
AEROELASTICITY AND FLUID-STRUCTURE INTERACTION

Chapter 2:

Coupled formulation of fluid and solid motions

Dimensional Analysis for Flow Characterization

- ***In fluid mechanics, it is very common to express physical laws with the help of non-dimensional quantities only***

$$f(x_1, x_2, \dots, x_N) = 0$$

***where $x_1, \dots, x_N$ are dimensional quantities: $[x_i] = L^{\alpha_i} M^{\beta_i} T^{\gamma_i}$
(L : length, M : mass and T : time)***

The function f may be expressed in non-dimensional form F , such as:

$$F(X_1, X_2, \dots, X_P) = 0$$

where $X_1, \dots, X_P$ are dimensionless quantities: $[X] = L^0 M^0 T^0$

- ***Advantages:***
 - ***Universality of physical laws (e.g. scale independent)***
 - ***Useful to classify the large variety of complex flows***

Dimensional Analysis for Flow Characterization

- ***The Buckingham π Theorem:***

Any physically meaningful equation involving N physical variables

$$f(x_1, x_2, \dots, x_N) = 0 \qquad [x_i] = L^{\alpha_i} M^{\beta_i} T^{\gamma_i}$$

may be written with a set of P dimensionless parameters, constructed from the original variables:

$$F(X_1, X_2, \dots, X_P) = 0 \qquad [X_i] = L^0 M^0 T^0$$
$$[X_i] = \frac{\text{Force}}{\text{Force}} = \frac{\text{Time}}{\text{Time}} = \dots$$

with :

$$P = N - R \quad \text{and} \quad R = \text{rank} \begin{bmatrix} \alpha_1 & \dots & \alpha_N \\ \beta_1 & \dots & \beta_N \\ \gamma_1 & \dots & \gamma_N \end{bmatrix}$$

Dimensional Analysis for Flow Characterization

- ***Rank of a matrix:***
In linear algebra, the rank of a matrix A is the dimension of the vector space generated (or spanned) by its columns (or rows). This corresponds to the maximal number of linearly independent columns (or rows) of A .
- ***Examples:***

$$A = \begin{bmatrix} 1 & 0 & 1 \\ -2 & -3 & 1 \\ 3 & 3 & 0 \end{bmatrix} \quad \text{rank}(A) = 2$$

$$A = \begin{bmatrix} 1 & 1 & 0 & 2 \\ -1 & -1 & 0 & -2 \end{bmatrix} \quad \text{rank}(A) = \text{rank}(^T A) = 1$$

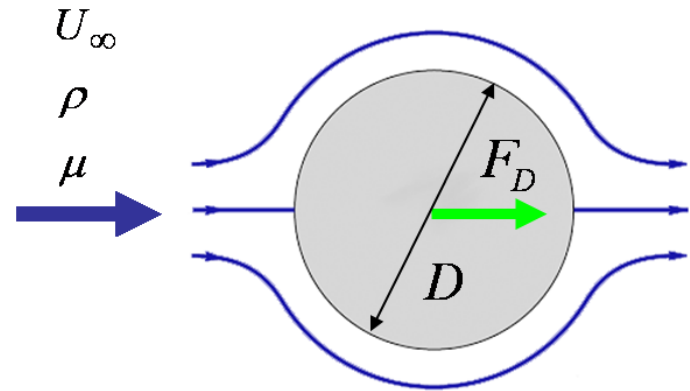
Fluid dynamics framework

Dimensional Analysis for Flow Characterization

- Example: Drag on a sphere*

$$f(F_D, U_\infty, \rho, \mu, D) = 0$$

5 dimensional variables



$$R = \text{rank} \begin{pmatrix} L \\ M \\ T \end{pmatrix} \begin{bmatrix} 1 & 1 & -3 & -1 & 1 \\ 1 & 0 & 1 & 1 & 0 \\ -2 & -1 & 0 & -1 & 0 \end{bmatrix} = 3$$

$\rightarrow P = N - R = 5 - 3 = 2$ *Only 2 dimensionless variables are required*

