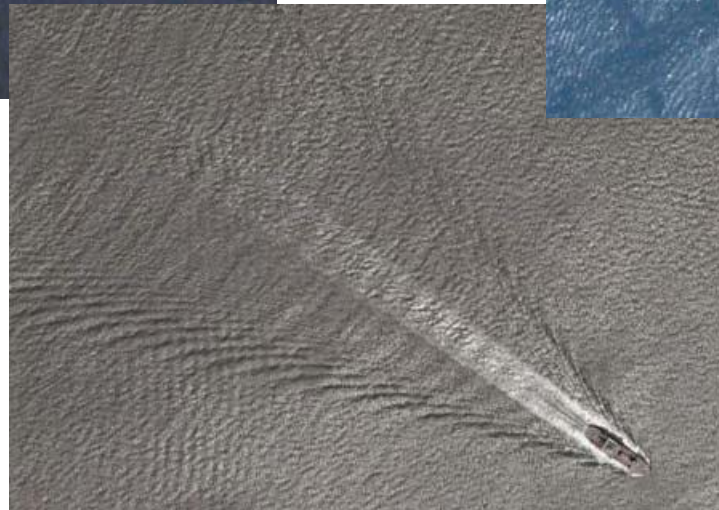


A gallery of detached flows

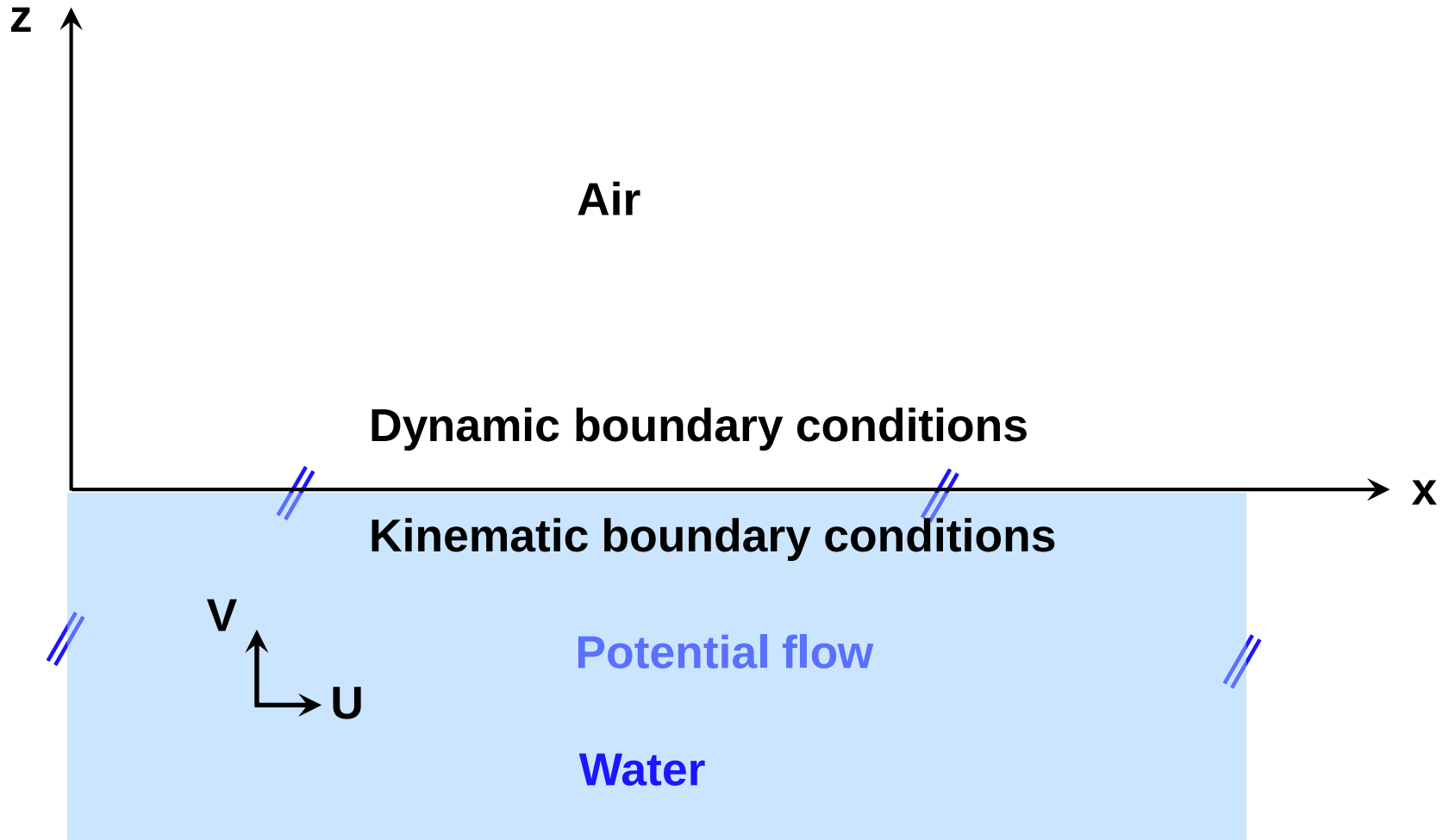


Hydrodynamics 13

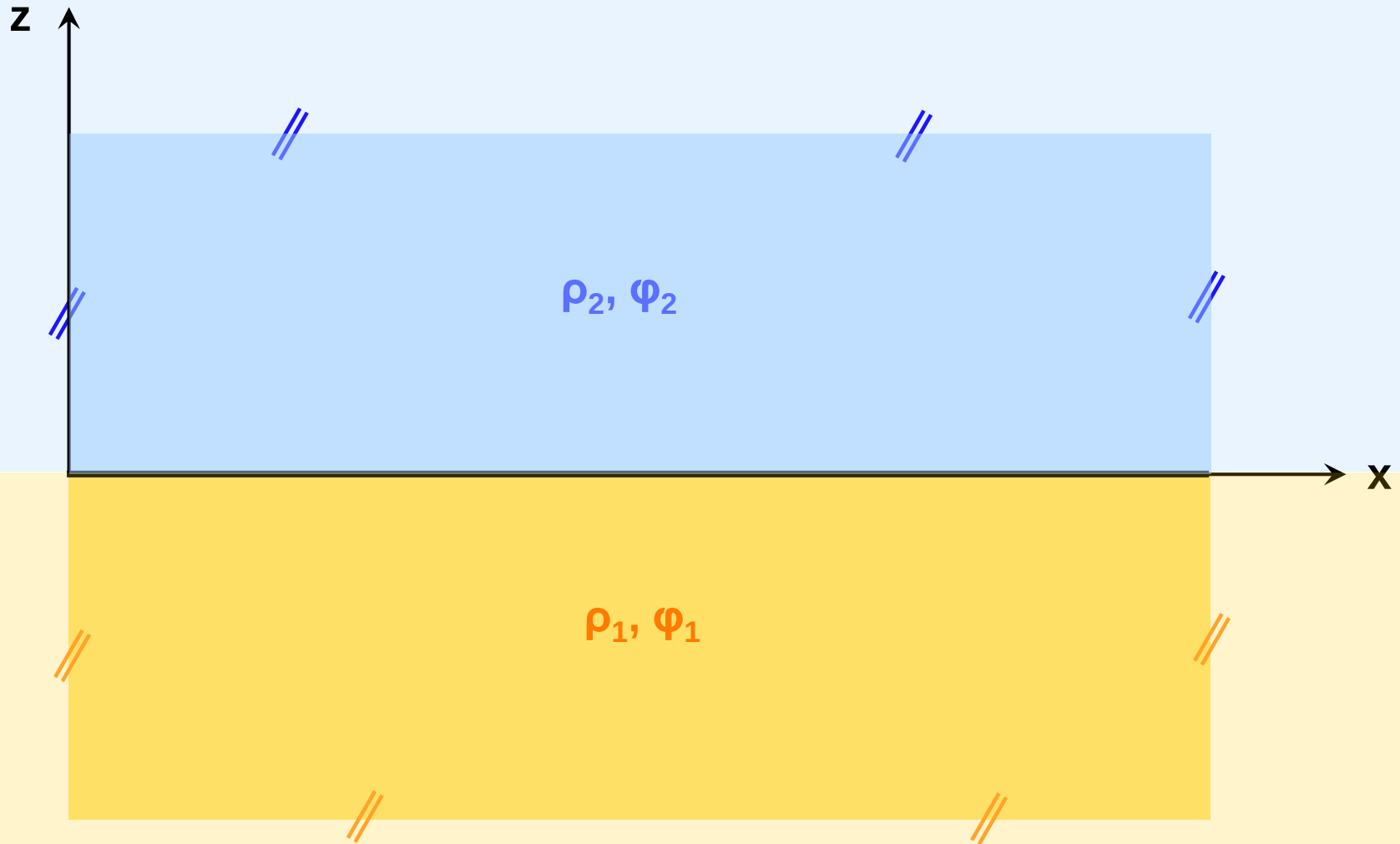
Waves



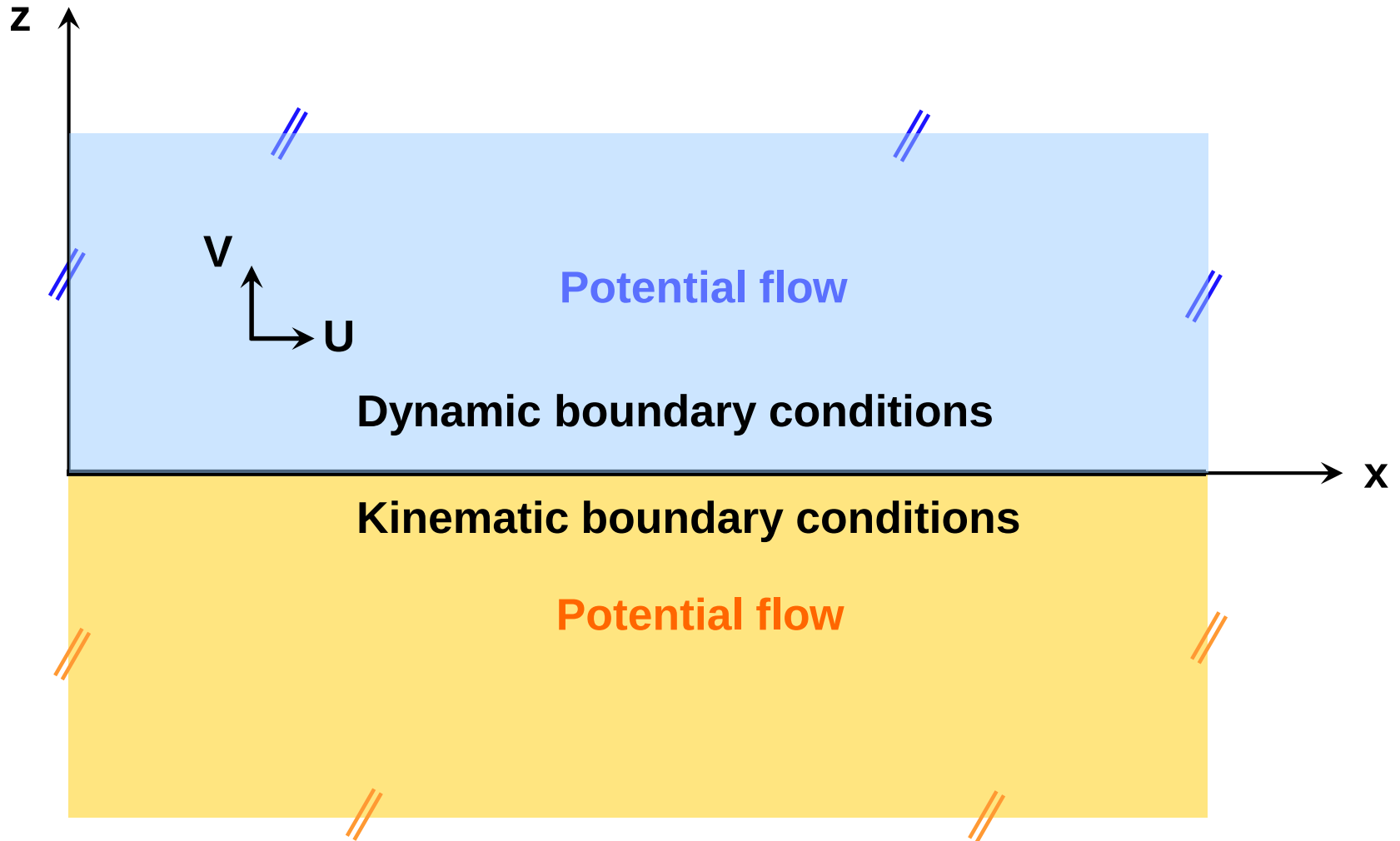
Waves



General case: two fluids



General case: two fluids



Linear waves dispersion relation

1. Equations and boundary conditions
2. Base state
3. Linearized equations
4. Normal mode expansion
5. Dispersion relation
6. Analysis of the dispersion relation

