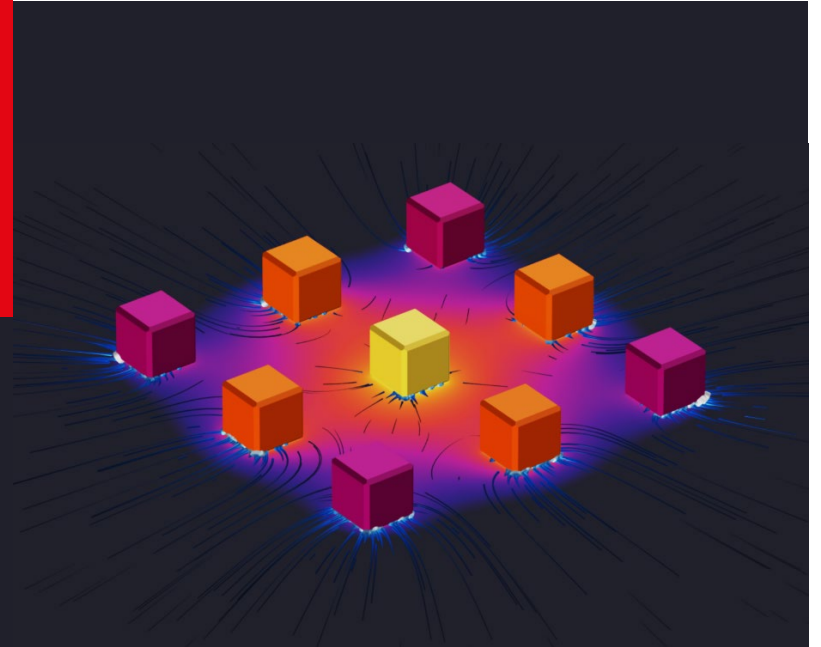


# Heat and Mass Transfer ME-341

*Instructor:* Giulia Tagliabue



Spring Semester

# Introduction to Heat Transfer

- ✓ ☒ Heat Transfer Mechanisms
- ✓ ☒ From Thermodynamics to Heat Transfer
- ✓ ☒ Heat Transfer Rate Equations

## Learning Objectives:

- ✓ ☒ From real-world to model:
  - identify the system and its boundaries
  - Identify heat transfer mechanisms involved
- ✓ ☒ Solve basic heat transfer problems

# From Thermodynamics to Heat Transfer

Thermodynamics



Heat Transfer

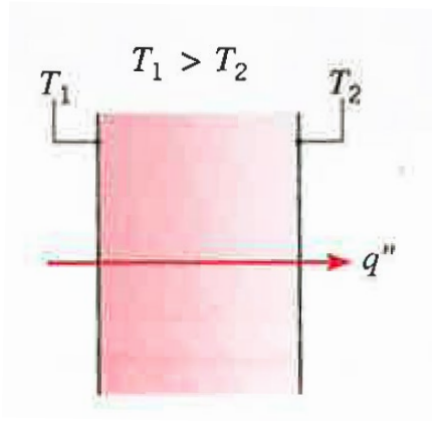
Although thermodynamics may be used to determine the amount of heat needed for a system to pass from one equilibrium state to another it does not acknowledge that heat transfer is inherently a non-equilibrium process. In fact, for heat transfer to occur there **MUST** be a TEMPERATURE GRADIENT. (Incropera, Ch. 1.3)

# Nomenclature & Units

- $Q = \text{heat transfer rate } [W]$
- $q'' = \text{heat flux } [W/m^2]$
- $\dot{q} = \text{volumetric heat source } [\frac{W}{m^3}]$
- $q' = \text{heat flux unit length } [W/m]$

# Transport Laws

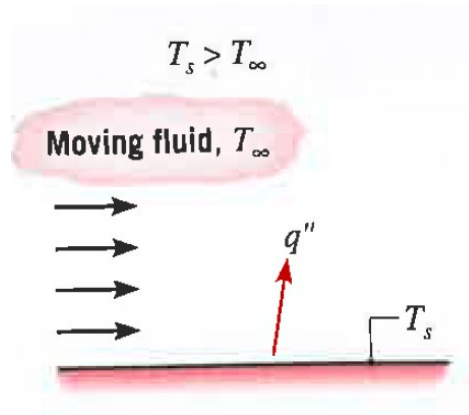
## Conduction



Fourier's Law

$$q'' = -k \frac{dT}{dx}$$

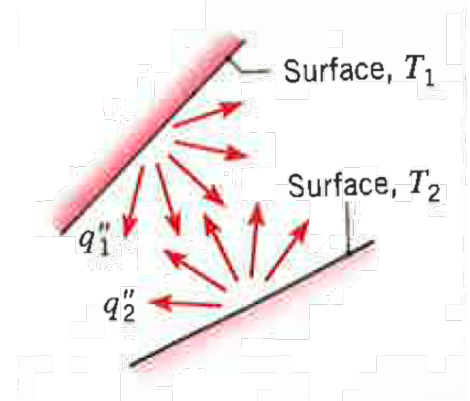
## Convection



Newton's Law

$$q'' = \bar{h} (T_s - T_\infty)$$

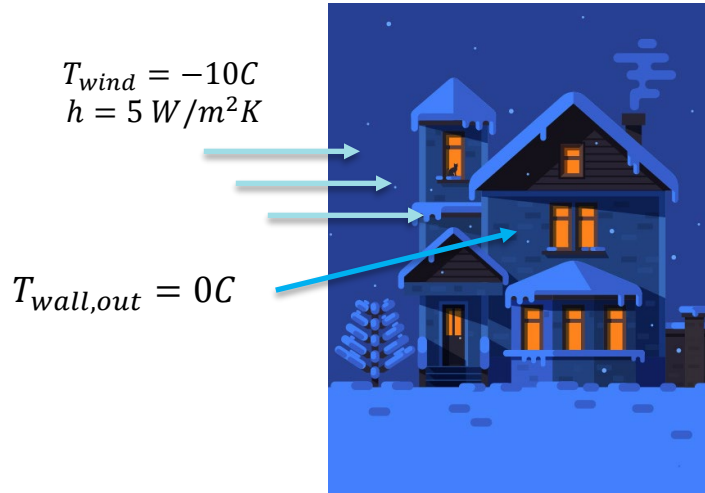
## Radiation



Stefan-Boltzmann Law

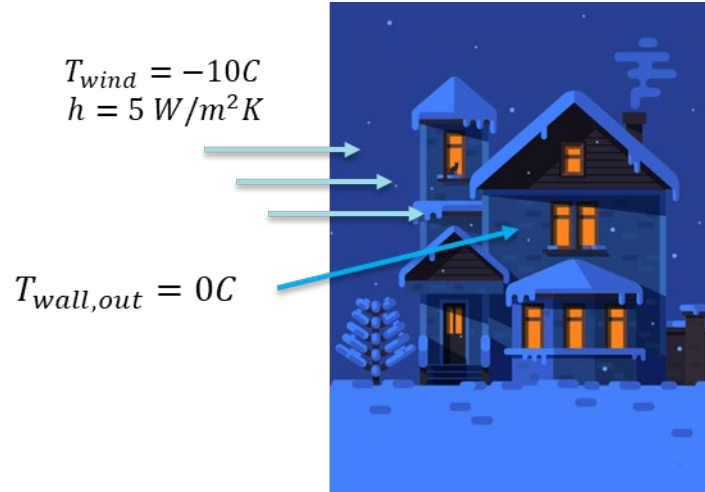
$$Q_{rad} = \epsilon \sigma A_s (T^4 - T_{sur}^4)$$

