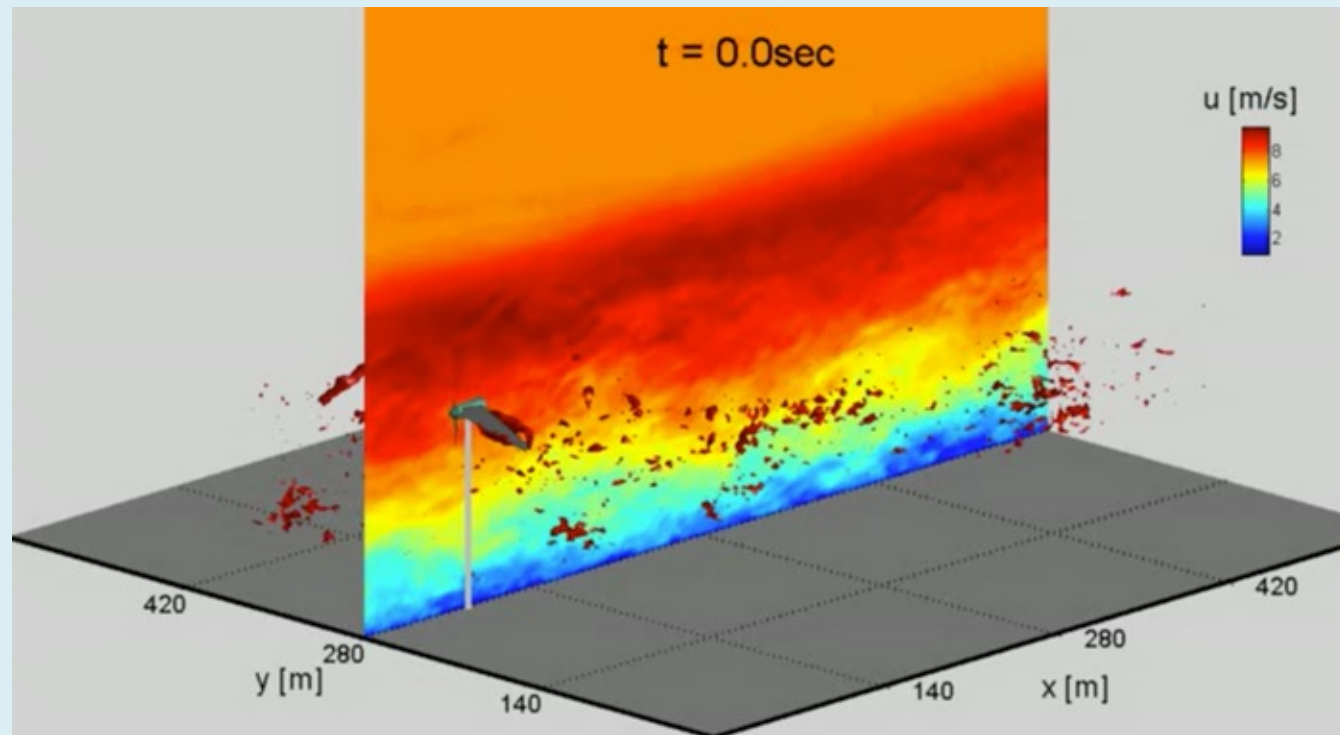


Environmental Transport Phenomena

Computational Fluid Dynamics

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**Wind engineering and
renewable energy laboratory
WiRE**



Computational Fluid Dynamics (CFD)

- I. Approaches for simulating turbulent flows**
- II. Direct Numerical Simulation (DNS)**
- III. RANS and the closure problem**
- IV. Large-Eddy Simulation (LES)**

Reference: Lecture + Handout (handout optional)

Motivation

- For turbulent flows, we know the transport equations (advection-diffusion equations in 3D), but there is **no analytical solution**
- In computational fluid dynamics (CFD), equations are discretized (in time and space) and **solved numerically (with computers)**
- To resolve all eddy motions (from integral scale to Kolmogorov scale), **one needs a resolution as fine as the Kolmogorov scale in 3-D** [this is called Direct Numerical Simulation].

Question: Is this possible for all turbulent flows?

Governing Transport (Advection-Diffusion) Equations

Incompressible flow

$$\frac{\partial u_i}{\partial x_i} = 0$$

Mass conservation (continuity)

$$\frac{\partial u_i}{\partial t} + \frac{\partial}{\partial x_j} (u_i u_j) = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left(\nu \left[\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right] \right) + F_i$$

Momentum conservation
(Navier-Stokes equations)

$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x_i} (u_i C) = + \frac{\partial}{\partial x_i} \left(D_m \frac{\partial C}{\partial x_i} \right) + Q$$

Advection-diffusion equation
for conservation of Scalars (e.g.
pollutant, temperature)

Note: F_i is any external forcing;
 Q is any source or sink of scalar.

Steps in CFD:

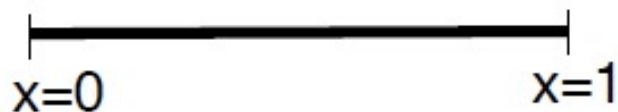
- **STEP 1: Meshing**
- **STEP 2: Discretize equations**
- **STEP 3: Solve discretized equations**

General Strategy in CFD (generally in numerical methods)

The general strategy consists of replacing a **continuous domain** with a **discrete domain** using a grid

Continuous Domain

$$0 \leq x \leq 1$$

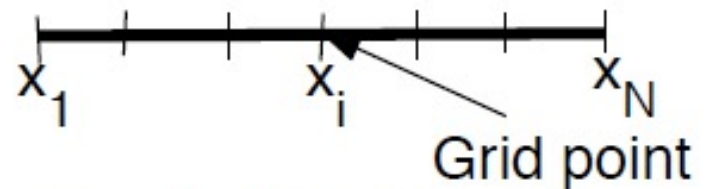


Coupled PDEs + boundary conditions in continuous variables



Discrete Domain

$$x = x_1, x_2, \dots, x_N$$

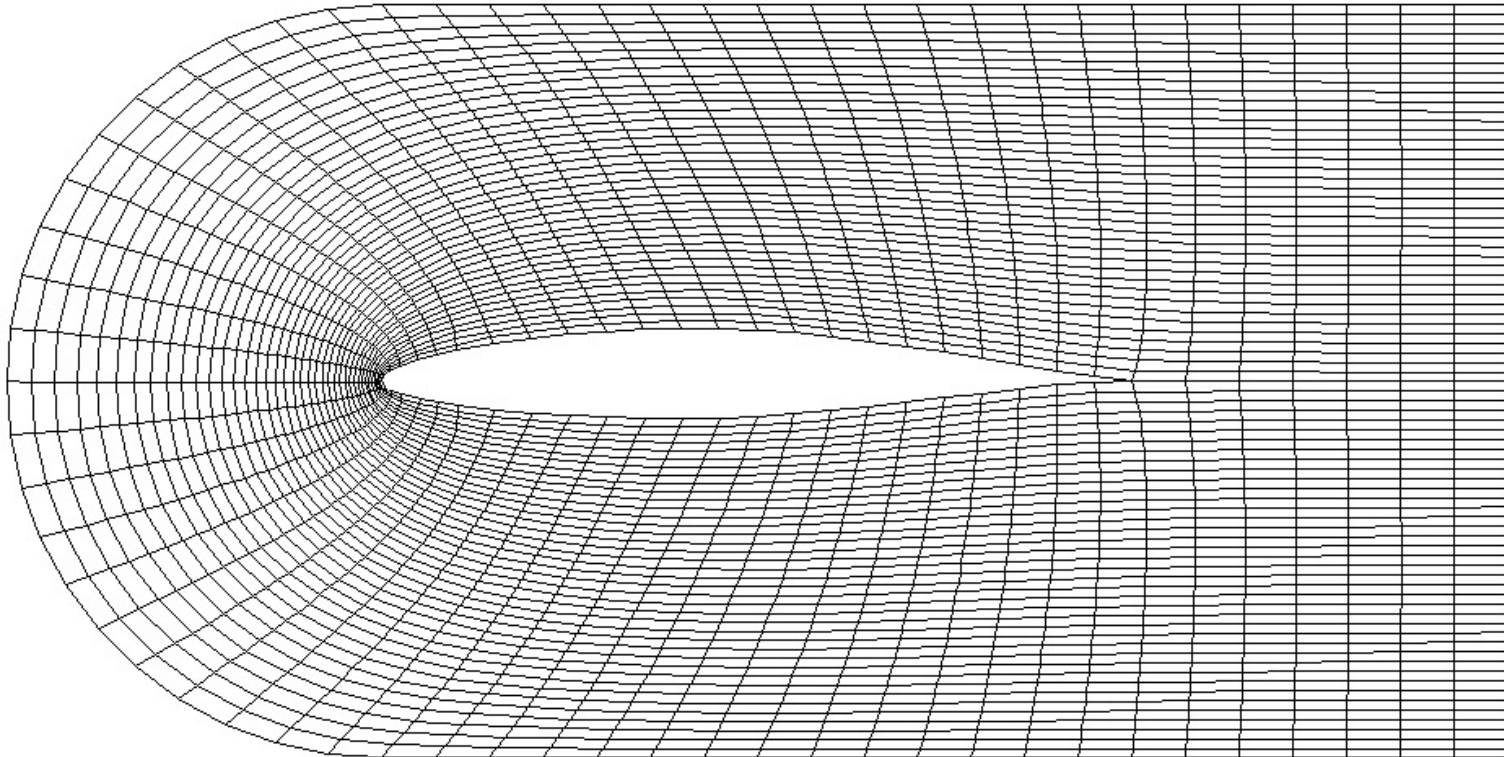


Coupled algebraic eqs. in discrete variables

Variables are only defined at the grid points

Step 1: Define a mesh (points where equations are solved)

**Example of 2-D computational mesh to simulate flow around an airfoil
(more details in FLUENT project)**

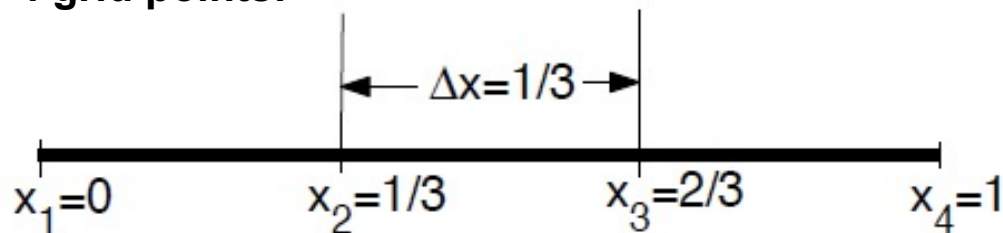


Step 2: Discretize the governing equations

A very simple example: 1-D equation

$$\frac{du}{dx} + u = 0; \quad 0 \leq x \leq 1; \quad u(0) = 1$$

In this case, using a mesh with only 4 grid points:



$$\left(\frac{du}{dx}\right)_i + u_i = 0$$

Discretizing each term of the governing partial differential equation using for example a *finite difference* approximation:

