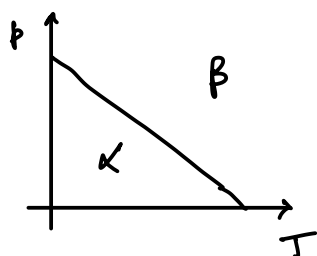


# CLAUSIUS - CLAPEYRON:



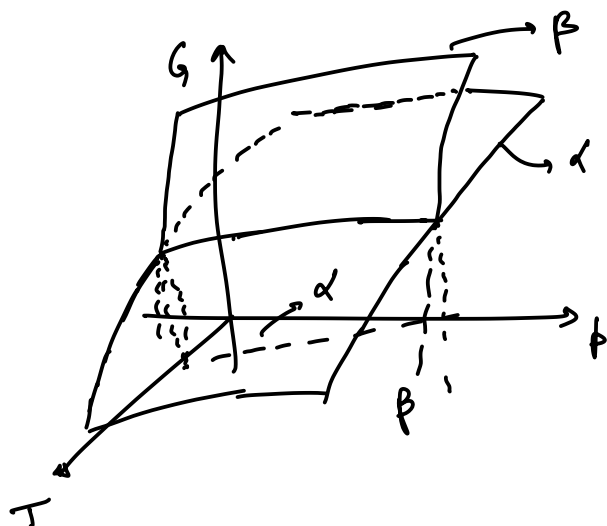
- Can we say anything about the slope of the coexistence lines in a T-p diagram?

Coexistence line defined by:

$$G^{\alpha} = G^{\beta}$$

$$\text{and } dG^{\alpha} = dG^{\beta}$$

Let the transition temperature be denoted as  $T^*$ , transition pressure as  $p^*$



$$dG^{\alpha} = dG^{\beta}$$

$$\Rightarrow V^{\alpha} dp^* - S^{\alpha} dT^* = V^{\beta} dp^* - S^{\beta} dT^*$$

$$\underbrace{(V^{\beta} - V^{\alpha})}_{\Delta V^{\alpha \rightarrow \beta}} dp^* = \underbrace{(S^{\beta} - S^{\alpha})}_{\Delta S^{\alpha \rightarrow \beta}} dT^*$$

$$\boxed{\frac{dp^*}{dT^*} = \frac{\Delta S^{\alpha \rightarrow \beta}}{\Delta V^{\alpha \rightarrow \beta}} = \frac{\Delta H^{\alpha \rightarrow \beta}}{T \Delta V^{\alpha \rightarrow \beta}}}$$

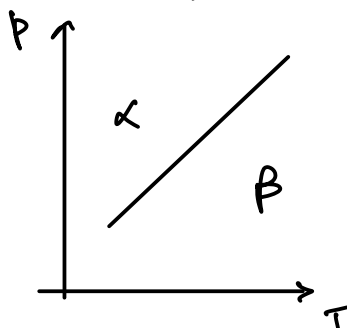
↑ gives the slope of the coexistence line

\* Going from a low-temperature phase ( $\alpha$ ) to a high-temperature phase ( $\beta$ )

$$H^{\beta} > H^{\alpha} \Rightarrow \Delta H^{\alpha \rightarrow \beta} > 0$$

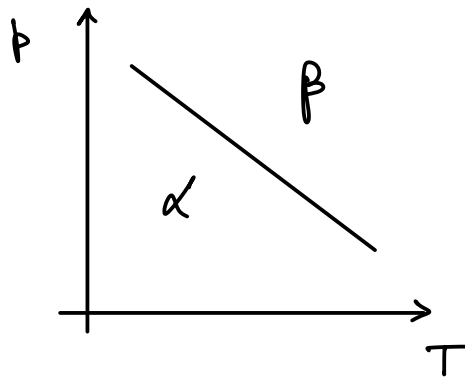
• if  $\Delta V^{\alpha \rightarrow \beta} > 0$  (expands upon transformation)

$$\frac{dp^*}{dT^*} > 0 \rightsquigarrow$$



• if  $\Delta V^{\alpha \rightarrow \beta} < 0$

$$\frac{dp^*}{dT^*} < 0$$

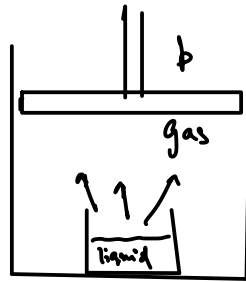


NOTICE: increase pressure  $\longrightarrow$  favor the phase with the smaller volume  
Le Chatelier principle