Fluid dynamics framework

Dimensional Analysis for Flow Characterization

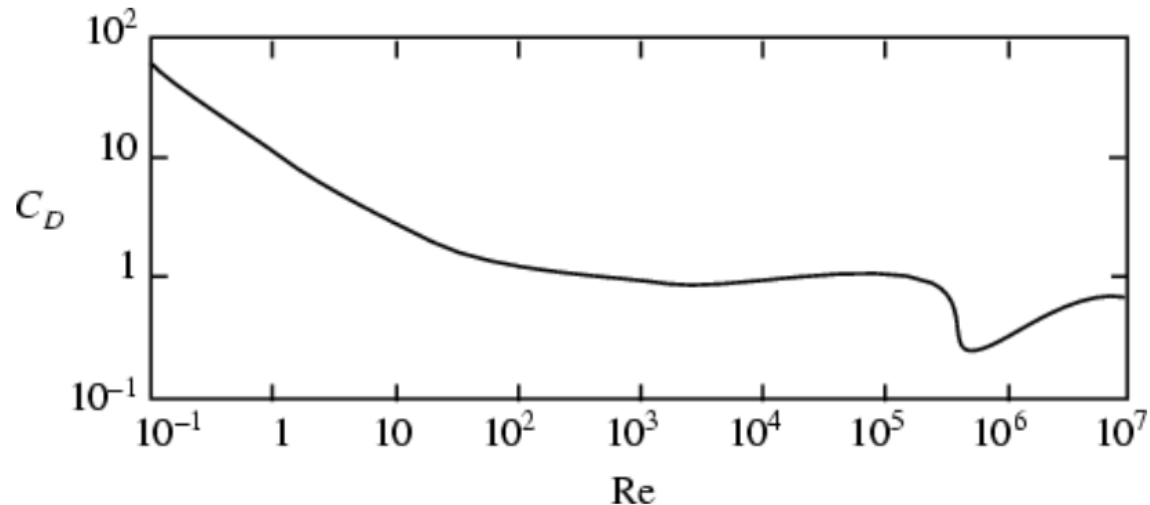
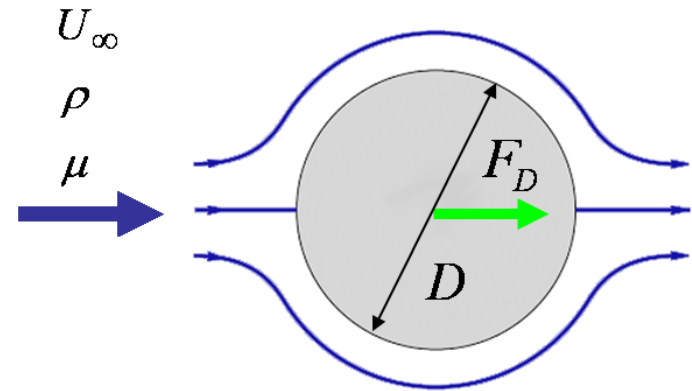
- **Example: Drag on a sphere**
 - **dimensionless equation:**

$$F\left(\frac{F_D}{\rho U_\infty^2 D^2}, \frac{\rho U_\infty D}{\mu}\right) = 0$$

$$F(C_D, Re) = 0$$

C_D : Drag Coefficient

Re : Reynolds Number



Dimensional Analysis for Flow Characterization

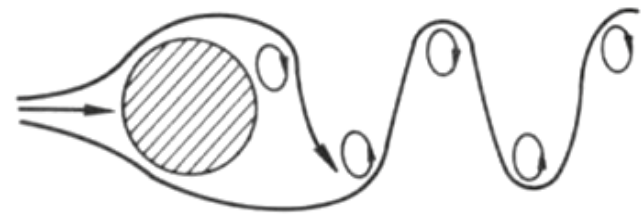
- Example:**

Vortex shedding from a cylinder (Karman vortices)

- Shedding Frequency f_s ?***
- Governing equation:***

$$f(f_s, U_\infty, \rho, \mu, D) = 0$$

5 dimensional variables



$$R = \text{rank} \begin{pmatrix} L \\ M \\ T \end{pmatrix} \begin{bmatrix} 0 & 1 & -3 & -1 & 1 \\ 0 & 0 & 1 & 1 & 0 \\ -1 & -1 & 0 & -1 & 0 \end{bmatrix} = 3$$

→ $P = N - R = 5 - 3 = 2$ Only 2 dimensionless variables are required

Dimensional Analysis for Flow Characterization

- **Example:**
Vortex shedding from a cylinder (Karman vortices)
 - *Shedding Frequency f_s ?*
 - *Dimensionless equation:*

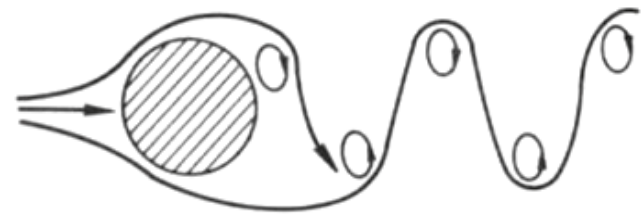
$$F\left(\frac{f_s D}{U_\infty}, \frac{\rho U_\infty D}{\mu}\right) = 0$$