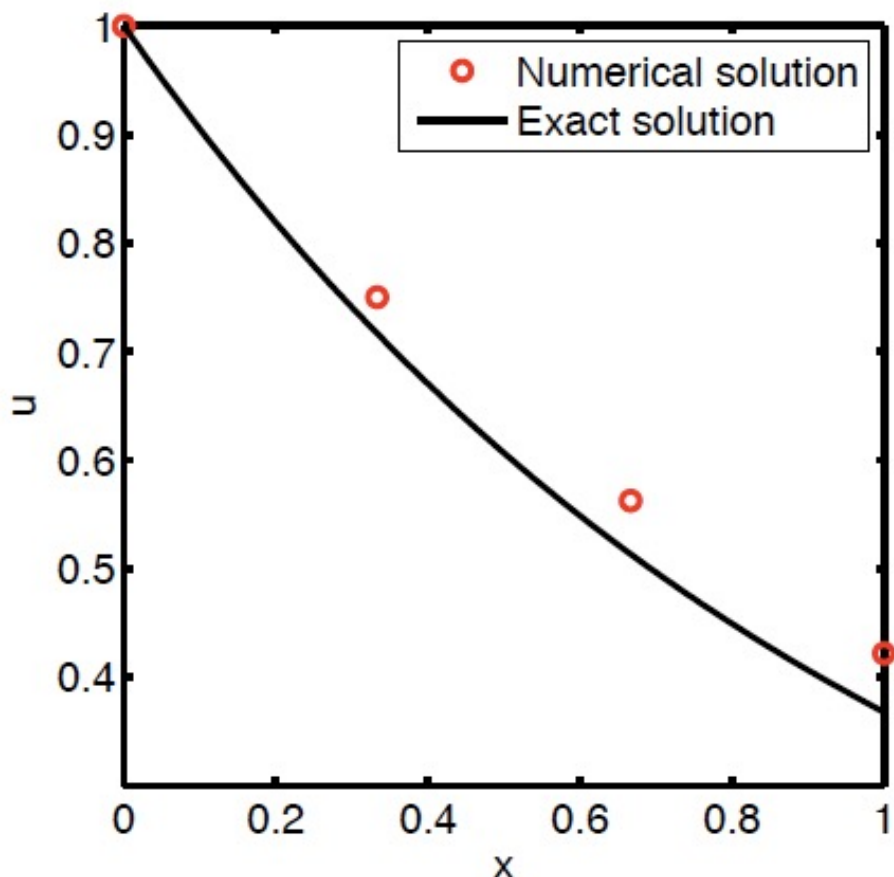
$$\left(\frac{du}{dx}\right)_i = \frac{u_i - u_{i-1}}{\Delta x} + O(\Delta x)$$

In this case, first order approximation

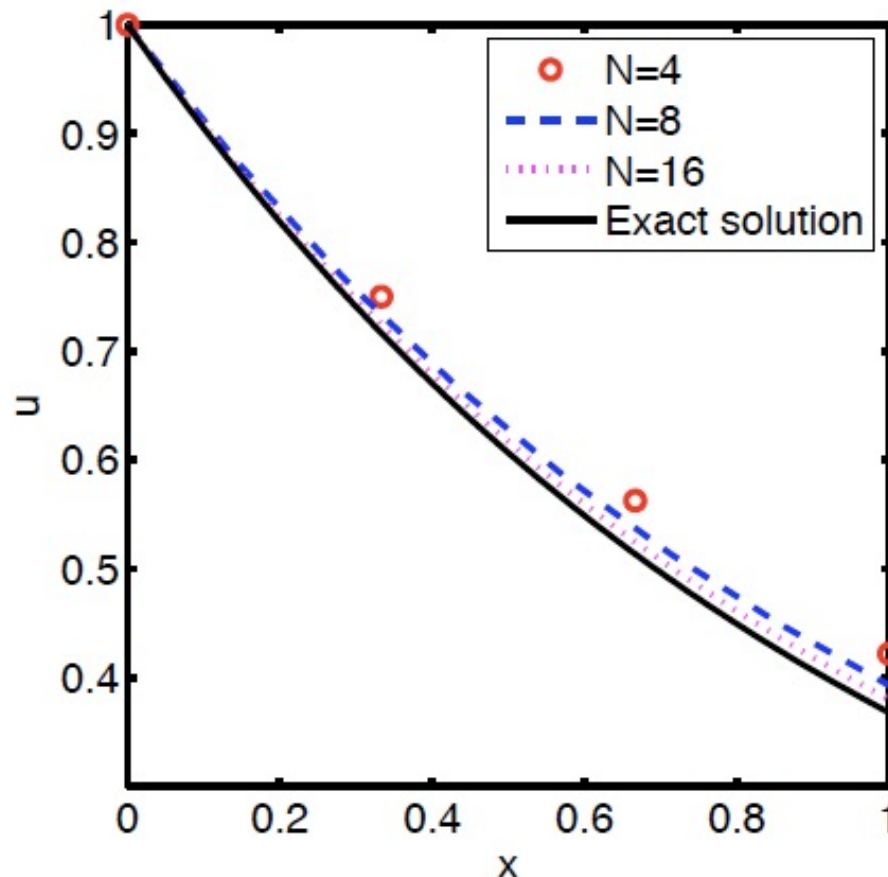
Discretization Error

Spatial and temporal discretization of the equations

NUMERICAL ERROR (due to discretization)



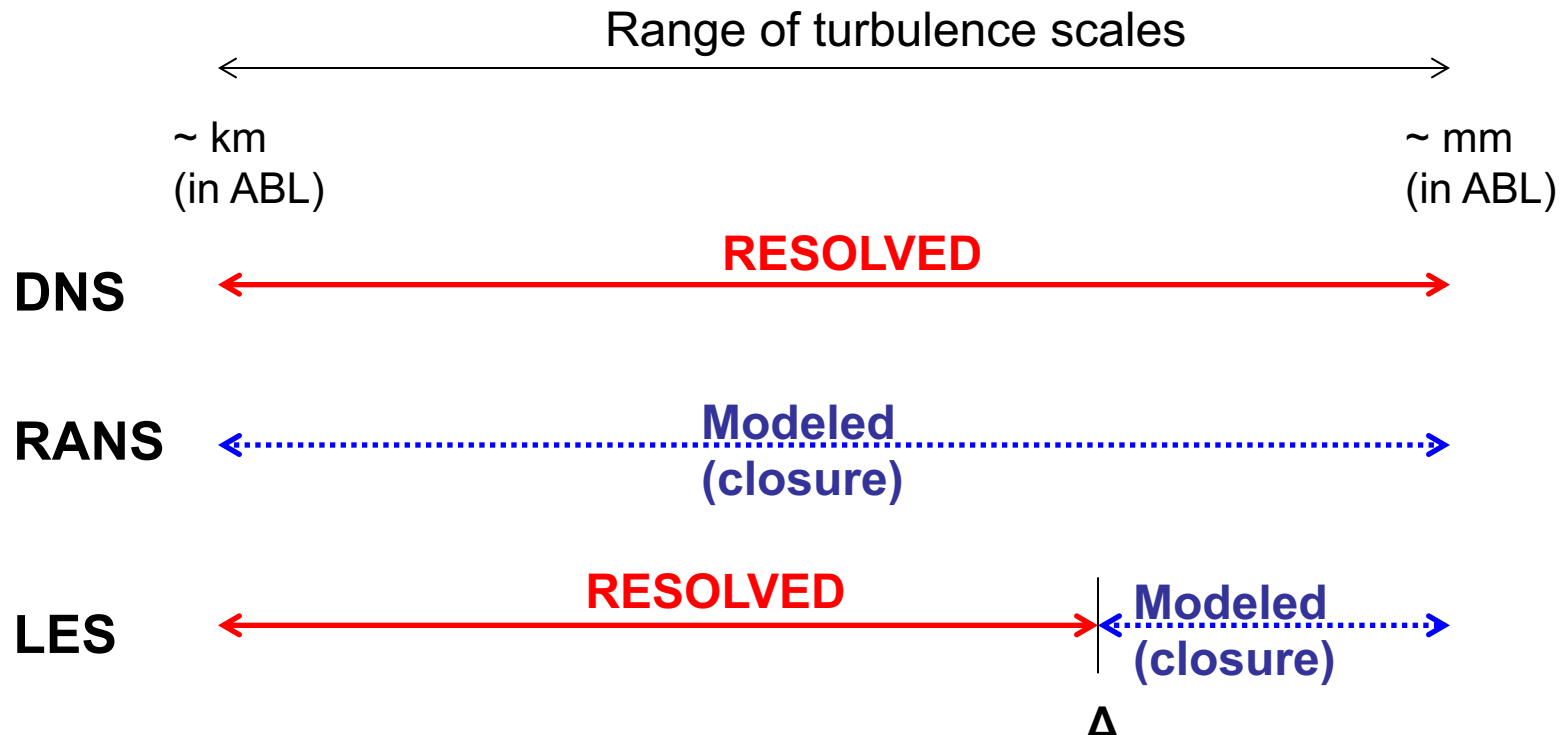
GRID CONVERGENCE



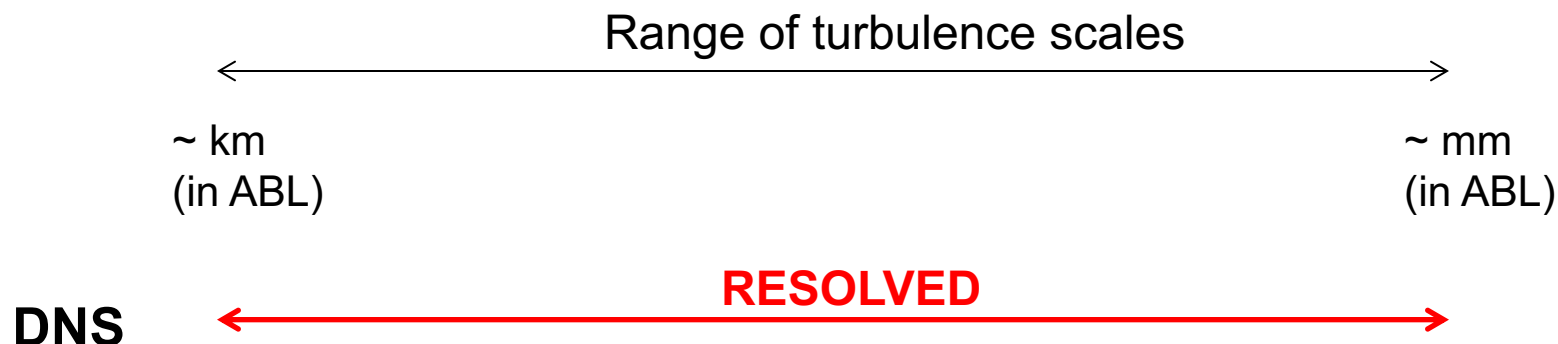
Effect of Grid Refinement (resolution): The finer the grid (smaller Δx), the smaller the discretization (numerical) error.

