

## Thermodynamics of Earth systems

Lecture 6:  
Entropy, the Second Law  
of Thermodynamics  
(continued)

# Material covered in Lecture

## Part 2: Framework

### *Entropy and the 2nd law*

- Entropy: reversible and irreversible processes; Clausius inequality; Boltzmann-Gibbs statistical picture of entropy
- Heat engines, Carnot Cycle and the maximum efficiency
- Applications of heat engines and Carnot Efficiency to atmosphere, ocean and deep earth
- 2nd Law of thermodynamics
- First and second laws combined; Energy functions (Gibbs and Helmholtz)

### *Other*

- Energy functions; Maxwell Equations
- Definition of Thermodynamic Equilibrium (single component system, multicomponent system).

### *Phase Equilibria*

- Gibbs phase rule: thermodynamic degrees of freedom, phases and components
- Energy in phase changes and chemical reactions

# Thermodynamic relationships

Euler's relationship :  $du = M dx + N dy$

and  $du$  is an exact differential, then

$$\frac{\partial M}{\partial y} = \frac{\partial N}{\partial x}$$

so:  $du = -pdv + Tds \Rightarrow \frac{\partial(-p)}{\partial s} = \left(\frac{\partial T}{\partial v}\right)$

$dh = vdp + Tds \Rightarrow \left(\frac{\partial T}{\partial p}\right) = \left(\frac{\partial v}{\partial s}\right)$

$da = -pdv - SdT \Rightarrow \frac{\partial(-S)}{\partial v} = \frac{\partial(-p)}{\partial T}$

$dg = vdp - SdT \Rightarrow \frac{\partial(-S)}{\partial p} = \frac{\partial v}{\partial T}$

Maxwell's relation

# Thermodynamic relationships

Also, form the definition of equilibrium:

$$du=0 = Tds - pdv \Rightarrow \left(\frac{\partial s}{\partial v}\right)_{u=\text{const}} = \frac{p}{T}$$

$$dh=0 = Tds + vdp \Rightarrow \left(\frac{\partial s}{\partial p}\right)_{h=\text{const}} = -\frac{v}{T}$$

$$da=0 = -sdt - pdv \Rightarrow \left(\frac{\partial v}{\partial t}\right)_{a=\text{const}} = -\frac{s}{p}$$

$$dq=0 = -sdt + vdp \Rightarrow \left(\frac{\partial p}{\partial t}\right)_{q=\text{const}} = -\frac{s}{v}$$

# Thermodynamic relationships



Finally, from the definition of an exact diff

$$u(s, v) : du = \frac{\partial u}{\partial s} ds + \frac{\partial u}{\partial v} dv \quad \left. \begin{array}{l} \frac{\partial u}{\partial s} = T \\ \frac{\partial u}{\partial v} = -p \end{array} \right\} \quad \text{but } du = T \cdot ds - p \cdot dv \quad \left. \begin{array}{l} \frac{\partial u}{\partial s} = T \\ \frac{\partial u}{\partial v} = -p \end{array} \right\}$$

$$h(s, p) : dh = \frac{\partial h}{\partial s} ds + \frac{\partial h}{\partial p} dp \quad \left. \begin{array}{l} \frac{\partial h}{\partial s} = T \\ \frac{\partial h}{\partial p} = v \end{array} \right\} \quad \text{but } dh = T \cdot ds + v \cdot dp \quad \left. \begin{array}{l} \frac{\partial h}{\partial s} = T \\ \frac{\partial h}{\partial p} = v \end{array} \right\}$$

$$a(T, v) : da = \frac{\partial a}{\partial T} dT + \frac{\partial a}{\partial v} dv \quad \left. \begin{array}{l} \frac{\partial a}{\partial T} = -s \\ \frac{\partial a}{\partial v} = -p \end{array} \right\} \quad \text{but } da = -s \cdot dT - p \cdot dv \quad \left. \begin{array}{l} \frac{\partial a}{\partial T} = -s \\ \frac{\partial a}{\partial v} = -p \end{array} \right\}$$



$$g(T, p) : dg = \frac{\partial g}{\partial T} dT + \frac{\partial g}{\partial p} dp \quad \left. \begin{array}{l} \frac{\partial g}{\partial T} = -s \\ \frac{\partial g}{\partial p} = v \end{array} \right\} \quad \text{but } dg = -s \cdot dT + v \cdot dp \quad \left. \begin{array}{l} \frac{\partial g}{\partial T} = -s \\ \frac{\partial g}{\partial p} = v \end{array} \right\}$$

# What is Thermodynamic Equilibrium?

---

It is the state a given system tends to reach (given enough time).