# Transport Laws

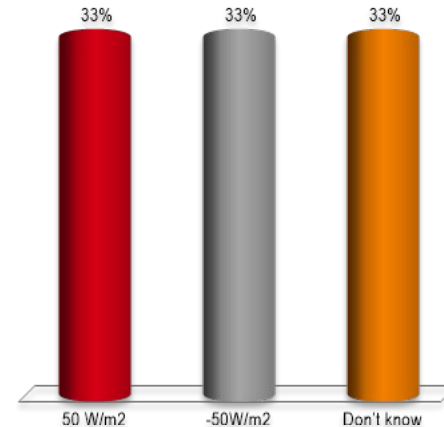


- Draw a simplified system representing the heat transfer.
- Calculate the amount of heat transferred per unit area (heat flux)

# Heat Flux in Winter:



- A.  $50 W/m^2$
- B.  $-50W/m^2$
- C. Don't know



# Transport Laws



$$T_{wall,out} = 30C$$

$$t_{wall} = 30 \text{ cm}$$

$$k_{wall} = 1.5 \frac{W}{mK}$$

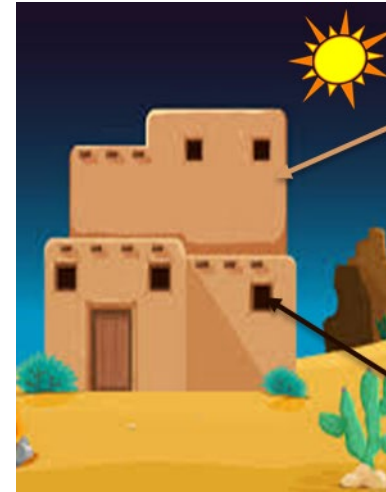
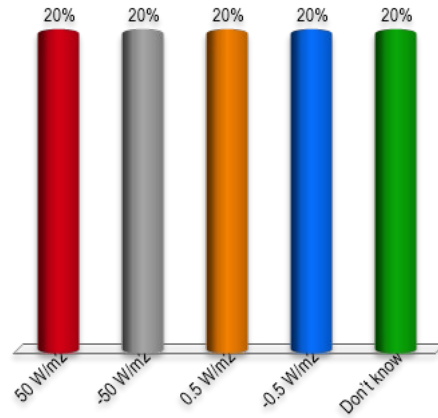
$$T_{indoor} = 20C$$

- Draw a simplified system representing the heat transfer.
- Calculate the amount of heat transferred per unit area (heat flux)



# Heat Flux in Summer

- A.  $50 \text{ W/m}^2$
- B.  $-50 \text{ W/m}^2$
- C.  $0.5 \text{ W/m}^2$
- D.  $-0.5 \text{ W/m}^2$
- E. Don't know

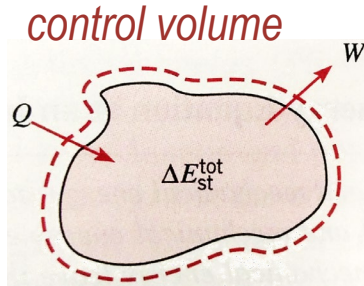


$$T_{wall,out} = 30C$$

$$t_{wall} = 30 \text{ cm}$$
$$k_{wall} = 1.5 \frac{W}{mK}$$

$$T_{indoor} = 20C$$

# Part I – Fourier's Law and Heat Conduction



- ☐ Heat Diffusion Equation (HDE) 3D
- ☐ HDE Steady-state 1D Solutions with/without Heat Sources
- ☐ Thermal Resistances and Equivalent Electrical Circuits
- ☐ Fins and Arrays of Fins
- ☐ Transient HDE
  - ☐ Lumped Capacitance Model  $T(t)$
  - ☐ 1D Spatial Effects  $T(X,t)$
  - ☐ Semi-Infinite Solid
  - ☐ Periodic BC

$$\frac{dE_{st}}{dt} = \dot{U} = Q - W + \dot{E}_{gen}$$

$$q'' = -k \frac{dT}{dx}$$

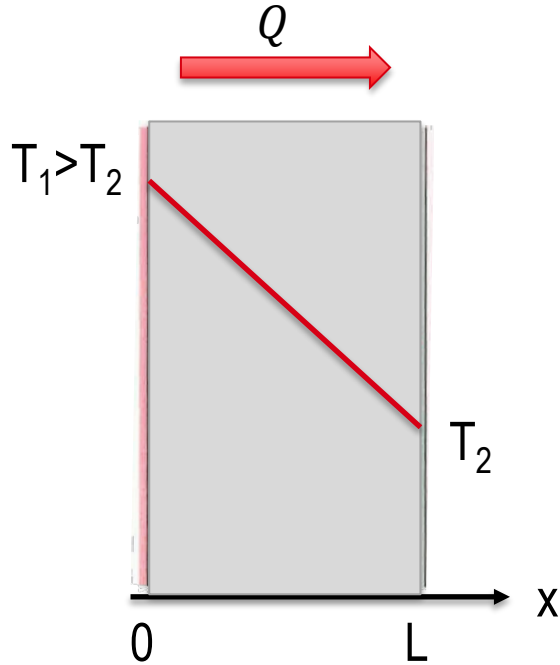
# Conductive Heat Transfer - 1

- ☐ Heat diffusion equation
- ☐ Thermal conductivity and diffusivity

## Learning Objectives:

- ☐ Understand material parameters and know their magnitude
- ☐ Derive the general heat diffusion equation

# The Conduction Rate Equation – From 1D to 3D



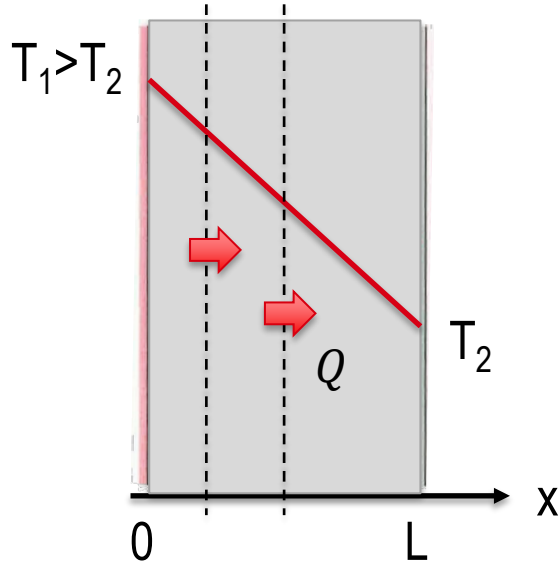
$$Q = -kA \frac{T_2 - T_1}{L} \Rightarrow \frac{Q}{A} = q'' = -k \frac{\Delta T}{L}$$