St : Strouhal Number



Re : Reynolds Number

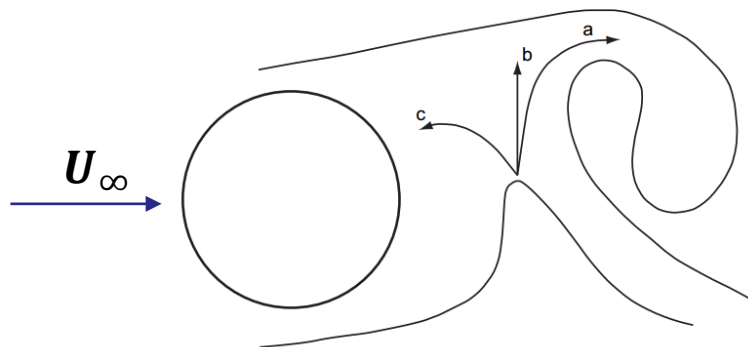


Fluid dynamics framework

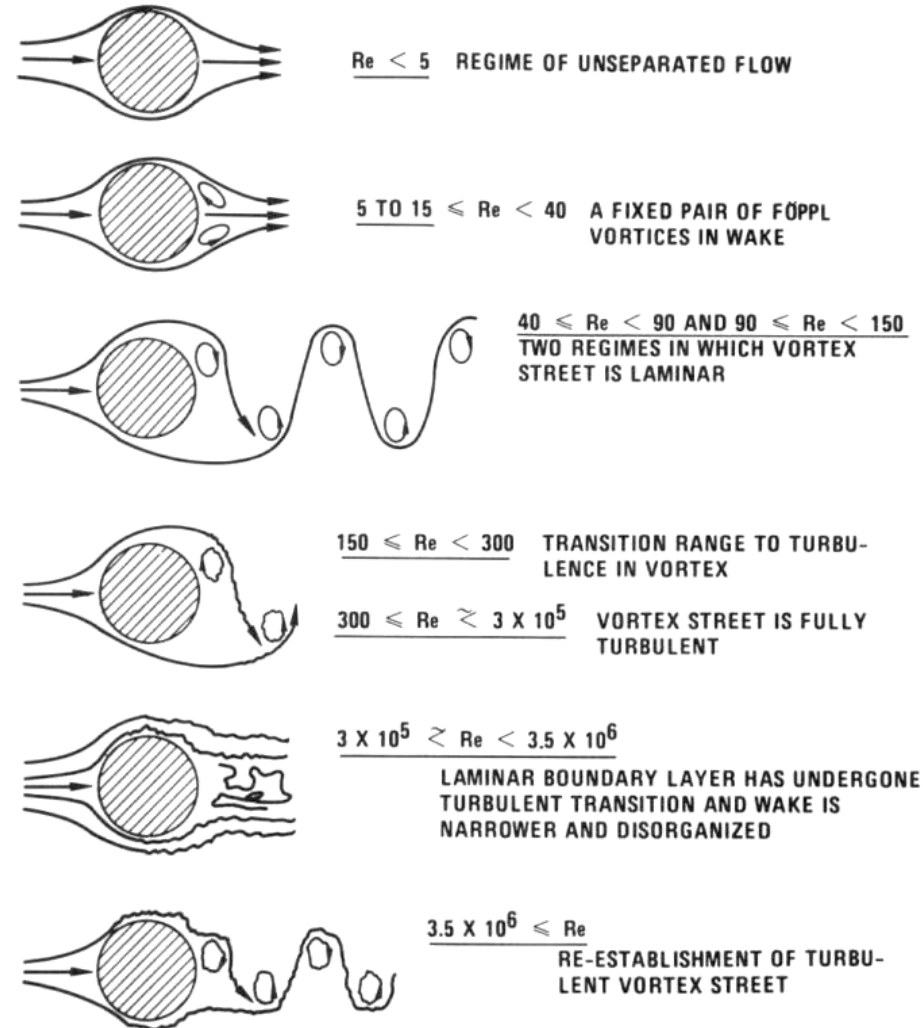
Dimensional Analysis for Flow Characterization

- **Example:**
Vortex shedding from a cylinder
- **Experimental Observations:**

$$St = \frac{f_s D}{U_\infty} \quad Re = \frac{\rho U_\infty D}{\mu}$$



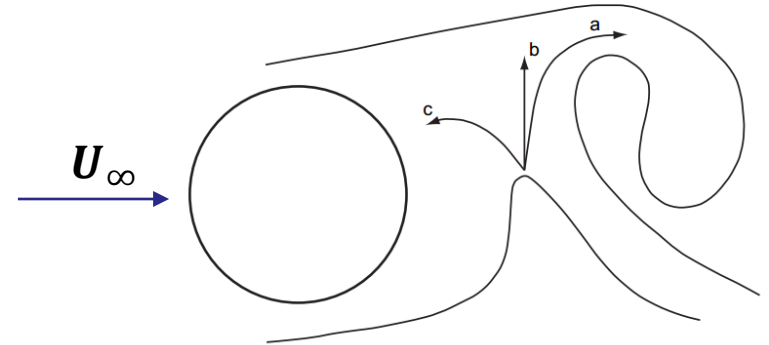
Vortex-formation model, Gerrard (1966)