This state is characterized by:

- **Thermal** equilibrium  
No net heat flux between components of the system
- **Mechanical** equilibrium  
Pressure tends to become uniform
- **Diffusional** equilibrium  
No net mass flux between components of a system

# Formulating Thermodynamic Equilibrium

---

A criterion for equilibrium in terms of measurable quantities would be very useful (hard to measure  $S$ ).

Gibbs Free Energy " $G$ " is perfectly suited for this.

$$G(T, P) = U + PV - TS$$

$P$ : pressure,  $V$ : system volume,  $T$ : temperature,  $S$ : entropy and  $U$ : internal energy

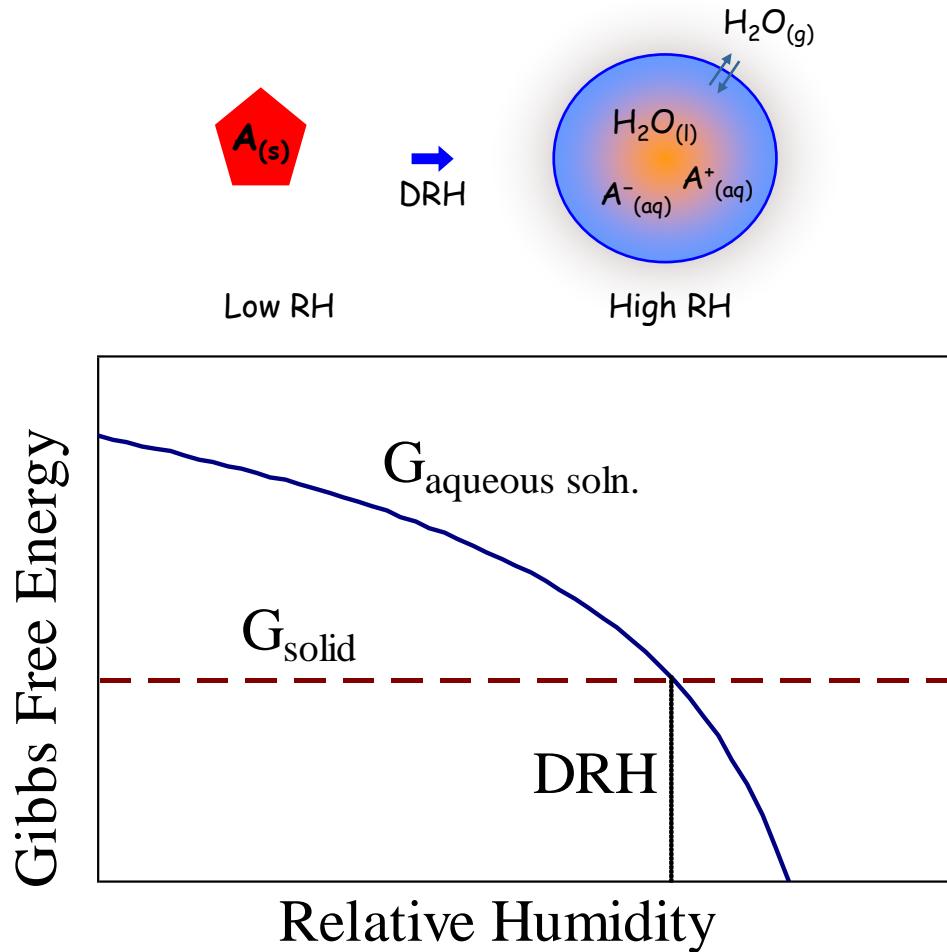
Changes in  $G$  are then expressed as:

$$dG = \boxed{dU + PdV - TdS} + VdP - SdT$$

Zero from combined First & Second Law

# How useful is this criterion? Very!

**Deliquescence Relative Humidity (DRH):** RH at which an aerosol transitions from a solid to an aqueous solution



# Formulating Thermodynamic Equilibrium

---

In other words,

$$dG = VdP - SdT$$

If  $P$  and  $T$  are kept constant,  $dG=0$ , with  $d^2G > 0$

So  $G$  of a closed system at constant  $P,T$  is  
minimum at equilibrium

How useful is this relationship?