In the limit of an infinitesimal thickness  $dx$  :

$$q'' = -k \frac{dT}{dx} \quad [ \text{W/m}^2 ]$$

$k$  = thermal conductivity, [ W/mK ]

# The Conduction Rate Equation – From 1D to 3D

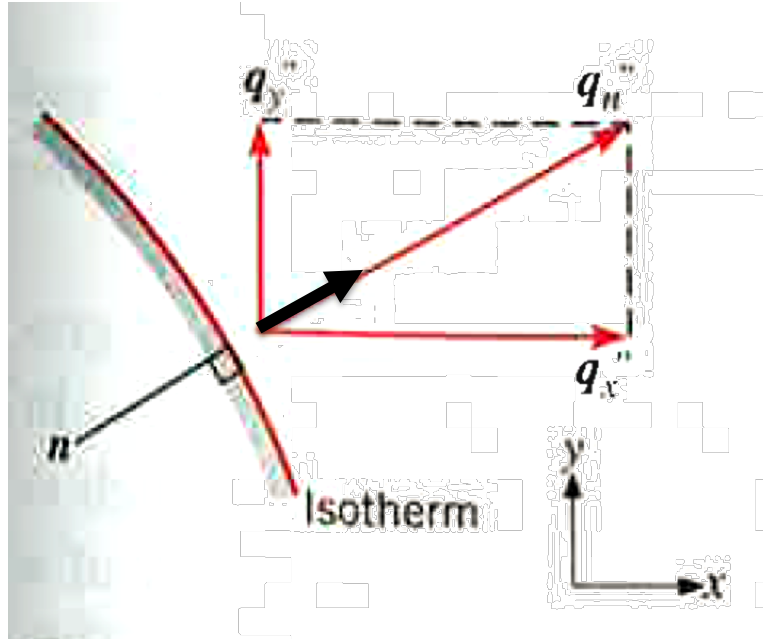


Heat flux is perpendicular to the isotherm surface,  
i.e. it along the temperature gradient

$$q'' = -k \frac{dT}{dx} \quad [ \text{W/m}^2 ]$$

$k$  = thermal conductivity, [ W/mK ]

# The Conduction Rate Equation – From 1D to 3D

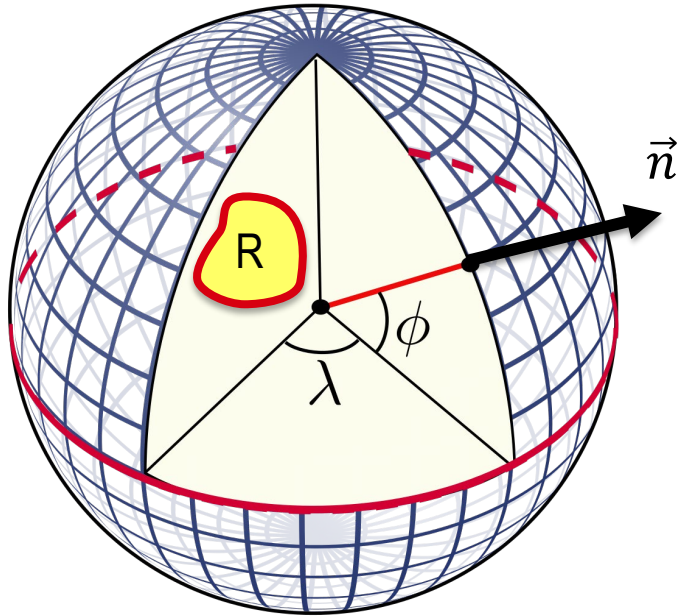


Heat flux is perpendicular to the isotherm surface,  
i.e. it along the temperature gradient

$$\vec{q}_n'' = -k \frac{\partial T}{\partial n} \vec{n}$$

$$\vec{q}'' = \vec{q}_x'' + \vec{q}_y'' = -k \frac{\partial T}{\partial x} \vec{i} - k \frac{\partial T}{\partial y} \vec{j} = -k \nabla T$$

# The Conduction Rate Equation – From 1D to 3D



3D isothermal surface

$$\vec{q}'' = -k \nabla T = -k \left( \frac{\partial T}{\partial x} \vec{i} + \frac{\partial T}{\partial y} \vec{j} + \frac{\partial T}{\partial z} \vec{k} \right)$$

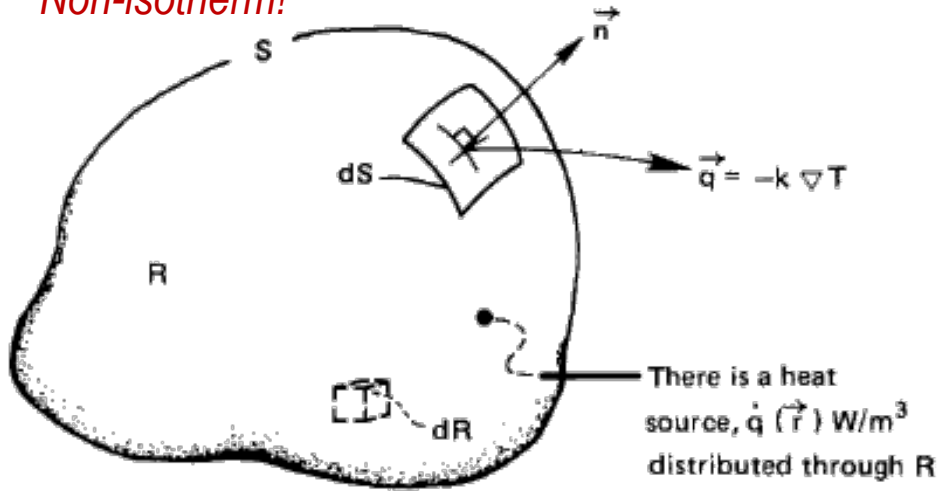
If the material is ANISOTROPIC:

$$\vec{q}'' = -\bar{\bar{k}} \nabla T \quad \bar{\bar{k}} = \begin{bmatrix} k_x & 0 & 0 \\ 0 & k_y & 0 \\ 0 & 0 & k_z \end{bmatrix}$$

$$\vec{q}'' = - \left( k_x \frac{\partial T}{\partial x} \vec{i} + k_y \frac{\partial T}{\partial y} \vec{j} + k_z \frac{\partial T}{\partial z} \vec{k} \right)$$

# Heat Diffusion Equation – 3D

*Non-isotherm!*



Assumption 1: incompressible medium

Assumption 2: medium at rest (no convection)

