

CLAUSIUS-CLAPEYRON:

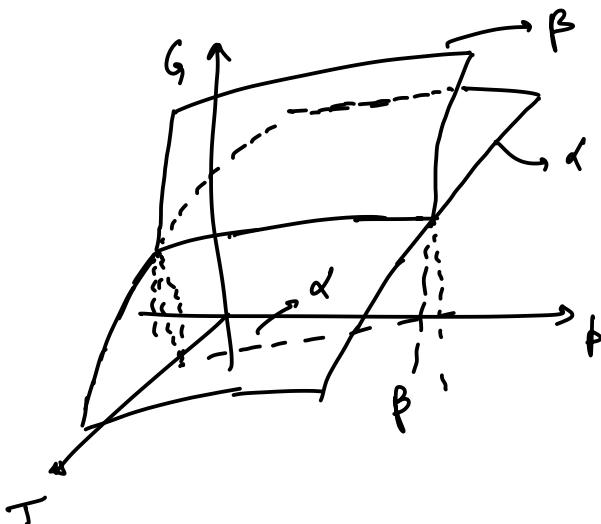
- Can we say anything about the slope of the coexistence lines in a $T-p$ diagram?

Coexistence line defined by:

$$G^\alpha = G^\beta$$

$$\text{and } dG^\alpha = dG^\beta$$

Let the transition temperature be denoted as T^* , transition pressure as p^*



$$dG^\alpha = dG^\beta$$

$$\Rightarrow V^\alpha dp^* - S^\alpha dT^* = V^\beta dp^* - S^\beta dT^*$$

$$(V^\beta - V^\alpha) dp^* = (S^\beta - S^\alpha) dT^*$$

$\underbrace{\Delta V}_{\Delta V^{\alpha \rightarrow \beta}}$ $\underbrace{\Delta S}_{\Delta S^{\alpha \rightarrow \beta}}$

$$\boxed{\frac{dp^*}{dT^*} = \frac{\Delta S^{\alpha \rightarrow \beta}}{\Delta V^{\alpha \rightarrow \beta}} = \frac{\Delta H^{\alpha \rightarrow \beta}}{T \Delta V^{\alpha \rightarrow \beta}}}$$

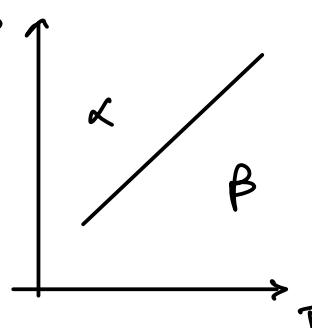
gives the slope of the coexistence line

* Going from a low-temperature phase (α) to a high-temperature phase (β)

$$H^\beta > H^\alpha \Rightarrow \Delta H^{\alpha \rightarrow \beta} > 0$$

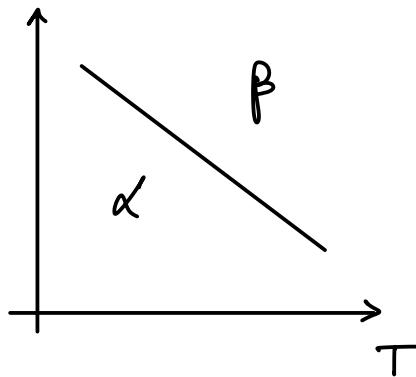
• if $\Delta V^{\alpha \rightarrow \beta} > 0$ (expands upon transformation)

$$\frac{dp^*}{dT^*} > 0$$



• if $\Delta V^{\alpha \rightarrow \beta} < 0$

$$\frac{dp^*}{dT^*} < 0$$



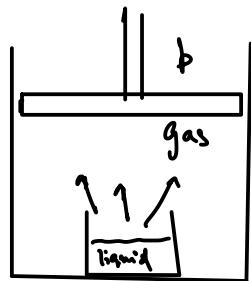
NOTICE: increase pressure \rightarrow favor the phase with the smaller volume

Le Chatelier principle

↳ impose a force \rightarrow system favors the state that somewhat undoes that force