$\longrightarrow$  impose a force  $\longrightarrow$  system favors the state that somewhat undoes that force

★ Liquid - gas coexistence line

$$\frac{dp^*}{dT^*} = \frac{\Delta H^{l \rightarrow g}}{T^* \Delta V^{l \rightarrow g}}$$



$V^g \gg V^l$  for fixed # of moles

$$\Delta V^{l \rightarrow g} \approx V^g \approx \frac{nRT}{p} > 0$$

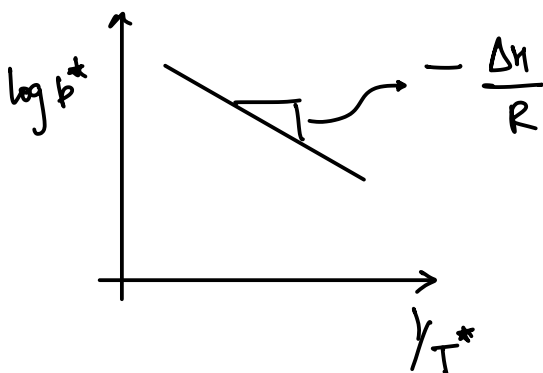
$$nR \frac{dp^*}{p^*} = \frac{\Delta H^{l \rightarrow g}}{T^{*2}} dT^*$$

Assume  $\Delta H^{l \rightarrow g}$  is independent of  $T$  &  $p$

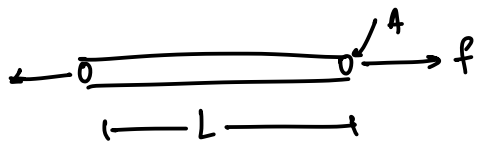
$$nR \log \left( \frac{p^*}{p_0^*} \right) = -\Delta H^{l \rightarrow g} \left( \frac{1}{T^*} - \frac{1}{T_0^*} \right)$$

$$p^* = C \exp \left( - \frac{\Delta \bar{H}^{l \rightarrow g}}{RT^*} \right)$$

where  $\Delta \bar{H} = \frac{\Delta H}{n}$



# \* MORE FUN WITH PHASE DIAGRAMS:



at constant  $T$

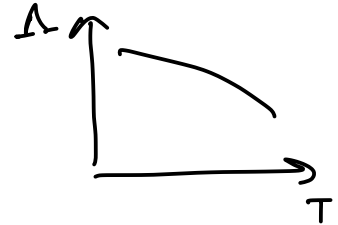
$$dU = Tds + fdL$$

we control  $f$  &  $T$

$$\Lambda = U - TS - fL$$

$$d\Lambda = -SdT - Ldf$$

$$\left( \frac{\partial \Lambda}{\partial T} \right)_f = -S \quad \left( \frac{\partial \Lambda}{\partial f} \right)_T = -L \quad \underline{\underline{\text{EOS}}}$$