Assumption 3: isotropic material

The energy conservation equation requires:

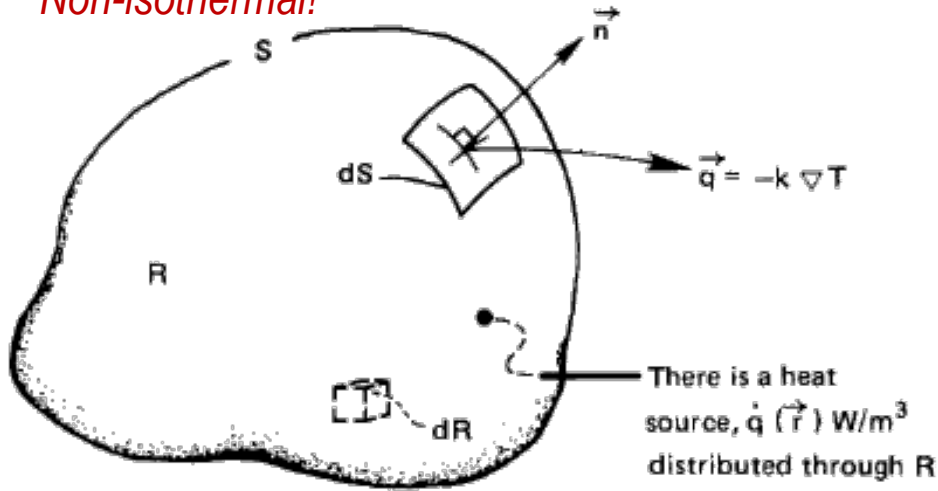
$$\dot{U} = mc \frac{dT}{dt} = \underbrace{Q}_{\nearrow 0} - \cancel{W} + \dot{E}_{gen}$$

Remember that  $Q > 0$  when flows INTO the volume. Hence its sign is opposite to the normal vector  $\vec{n}$



# Heat Diffusion Equation – 3D

*Non-isothermal!*



Heat transfer across  $S$  only through conduction

Heat flux is along  $T$  gradient

$$\vec{q} = -k \nabla T$$



**Heat transfer rate OUT of  $dS$**

$$\delta Q = (-k \nabla T) \cdot (\vec{n} dS)$$

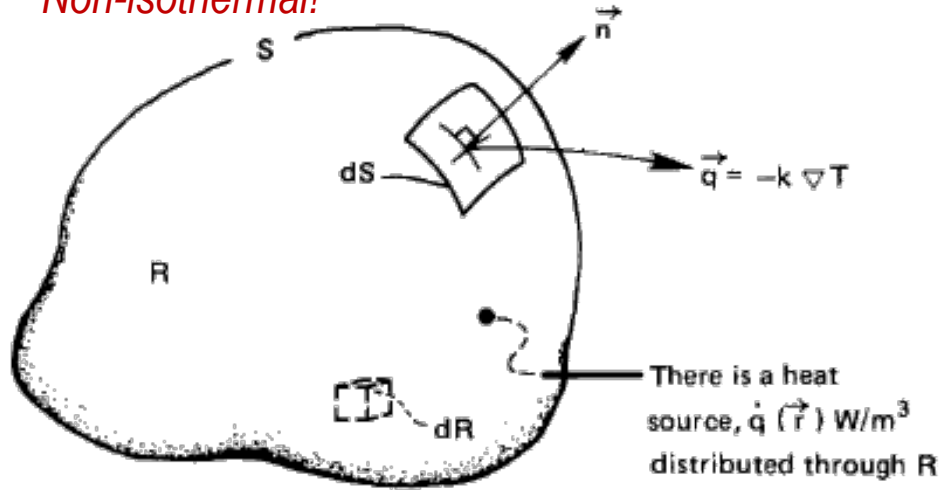
Assumption 1: incompressible medium

Assumption 2: medium at rest (no convection)

Assumption 3: isotropic material

# Heat Diffusion Equation – 3D

*Non-isothermal!*



Assumption 1: incompressible medium

Assumption 2: medium at rest (no convection)

Assumption 3: isotropic material

**Total Heat Transfer Rate INTO non-isothermal  $S$**

$$Q = - \int_S (-k \nabla T) \cdot (\vec{n} dS) = \int_S (k \nabla T) \cdot (\vec{n} dS)$$

**Total Generation Rate in Volume  $R$**

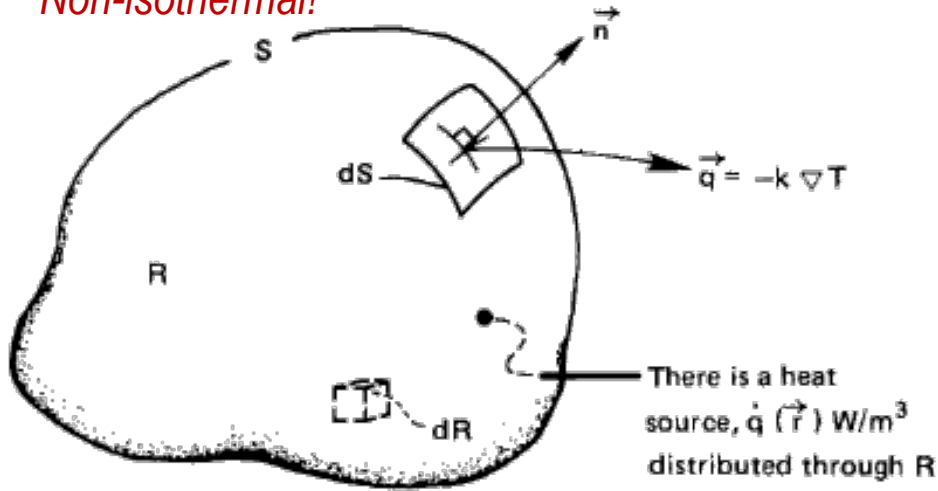
$$E_{gen} = \int_V \dot{q} dR$$

**Change in Internal Energy of the Volume**

$$\frac{dU}{dt} = \int_V \rho c \frac{\partial T}{\partial t} dR$$

# Heat Diffusion Equation – 3D

*Non-isothermal!*



Assumption 1: incompressible medium

Assumption 2: medium at rest (no convection)

Assumption 3: isotropic material

So we can write:  $\dot{U} = Q + \dot{E}_{gen}$

$$\int_V \rho c \frac{\partial T}{\partial t} dR = \int_S (k \nabla T) \cdot (\vec{n} dS) + \int_V \dot{q} dR$$