* Liquid - gas coexistence line

$$\frac{dp^*}{dT^*} = \frac{\Delta H^{l \rightarrow g}}{T^* \Delta V^{l \rightarrow g}}$$



$V^g \gg V^l$ for fixed # of moles

$$\Delta V^{l \rightarrow g} \approx V^g \approx \frac{nRT}{P} > 0$$

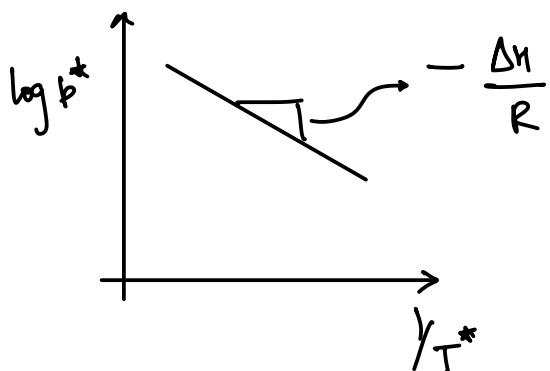
$$nR \frac{dp^*}{P^*} = \frac{\Delta H^{l \rightarrow g}}{T^{*2}} dT^*$$

Assume $\Delta H^{l \rightarrow g}$ is independent of T & P

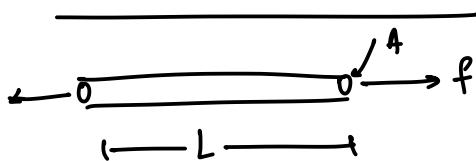
$$nR \log\left(\frac{P^*}{P_0}\right) = -\Delta H^{l \rightarrow g} \left(\frac{1}{T^*} - \frac{1}{T_0}\right)$$

$$\boxed{P^* = C \exp\left(-\frac{\Delta H^{l \rightarrow g}}{RT^*}\right)}$$

where $\bar{\Delta H} = \frac{\Delta H}{n}$



* MORE FUN WITH PHASE DIAGRAMS:



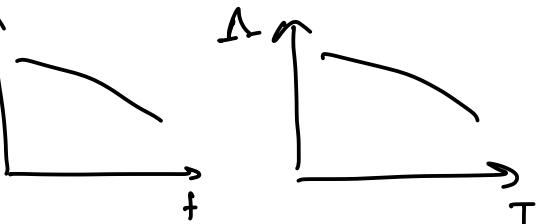
at constant T

$$dU = TdS + f dL$$

we control f & T

$$\underline{\Lambda} = U - TS - fL$$

$$\boxed{d\underline{\Lambda} = -SdT - Ldf} \\ \left(\frac{\partial \underline{\Lambda}}{\partial T} \right)_f = -S \quad \left(\frac{\partial \underline{\Lambda}}{\partial f} \right)_T = -L \quad \boxed{\text{EOS}}$$

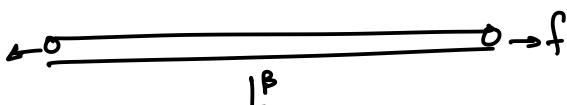
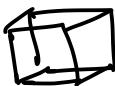


Response functions:

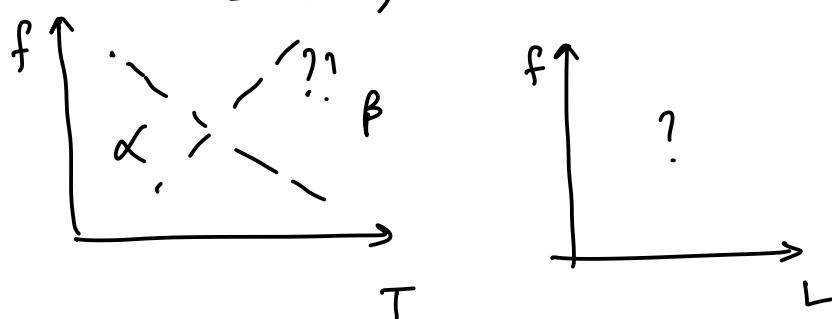
$$T \left(\frac{\partial S}{\partial T} \right)_f = C_f \quad \frac{A_0}{L_0} \left(\frac{\partial L}{\partial f} \right)_T = \frac{1}{E} \quad \text{where } \tau = E\varepsilon$$

$$\frac{1}{L} \left(\frac{\partial L}{\partial T} \right) = \beta_L$$

Martensitic phase transformations:



$L^\beta > L^\alpha$; α is the stable phase at low temperature



2-phase coexistence line is determined by:

$$\underline{\Lambda}^\alpha = \underline{\Lambda}^\beta$$

$$d\underline{\Lambda}^\alpha = d\underline{\Lambda}^\beta$$

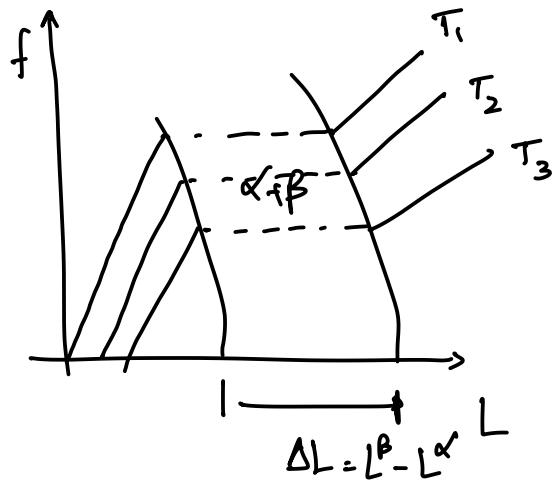
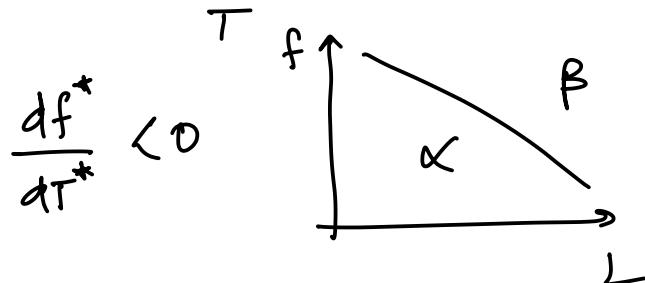
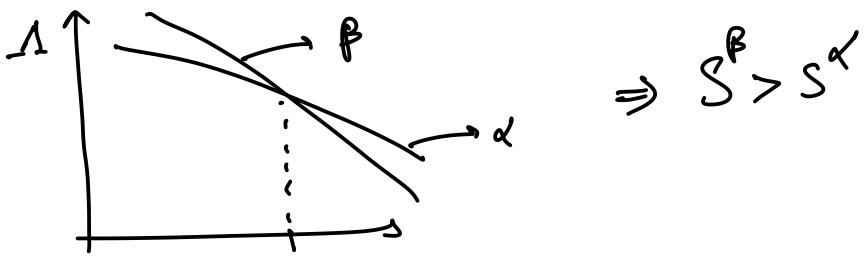
$$-S^{\alpha}dT^* - L^{\alpha}df^* = -S^{\beta}dT^* - L^{\beta}dT^*$$

$$\Rightarrow \boxed{\frac{df^*}{dT^*} = - \frac{(S^{\beta} - S^{\alpha})}{(L^{\beta} - L^{\alpha})}}$$

$$L^{\beta} > L^{\alpha} \rightarrow \text{given}$$

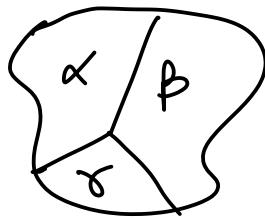
$$\text{what about } S^{\beta}, S^{\alpha} ??$$

$\Rightarrow \alpha$ is the stable phase at low temperatures.



* MULTI-PHASE SYSTEMS:

Objective: describe multi-phase systems with multiple chemical elements.



- ① Compute properties of each phase as a function of composition
- ② " " " total system as a function of composition.
- ③ How do I compute eq^m in multiphase systems?