1. Equations

$$\begin{array}{l} \Delta \Phi_1 = 0 \\ \Delta \Phi_2 = 0 \end{array}$$

Potential flow

$$\begin{array}{ll} U_1 = \frac{\partial \Phi_1}{\partial x}, & V_1 = \frac{\partial \Phi_1}{\partial z} \\ U_2 = \frac{\partial \Phi_2}{\partial x}, & V_2 = \frac{\partial \Phi_2}{\partial z} \end{array}$$

Velocity field

1. Boundary conditions

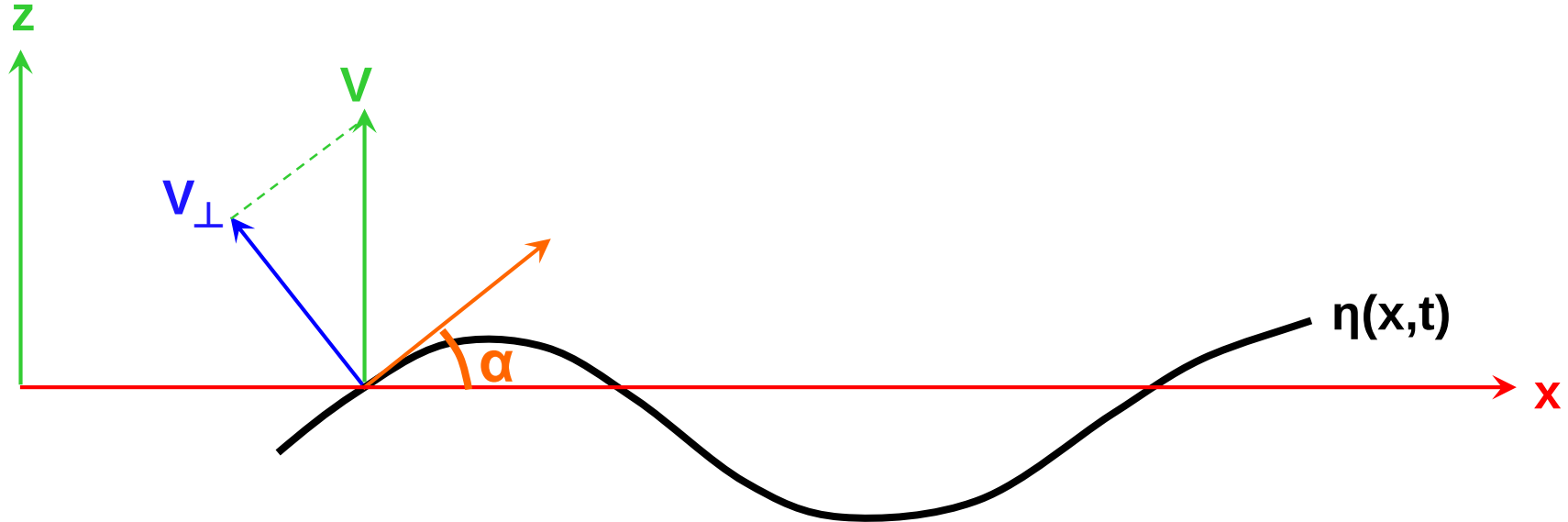
$$\Phi_1 = 0 \text{ at } z = -\infty$$

$$\Phi_2 = 0 \text{ at } z = +\infty$$

far-field

at $z = \eta$?