# Formulating Thermodynamic Equilibrium

---

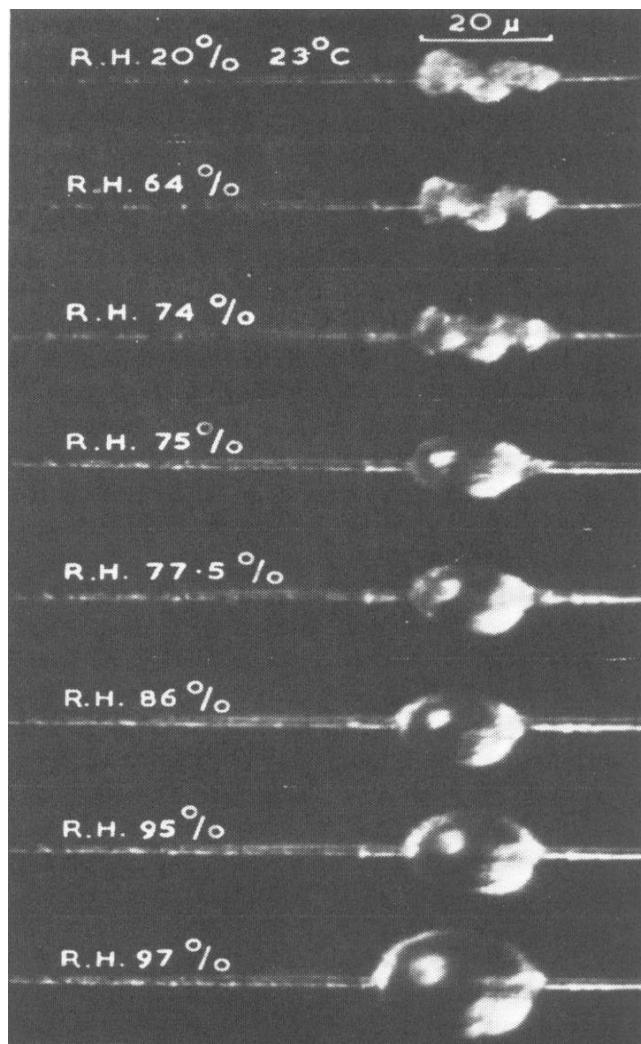
In other words,

$$dG = VdP - SdT$$

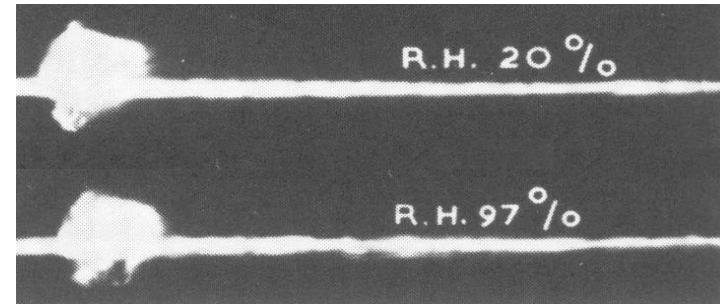
If  $P$  and  $T$  are kept constant,  $dG=0$ , with  $d^2G > 0$