Approaches for simulation/modeling of turbulent flows

- **DNS** (Direct Numerical Simulation)
- **RANS** (Reynolds-Averaged Navier Stokes)
- **LES** (Large-Eddy Simulation)

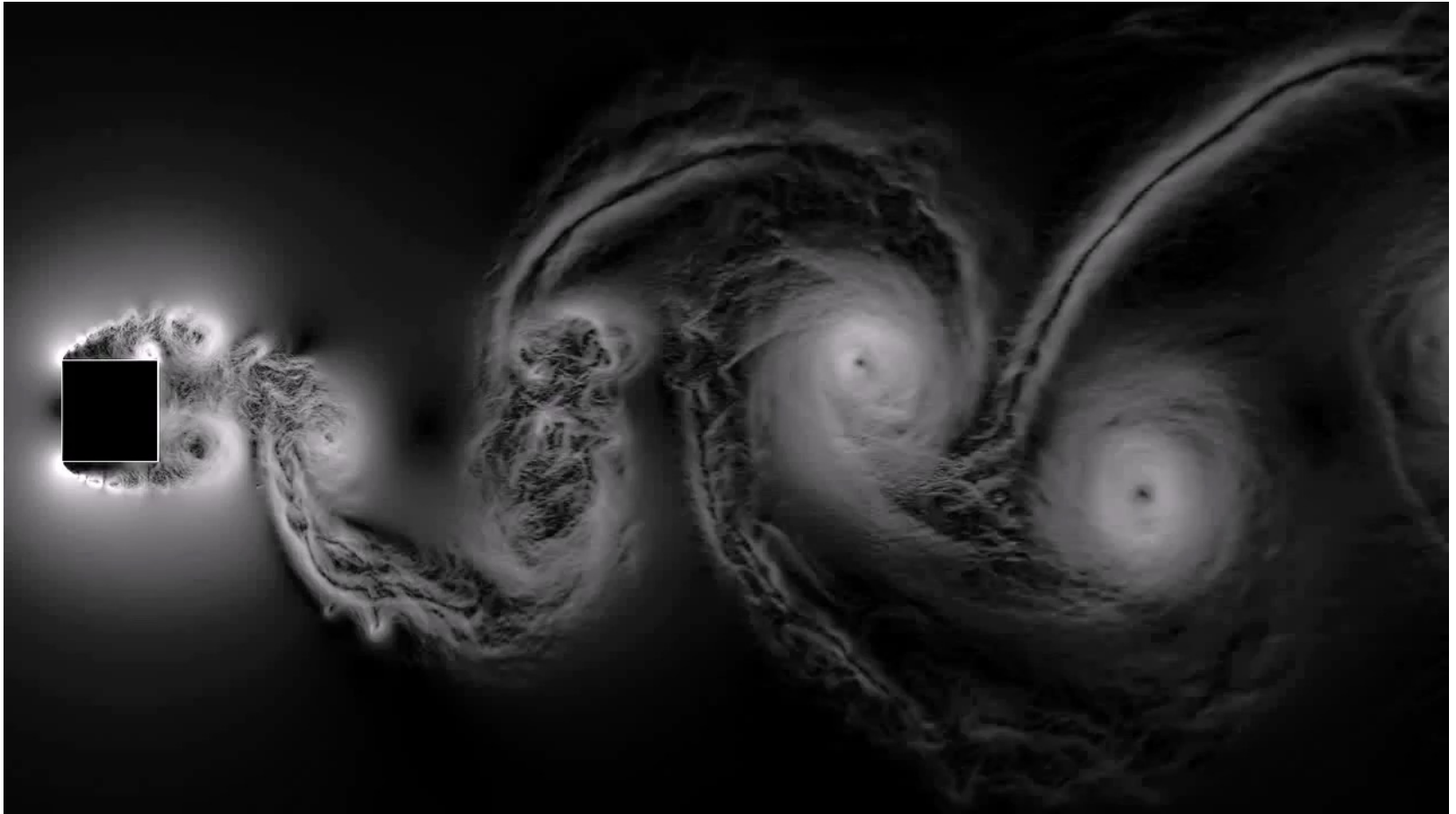


Direct Numerical Simulation (DNS)



- **All the eddy motions are resolved in 3D** (from the integral scale to the Kolmogorov scale). **No need for turbulence model.**
- To achieve that, the governing (advection-diffusion) equations are discretized in space (using resolution $\Delta x, \Delta y, \Delta z$) and time (using resolution Δt) such that:
 - (a) The total **computational domain is large enough to capture the largest eddies** (need to simulate all the eddy sizes).
 - (b) **Resolution Δ is FINE ENOUGH to capture the smallest eddy motions**

Direct Numerical Simulation (DNS): Example



DNS of the turbulent flow around a square cylinder at $Re=22000$

(Number of grid points: 325×10^6)

<https://www.youtube.com/watch?v=c8zKWaxohng>

Direct Numerical Simulation (DNS): Example



DNS of a turbulent hydraulic jump

<https://www.cambridge.org/core/journals/journal-of-fluid-mechanics/article/direct-numerical-simulation-of-a-turbulent-hydraulic-jump-turbulence-statistics-and-air-entrainment/84800BF335F44F8A13EE5C648CDC388D#fndtn-supplementary-materials>

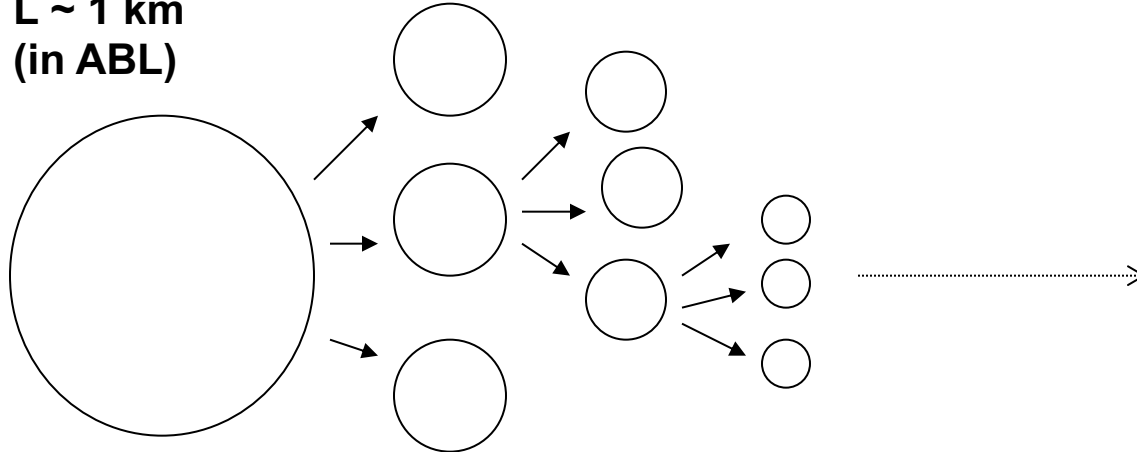
*Integral
scale*

Range of flow scales

*Kolmogorov
scale*

$L \sim 1 \text{ km}$
(in ABL)

$L_K \sim 1 \text{ mm}$
(in ABL)



$$\frac{L_I}{L_K} \sim \text{Re}^{3/4}$$

Energy production

(Inertial effects)

(Energy cascade)

Energy dissipation

(Viscous effects)

- **Full resolution (Direct Numerical Simulation):**

How many grid points
are required for ABL
simulations?

$$\left(\frac{L_I}{L_K} \right)^3 \sim \text{Re}^{9/4} \sim 10^{20}$$

Atmospheric BL: $\text{Re} \sim 10^8 - 10^9$

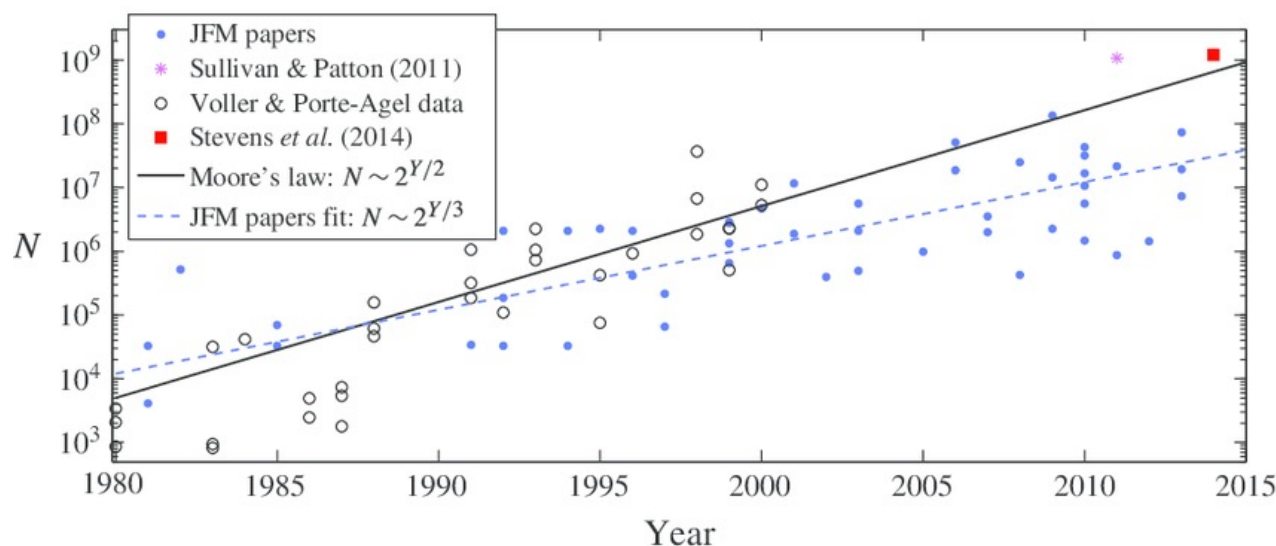
Computational Resources

- Direct Numerical Simulation is **IMPOSSIBLE** for many high-Re flows

- Example: ABL: (needs $\Delta x \sim 1$ mm ; $\Delta t \sim 1$ ms)

→ It requires $Re^{9/4} \sim 10^{20}$ grid points!!