1. Kinematic boundary condition

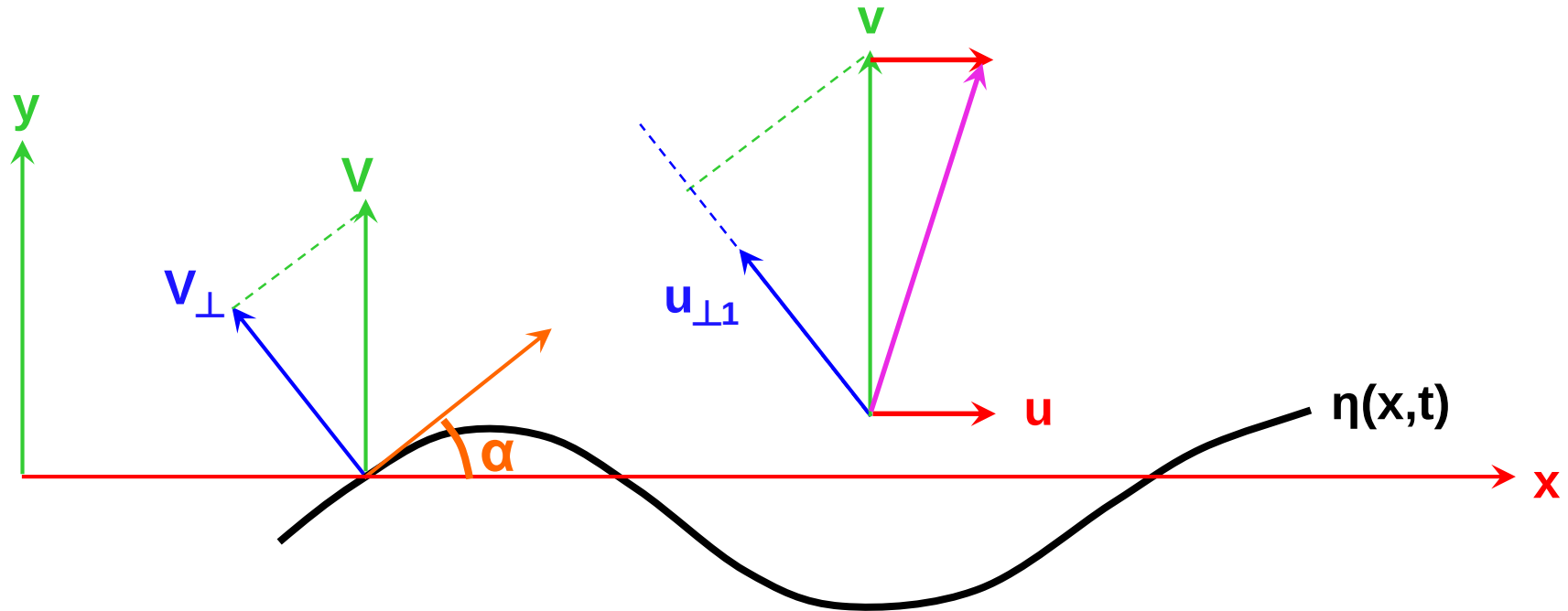


Kinematic condition : impermeability (no penetration)

No fluid particles going across the interface through the normal direction

$$\mathbf{V}_\perp = \partial\eta/\partial t \cos(\alpha)$$

1. Kinematic boundary condition



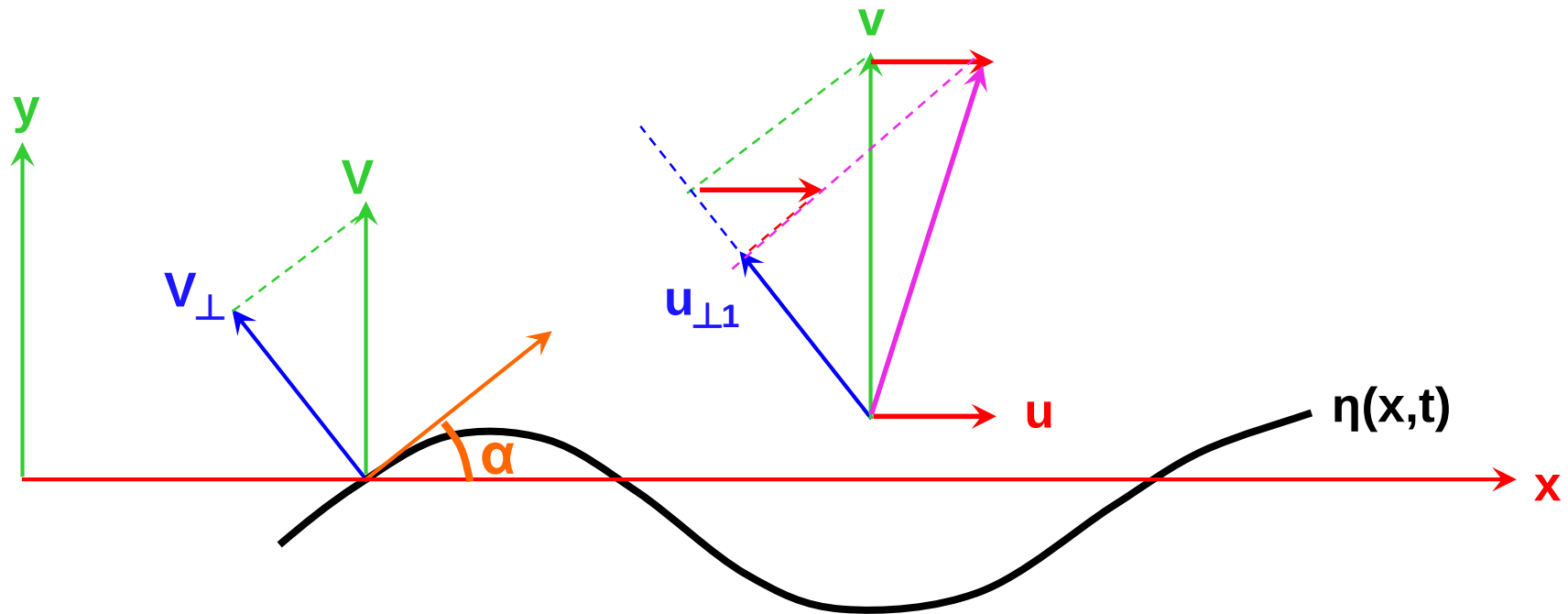
Kinematic condition : impermeability (no penetration)

No fluid particles going across the interface through the normal direction

$$\mathbf{v}_\perp = \frac{\partial \eta}{\partial t} \cos(\alpha)$$

$$\mathbf{u}_{\perp 1} = \mathbf{v}_1 \cos(\alpha) +$$

1. Kinematic boundary condition



Kinematic condition : impermeability (no penetration)

No fluid particles going across the interface through the normal direction

$$\left. \begin{aligned} V_{\perp} &= \frac{\partial \eta}{\partial t} \cos(\alpha) \\ u_{\perp 1} &= v_1 \cos(\alpha) - u_1 \sin(\alpha) \end{aligned} \right\} \frac{\partial \eta}{\partial t} = v_1 - u_1 \tan(\alpha) \Rightarrow \boxed{\frac{\partial \eta}{\partial t} = v_1 - u_1 \frac{\partial \eta}{\partial x}}$$

1. Kinematic boundary conditions

$$\Phi_1 = 0 \text{ at } z = -\infty$$

$$\Phi_2 = 0 \text{ at } z = +\infty$$

far-field

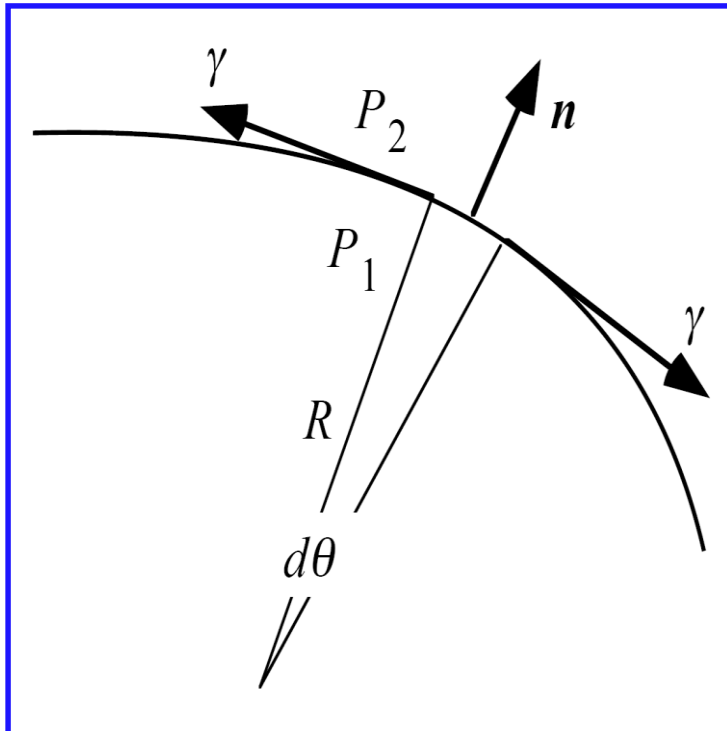
$$U_1 \frac{\partial \eta}{\partial x} - V_1 = - \frac{\partial \eta}{\partial t}$$

$$U_2 \frac{\partial \eta}{\partial x} - V_2 = - \frac{\partial \eta}{\partial t}$$

at $z = \eta$

1. Dynamic boundary conditions

$$P_1 - P_2 = -\gamma \frac{\frac{\partial^2 \eta}{\partial x^2}}{\left(1 + \frac{\partial \eta}{\partial x}\right)^{3/2}} \text{ at } z = \eta$$



$$\mathbf{n} = \frac{(-\partial_x \eta, 1)}{\sqrt{1 + \partial_x^2 \eta}}$$

$$\mathcal{C} = \nabla \cdot \mathbf{n}$$

1. More equations

$$\begin{aligned} \frac{\partial \Phi_1}{\partial t} + \frac{U_1^2 + V_1^2}{2} + \frac{P_1}{\rho_1} + gz &= C_1(t) = 0 \\ \frac{\partial \Phi_2}{\partial t} + \frac{U_2^2 + V_2^2}{2} + \frac{P_2}{\rho_2} + gz &= C_2(t) = 0 \end{aligned}$$