Response functions:

$$T \left( \frac{\partial S}{\partial T} \right)_f = C_f$$

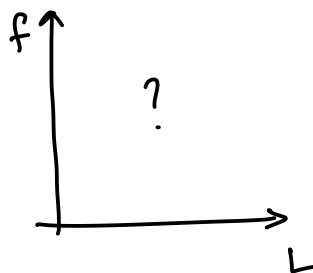
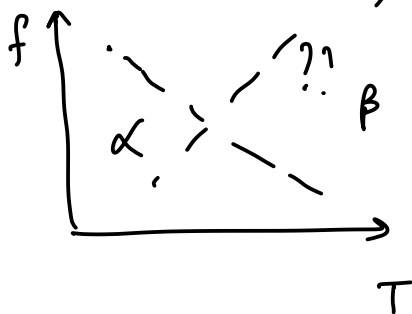
$$\frac{A_0}{L_0} \left( \frac{\partial L}{\partial f} \right)_T = \frac{1}{E} \quad \text{where } \tau = E\varepsilon$$

$$\frac{1}{L} \left( \frac{\partial L}{\partial T} \right) = \beta_L$$

Martensitic phase transformations:



$L^\beta > L^\alpha$ ;  $\alpha$  is the stable phase at low temperature



2-phase coexistence line is determined by:

$$\Lambda^\alpha = \Lambda^\beta$$

$$d\Lambda^\alpha = d\Lambda^\beta$$

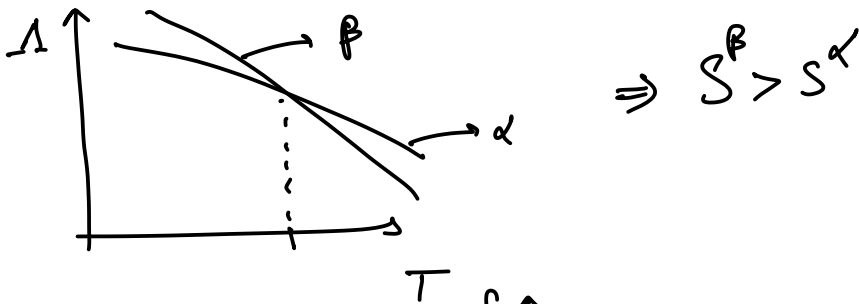
$$-S^{\alpha}dT^* - L^{\alpha}df^* = -S^{\beta}dT^* - L^{\beta}dT^*$$

$$\Rightarrow \left[ \frac{df^*}{dT^*} = - \frac{(S^{\beta} - S^{\alpha})}{(L^{\beta} - L^{\alpha})} \right]$$

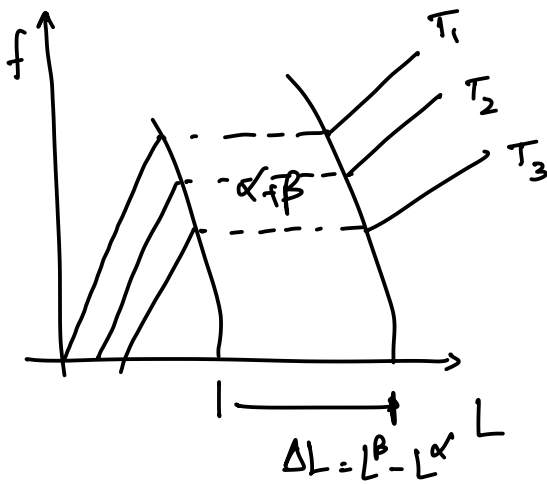
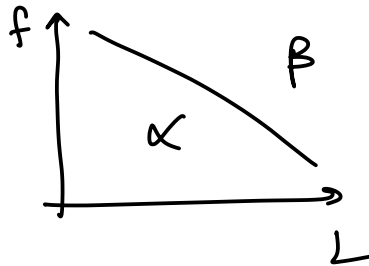
$L^{\beta} > L^{\alpha} \rightarrow$  given

what about  $S^{\beta}, S^{\alpha}$  ??

$\Rightarrow \alpha$  is the stable phase at low temperatures.

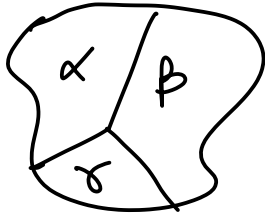


$$\frac{df^*}{dT^*} < 0$$



# \* MULTI-PHASE SYSTEMS:

Objective: describe multi-phase systems with multiple chemical elements.