↓ Gauss' law

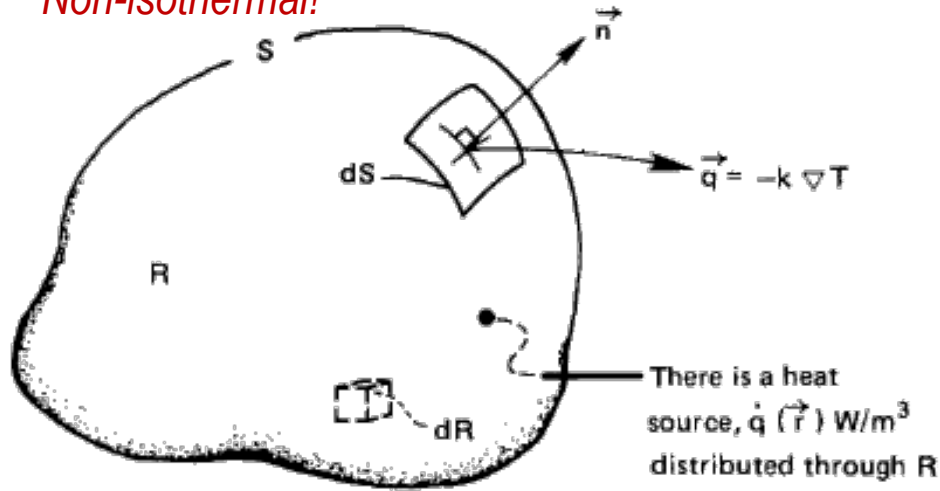
$$\int_V \rho c \frac{\partial T}{\partial t} dR = \int_V (\nabla \cdot (k \nabla T) + \dot{q}) dR$$

↓

$$0 = \int_V \left( \nabla \cdot (k \nabla T) + \dot{q} - \rho c \frac{\partial T}{\partial t} \right) dR$$

# Heat Diffusion Equation – 3D

*Non-isothermal!*



Assumption 1: incompressible medium

Assumption 2: medium at rest (no convection)

Assumption 3: isotropic material

Heat Diffusion Equation:

$$\nabla \cdot (k \nabla T) + \dot{q} = \rho c \frac{\partial T}{\partial t}$$

Assumption 4:  $k$  is independent of  $T$

$$k \nabla^2 T + \dot{q} = \rho c \frac{\partial T}{\partial t}$$

$$\nabla^2 T + \frac{\dot{q}}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

$$\alpha = \frac{k}{\rho c} = \text{thermal diffusivity} \left[ \frac{m^2}{s} \right]$$

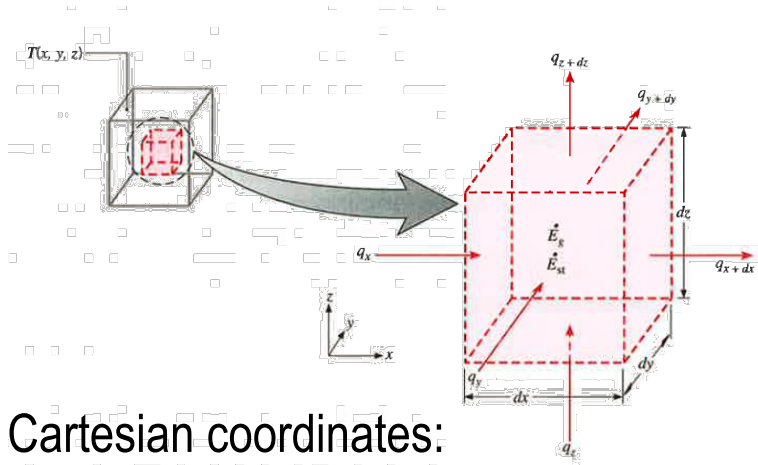
# Heat Diffusion Equation – 3D

Assumption 1: incompressible medium

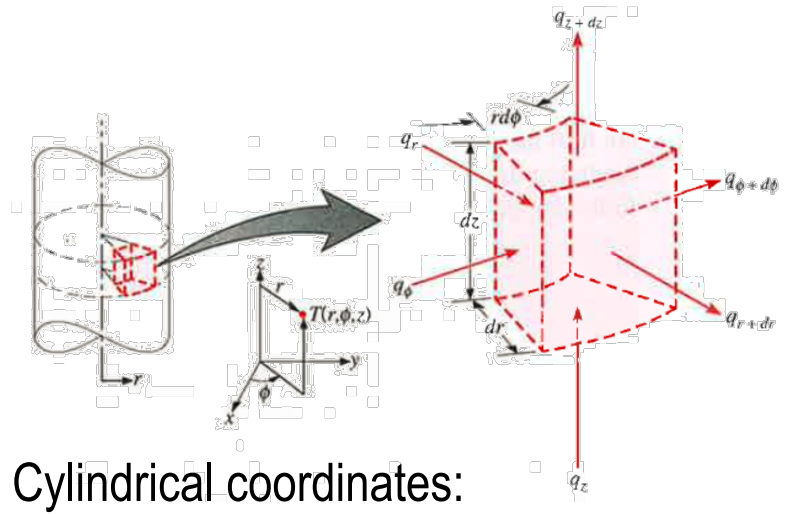
Assumption 2: medium at rest (no convection)

Assumption 3: isotropic material

$$\nabla \cdot (k \nabla T) + \dot{q} = \rho c \frac{\partial T}{\partial t}$$



$$\frac{\partial}{\partial x} \left( k \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left( k \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left( k \frac{\partial T}{\partial z} \right) + \dot{q} = \rho c_p \frac{\partial T}{\partial t}$$



$$\frac{1}{r} \frac{\partial}{\partial r} \left( k r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial}{\partial \phi} \left( k \frac{\partial T}{\partial \phi} \right) + \frac{\partial}{\partial z} \left( k \frac{\partial T}{\partial z} \right) + \dot{q} = \rho c_p \frac{\partial T}{\partial t}$$

# Material Properties

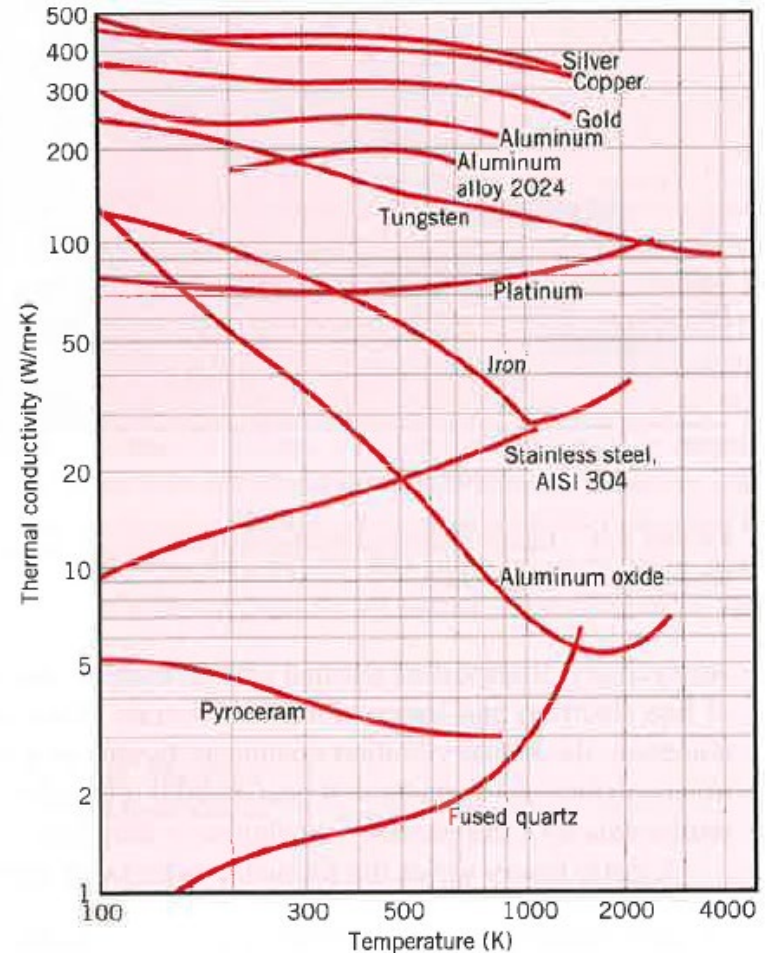
Thermal Conductivity  $k$  [W/mK]