2nd Bernouilli relations

2. Base state

$$\Phi_1 = 0,$$

$$\Phi_2 = 0$$

$$\eta = 0$$

$$P_1 = -\rho_1 g z$$

3. Perturb and linearize perturbation expansion

Φ_1	$= 0$	$+\epsilon\phi_1$
Φ_2	$= 0$	$+\epsilon\phi_2$
U_1	$= 0$	$+\epsilon u_1$
V_1	$= 0$	$+\epsilon v_1$
U_2	$= 0$	$+\epsilon u_2$
V_2	$= 0$	$+\epsilon v_2$
P_1	$= -\rho_1 g z$	$+\epsilon p_1$
P_2	$= -\rho_2 g z$	$+\epsilon p_2$
η	$= 0$	$+\epsilon\sigma$

$\epsilon \ll 1$

Variables **Base state** **Small perturbation**

3. Linearized equations

$$\begin{array}{l} \Delta\phi_1 = 0 \\ \Delta\phi_2 = 0 \end{array}$$

perturbed potential flow

$$\begin{array}{ll} u_1 = \frac{\partial\phi_1}{\partial x}, & v_1 = \frac{\partial\phi_1}{\partial z} \\ u_2 = \frac{\partial\phi_2}{\partial x}, & v_2 = \frac{\partial\phi_2}{\partial z} \end{array}$$

3. Perturbed kinematic boundary conditions

$$\phi_1 = 0 \text{ at } z = -\infty$$

$$\phi_2 = 0 \text{ at } z = +\infty$$

$$-\epsilon^2 u_1 \frac{\partial \sigma}{\partial x} + \epsilon v_1 = \epsilon \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma$$

$$-\epsilon^2 u_2 \frac{\partial \sigma}{\partial x} + \epsilon v_2 = \epsilon \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma$$

3. Perturbed kinematic boundary conditions

$$\phi_1 = 0 \text{ at } z = -\infty$$

$$\phi_2 = 0 \text{ at } z = +\infty$$

~~$$-\epsilon^2 u_1 \frac{\partial \sigma}{\partial x} + \epsilon v_1 = \epsilon \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma$$
$$-\epsilon^2 u_2 \frac{\partial \sigma}{\partial x} + \epsilon v_2 = \epsilon \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma$$~~

$$v_1 = \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma$$
$$v_2 = \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma$$

3. Flattened kinematic boundary conditions

$$\begin{aligned}\frac{\partial \phi_1}{\partial z} &= \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma \\ \frac{\partial \phi_2}{\partial z} &= \frac{\partial \sigma}{\partial t} \text{ at } z = \epsilon \sigma\end{aligned}$$

Taylor expansion around 0: $\phi(\epsilon \sigma) = \phi(0) + (\epsilon \sigma) \frac{\partial \phi}{\partial z} \Big|_0$

$$\begin{aligned}\frac{\partial \phi_1}{\partial z} &= \frac{\partial \sigma}{\partial t} \text{ at } z = 0 \\ \frac{\partial \phi_2}{\partial z} &= \frac{\partial \sigma}{\partial t} \text{ at } z = 0\end{aligned}$$

⇒ transforms a b.c. at an unknown interface into a fixed place!

3. Perturbed dynamic boundary conditions

$$(P_1 + \epsilon p_1 - P_2 - \epsilon p_2)|_{\epsilon\sigma} = -\gamma\epsilon \frac{\partial^2 \sigma}{\partial x^2} \left(1 - 3/2\epsilon^2 \left(\frac{\partial \sigma}{\partial x} \right)^2 \right)$$

Replace $P_1 = -g\rho_1 z$, ...

and linearize

$$g(\rho_2 - \rho_1)\sigma + (p_1 - p_2)|_{\epsilon\sigma} = -\gamma \frac{\partial^2 \sigma}{\partial x^2}$$

flatten

$$(\rho_2 - \rho_1)g\sigma + (p_1 - p_2)|_0 = -\gamma \frac{\partial^2 \sigma}{\partial x^2}$$

3. Perturbed and linearized Bernoulli

Perturbed 2nd Bernoulli relations

$$\begin{aligned}\epsilon \frac{\partial \phi_1}{\partial t} + \cancel{\epsilon^2 \frac{u_1^2 + v_1^2}{2}} + \epsilon \frac{p_1}{\rho_1} &= 0 \\ \epsilon \frac{\partial \phi_2}{\partial t} + \cancel{\epsilon^2 \frac{u_2^2 + v_2^2}{2}} + \epsilon \frac{p_2}{\rho_2} &= 0\end{aligned}$$

Linearized 2nd Bernoulli relations

$$\begin{aligned}\frac{\partial \phi_1}{\partial t} + \frac{p_1}{\rho_1} &= 0 \\ \frac{\partial \phi_2}{\partial t} + \frac{p_2}{\rho_2} &= 0\end{aligned}$$

4. Normal mode expansion

Fourier transform in x and t

$$\begin{aligned}\phi_1 &= f_1(z)\exp(i(kx - \omega t)), \\ \phi_2 &= f_2(z)\exp(i(kx - \omega t)), \\ \sigma &= C\exp(i(kx - \omega t)),\end{aligned}$$

k is the wavenumber and ω the frequency (in rad/s)