So  $G$  of a closed system at constant  $P,T$  is  
minimum at equilibrium

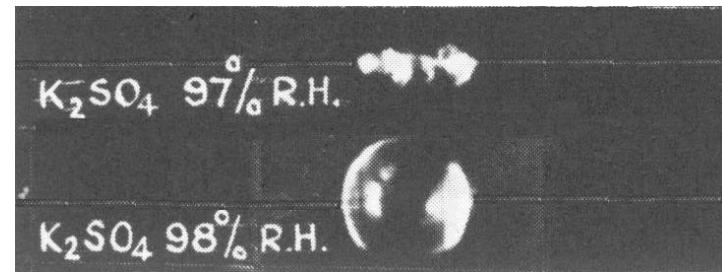
# Deliquescence: Some examples



Sea Salt Particle: DRH  $\sim$  75%



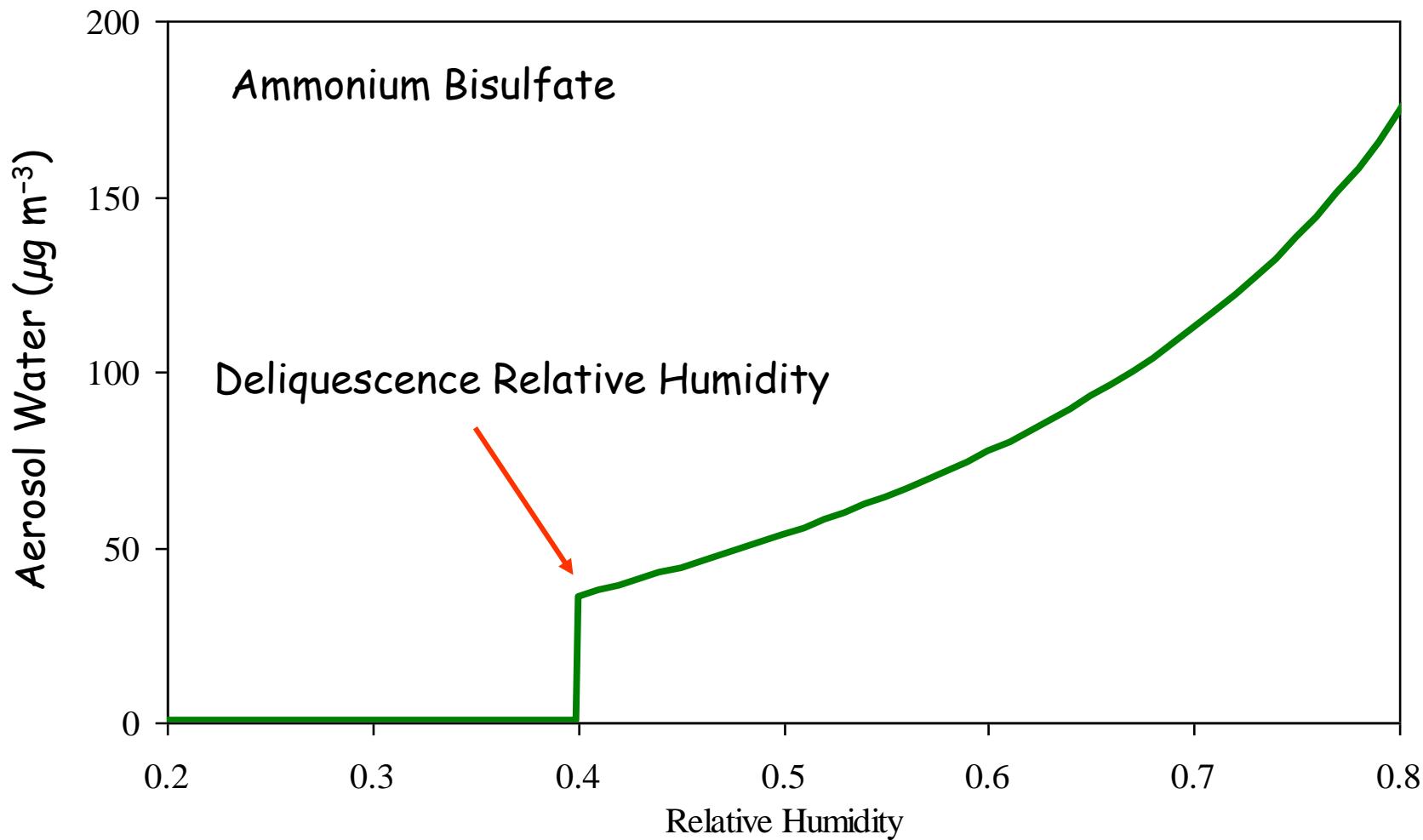
Dust Particle: no DRH



$K_2SO_4$  particle: DRH = 98%

# Aerosol water uptake: deliquescence

---



# Formulating Thermodynamic Equilibrium

---

In other words,

$$dG = VdP - SdT$$

If  $P$  and  $T$  are kept constant,  $dG=0$ , with  $d^2G > 0$

So  $G$  of a closed system at constant  $P,T$  is  
minimum at equilibrium

What happens if the system is open or it has  
multiple phases and components?

We need to consider mass in the Gibbs Energy  
formulation

# Formulating Thermodynamic Equilibrium

In other words,

$$G(P, T, \underbrace{n_1, \dots, n_n}_{1, 2, \dots, n}) \quad \begin{matrix} \text{mass of components} \\ 1, 2, \dots, n \end{matrix}$$

Chain rule:

$$dG = \left( \frac{\partial G}{\partial T} \right) dT + \left( \frac{\partial G}{\partial P} \right) dP + \left( \frac{\partial G}{\partial n_1} \right) dn_1 + \dots + \left( \frac{\partial G}{\partial n_n} \right) dn_n$$

$-S$

$V$

Contribution of each component to the free energy

$\left( \frac{\partial G}{\partial n_1} \right), \dots, \left( \frac{\partial G}{\partial n_n} \right)$  are the chemical potentials  $\mu_1, \dots, \mu_n$

# Formulating Thermodynamic Equilibrium

---

So:  $dG = -SdT + VdP + \mu_1dn_1 + \dots + \mu_ndn_n$

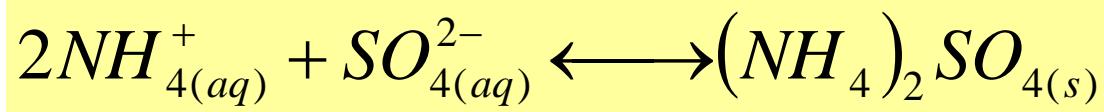
At thermodynamic equilibrium,  $dG = 0$

For constant  $P, T$  this means:  $\mu_1dn_1 + \dots + \mu_ndn_n = 0$

This statement is known as "chemical equilibrium" and is the basis of any aerosol thermodynamic model

Let's apply this to a chemical reaction found in aerosols:  
Dissolution of ammonium sulfate in water.