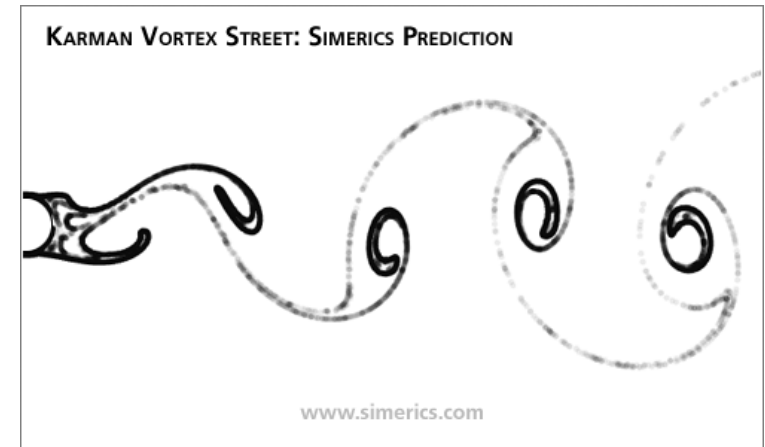
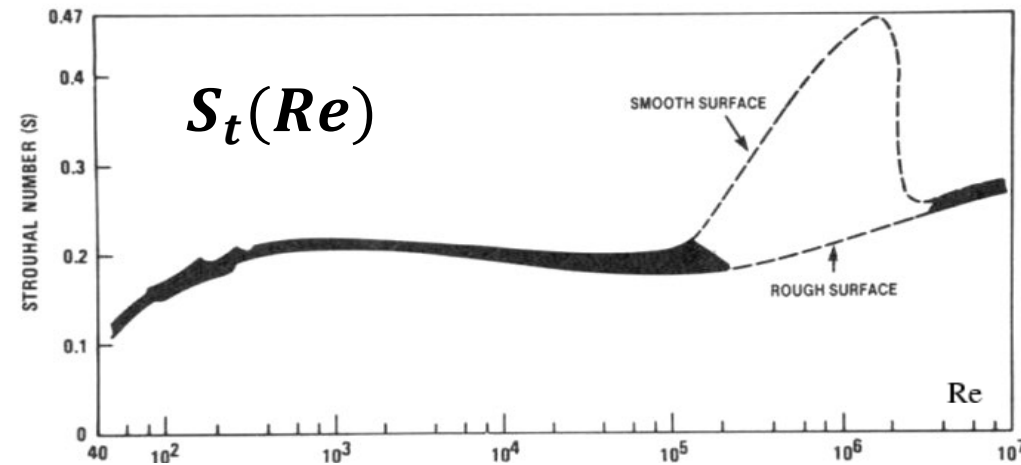
Fluid dynamics framework

Dimensional Analysis for Flow Characterization

- *Example:*
Vortex shedding from a cylinder
- *Experimental Observations:*



Vortex-formation model, Gerrard (1966)

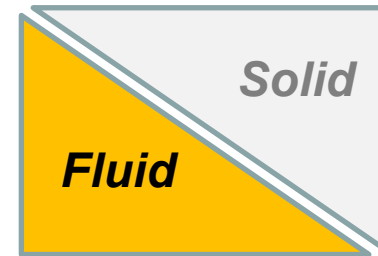


Fluid-Solid Interaction: General Formulation

Uncoupled formulation of fluid-solid interaction:

- *We consider a flow interacting with a moving/deforming solid:*
 - *The fluid and the solid are treated separately*
 - *Relevant variables for the fluid motion:*

U Velocity field
x Coordinates
t Time
 μ Viscosity
 ρ Density
g Gravity
 U_0 Reference Velocity
L Reference Length

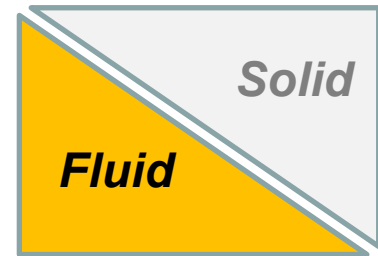


Fluid-Solid Interaction: General Formulation

Uncoupled formulation of fluid-solid interaction:

- *We consider a flow interacting with a moving/deforming solid:*
 - *The fluid and the solid are treated separately*
 - *Dimensional form of the equation of fluid motion :*

$$f(x, t, U, \mu, L, g, \rho, U_0) = 0$$



- *Dimensionless form of the equation of motion:*

$$R = \text{rank} \begin{pmatrix} L \\ M \\ T \end{pmatrix} \begin{bmatrix} 1 & 0 & 1 & -1 & 1 & 1 & -3 & 1 \\ 0 & 0 & 0 & 1 & 0 & 0 & 1 & 0 \\ 0 & 1 & -1 & -1 & 0 & -2 & 0 & -1 \end{bmatrix} = 3$$

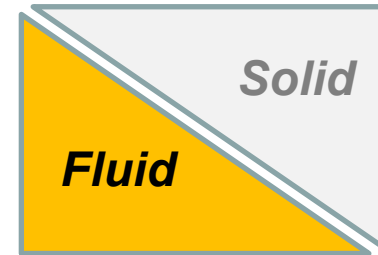
$\rightarrow$ *Problem dimension = 8-3=5*

Fluid-Solid Interaction: General Formulation

Uncoupled formulation of fluid-solid interaction:

- ***We consider a flow interacting with a moving/deforming solid:***
 - ***The fluid and the solid are treated separately***
 - ***Dimensionless form of the equation of fluid motion:***

$$F\left(\frac{x}{L}, \frac{U}{U_0}, \frac{t}{L/U_0}, \frac{\rho U_0 L}{\mu}, \frac{U_0}{\sqrt{gL}}\right) = 0$$



$\rho U_0 L / \mu$: Reynolds Number (Ratio of inertia to the viscous forces)