$$\lambda = 2\pi/k$$

$$T = 2\pi/\omega$$

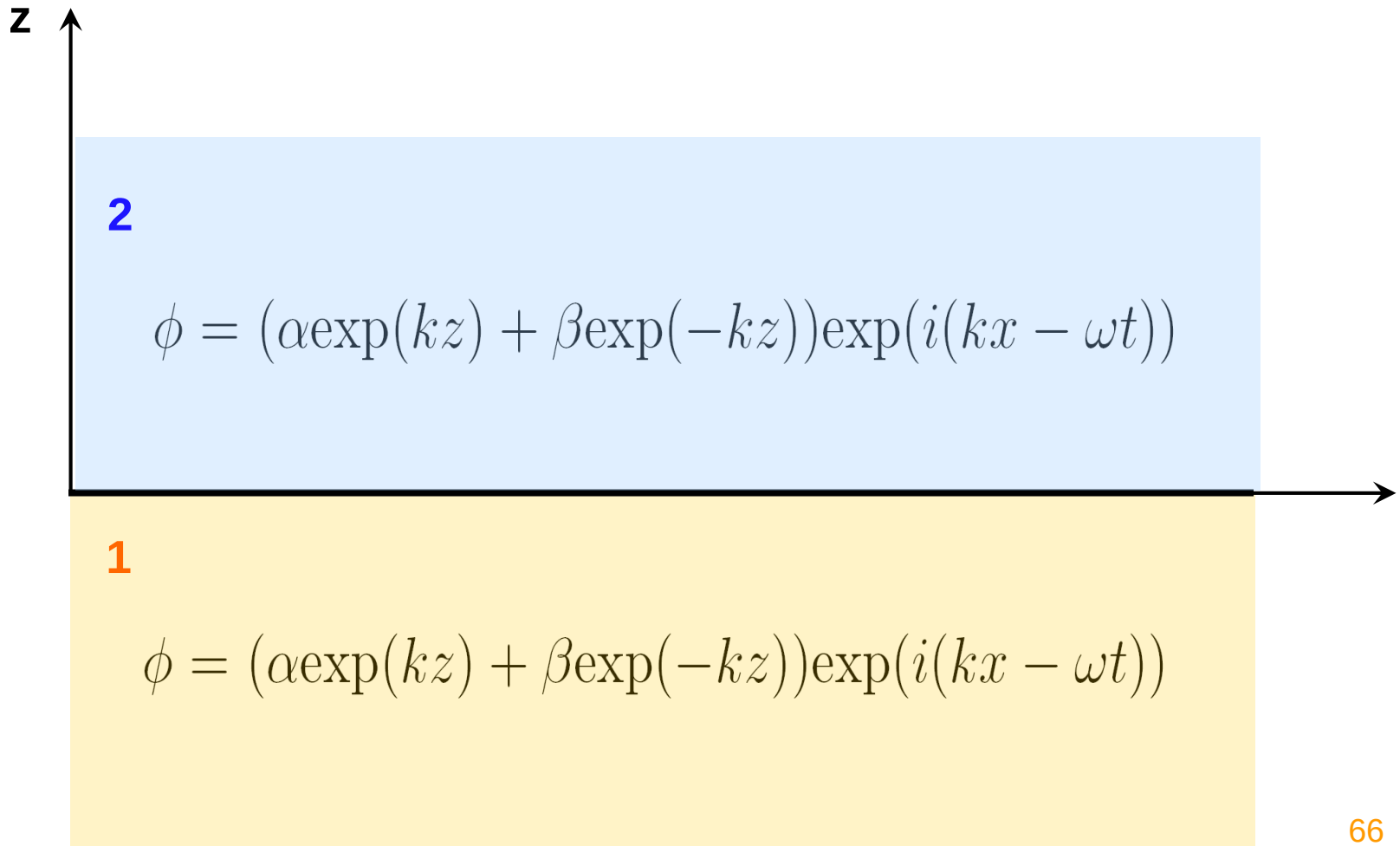
$$f = \omega/(2\pi)$$

4. Normal mode expansion

Solution to Laplace equation:

4. Normal mode expansion

Solution to Laplace equation:



4. Normal mode expansion

Solution to Laplace equation:

$$\begin{aligned}\phi_1 &= A \exp(kz) \exp(i(kx - \omega t)), \\ \phi_2 &= B \exp(-kz) \exp(i(kx - \omega t)), \\ \sigma &= C \exp(i(kx - \omega t)).\end{aligned}$$

4. Normal mode expansion

Replace in boundary conditions

$$\begin{aligned} g(\rho_2 - \rho_1)C + i\omega\rho_1 A - i\omega\rho_2 B &= \gamma k^2 C \\ kA &= -i\omega C \\ -kB &= -i\omega C \end{aligned}$$

This is an eigenvalue problem $i\omega X = MX$!

$$kg(\rho_2 - \rho_1)C + \omega^2\rho_1 C + \omega^2\rho_2 C = \gamma k^3 C,$$

5. Dispersion relation

$$\omega^2 = \frac{-kg(\rho_2 - \rho_1) + \gamma k^3}{\rho_1 + \rho_2}$$

•Unstable if there exists one ω , $\text{Im}(\omega) > 0$

$$\rho_2 > \rho_1$$

•Neutral if for all ω , $\text{Im}(\omega) = 0$:

$$\rho_1 > \rho_2$$

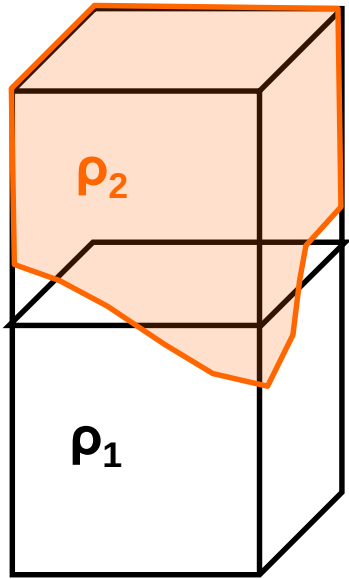
•Stable (or damped) if for all ω , $\text{Im}(\omega) < 0$:

The flow considered is not damped, we have neglected dissipation by neglecting viscosity

Instability analysis:

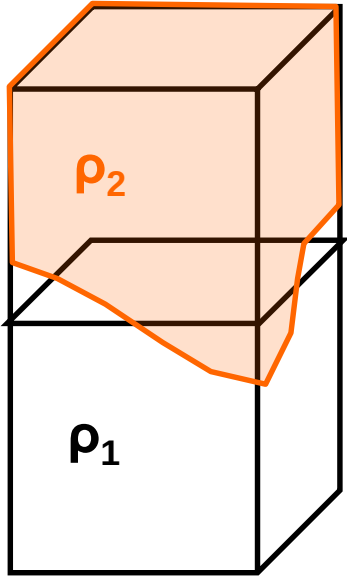
1. Equations and boundary conditions
2. Base state
3. Linearized equations
4. Normal mode expansion
5. Dispersion relation
6. Analysis of the dispersion relation

Dispersion relation



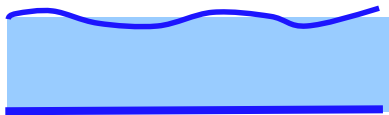
$$\omega^2 = \frac{-kg(\rho_2 - \rho_1) + \gamma k^3}{\rho_1 + \rho_2}$$

Dispersion relation



$$\omega^2 = \frac{-kg(\cancel{\rho_2} - \rho_1) + \gamma k^3}{\rho_1 + \cancel{\rho_2}}$$

$$\omega^2 = \tanh(kH) \left(\frac{\gamma k^3}{\rho} + gk \right)$$



Dispersion relation

$$\omega^2 = \tanh(kH) \left(\frac{\gamma k^3}{\rho} + gk \right)$$

Capillary wavenumber: $k_c = \sqrt{\rho g / \gamma}$

Length scale: $\tilde{k} = k / k_c$

Time scale $\tilde{\omega} = \omega / \sqrt{g k_c}$

One single non-dimensional parameter $\tilde{H} = H k_c$

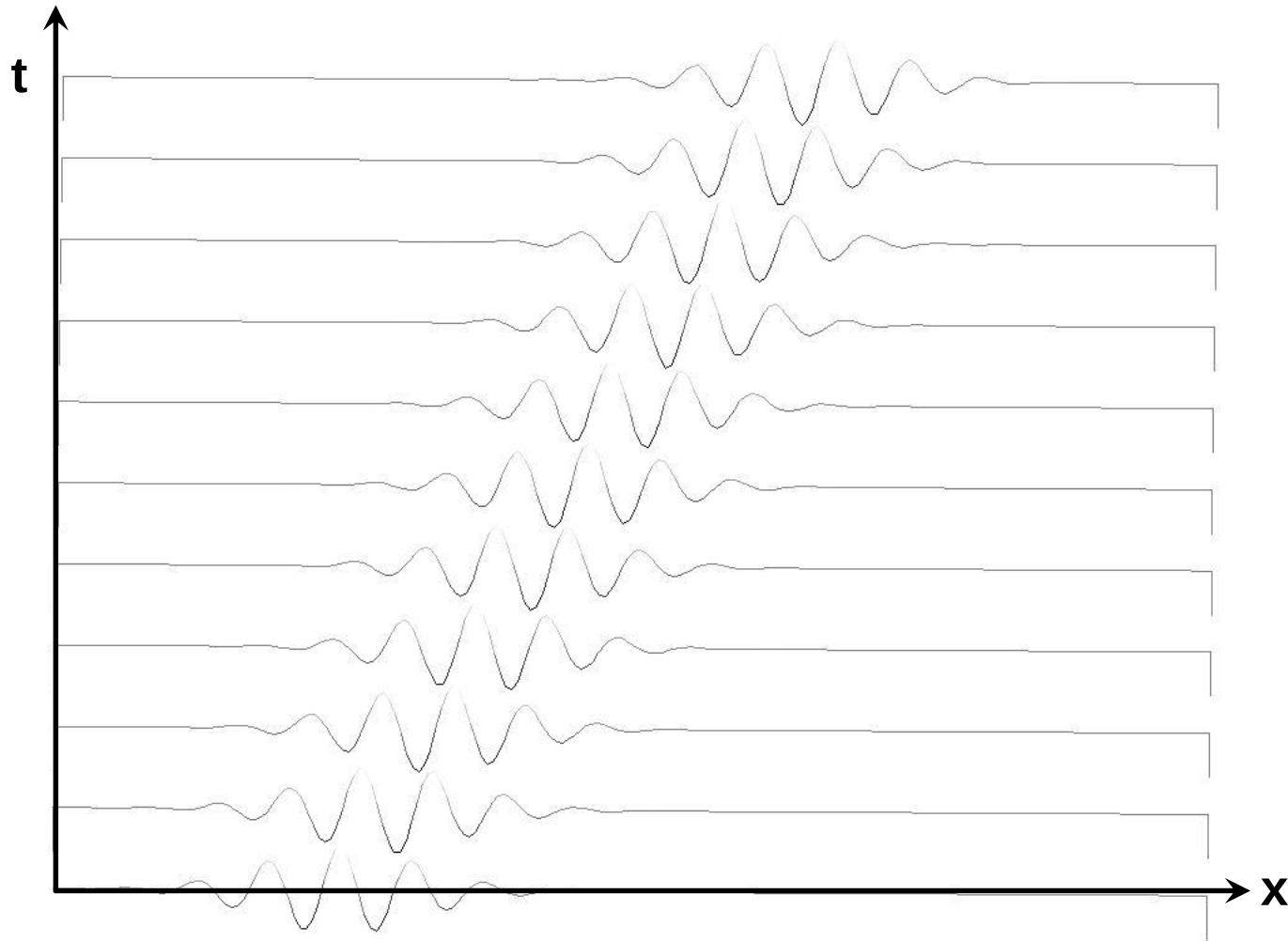
$$\tilde{\omega}^2 = \tanh(\tilde{k} \tilde{H}) \left(\tilde{k}^3 + \tilde{k} \right)$$