For a general material we have:

$$\vec{q}'' = -\bar{k} \nabla T \quad \Rightarrow \quad q_x'' = -k_x \frac{\partial T}{\partial x}$$

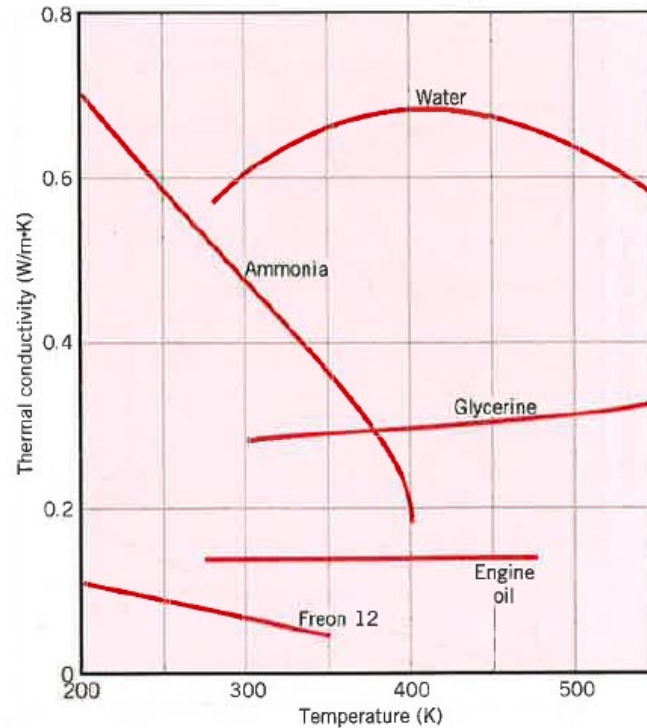
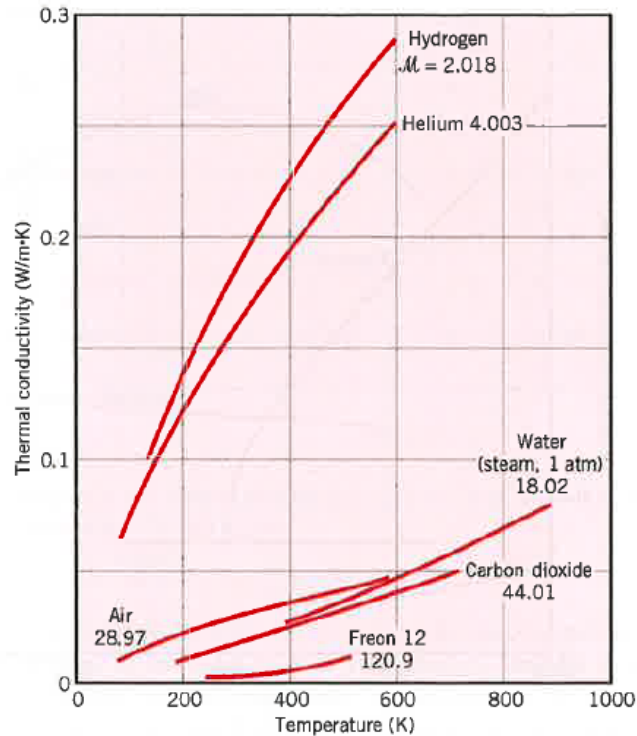
So we can define:

$$k_i \equiv \frac{q_i''}{\frac{\partial T}{\partial x}} \quad i = x, y, z$$



# Material Properties

Thermal Conductivity  $k$  [W/mK]



# Material Properties

*Thermal Diffusivity  $\alpha$  [ $m^2/s$ ]*

$$\alpha = \frac{k}{\rho c}$$

Relates to the speed with which a body responds to changes in the thermal environment.  
Indeed:

- Conduction  $k$  removes heat
- Thermal capacity ( $\rho c$ ) cumulates energy

The higher the thermal conductivity and the lower the thermal capacity, the higher the material diffusivity, i.e. the material will respond quickly to thermal changes.



# Material Properties

Thermal Diffusivity  $\alpha$  [ $\text{m}^2/\text{s}$ ]

$$\alpha = \frac{k}{\rho c}$$

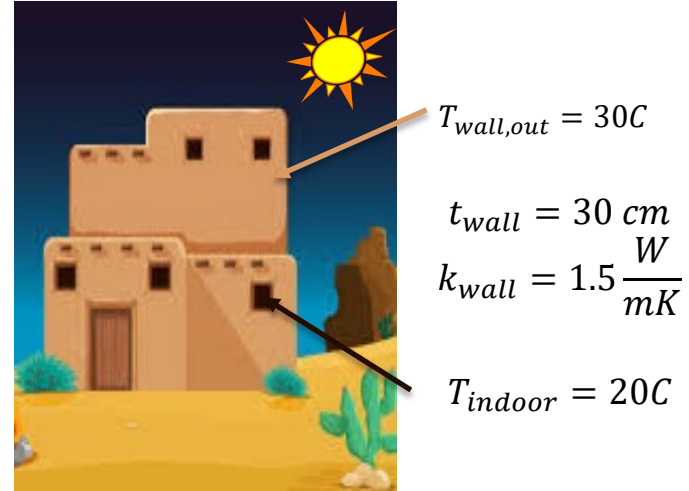
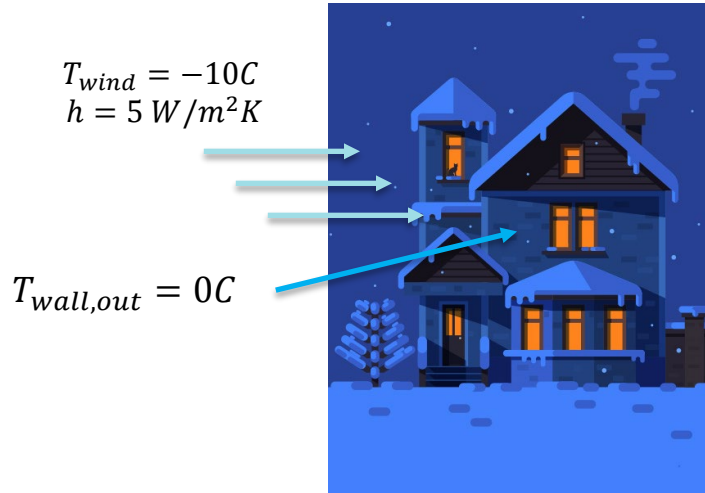
Table A.1, pure aluminum (300 K):

