

Water Resources Engineering and Management

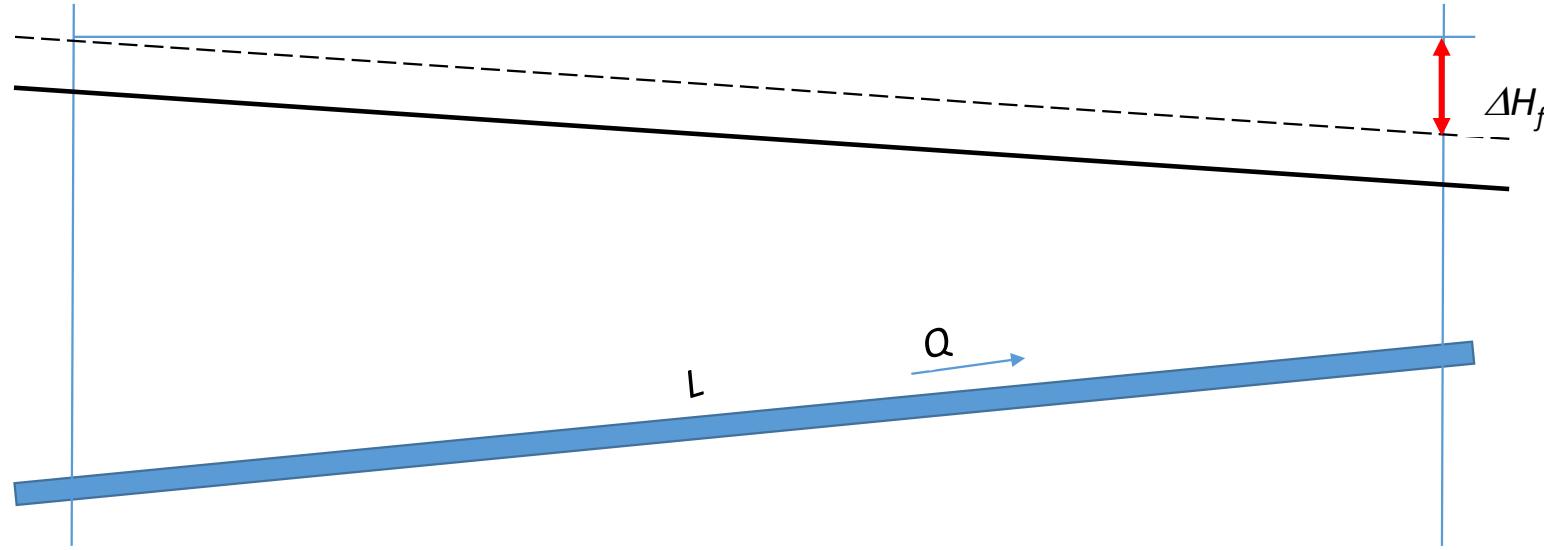
Exercises Lecture 3: pipe hydraulics,
energy and hydraulic grade lines, pipe
loops, pumping systems



03/03/2025

Exercise 1. Friction losses in rectilinear pipe

A 20m-long rectilinear pipe is used to convey a flowrate of $Q=5$ L/s.
The pipe diameter is 6.5 cm and the wall roughness is $k_s=0.26$ mm.



QUESTIONS

- The energy loss, ΔH_f , at the end of the pipe
- The energy loss, ΔH_{SM} , in the hypothesis of hydraulically smooth pipe

Exercise 1. Friction losses in rectilinear pipe - SOLUTION

$$\frac{1}{\sqrt{\lambda}} = -2 \log_{10} \left(\frac{k_s}{3.71 D} + \frac{2.51}{\text{Re} \sqrt{\lambda}} \right)$$

Colebrook-White equation
To be solved numerically!!

Alternatively, iterative method:

1) Consider “rough turbulent” regime $\rightarrow \lambda_1 = \left(2 \log_{10} \left(\frac{3.71 D}{k_s} \right) \right)^{-2}$
Hyp) $\text{Re} \rightarrow \infty$