[Using best available supercomputers: maximum number of grid points in DNS $\sim 10^{12}$]

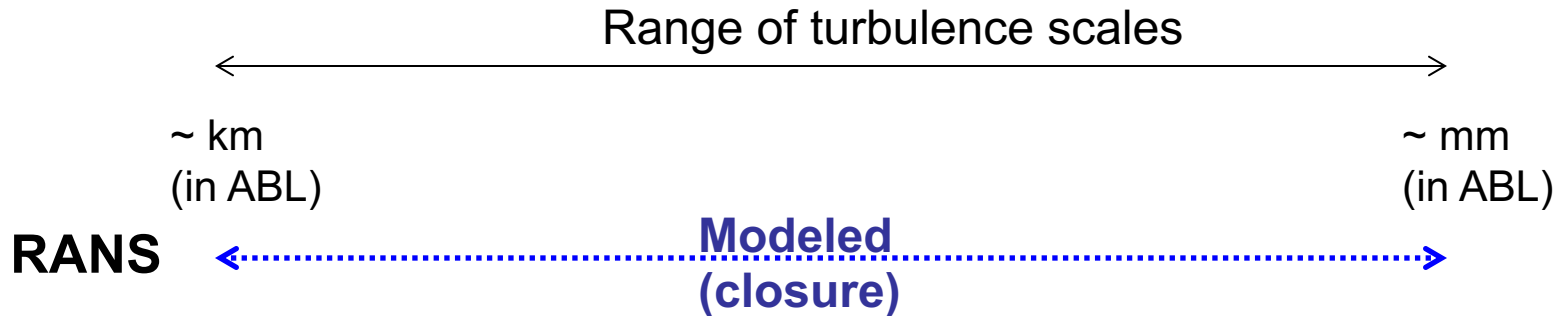


Bou-Zeid et al. (2015)

If Moore's law on computer power [doubling every 18 months] holds:

DNS of atmospheric turbulence over a 10 km x 10 km x 1 km domain may be possible in \sim year **2080**.

Reynolds-Averaged Navier Stokes (RANS) Approach



- **RANS**: It solves 'Reynolds-Averaged Navier Stokes' equations.
 - *When the flow is 'steady' ($\partial \bar{C} / \partial t = 0$) \rightarrow average=time average.*
- **URANS (Unsteady RANS)**: It also solves the RANS equations, but including the time evolution of the averaged quantities (with time derivative).
 - **Question: What type of averaging allows to do that?**

RANS (Reynolds-Averaged Navier Stokes)

Incompressible flow

$$\frac{\partial \bar{u}_i}{\partial x_i} = 0$$

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial}{\partial x_j} (\bar{u}_i \bar{u}_j) = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_i} - \frac{\partial \tau_{ij}}{\partial x_j} + \frac{\partial}{\partial x_j} \left(\nu \left[\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right] \right) + \bar{F}_i$$

**Turbulent
(Reynolds) stress**

$$\tau_{ij} = \overline{u'_i u'_j}$$

$$\frac{\partial \bar{C}}{\partial t} + \frac{\partial}{\partial x_i} (\bar{u}_i \bar{C}) = -\frac{\partial q_i}{\partial x_i} + \frac{\partial}{\partial x_i} \left(D_m \frac{\partial \bar{C}}{\partial x_i} \right) + \bar{Q}$$

Turbulent flux

$$q_i = \overline{u'_i C'}$$

*Effect of turbulent
fluctuations on the average
fields*

CLOSURE PROBLEM:

**Fundamental problem in turbulence
(equations are not closed: more unknowns than equations)**

Reynolds-Averaged Navier Stokes (RANS) Approach

Reynolds
decomposition:

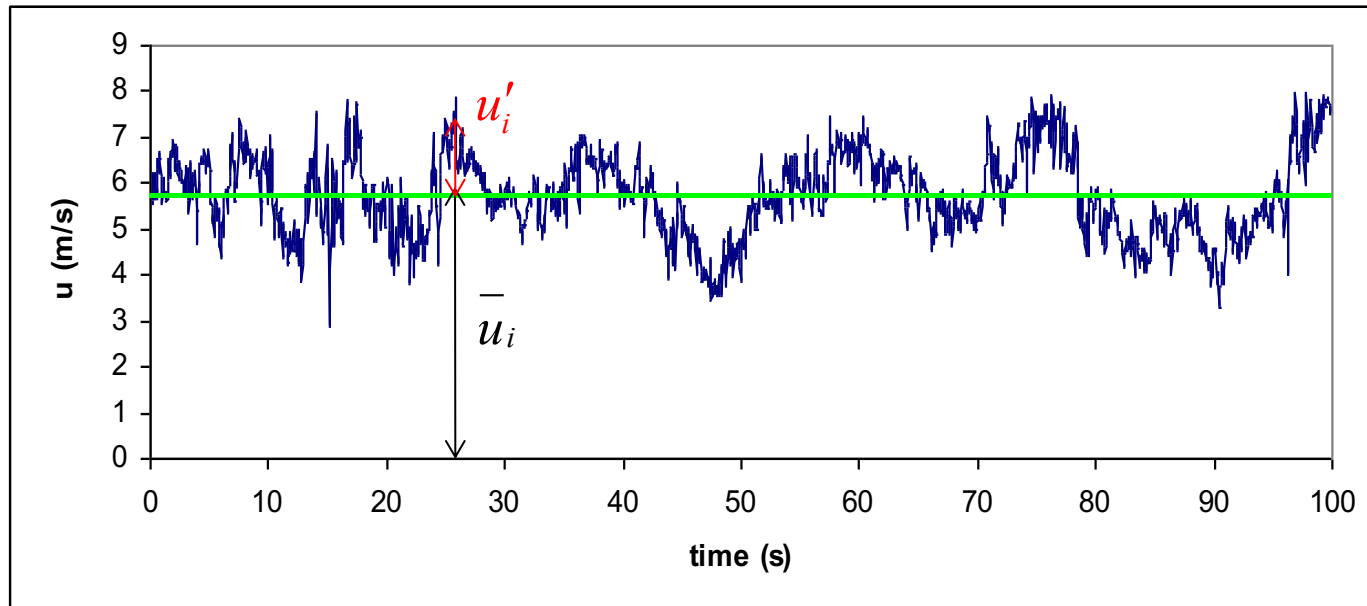
$$\left\{ \begin{array}{l} u_i = \bar{u}_i + u'_i \\ C = \bar{C} + C' \end{array} \right.$$

Types of averages:

- **Time Averaging**
- **Ensemble Averaging**
(over different realizations of the same 'experiment')

Note: for turbulent **stationary** flows,
time averages are equal to ensemble averages

Example of time averaging



Turbulence models: Eddy-viscosity/diffusivity models

NOTE: In laminar flows, energy dissipation and transport of mass, momentum and energy normal to the streamlines is mediated by molecular viscosity/diffusivity

EFFECT of TURBULENCE can be represented as an INCREASED VISCOSITY/DIFFUSIVITY

EDDY-VISCOSITY/DIFFUSIVITY MODEL

$$\overline{u_i' \xi'} = -D_{t,\xi} \frac{\partial \bar{\xi}}{\partial x_i}$$

TURBULENT FLUX: sought to mimic the molecular gradient diffusion process

Note: Although the eddy viscosity hypothesis is NOT CORRECT in detail, it is easy to implement and can provide REASONABLY GOOD RESULTS

CHALLENGE: How to specify the eddy viscosity/diffusivity D_t ?

Turbulence models: Eddy-viscosity/diffusivity models

$$\overline{u'_i \xi'} = -D_{t,\xi} \frac{\partial \bar{\xi}}{\partial x_i}$$


D_t has units of m^2/s

$$\overline{u' w'} = -D_{t,mom} \frac{\partial \bar{u}}{\partial z}$$

Eddy-viscosity model (for momentum);

Eddy viscosity:

$$D_{t,mom} = \nu_t$$

$$\overline{w' \theta'} = -D_{t,\theta} \frac{\partial \bar{\theta}}{\partial z}$$


Eddy-diffusivity model (for scalars like temperature or pollutants)

Analogy with molecular viscosity/diffusivity

- Reynolds stress modeled like viscous stress
- Turbulence more effective than viscosity at mixing:

$$D_{t,mom} \gg \nu$$

$$\left| \begin{array}{l} D_{t,mom} \sim 0.1 - 2 \times 10^3 m^2 s^{-1} \\ \nu \sim 1.5 \times 10^{-5} m^2 s^{-1} \end{array} \right.$$

Reynolds analogy ($Pr_t=1$)



$$D_{t,\theta} \text{ Eddy-diffusivity}$$

$$D_{t,\theta} = \frac{D_{t,mom}}{Pr_t} \approx D_{t,mom}$$

Example:

Using a combination of a length scale (l_{scale}) and a velocity scale (u_{scale})

$$D_{t,mom} \propto u_{scale} \cdot l_{scale}$$

CHALLENGE: How to specify the scales l_{scale} and u_{scale} ?