$$\left. \begin{array}{l} \rho = 2702 \text{ kg/m}^3 \\ c_p = 903 \text{ J/kg} \cdot \text{K} \\ k = 237 \text{ W/m} \cdot \text{K} \end{array} \right\} \alpha = \frac{k}{\rho c_p} = \frac{237 \text{ W/m} \cdot \text{K}}{2702 \text{ kg/m}^3 \times 903 \text{ J/kg} \cdot \text{K}}$$
$$= 97.1 \times 10^{-6} \text{ m}^2/\text{s}$$

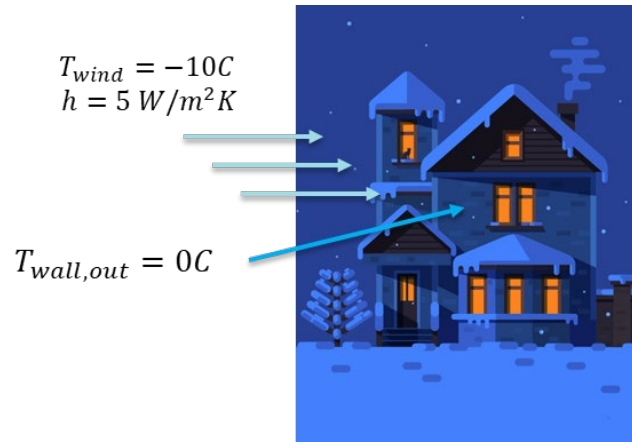
paraffin (300 K):

$$\left. \begin{array}{l} \rho = 900 \text{ kg/m}^3 \\ c_p = 2890 \text{ J/kg} \cdot \text{K} \\ k = 0.24 \text{ W/m} \cdot \text{K} \end{array} \right\} \alpha = \frac{k}{\rho c_p} = \frac{0.24 \text{ W/m} \cdot \text{K}}{900 \text{ kg/m}^3 \times 2890 \text{ J/kg} \cdot \text{K}}$$
$$= 9.2 \times 10^{-8} \text{ m}^2/\text{s}$$

# Transport Laws

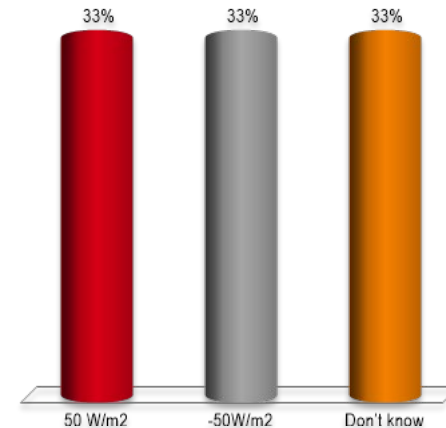


- Draw a simplified system representing the heat transfer.
- Calculate the amount of heat transferred per unit area (heat flux) in the two situations.



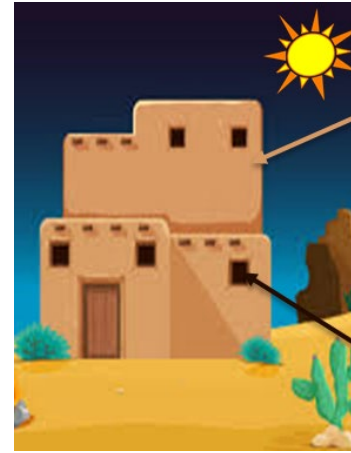
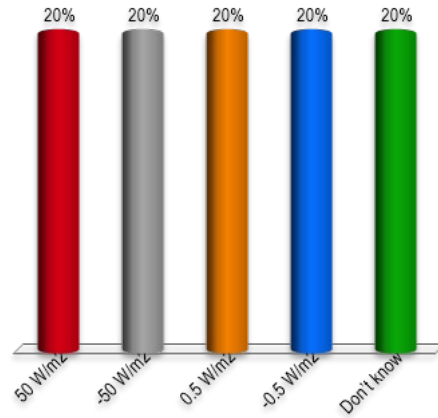
# Heat Flux in Winter:

- A.  $50 W/m^2$
- B.  $-50W/m^2$
- C. Don't know



# Heat Flux in Summer

- A.  $50 \text{ W/m}^2$
- B.  $-50 \text{ W/m}^2$
- C.  $0.5 \text{ W/m}^2$
- D.  $-0.5 \text{ W/m}^2$
- E. Don't know



$$T_{wall,out} = 30C$$

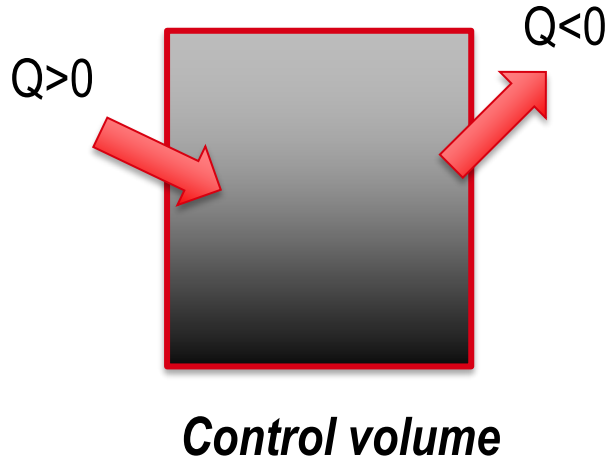
$$t_{wall} = 30 \text{ cm}$$
$$k_{wall} = 1.5 \frac{W}{mK}$$

$$T_{indoor} = 20C$$

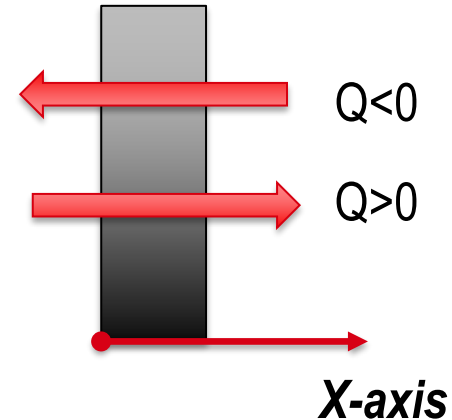
# Transport Laws

Be careful with the signs and their meaning!