2) Use λ_1 to use Colebrook-White equation $\rightarrow \frac{1}{\sqrt{\lambda_2}} = -2 \log_{10} \left(\frac{k_s}{3.71 D} + \frac{2.51}{\text{Re} \sqrt{\lambda_1}} \right)$

$$\text{Re} = \frac{U D}{\nu} \quad \text{Reynolds number}$$

3) Repeat the previous step until convergence ($\left| \frac{\lambda_{i+1} - \lambda_i}{\lambda_{i+1}} \right| \leq 0.1\%$, usually 2-3 iterations) $\rightarrow \frac{1}{\sqrt{\lambda_{i+1}}} = -2 \log_{10} \left(\frac{k_s}{3.71 D} + \frac{2.51}{\text{Re} \sqrt{\lambda_i}} \right)$

$$\lambda_1 = 0.0283931$$

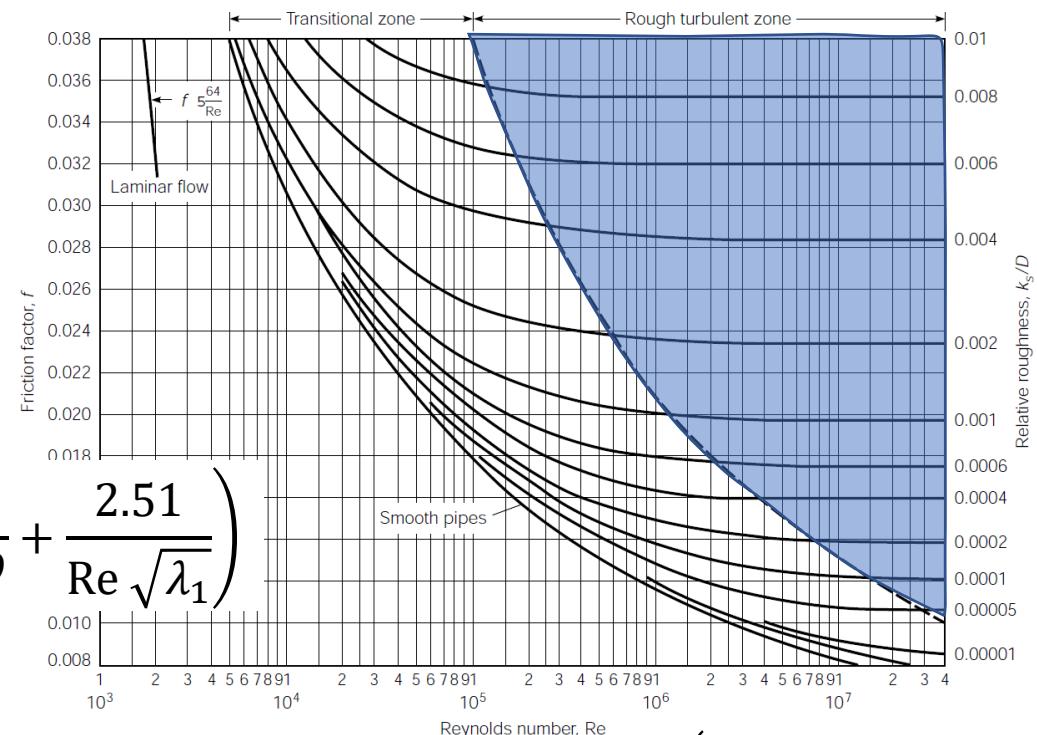
$$\lambda_2 = 0.0295225 \quad \Delta\lambda_{12} = 3.826\%$$

$$\lambda_3 = 0.0295014 \quad \Delta\lambda_{23} = -0.0715\%$$

$$\lambda_4 = 0.0295018 \quad \Delta\lambda_{34} = 0.0014\%$$

Iterative solution
 $\rightarrow \lambda = \lambda_4 = 0.0295018$

Numerical solution
 $\lambda_{\text{NUM}} = 0.029501798$



$$\Delta H_f = \frac{\lambda}{D} \frac{U^2}{2g} L = \frac{\lambda}{D} \frac{16 Q^2}{\pi^2 D^4 2g} L = \frac{8 \lambda}{\pi^2 g} \frac{Q^2}{D^5} L = 1.05 \text{ m}$$

Exercise 1. Friction losses in rectilinear pipe - SOLUTION

In the case of hydraulically smooth pipe, $k_s = 0$

$$\frac{1}{\sqrt{\lambda}} = -2 \log_{10} \left(\frac{2.51}{\text{Re} \sqrt{\lambda}} \right)$$