Dispersion relation

$$\tilde{\omega}^2 = \tanh(\tilde{k}\tilde{H}) \left(\tilde{k}^3 + \tilde{k} \right)$$

	gravity $\tilde{k} \ll 1$	capillary $\tilde{k} \gg 1$
shallow water $\tilde{k} \ll 1/\tilde{H}$	$\pm \tilde{k}$	$\pm \tilde{k}^2 \sqrt{\tilde{H}}$
Deep water $\tilde{k} \gg 1/\tilde{H}$	$\pm \sqrt{\tilde{k}}$	$\pm \tilde{k} \sqrt{\tilde{k}}$

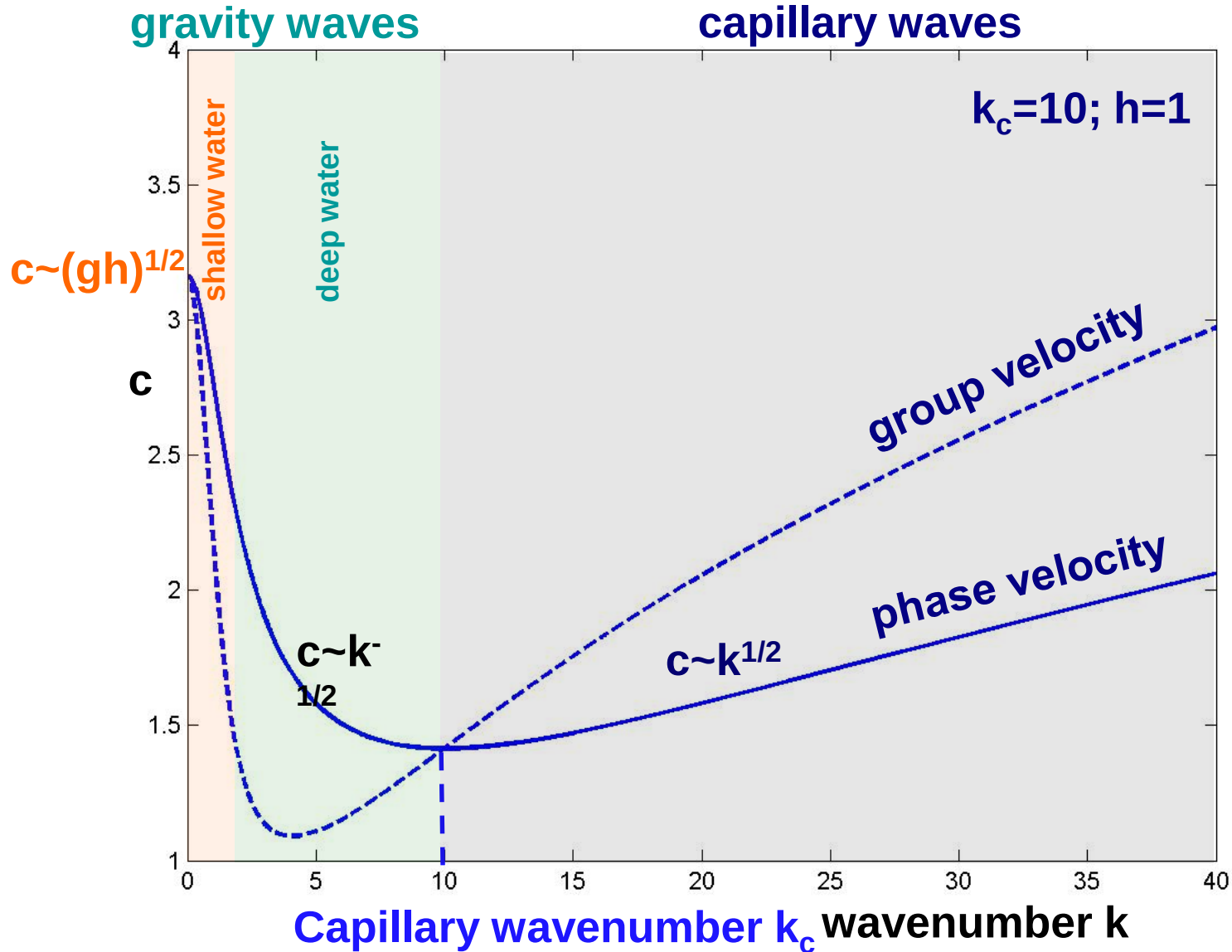
Difference between group velocity v and phase velocity c