- ① Compute properties of each phase as a function of composition
- ② " " " " " total system as a function of composition.
- ③ How do I compute  $eq^m$  in multi-phase systems?

- The system has  $c$  components (different species)
- $N_1, N_2, \dots, N_c \rightarrow$  # of mole of each component

## FUNDAMENTAL EQUATION OF THERMO:

$$U(S, X_i, N_i):$$

$$dU = TdS + \sum Y_i dx_i + \sum_{i=1}^c \mu_i dN_i$$

$$\mu_i = \left( \frac{\partial U}{\partial N_i} \right)_{T, X_i, N_{j \neq i}} \quad \leftarrow \text{definition of the chemical potential}$$

\* Review of some eqns. we derived before

- EULER:  $U = TS - pV + \sum_i \mu_i N_i$

other potentials:

$$H(S, p, N_i) = \text{enthalpy} = U + pV = TS + \sum_i \mu_i N_i$$

$$F(T, V, N_i) = \text{Helmholtz free energy} = U - TS = -pV + \sum_i \mu_i N_i$$

$$G(T, p, N_i) = U - TS + pV = \sum_i \mu_i N_i$$

- GIBBS-DUNEM:

$$SdT - Vdp + \sum_i N_i d\mu_i = 0$$

↑     ↑     ↗  
all intensive

$$G = U - TS + pV$$

$$dG = Vdp - SdT + \sum_{i=1}^c \mu_i dN_i$$

Eos (for the multicomponent free energy)  $\rightarrow N_c + 2$  equations of state

new eos:  $\left( \frac{\partial G}{\partial N_i} \right)_{T, p, N_{j \neq i}} = \mu_i \rightarrow \mu_i(T, p, \{N_j\})$  all mole numbers!

Hessian:

	T	p	:	$N_i$	
T	$-G/T$	$\alpha V$	:	$\frac{\partial^2 G}{\partial N_i \partial T}$	$\rightarrow = -\frac{\partial S}{\partial N_i} = -\bar{S}_i \rightarrow$ PARTIAL MOLAR ENTROPY of i
p	$\alpha V$	$-V\alpha$	:	$\frac{\partial^2 G}{\partial N_i \partial p}$	$\rightarrow \frac{\partial V}{\partial N_i} = \bar{V}_i \rightarrow$ PARTIAL MOLAR VOLUME of i
$N_i$	-	-	-	$\frac{\partial^2 G}{\partial N_i^2}$	$\rightarrow \left( \frac{\partial \mu}{\partial N_i} \right) = \chi_{ii}$

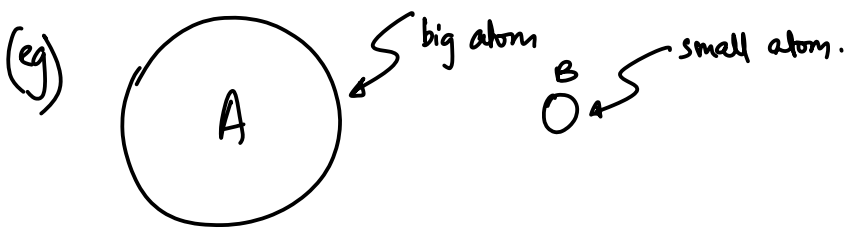
In general: A partial molar quantity:

$$\left( \frac{\partial X}{\partial N_i} \right)_{N_{j \neq i}, T, p} = \bar{X}_i$$