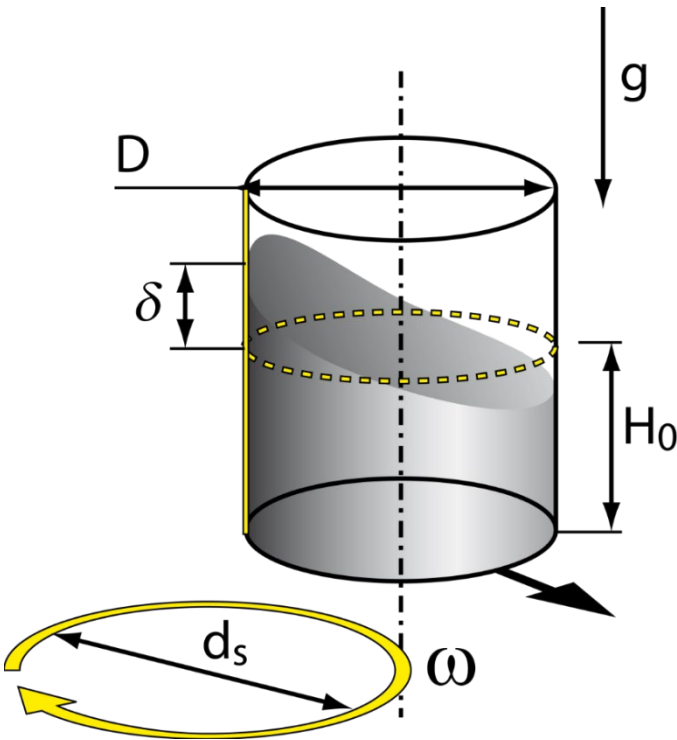
$\frac{U_0 t}{L} = \frac{t}{T_{Fluid}}$: Time t is normalized by the time required for a particle moving at the reference velocity U_0 to travel the reference distance L

$U_0 / \sqrt{gL}$: Froude Number (Ratio of inertia to the gravity forces)

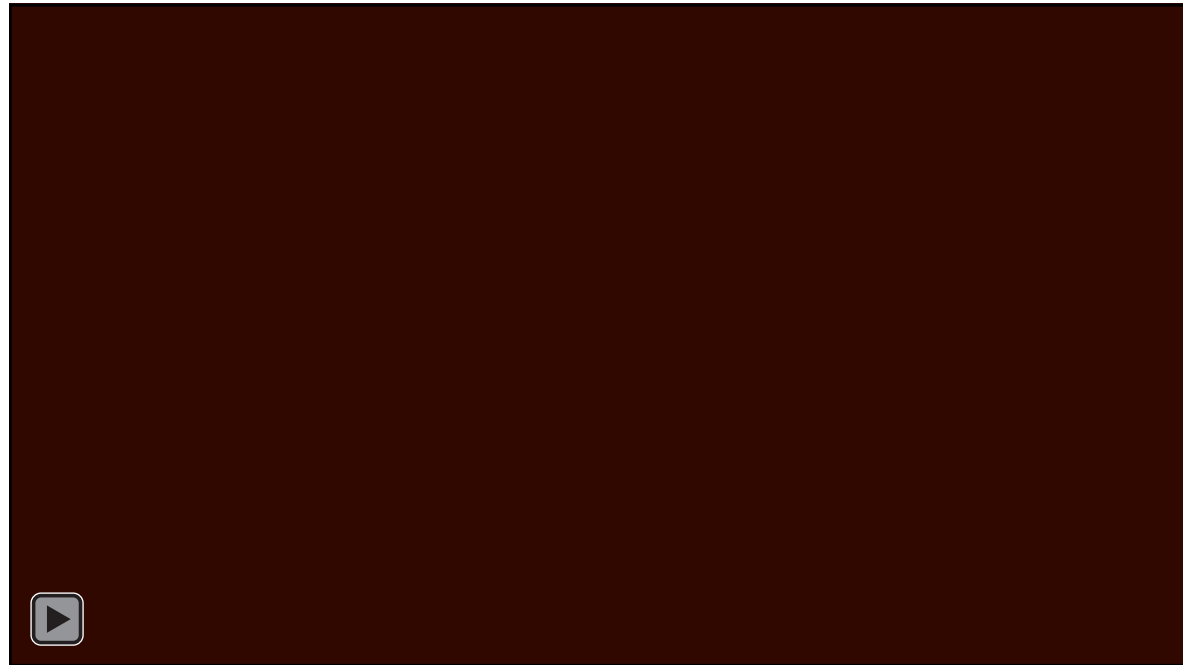
Fluid-Solid Interaction: General Formulation

Illustration of the role of Froude Number

- *Sloshing phenomena in an orbitally shaken reservoir:*
 - *The gentle motion enhances mixing and oxygenation (Used in cell cultivation)*
 - *The sloshing is mainly governed by the Froude number*



[Link to video on Youtube](#)



Fluid-Solid Interaction: General Formulation

Uncoupled formulation of fluid-solid interaction:

- ***We consider a flow interacting with a moving/deforming solid:***
 - ***The fluid and the solid are treated separately***
 - ***Relevant variables for the solid motion:***