➤ In channel flow: *See previous lecture*

$$l_{scale} \approx k \cdot z$$

➤ In boundary layers:

$$u_{scale} \approx u_*$$

k = von Karman constant ($k \approx 0.4$)

➤ In complex flows: **CHALLENGING**

Note: More on RANS turbulence models during Fluent Project sessions

A common RANS turbulence model: the k-ε model

(Jones and Launder, 1972)

- It requires solving two additional equations:

(1) One p.d.e. for TKE: k

Note: $[k] = L^2 T^{-2}$

$$\frac{Dk}{Dt} = \underbrace{\frac{\partial}{\partial x_i} \left[\frac{\mu_{\text{eff}}}{\sigma_k} \frac{\partial k}{\partial x_i} \right]}_{\text{diffusion}} + \underbrace{\left[\mu_t \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \frac{2}{3} \rho \delta_{ij} k \right] \frac{\partial U_j}{\partial x_i}}_{\text{production}} - \underbrace{c_D \frac{\rho k^{3/2}}{\ell_m}}_{\text{dissipation}}$$

to obtain velocity scale

velocity scale

$$u_{\text{scale}} \approx \sqrt{2k}$$

(2) One p.d.e. for energy dissipation ε

Note: $[\epsilon] = L^2 T^{-3}$

$$\frac{D\epsilon}{Dt} = \underbrace{\frac{\partial}{\partial x_i} \left[\frac{\mu_{\text{eff}}}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial x_i} \right]}_{\text{diffusion}} + c_{\epsilon,1} \underbrace{\left[\mu_t \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) - \frac{2}{3} \rho \delta_{ij} k \right] \frac{\partial U_j}{\partial x_i}}_{\text{production}} - \underbrace{c_{\epsilon,2} \frac{\rho \epsilon^2}{k}}_{\text{dissipation}}$$

to obtain length scale

length scale

$$l_{\text{scale}} \approx \frac{k^{3/2}}{\epsilon}$$

$$D_{t,mom} \propto u_{\text{scale}} \cdot l_{\text{scale}}$$

$$D_{t,m} \propto \frac{k^2}{\epsilon}$$

$$\text{Also: } \mu_t = C_\mu \frac{k^2}{\epsilon}$$

(Note: Momentum diffusivity = kinematic viscosity: $D_{t,m} = \nu_t = \frac{\mu_t}{\rho}$)

Model coefficients (obtained by data fitting for several flows):

$$C_\mu = 0.09$$

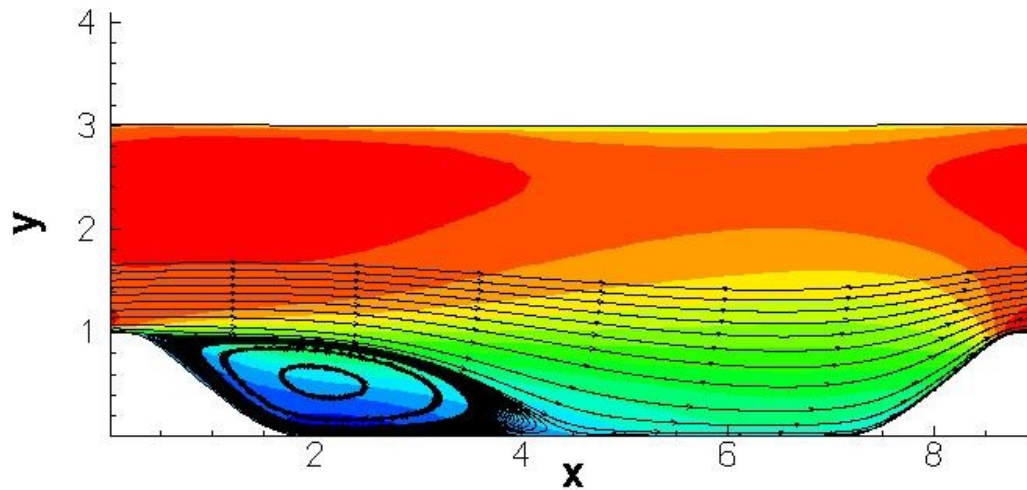
$$\sigma_k = 1.00$$

$$\sigma_\epsilon = 1.30$$

$$C_{1\epsilon} = 1.44$$

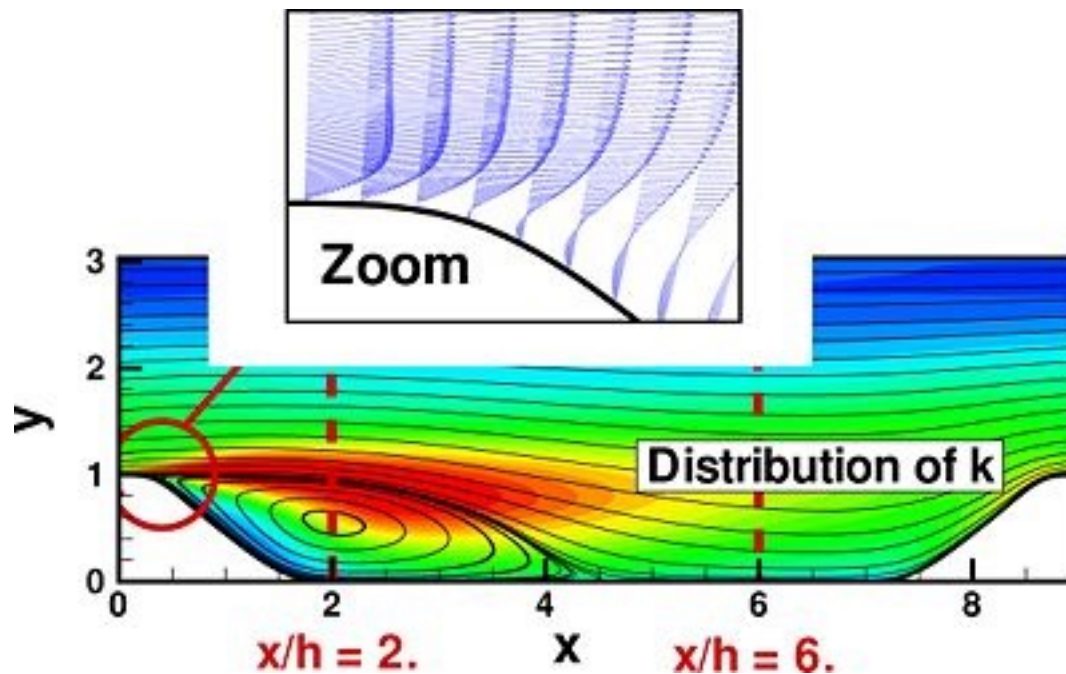
$$C_{2\epsilon} = 1.92$$

RANS example: flow over complex terrain



Mean velocity and streamlines

(Red: high; Blue: low)

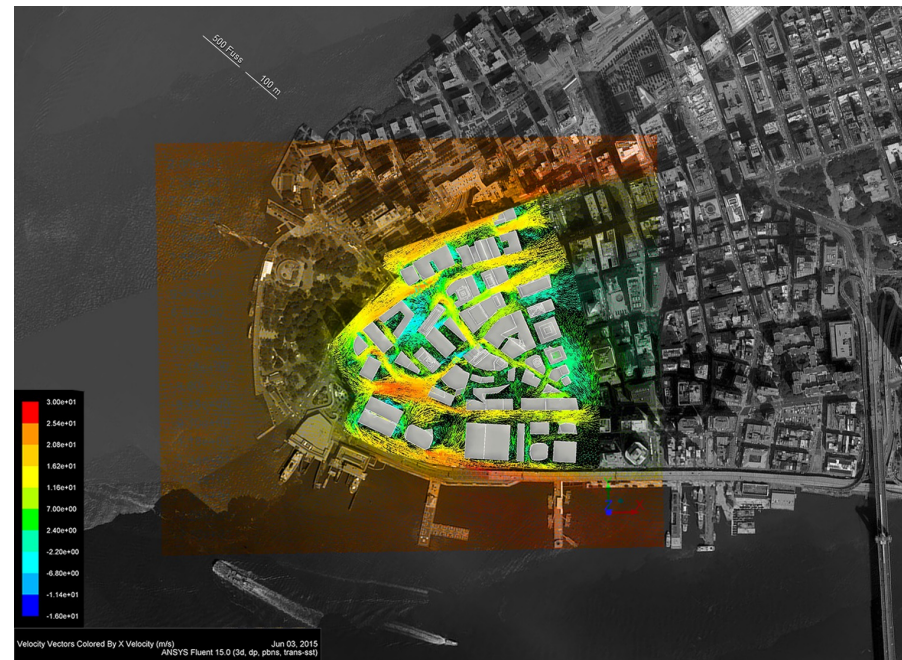
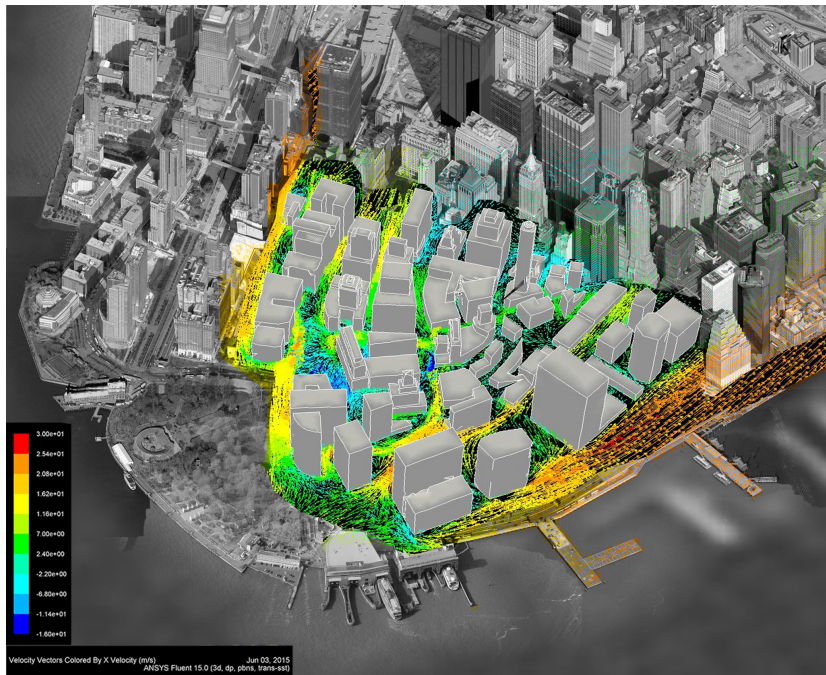


Turbulence Kinetic Energy k (T.K.E.)