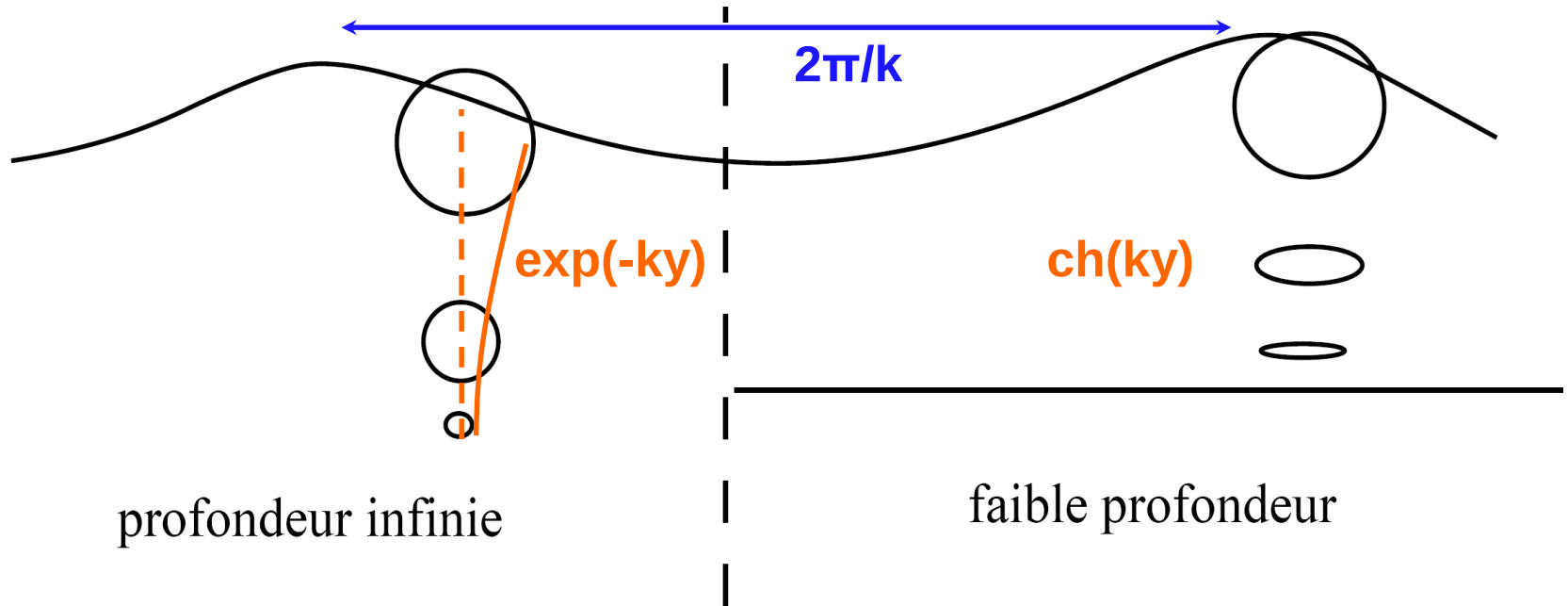
Dispersion relation

	gravity $\tilde{k} \ll 1$	capillary $\tilde{k} \gg 1$
shallow water $\tilde{k} \ll 1/\tilde{H}$	$\omega_{\text{shallow/gravity}} \sim \pm k \sqrt{gH}$ $c_{\text{shallow/gravity}} \sim \pm \sqrt{gH}$ $v_{\text{shallow/gravity}} \sim \pm \sqrt{gH}$	$\omega_{\text{shallow/capillary}} \sim \pm k^2 \sqrt{\gamma H / \rho}$ $c_{\text{shallow/capillary}} \sim \pm k \sqrt{\gamma H / \rho}$ $v_{\text{shallow/capillary}} \sim \pm 2k \sqrt{\gamma H / \rho}$
Deep water $\tilde{k} \gg 1/\tilde{H}$	$\omega_{\text{deep/gravity}} \sim \pm \sqrt{gk}$ $c_{\text{deep/gravity}} \sim \pm \sqrt{\frac{g}{k}}$ $v_{\text{deep/gravity}} \sim \pm \frac{1}{2} \sqrt{\frac{g}{k}}$	$\omega_{\text{deep/capillary}} \sim \pm k^{3/2} \sqrt{\gamma / \rho}$ $c_{\text{deep/capillary}} \sim \pm k^{1/2} \sqrt{\gamma / \rho}$ $v_{\text{deep/capillary}} \sim \pm 3/2 k^{1/2} \sqrt{\gamma / \rho}$

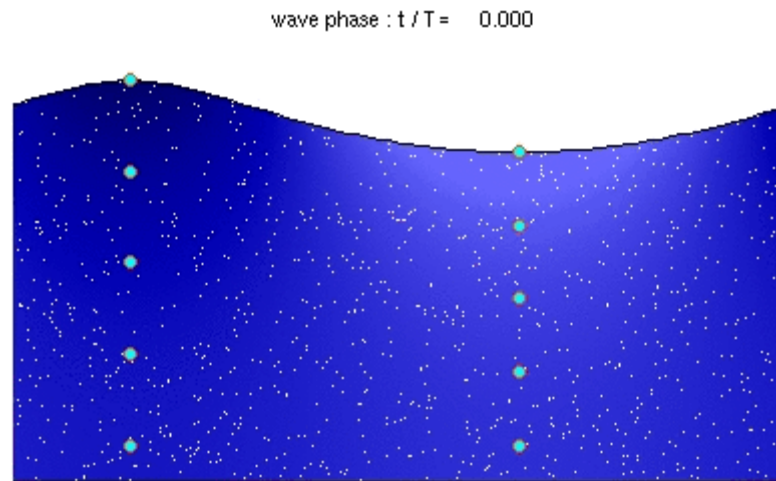
Dispersion relation



Trajectories below the waves



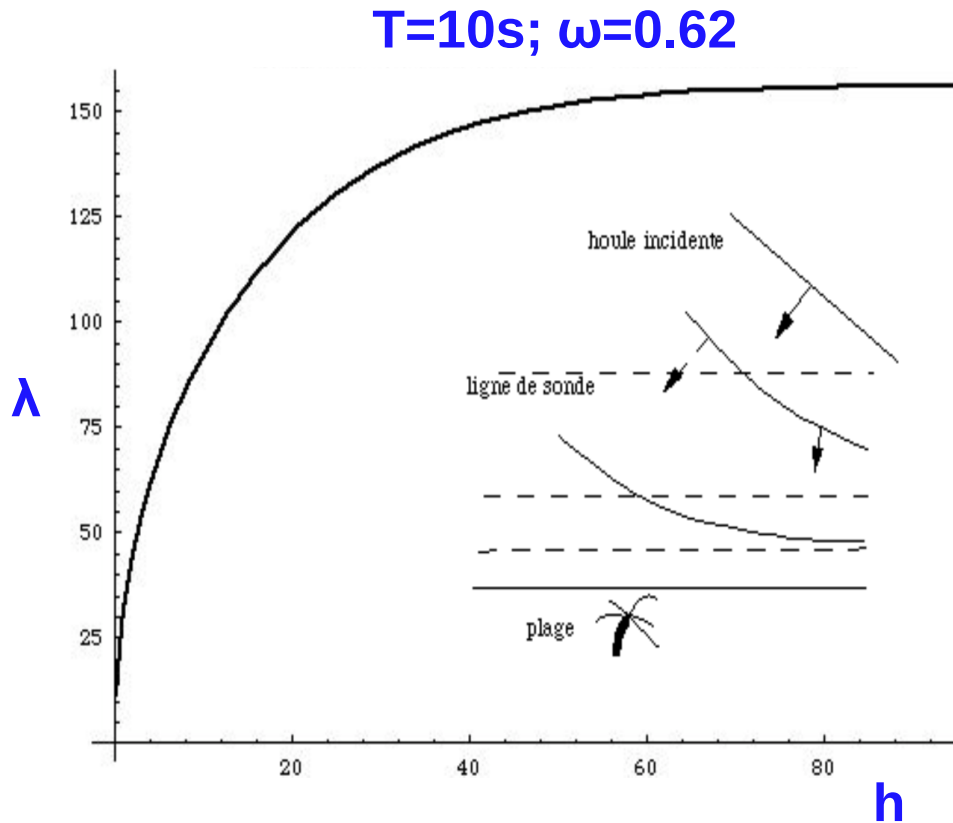
Stokes drift!



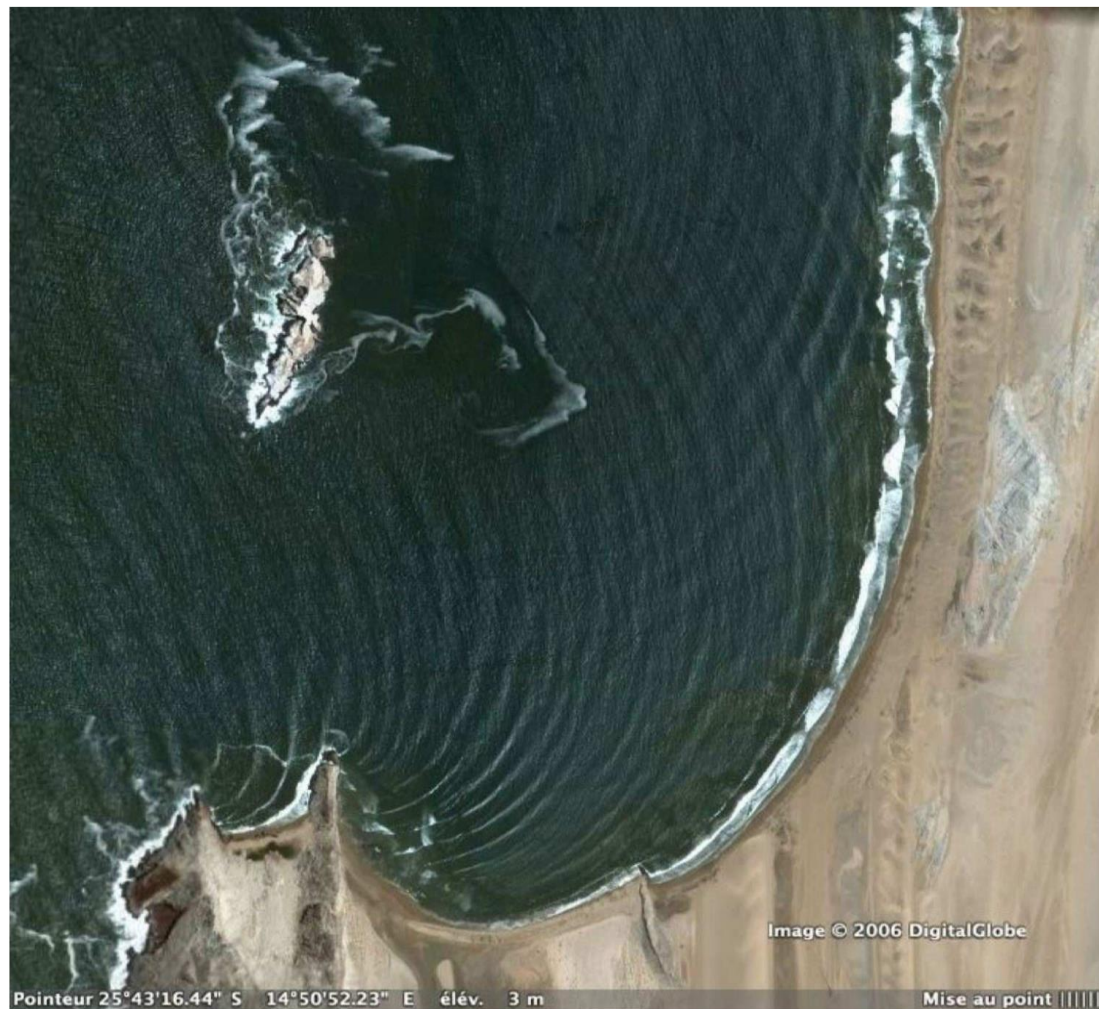
Why are the waves parallel to the shore?