ξ Displacement field

x Coordinates

t Time

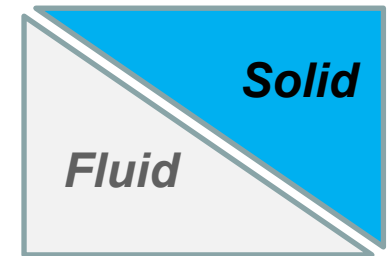
E Stiffness

L Reference Length

g Gravity

ρ_s Density

ξ_0 Reference
Displacement

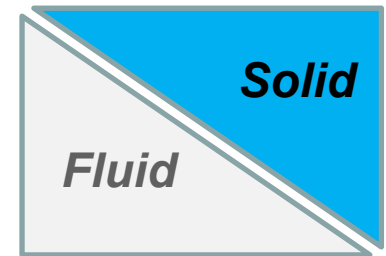


Fluid-Solid Interaction: General Formulation

Uncoupled formulation of fluid-solid interaction:

- *We consider a flow interacting with a moving/deforming solid:*
 - *The fluid and the solid are treated separately*
 - *Dimensional form of the equation of solid motion:*

$$f(x, t, \xi, E, L, g, \rho_s, \xi_0) = 0$$



- *Dimensionless form of the equation of solid motion:*

$$R = \text{rank} \begin{pmatrix} L \\ M \\ T \end{pmatrix} \begin{bmatrix} 1 & 0 & 1 & -1 & 1 & 1 & -3 & 1 \\ 0 & 0 & 0 & 1 & 0 & 0 & 1 & 0 \\ 0 & 1 & -1 & -1 & 0 & -2 & 0 & -1 \end{bmatrix} = 3$$

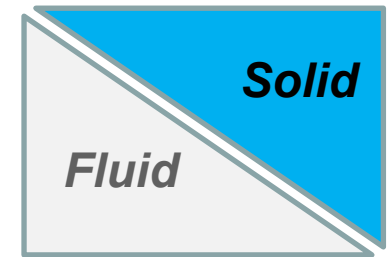
$\rightarrow$ *Problem dimension = 8-3=5*

Fluid-Solid Interaction: General Formulation

Uncoupled formulation of fluid-solid interaction:

- *We consider a flow interacting with a moving/deforming solid:*
 - *The fluid and the solid are treated separately*
 - *Dimensionless form of the equation of solid motion:*

$$F\left(\frac{x}{L}, \frac{\xi}{L}, \frac{t\sqrt{E/\rho_s}}{L}, \frac{\xi_0}{L}, \frac{\rho_s g L}{E}\right) = 0$$



$\frac{\xi_0}{L}$: Displacement number (Displacement scaled by the reference length)

$\frac{\rho_s g L}{E}$: Elastogravity number (ratio of gravity force over elastic force)

$\frac{t\sqrt{E/\rho_s}}{L} = \frac{t}{T_{solid}} ; T_{solid} = \frac{L}{\sqrt{E/\rho_s}} = \frac{L}{c}$: Time for elastic waves to travel the reference length L

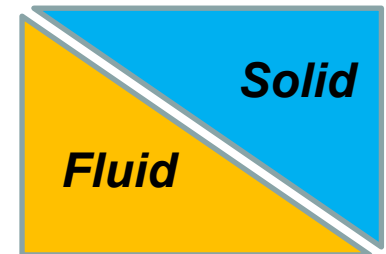
Fluid-Solid Interaction: General Formulation

Coupled formulation of fluid-solid interaction:

- *We consider a flow interacting with a moving/deforming solid:*
 - *Fluid motion depends on both fluid and solid variables:*

$$g(U, x, t, \mu, \rho, U_0, L, g, E, \rho_s, \xi_0) = 0$$

11 variables related to solid and fluid domains



$$\text{Rank} \begin{matrix} & U & x & t & \mu & \rho & U_0 & L & g & E & \rho_s & \xi_0 \\ \begin{bmatrix} 1 & 1 & 0 & -1 & -3 & 1 & 1 & 1 & -1 & -3 & 1 \\ 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 & 1 & 0 \\ -1 & 0 & 1 & -1 & 0 & -1 & 0 & -2 & -2 & 0 & 0 \end{bmatrix} & = & 3 \end{matrix}$$

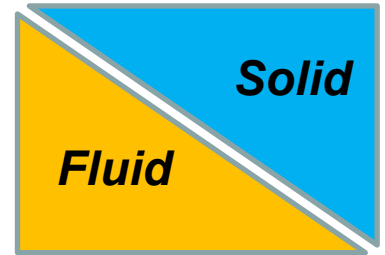
→ Problem dimension = 11-3=8

Fluid-Solid Interaction: General Formulation

Coupled formulation of fluid-solid interaction:

- ***We consider a flow interacting with a moving/deforming solid:***

- ***Dimensionless form:***



$$G\left(\frac{U}{U_0}, \frac{x}{L}, \frac{t}{L/U_0}, \frac{\rho U_0 L}{\mu}, \frac{U_0}{\sqrt{gL}}, \frac{\xi_0}{L}, \frac{\rho_s g L}{E}, A\right) = 0$$