(Red: high; Blue: low)

Reynolds-Averaged Navier Stokes (RANS): Example

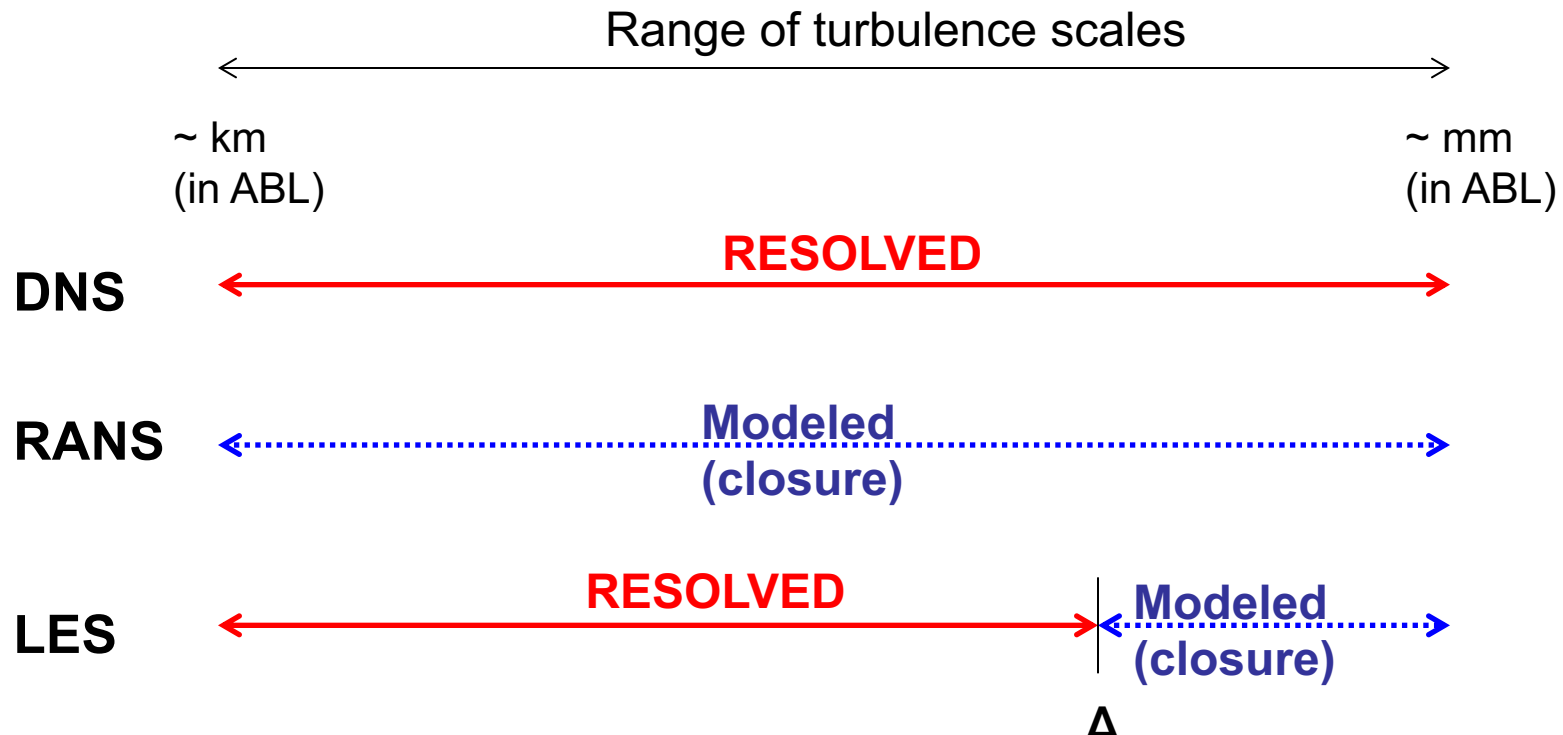
Simulated mean wind velocity vectors (color represents magnitude) in Manhattan (New York)



(Red: high; Blue: low)

Approaches for simulation/modeling of turbulent flows

- **DNS** (Direct Numerical Simulation)
- **RANS** (Reynolds-Averaged Navier Stokes)
- **LES** (Large-Eddy Simulation)



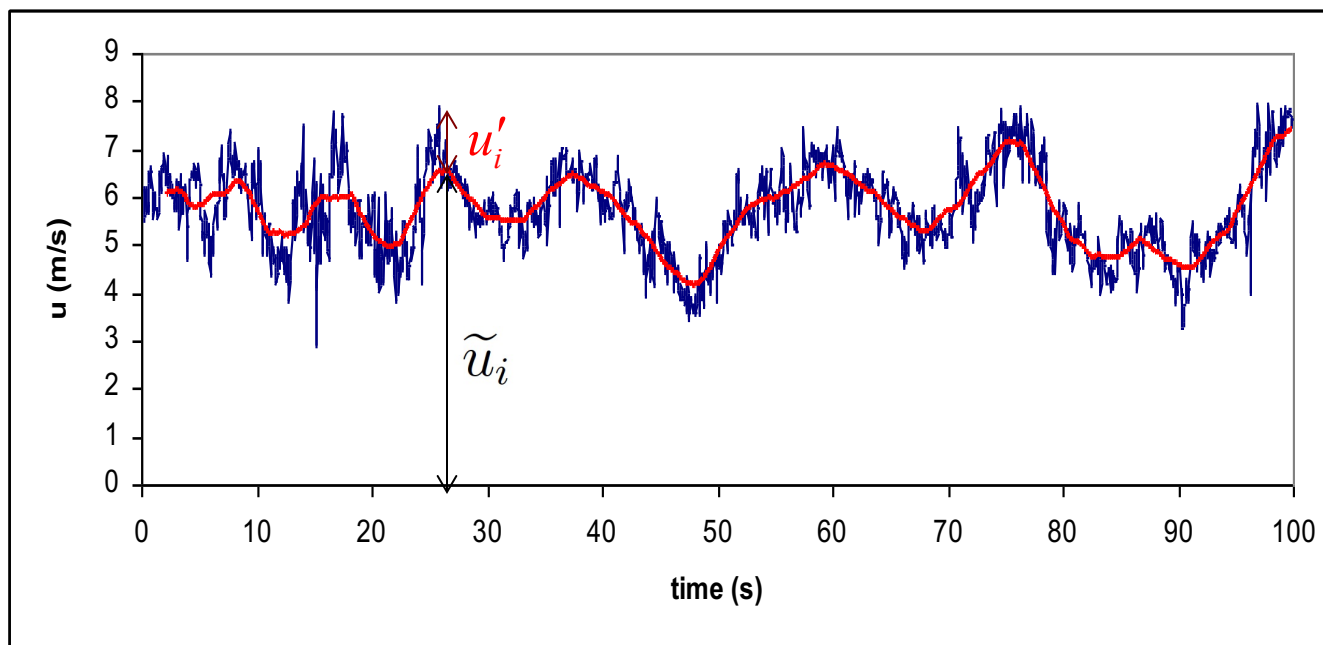
Large-Eddy Simulation (LES)

- DNS (Direct Numerical Simulation)
- LES (Large-Eddy Simulation)

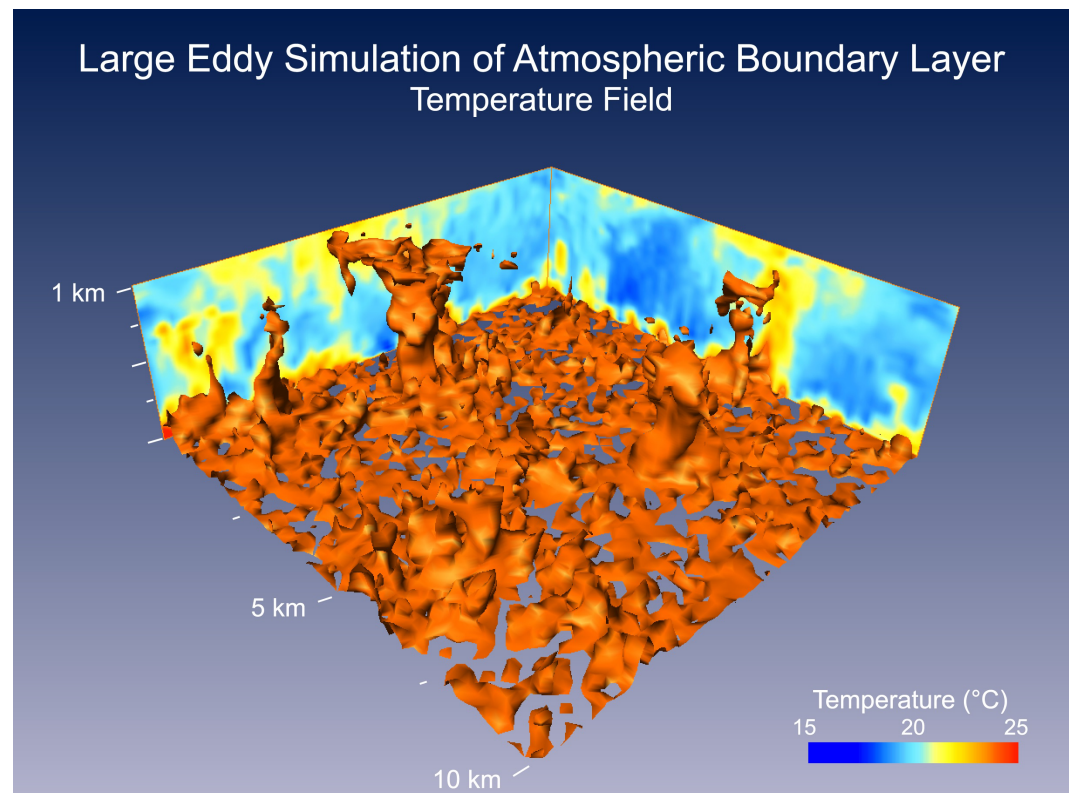
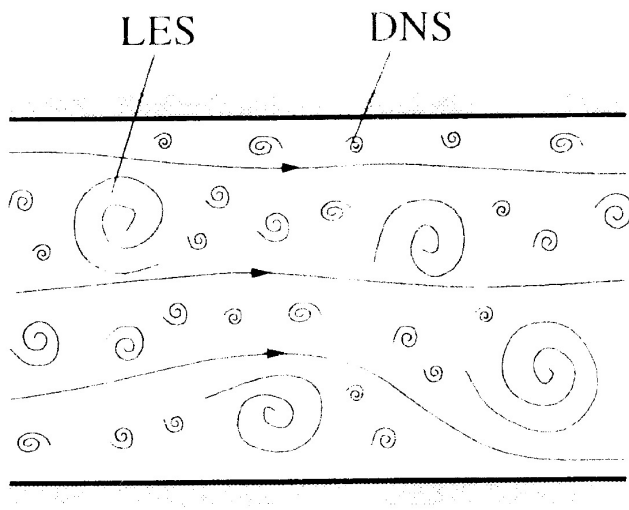
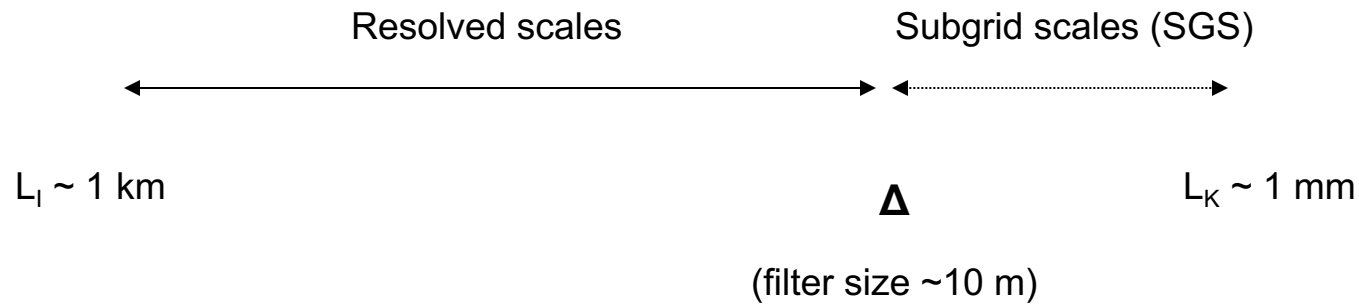
$$u_i = \tilde{u}_i + u_i'$$