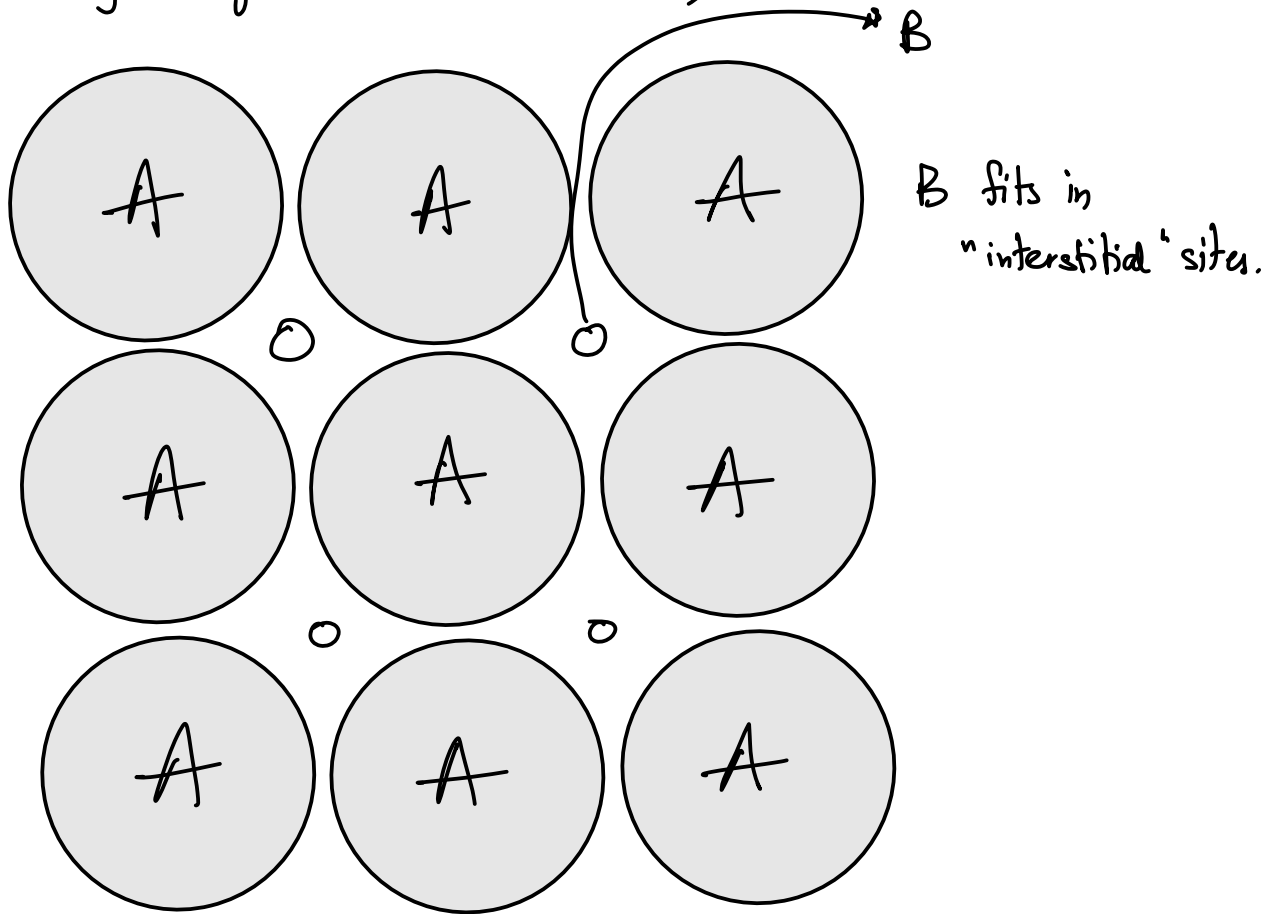
New Maxwell relations:

$$\bar{V}_i = \left( \frac{\partial V}{\partial N_i} \right)_{T, p, N_{j \neq i}} = \left( \frac{\partial \mu_i}{\partial p} \right)_{N_i, T}$$

$$\bar{S}_i = \left( \frac{\partial S}{\partial N_i} \right)_{T, p, N_{j \neq i}} = - \left( \frac{\partial \mu_i}{\partial T} \right)_{N_i, p}$$