# Chemical Equilibrium: Example



At equilibrium ( $P, T = \text{const}$ ):

$$\mu_{\text{NH}_4^+} dn_{\text{NH}_4^+} + \mu_{\text{SO}_4^{2-}} dn_{\text{SO}_4^{2-}} + \mu_{(\text{NH}_4)_2\text{SO}_4} dn_{(\text{NH}_4)_2\text{SO}_4} = 0$$

From stoichiometry:  $dn_{\text{NH}_4^+} = 2dn_{\text{SO}_4^{2-}} = -2dn_{(\text{NH}_4)_2\text{SO}_4}$

So:  $(-2\mu_{\text{NH}_4^+} - \mu_{\text{SO}_4^{2-}} + \mu_{(\text{NH}_4)_2\text{SO}_4})dn_{(\text{NH}_4)_2\text{SO}_4} = 0$

Or simply:  $-2\mu_{\text{NH}_4^+} - \mu_{\text{SO}_4^{2-}} + \mu_{(\text{NH}_4)_2\text{SO}_4} = 0$

# Chemical Equilibrium: General Reaction

---



At equilibrium, and constant  $P, T$  :

$$d\mu_D + c\mu_C - a\mu_A - b\mu_B = 0$$

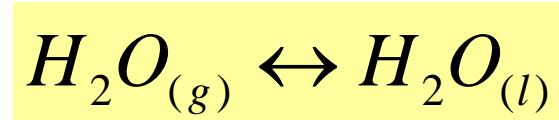
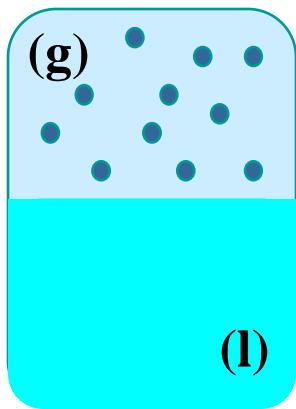
$$\sum_i \nu_i \mu_i = 0$$

i.e., chemical potential of the reactants  
equals chemical potential of the products

# Chemical Equilibrium: Phase Equilibria

---

Even phase equilibria is (for thermo) a reaction:



$$\mu_{H_2O_{(g)}} - \mu_{H_2O_{(l)}} = 0 \quad \text{or} \quad \mu_{H_2O_{(g)}} = \mu_{H_2O_{(l)}}$$

when two phases are in equilibrium with each other, they share the same chemical potential

# What is Thermodynamic Equilibrium?

---

It is the state a given system tends to reach (given enough time).

This state is characterized by:

- **Thermal** equilibrium

$dT=0$ ,  $T=\text{constant everywhere}$

- **Mechanical** equilibrium

$dP=0$ ,  $P=\text{constant everywhere}$

- **Diffusional** equilibrium

$\mu_i^g = \mu_i^l$  a compound  $i$  between phases shares the same chemical potential.

# Some things more about G

$G$  however is also the sum of its partial contributions. For constant  $T, P$ :

$$G = \sum g_i n_i \leftarrow \# \text{ of moles of substance } "i".$$

$\hookrightarrow$  GFE per mole and of substance "i"

and, since we showed already that  $\mu_i = g_i$ .

$$G = \sum \mu_i n_i \quad \text{const } T, P.$$

Total GFE of the system is given by the sum of the chemical potentials  $\times$  # of moles of each constituent.

# Is the number of species limited?

---

Yes. It's given by the Gibbs Phase Rule

$$F = C - P + 2$$

- ◆  $F$ : number of independent variables
- ◆  $P$ : number of phases
- ◆  $C$ : Number of compounds

Components: water, ethanol, benzene, salt

Phases: gas, liquid, solid

e.g., pure water in equilibrium with its vapor:

$C=1$ ,  $P=2$  so  $F=1$  (one independent variable, e.g. T)

e.g., a water/salt mixture in equilibrium with its vapor:

$C=2$ ,  $P=2$  so  $F=2$  (two independent variables, e.g. T +  $n_{\text{NaCl}}$ )