Note: In LES, the 'tilde' denotes a filtering operation (a local spatial average in 3D)

$$\tilde{u}_i(x) = \int G(x, x') u_i(x') dx'$$



Large-Eddy Simulation (LES)



LES (filtered) transport equations

$$\frac{\partial \tilde{u}_i}{\partial x_i} = 0$$
$$\frac{\partial \tilde{u}_i}{\partial t} + \frac{\partial}{\partial x_j} (\tilde{u}_i \tilde{u}_j) = -\frac{1}{\rho} \frac{\partial \tilde{p}}{\partial x_i} - \frac{\partial \tau_{ij}}{\partial x_j} + F_i$$

SGS stress
 $\tau_{ij} = \widetilde{u_i u_j} - \tilde{u}_i \tilde{u}_j$

$$\frac{\partial \tilde{C}}{\partial t} + \frac{\partial}{\partial x_i} (\tilde{u}_i \tilde{C}) = -\frac{\partial q_i^{sgs}}{\partial x_i} + \tilde{Q}$$

(Derivation in next slide)

SGS flux
 $q_i^{sgs} = \widetilde{u_i C} - \tilde{u}_i \tilde{C}$

Effect of sub-grid scales on the resolved (filtered) scales

EXAMPLES of LES: All movies shown of ABL simulations in next lectures.

LES (filtered) scalar transport equation: derivation

Starting with advection-diffusion equation:

$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x_i} (u_i C) = \frac{\partial}{\partial x_i} \left[D_m \frac{\partial C}{\partial x_i} \right] + Q$$

[Note: Q is a source/sink term]

Applying LES filtering operation (of size Δ):

$$\frac{\partial \tilde{C}}{\partial t} + \frac{\partial}{\partial x_i} (\widetilde{u_i C}) = \frac{\partial}{\partial x_i} \left[D_m \frac{\partial \tilde{C}}{\partial x_i} \right] + \tilde{Q}$$

Adding and subtracting the same term:

$$\frac{\partial \tilde{C}}{\partial t} + \frac{\partial}{\partial x_i} (\widetilde{u_i C} - \tilde{u}_i \tilde{C} + \tilde{u}_i \tilde{C}) = \frac{\partial}{\partial x_i} \left[D_m \frac{\partial \tilde{C}}{\partial x_i} \right] + \tilde{Q}$$

Rearranging:

$$\frac{\partial \tilde{C}}{\partial t} + \frac{\partial}{\partial x_i} (\tilde{u}_i \tilde{C}) = - \frac{\partial}{\partial x_i} (\widetilde{u_i C} - \tilde{u}_i \tilde{C}) + \frac{\partial}{\partial x_i} \left[D_m \frac{\partial \tilde{C}}{\partial x_i} \right] + \tilde{Q}$$

$$q_i^{sgs} = \widetilde{u_i C} - \tilde{u}_i \tilde{C}$$

SUBGRID-SCALE (SGS) FLUX

- Represents the effect of subgrid-scales (eddies smaller than Δ)
- Closure Problem
- Need a model (**SGS Model**)
- Q : *What could be a reasonable model?**
- Note:

$$q_i^{sgs} < \overline{u'_i C'}$$

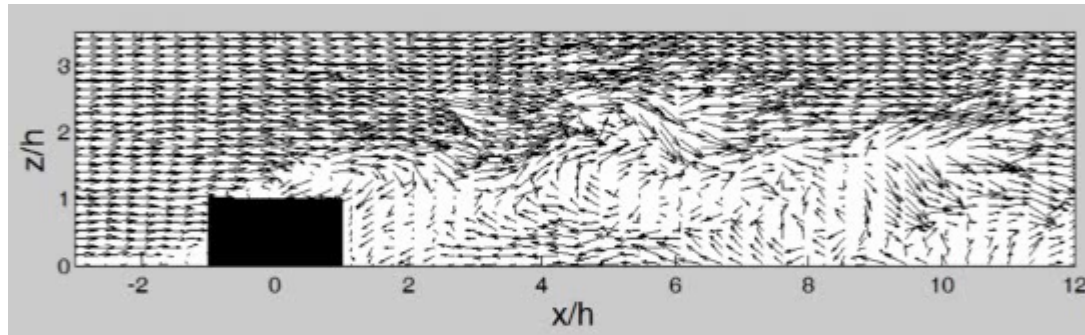
Represents the effect of **only subgrid scale (SGS) eddies** (smaller than Δ)

Represents the effect of **ALL turbulent eddies**

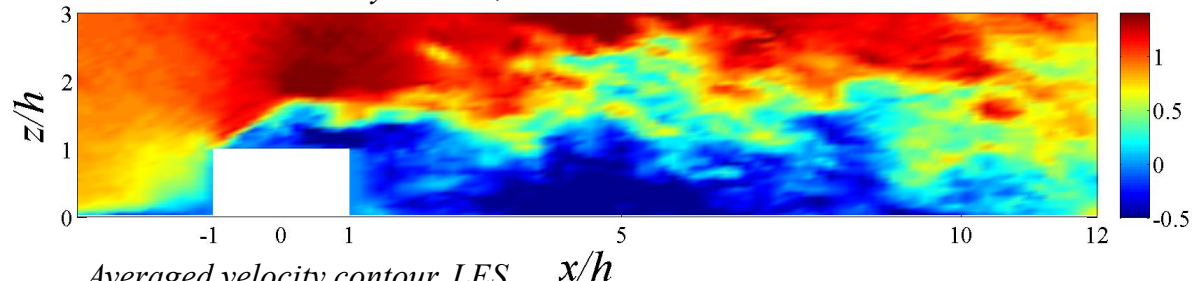
* Standard SGS model:
Eddy-diffusion model