$$c \sim (gh)^{1/2}$$

$$\lambda \sim T(gh)^{1/2}$$

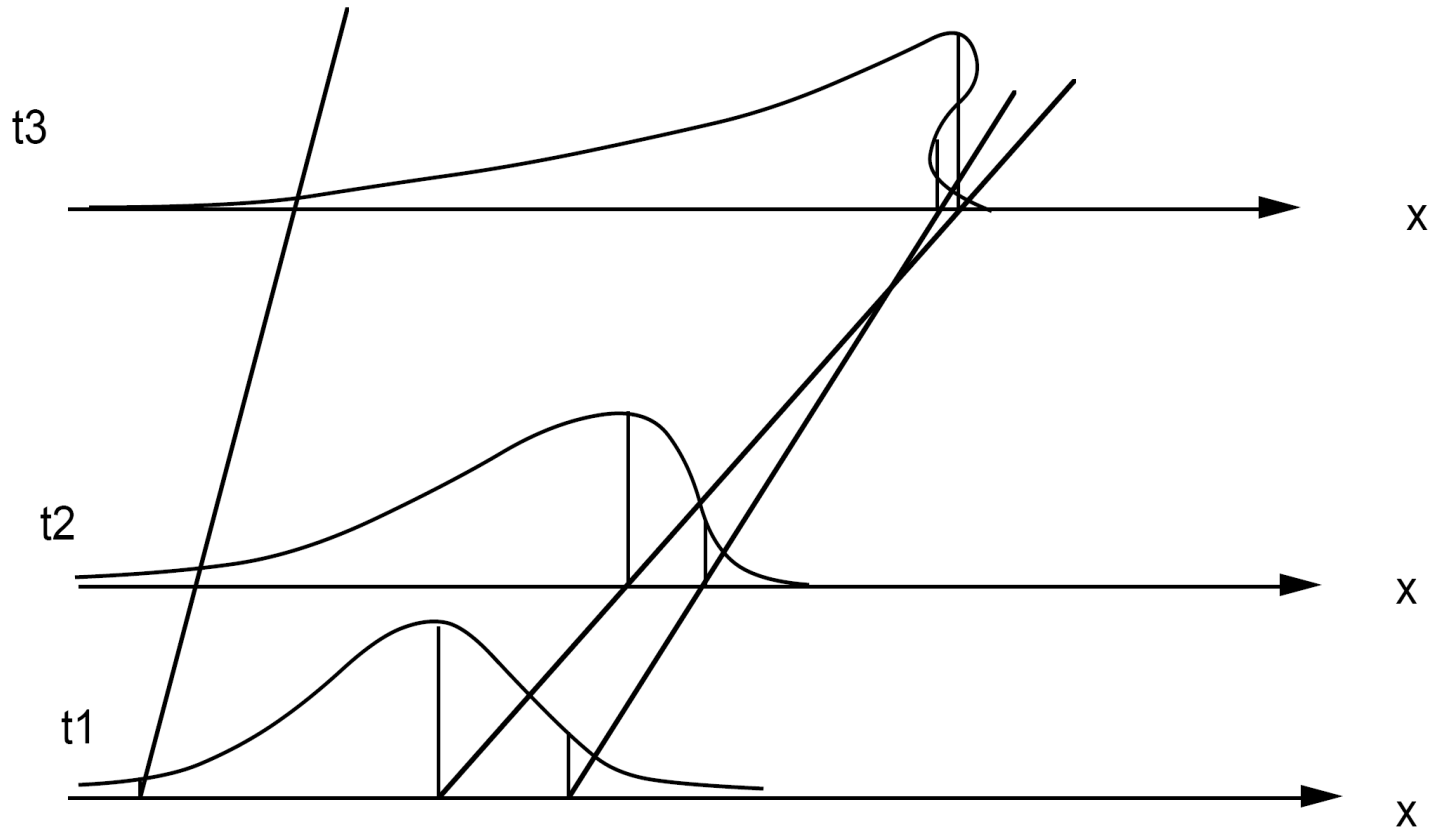


Refraction and diffraction of waves



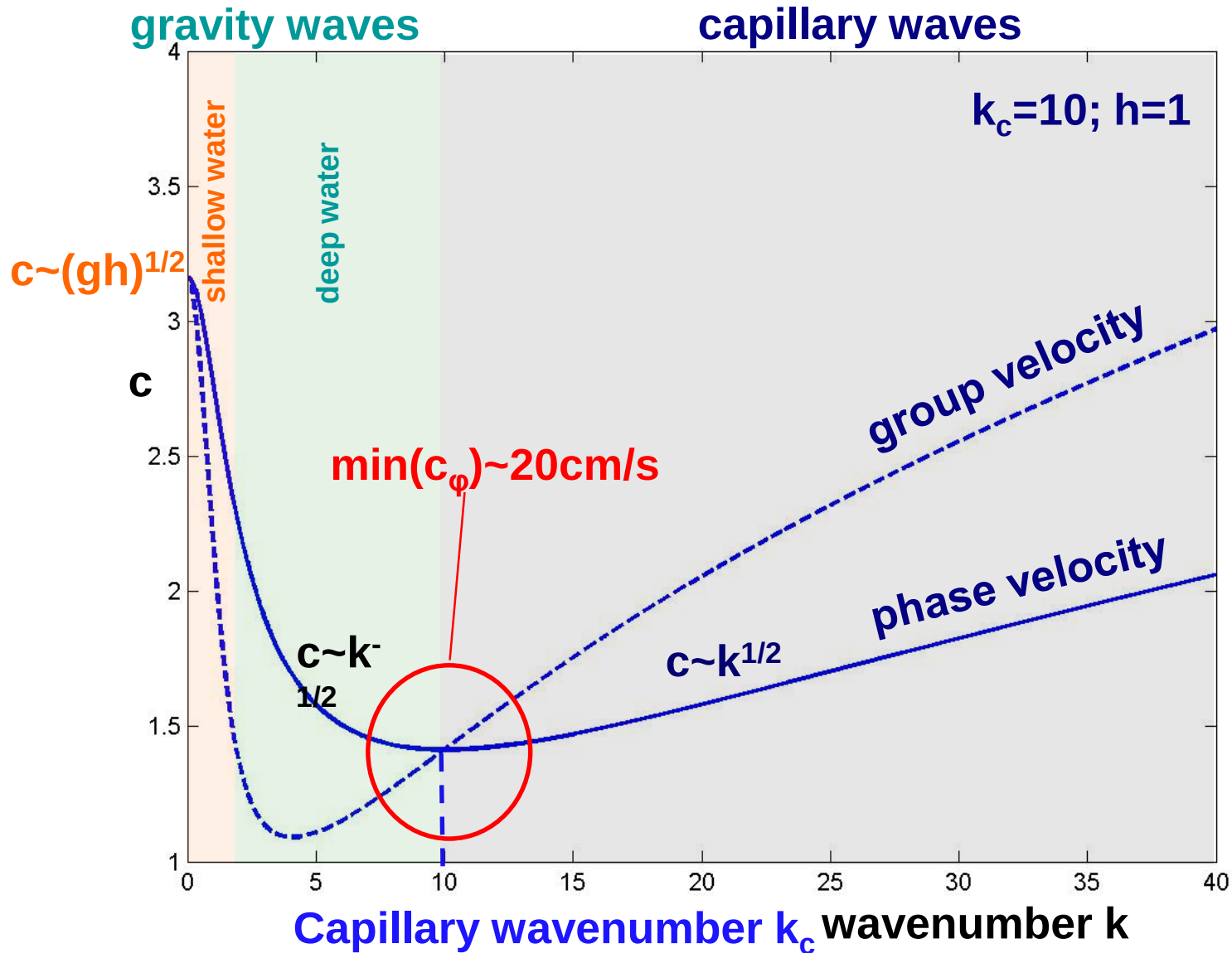
Satellite view Namibian coast

Nonlinear waves, wavebreaking



The celerity increases with the depth

Dispersion relation



Conditions for wave pattern formation?



$$V_{\text{duck}} \leq c_{\text{min}} \quad ?$$