- The system has c components (different species)
- $N_1, N_2, \dots, N_c \rightarrow$ # of mole of each component

FUNDAMENTAL EQUATION OF THERMO:

$$U(S, X_i, N_i):$$

$$dU = TdS + \sum Y_i dX_i + \sum_{i=1}^c \mu_i dN_i$$

$$\mu_i = \left(\frac{\partial U}{\partial N_i} \right)_{T, X_i, N_{j \neq i}} \quad \leftarrow \text{definition of the chemical potential}$$

* Review of some eqns. we derived before

$$- \text{EULER: } U = TS - pV + \sum_i \mu_i N_i$$

other potentials:

$$H(S, p, N_i) = \text{enthalpy} = U + pV = TS + \sum \mu_i N_i$$

$$F(T, V, N_i) = \text{Helmholtz free energy} = U - TS = -pV + \sum_i \mu_i N_i$$

$$G(T, p, N_i) = U - TS + pV = \sum_i \mu_i N_i$$

- GIBBS-DOMFEM:

$$SdT - Vdp + \sum_i N_i d\mu_i = 0$$

all intensive

$$G = U - TS + PV$$

$$dG = Vdp - SdT + \sum_{i=1}^c \mu_i dN_i$$

EOS (for the multicomponent free energy) $\rightarrow N_c + 2$ equations of state

new eos: $\left(\frac{\partial G}{\partial N_i}\right)_{T, p, N_j \neq i} = \mu_i \rightarrow \mu_i (T, p, \xi_{N_j}) \xrightarrow{\text{all mole numbers!}}$

Hessian:

$$\begin{array}{c|ccc|c} & T & p & \vdots & N_i \\ \hline T & -C_p/T & \alpha T & \vdots & \frac{\partial^2 G}{\partial N_i \partial T} \\ p & \alpha T & -V/T & \vdots & \frac{\partial^2 G}{\partial N_i \partial p} \\ \hline - & - & - & \vdots & - \\ N_i & & & \frac{\partial^2 G}{\partial N_i^2} & \end{array} \rightarrow \begin{aligned} \frac{\partial S}{\partial N_i} &= -\bar{S}_i \rightarrow \text{PARTIAL MOLEAR ENTHALPY of } i \\ \frac{\partial V}{\partial N_i} &= \bar{V}_i \rightarrow \text{PARTIAL MOLEAR VOLUME of } i \\ \left(\frac{\partial \mu}{\partial N_i}\right) &= \gamma_{ii} \end{aligned}$$

In general: A partial molal quantity:

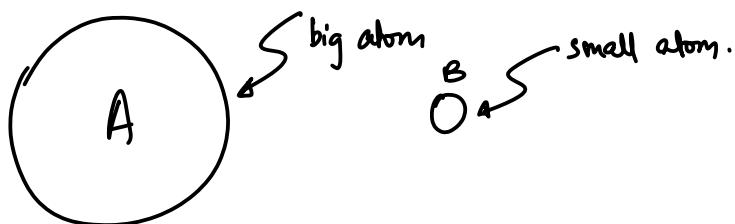
$$\left(\frac{\partial X}{\partial N_i}\right)_{N_j \neq i, T, p} = \bar{X}_i$$

New Maxwell relation:

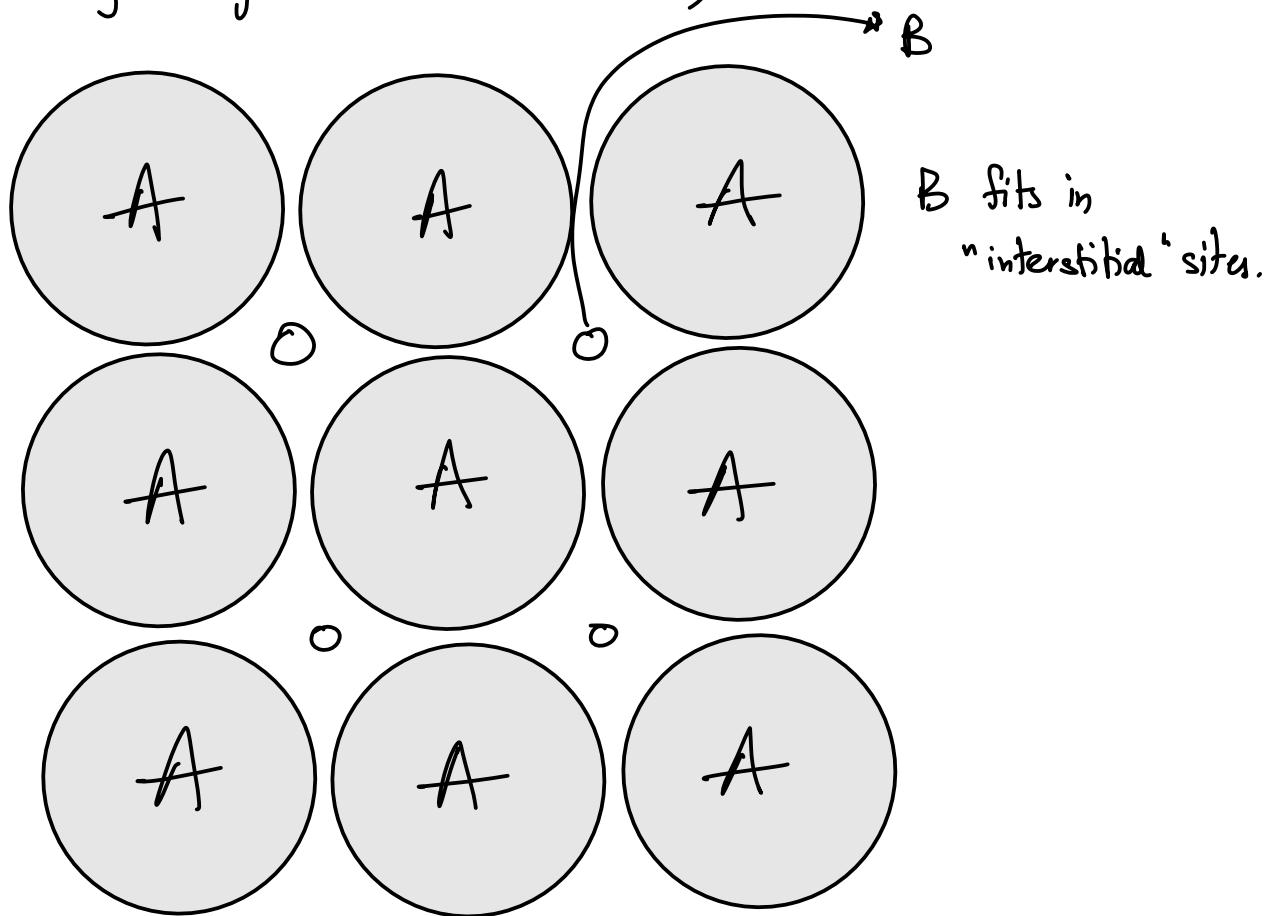
$$\bar{V}_i = \left(\frac{\partial V}{\partial N_i}\right)_{T, p, N_{j \neq i}} = \left(\frac{\partial \mu_i}{\partial p}\right)_{N_i, T}$$

$$\bar{S}_i = \left(\frac{\partial S}{\partial N_i}\right) = -\left(\frac{\partial \mu_i}{\partial T}\right)_{N_i, p}$$

(eg)

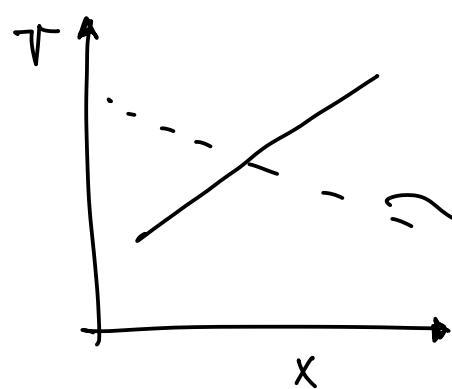


A is usually arranged (in the solid state) in a "pattern".