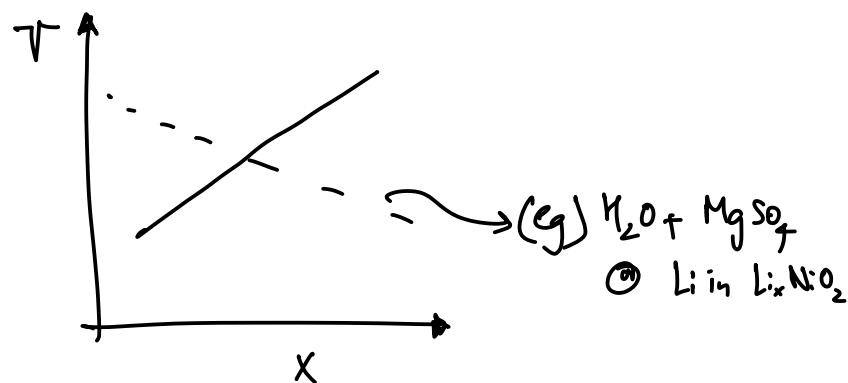
A is usually arranged (in the solid state) in a "pattern".



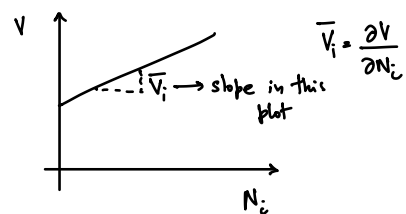
$$\bar{V}_A(x_A=1) = \left( \frac{V(x_A=1)}{N} \right)$$

Volume per atom of pure A

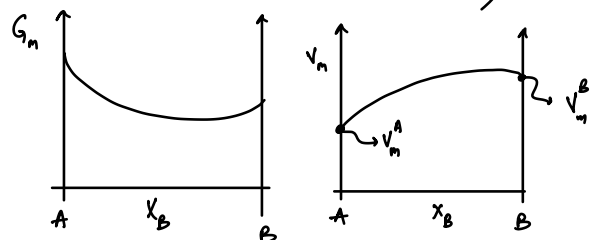
$$\bar{V}_B(x_A=1) = 0$$



\* GRAPHICAL REPRESENTATION OF  $\bar{Z}_i$



In most applications we plot molar quantities  $\left( \frac{Z}{N} \right)$



# \* DEFINITIONS:

total number of atoms

$$N = N_1 + N_2 + \dots + N_c$$

\* molar quantity: so far we have avoided normalizing extensive variables

$$X_m \rightsquigarrow (eq) \quad G_m = \frac{G}{N}$$

$$H_m = \frac{H}{N}$$

$$V_m = \frac{V}{N}$$

NOTE: Sometimes these quantities are also written as

$$\bar{G}, \bar{H}, \bar{V}$$

↳ not to be confused with partial molar quantities

\* What is the chemical potential @ const.  $T, p$ ?

$$\left( \frac{\partial G}{\partial N_i} \right)_{T, p, N_{j \neq i}} = \mu_i \quad \rightarrow \text{change in Gibbs free energy when I add a small amount of element } i$$

$N$  is NOT constant!

what we usually want is to compute the effects of changing compositions.

Say we have a binary:  $n_A, n_B, p, T$

$$dG = Vdp - SdT + \mu_A dn_A + \mu_B dn_B$$

$$n_A + n_B = n_{tot} \Rightarrow n_B = n_{tot} - n_A$$

$$\Rightarrow dG = Vdp - SdT + \mu_A dn_A + \mu_B dn_{tot} - \mu_B dn_A$$

$$dG = Vdp - SdT + (\mu_A - \mu_B) dn_A + \mu_B dn_{tot}$$

$$\left( \frac{\partial G}{\partial n_A} \right)_{p, T, n_{tot}} = \mu_A - \mu_B$$

↑  
Constant

$$\Rightarrow \left( \frac{\partial \left( \frac{G}{n_{tot}} \right)}{\partial \left( \frac{n_A}{n_{tot}} \right)} \right)_{p, T, n_{tot}} = \left( \frac{\partial G_m}{\partial x_A} \right)_{p, T, n_{tot}} = \mu_A - \mu_B$$

$(\mu_A - \mu_B) \rightarrow$  Molar Gibbs energy change when we change the composition