- ***Dimensionless parameter A ? (must combine fluid & solid)***

Fluid-Solid Interaction: General Formulation

Coupled formulation of fluid-solid interaction:

- *Possible choices for the dimensionless number A:*

$\frac{\rho}{\rho_s}$: *Mass number (mass of the fluid vs mass of the solid)*

$\frac{U_0}{\sqrt{E/\rho_s}}$: *Reduced velocity (Ratio of fluid velocity & elastic wave celerity)*

$\frac{\rho U_0^2}{E}$: *Cauchy number (combines fluid forces and solid stiffness)*
High Cauchy number $\rightarrow$ The solid is more deformable under the action of the fluid forces

Fluid-Solid Interaction: General Formulation

Equations of motion of fluid and solid:

- *On the Fluid side: Navier-Stokes equations*

Mass conservation or Continuity (incompressible): $\vec{\nabla} \cdot \vec{U} = 0$

Momentum conservation:

$$\rho \frac{d\vec{U}}{dt} = -\rho g \vec{e}_z - \vec{\nabla} p + \mu \Delta \vec{U}$$

The diagram illustrates the physical components of the momentum equation. Arrows point from the terms in the equation to their respective physical interpretations: from $\rho \frac{d\vec{U}}{dt}$ to *Inertia*, from $-\rho g \vec{e}_z$ to *Gravity force*, from $-\vec{\nabla} p$ to *Pressure gradient*, and from $\mu \Delta \vec{U}$ to *Viscous force*.

Fluid-Solid Interaction: General Formulation

Equations of motion of fluid and solid:

- *On the Solid side:*

Single mode approximation:

$$\xi(x, t) = q(t)\phi(x)$$

Modal displacement

Modal shape
(Always known)

Example:  $\xrightarrow{\vec{e}_x}$ $\phi(x) = \vec{e}_x$

Oscillator equation:

$$m \frac{d^2 q}{dt^2} + kq = f$$

Modal mass Modal stiffness Modal load

Fluid-Solid Interaction: General Formulation

Equations of motion of fluid and solid:

- *At the interface between fluid and solid (Continuity equations):*
 - *Kinematic condition*
(no mixing and no sliding between solid and fluid):

$$U = \frac{d\xi(x, t)}{dt} = \frac{dq(t)}{dt} \phi(x)$$

- *Dynamic conditions: Continuity of forces at the interface*

$$\int \{ [-pI + \mu(\nabla U + \nabla^t U)] \cdot n \} \cdot \phi dS = f$$

 Modal load

Fluid-Solid Interaction: General Formulation

Equations of motion of fluid and solid:

Navier-Stokes

$$\vec{\nabla} \vec{U} = 0$$

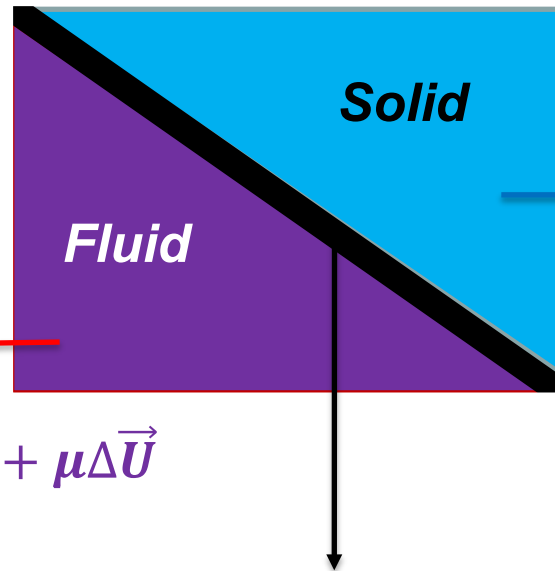
$$\rho \frac{d\vec{U}}{dt} = -\rho g \vec{e}_z - \vec{\nabla} p + \mu \Delta \vec{U}$$

At the interface:

$$U = \frac{dq(t)}{dt} \phi(x)$$

$$\int \{ [-pI + \mu(\nabla U + \nabla^t U)] \cdot n \} \cdot \phi dS = f$$

+ boundary conditions in the fluid and solid domains



$$m \frac{d^2 q}{dt^2} + kq = f$$

Oscillator equation

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *Dimensionless variables in the fluid:*

$$x_f = \frac{x}{L} \quad U_f = \frac{U}{U_0} \quad p_f = \frac{p}{\rho U_0^2} \quad t_f = \frac{t}{T_{fluid}}$$

- *Dimensionless variables in the solid:*

$$x_s = \frac{x}{L} \quad q_s = \frac{q}{\xi_0} \quad f_s = \frac{f}{k\xi_0} \quad t_s = \frac{t}{T_{solid}}$$

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *Dimensionless time ?*

- *In the solid:* $T_{solid} = \sqrt{m/k} \rightarrow t_s \frac{t}{\sqrt{m/k}}$
or $T_{solid} = \frac{L}{c} \rightarrow t_s = \frac{t}{L/c}$