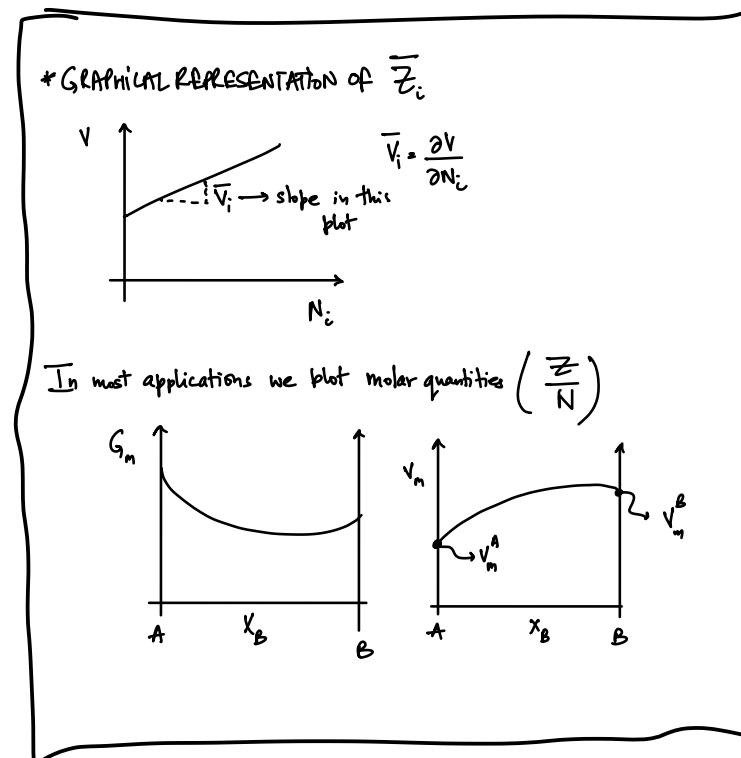


$$\bar{V}_A(x_A=1) = \left(\frac{V(x_A=1)}{N} \right) \quad \text{Volume per atom of pure A}$$

$$\bar{V}_B(x_A=1) = 0$$



(eg) $\text{H}_2\text{O} + \text{MgSO}_4$
② Li in Li_xNiO_2



* Definitions:

total number of atoms

$$N = N_1 + N_2 + \dots + N_c$$

* Molar quantity: So far we have avoided normalizing extensive variables

$$X_m \rightarrow (eq) \quad G_m = \frac{G}{N}$$

$$H_m = \frac{H}{N}$$

$$V_m = \frac{V}{N}$$

NOTE: Sometimes these quantities are also written as

$$\bar{G}, \bar{H}, \bar{V}$$

not to be confused with partial molar quantities

* What is the chemical potential @ const. T, p?

$$\left(\frac{\partial G}{\partial N_i} \right)_{T, p, N_j \neq i} = \mu_i \quad \rightarrow \text{change in Gibbs free energy when I add a small amount of element } i$$

N is NOT constant!

what we usually want is to compute the effects of changing compositions.

Say we have a binary: n_A, n_B, b, T

$$dG = Vdp - SdT + \mu_A dn_A + \mu_B dn_B$$

$$n_A + n_B = n_{\text{tot}} \Rightarrow n_B = n_{\text{tot}} - n_A$$

$$\Rightarrow dG = Vdp - SdT + \mu_A dn_A + \mu_B dn_{\text{tot}} - \mu_B dn_A$$

$$dG = Vdp - SdT + (\mu_A - \mu_B) dn_A + \mu_B dn_{\text{tot}}$$

$$\left(\frac{\partial G}{\partial n_A} \right)_{b, T, n_{\text{tot}}} = \mu_A - \mu_B$$

$$\Rightarrow \left(\frac{\partial \left(\frac{G}{n_{\text{tot}}} \right)}{\partial \left(\frac{n_A}{n_{\text{tot}}} \right)} \right)_{b, T, n_{\text{tot}}} = \left(\frac{\partial G_m}{\partial X_A} \right)_{b, T, n_{\text{tot}}} = \mu_A - \mu_B$$

$(\mu_A - \mu_B) \rightarrow$ Molar Gibbs energy change when we change the composition