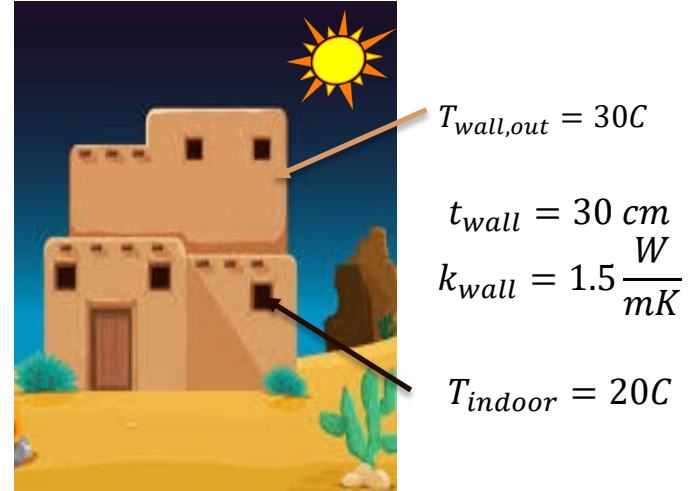
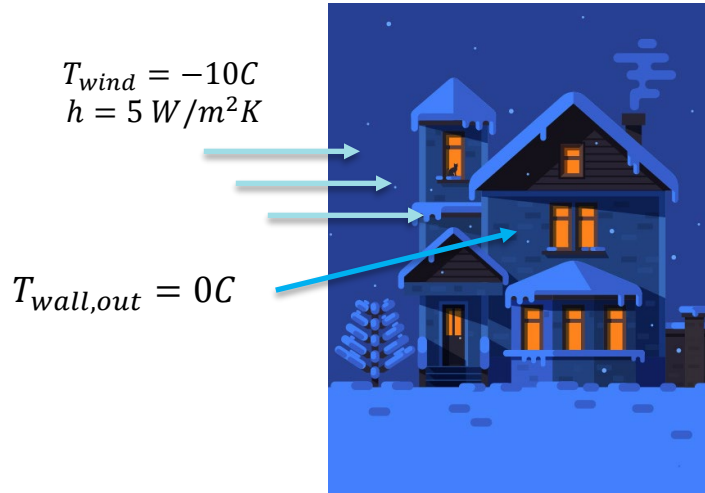
## *1<sup>st</sup> Law of Thermodynamics*



## *Fourier's Law (1D)*

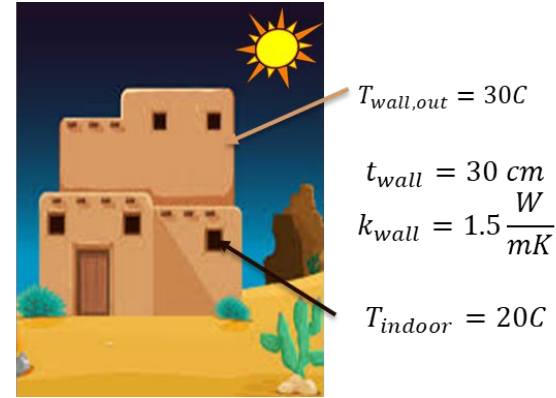
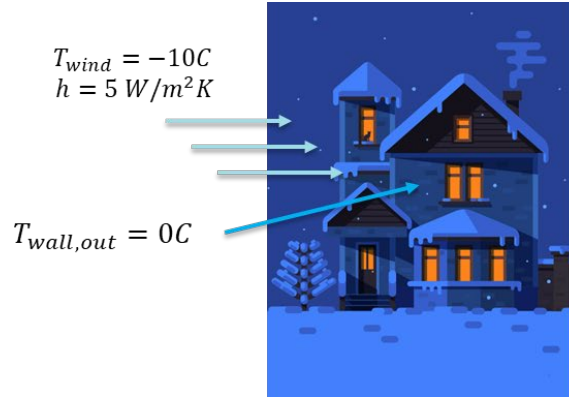


# Transport Laws

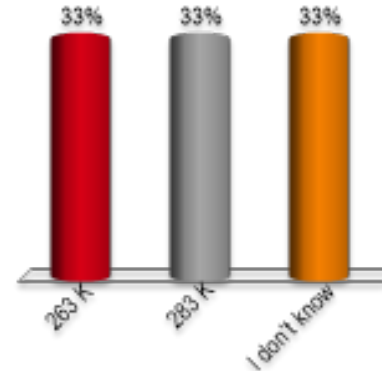


- If the wall is the same in both houses, what is the indoor wall temperature in the winter case?

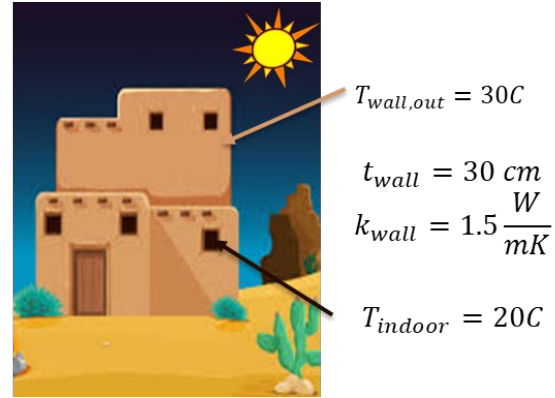
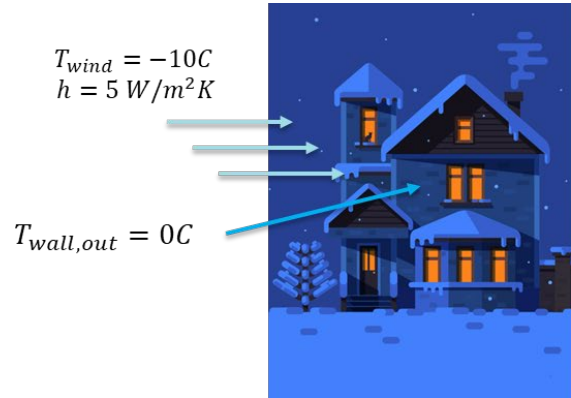
What is the indoor wall temperature in the winter case?



- A. 263 K
- B. 283 K
- C. I don't know



# Transport Laws



- If the wall is the same in both houses, what is the indoor wall temperature in the winter case?



# Conductive Heat Transfer - 1



Heat diffusion equation



Thermal conductivity and diffusivity

## Learning Objectives:



Understand material parameters and know their magnitude



Derive the general heat diffusion equation

# Tomorrow:

- ☐ Types of boundary conditions
- ☐ Planar and cylindrical (1D) solutions
- ☐ Thermal resistance
- ☐ Bi Number
- ☐ Intro to Thermal Circuits

## Learning Objectives:

- ☐ Identify the possible boundary conditions
- ☐ Express mathematically the various boundary conditions
- ☐ Calculate the temperature profile in a planar or cylindrical wall
- ☐ Calculate the thermal resistances
- ☐ Calculate the Bi number
- ☐ Solve 1D problems using thermal circuits