- *In the fluid:* $T_{fluid} = \frac{L}{U_0} \rightarrow t_f = \frac{t}{L/U_0}$

- *The time references (clocks) in the solid and in the fluid are not necessarily the same. We may have:*

$$T_{fluid} \gg T_{solid}, \quad T_{fluid} \ll T_{solid} \quad \text{or} \quad T_{fluid} \sim T_{solid}$$

- *Arbitrary choice:* $t_s = \frac{t}{T_{solid}}$

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *On the Fluid side: Navier-Stokes equations*

- *Continuity:* $\vec{\nabla} \vec{U} = 0 \Rightarrow \vec{\nabla} \vec{U}_f = 0$

- *Momentum conservation:* $\rho \frac{d\vec{U}}{dt} = -\rho g \vec{e}_z - \vec{\nabla} p + \mu \Delta \vec{U}$

$$\Rightarrow \frac{c}{U_0} \frac{d\vec{U}_f}{dt_s} = -\frac{gL}{U_0^2} \vec{e}_z - \vec{\nabla} p_f + \frac{\mu}{\rho U_0 L} \Delta \vec{U}_f$$

$$\frac{1}{U_R} \frac{d\vec{U}_f}{dt_s} = -\frac{1}{Fr^2} \vec{e}_z - \vec{\nabla} p_f + \frac{1}{Re} \Delta \vec{U}_f$$

$$U_R = \frac{T_{solid}}{T_{fluid}} \quad : \text{Reduced velocity. This term appears because the reference time is taken in the solid}$$

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *On the solid side:*

$$m \frac{d^2 q}{dt^2} + kq = f$$

$$q_s = \frac{q}{\xi_0}$$

$$f_s = \frac{f}{k\xi_0}$$

Dimensionless time ?

$$t_s = \frac{t}{\sqrt{\frac{m}{k}}}$$

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *On the solid side:*

$$m \frac{d^2 q}{dt^2} + kq = f \quad \Rightarrow \quad m \left[\sqrt{\frac{k}{m}} \right]^2 \xi_0 \frac{d^2 q_s}{dt_s^2} + k \xi_0 q_s = k \xi_0 f_s$$

$$\Rightarrow \quad \frac{d^2 q_s}{dt_s^2} + q_s = f_s$$

$\Rightarrow$ *Dimensionless oscillator's frequency = 1*
Obvious, since the oscillation period is taken as the reference time

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *At the fluid-solid interface:*
 - *Kinematic condition:*

$$U = \frac{dq(t)}{dt} \phi(x) \quad \Rightarrow \quad \frac{U_0 T_{solid}}{L} U_f = \frac{\xi_0}{L} \frac{dq_s}{dt_s} \phi(x)$$

$$\Rightarrow \quad U_R U_f = D \frac{dq_s}{dt_s} \phi(x)$$

↓

Displacement Nb

Fluid-Solid Interaction: General Formulation

Dimensionless equations of fluid and solid motions

- *On the fluid-solid interface*
 - *Dynamic condition:*

$$\int_{Interface} \{[-pI + \mu(\nabla U + \nabla^t U)] \cdot n\} \cdot \phi dS = f$$



$$\int_{Interface} \left\{ \frac{\rho U_0^2 L}{k} \left[-p_f I + \frac{\mu}{\rho U_0 L} (\nabla U_f + \nabla^t U_f) \right] \cdot n \right\} \cdot \phi dS = \frac{\xi_0}{L} f_s$$



$$\int_{Interface} \left\{ Cy \left[-p_f I + \frac{1}{Re} (\nabla U_f + \nabla^t U_f) \right] \cdot n \right\} \cdot \phi dS = D f_s$$

Fluid-Solid Interaction: General Formulation

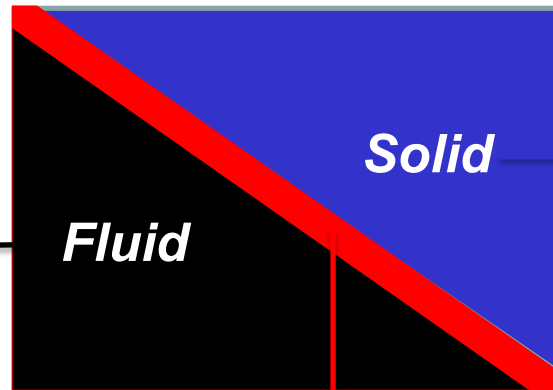
Summary: Dimensionless equations

Navier-Stokes

$$\vec{\nabla} \vec{U}_f = 0$$

$$\frac{1}{U_R} \frac{d\vec{U}_f}{dt_s} = -\frac{1}{Fr^2} \vec{e}_z - \vec{\nabla} p_f + \frac{1}{Re} \Delta \vec{U}_f$$

+ fluid boundary conditions



Oscillator equation

$$\frac{d^2 q_s}{dt_s^2} + q_s = f_s$$

+ solid boundary conditions

At the interface:

$$U_R U_f = D \frac{dq_s}{dt_s} \phi(x)$$

$$\int_{\text{Interface}} \left\{ Cy \left[-p_f I + \frac{1}{Re} (\nabla U_f + \nabla^t U_f) \right] \cdot n \right\} \cdot \phi dS = D f_s$$