$$q_i^{sgs} = -D_{sgs} \frac{\partial \tilde{C}}{\partial x_i}$$

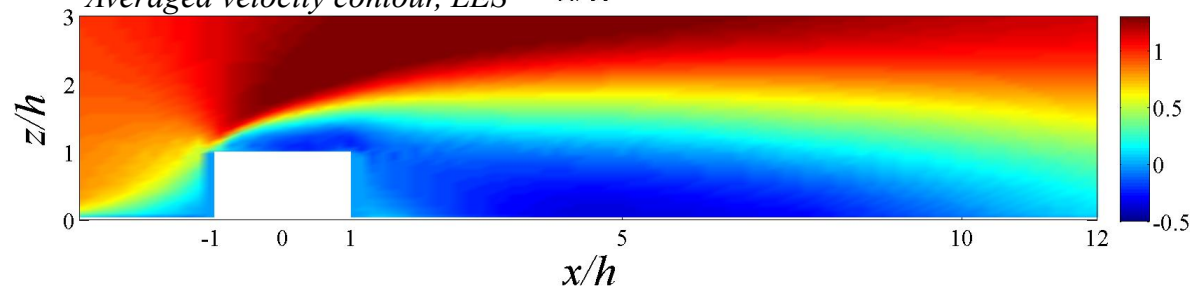
LES example: Flow around a building



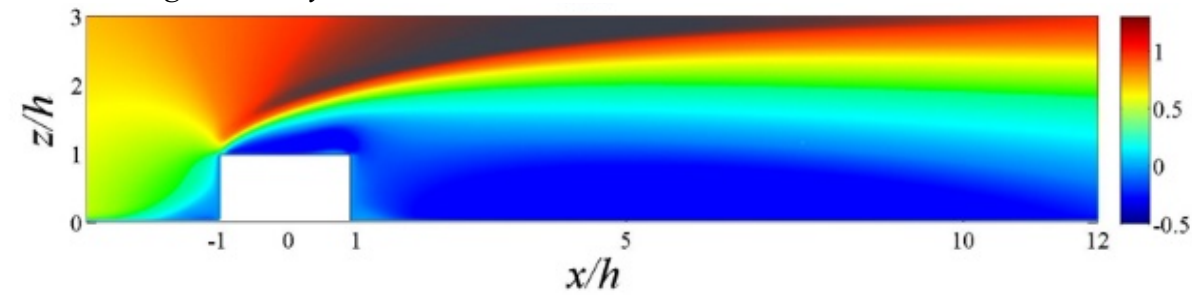
Instantaneous velocity contour, LES



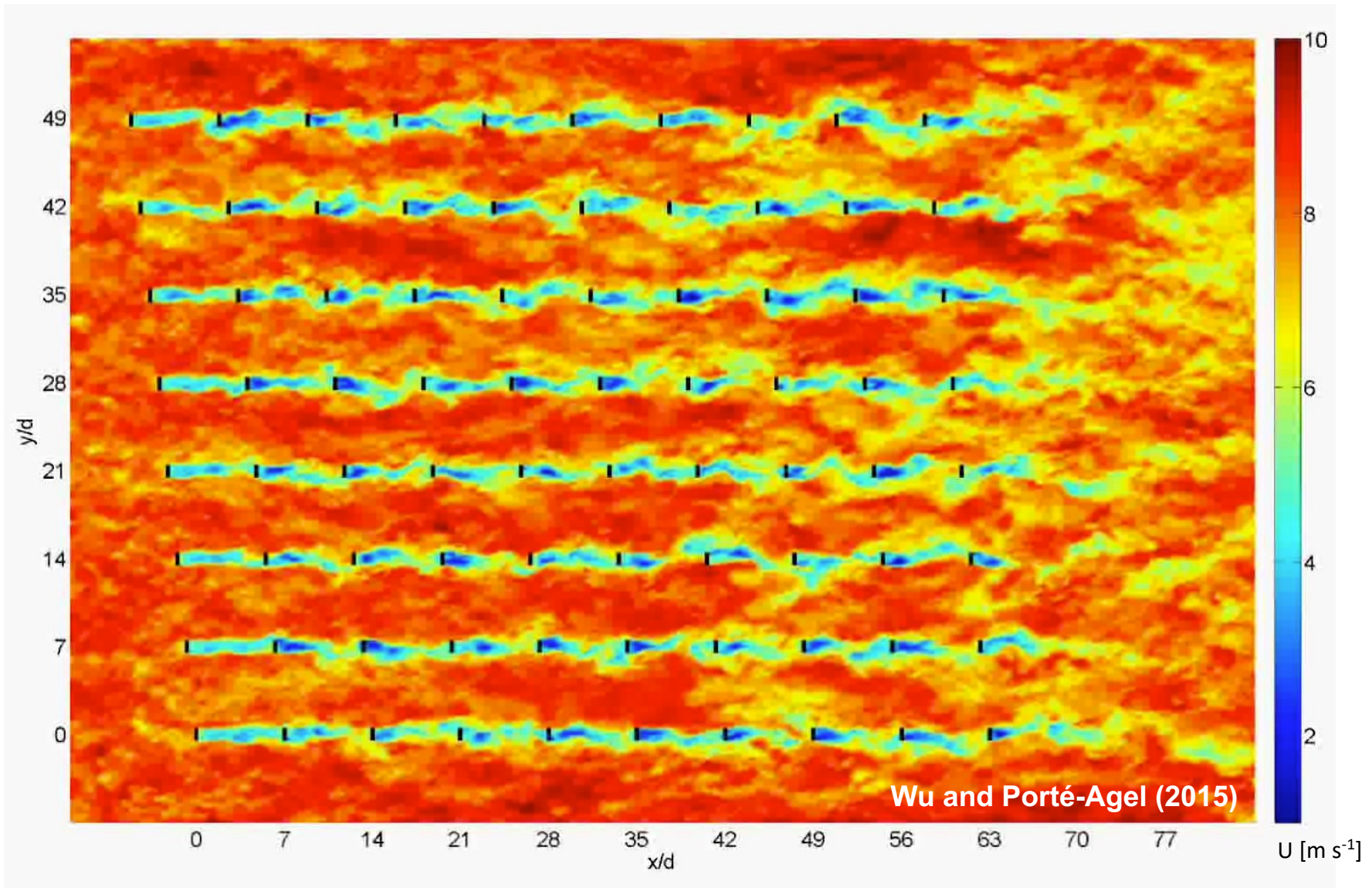
Averaged velocity contour, LES



Averaged velocity contour, RANS

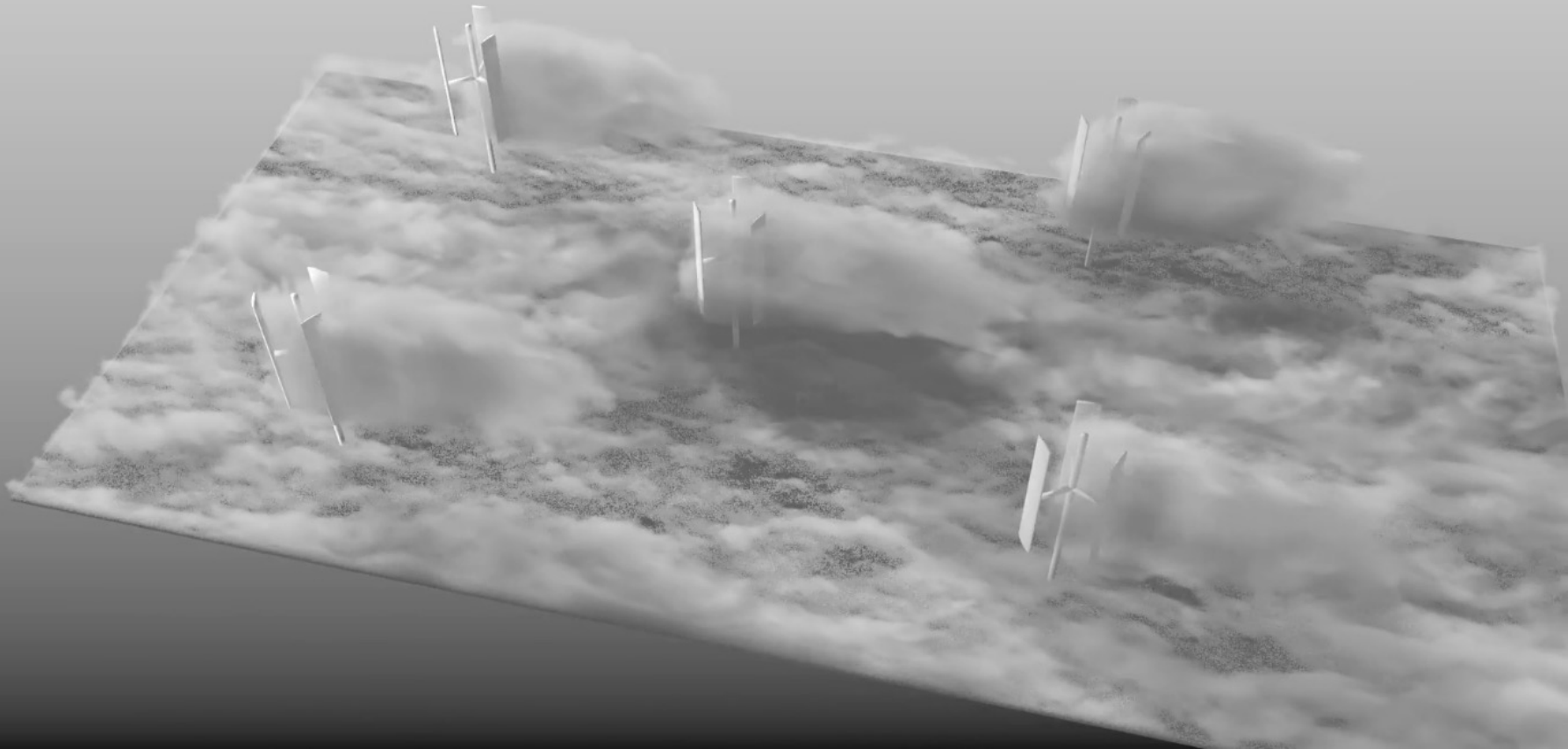


LES of flow inside a wind farm



Simulation with the highly-parallelized WiRE LES code using 1000 CPU-hours (100 processors, 10 hours)

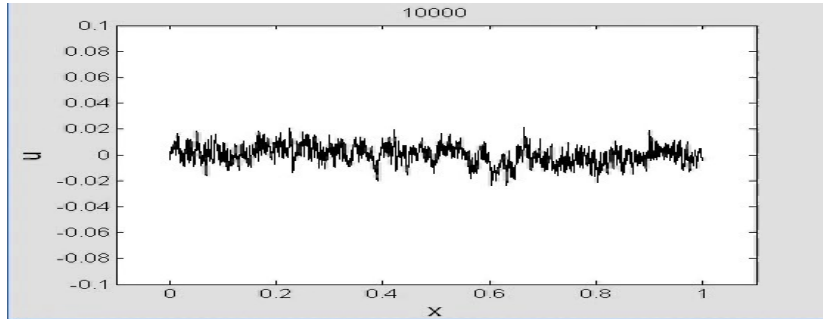
LES example: Flow inside a wind farm or vertical-axis wind turbines



<https://youtu.be/ferySLHLocw>

1-D Burgers Equation (a simple example – similar to turbulence)

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = \nu \frac{\partial^2 u}{\partial x^2} + F$$



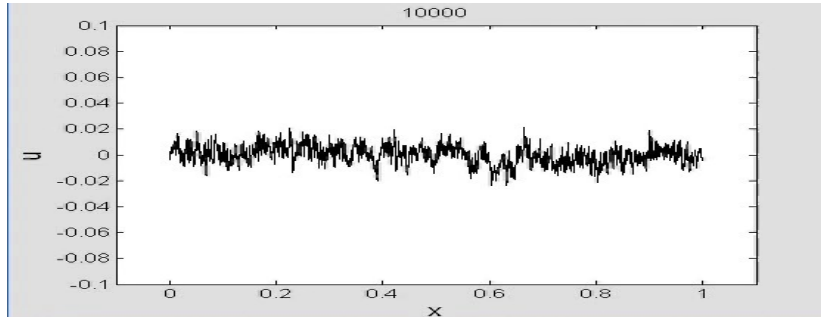
Direct Numerical Simulation - 1D Burgers equation

All scales are resolved

$L_I/L_k=8192$

1-D Burgers Equation (a simple example – similar to turbulence)

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} = \nu \frac{\partial^2 u}{\partial x^2} + F$$

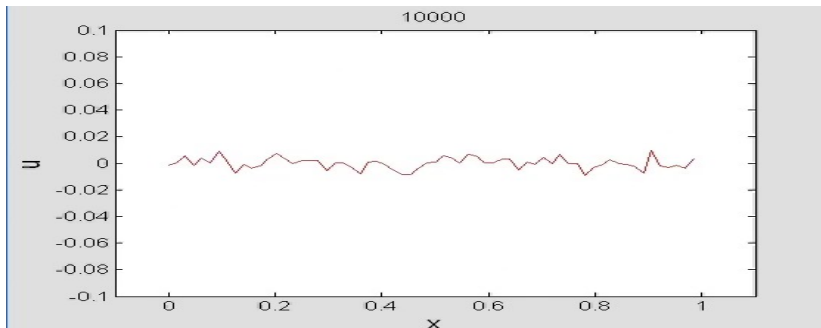


Direct Numerical Simulation - 1D Burgers equation

All scales are resolved

$$L_I/L_k=8192$$

Coarser resolution without subgrid model: Wrong statistics



Coarse resolution - 1D Burgers equation

NO subgrid model

$$L_I/L_k=64$$

Question: Why without SGS model there is an unrealistic accumulation of energy?