Colebrook-White equation for smooth pipe

Similar iterative procedure, starting from the same λ_1 (rough pipe, real k_s)

$$\lambda_1 = \left(2 \log_{10} \left(\frac{3.71 D}{k_s} \right) \right)^{-2}$$

$$\lambda_1 = 0.0283931$$

$$\lambda_2 = 0.0171511$$

$$\lambda_3 = 0.0181785 \quad \Delta\lambda_{23} = 5.65\%$$

$$\lambda_4 = 0.0180553 \quad \Delta\lambda_{34} = -0.682\%$$

$$\lambda_5 = 0.0180696 \quad \Delta\lambda_{45} = 0.0791\%$$

Iterative solution

$$\rightarrow \lambda_{SM} = \lambda_5 = 0.0180696$$

Numerical solution

$$\lambda_{SM, \text{NUM}} = 0.0180681$$

$$\Delta H_{SM} = \frac{\lambda_{SM}}{D} \frac{U^2}{2g} L = \frac{\lambda_{SM}}{D} \frac{16 Q^2}{\pi^2 D^4 2g} L = \frac{8 \lambda_{SM}}{\pi^2 g} \frac{Q^2}{D^5} L = 0.64 \text{ m}$$

Exercise 2. Hydraulic diagnostic (verification) problem

We consider a conduct constituted by two pipes and with diameter-dependent Darcy coefficients β_1 and β_2 .
 The pipe system delivers water from a tank with constant water elevation.

The geometry of the system is defined, as shown.

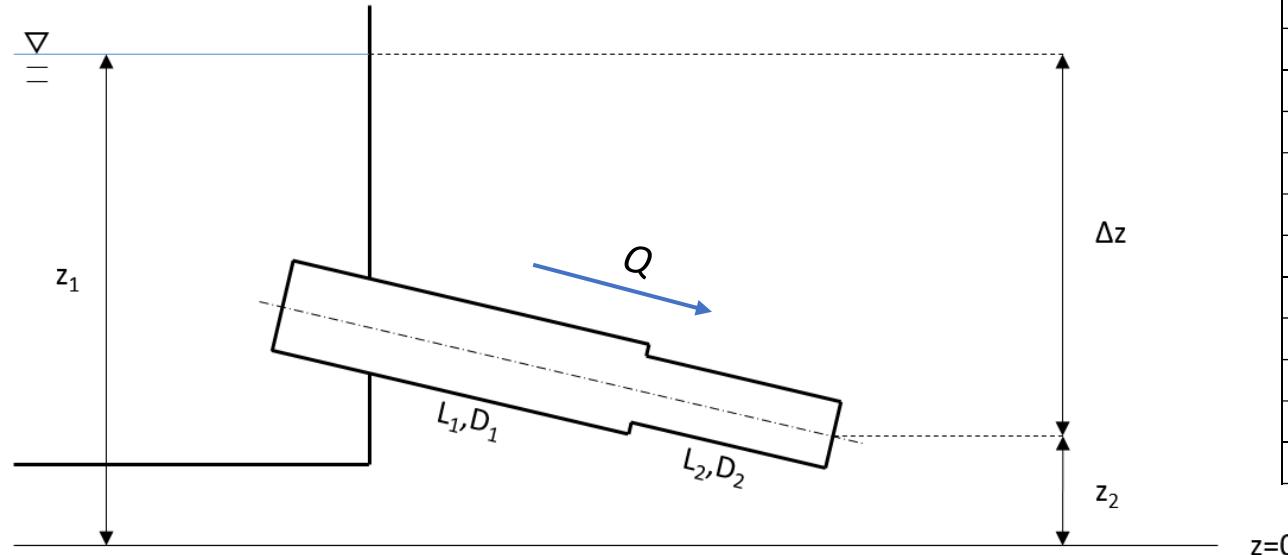
The energy loss coefficient ξ at the restriction is given in Table 1.

Table 1

D_2/D_1	ξ
0.01	0.5
0.1	0.477
0.2	0.452
0.3	0.425
0.4	0.396
0.5	0.358
0.6	0.31
0.7	0.243
0.8	0.166
0.9	0.086
1	0

DATA

- Diameter of pipe 1 $\rightarrow D_1 = 470$ mm
- Diameter of pipe 2 $\rightarrow D_2 = 300$ mm
- Length of pipe 1 $\rightarrow L_1 = 45$ m
- Length of pipe 2 $\rightarrow L_2 = 25$ m
- Water level in the tank $\rightarrow z_1 = 10$ m
- Elevation at the end of pipe 2 $\rightarrow z_2 = 5$ m



Darcy's law for β coefficient

$$\beta = 2 \left(0.00164 + \frac{0.000042}{D} \right)$$

Energy loss with β coefficient

$$\Delta H_i = \beta_i \frac{Q_i^2}{D_i^5} L_i$$

QUESTIONS

- The flow rate Q
- Draw the hydraulic grade (piezometric) line and the energy grade line

Exercise 2. Hydraulic diagnostic problem - SOLUTION

Determination of the minor loss coefficient at the restriction

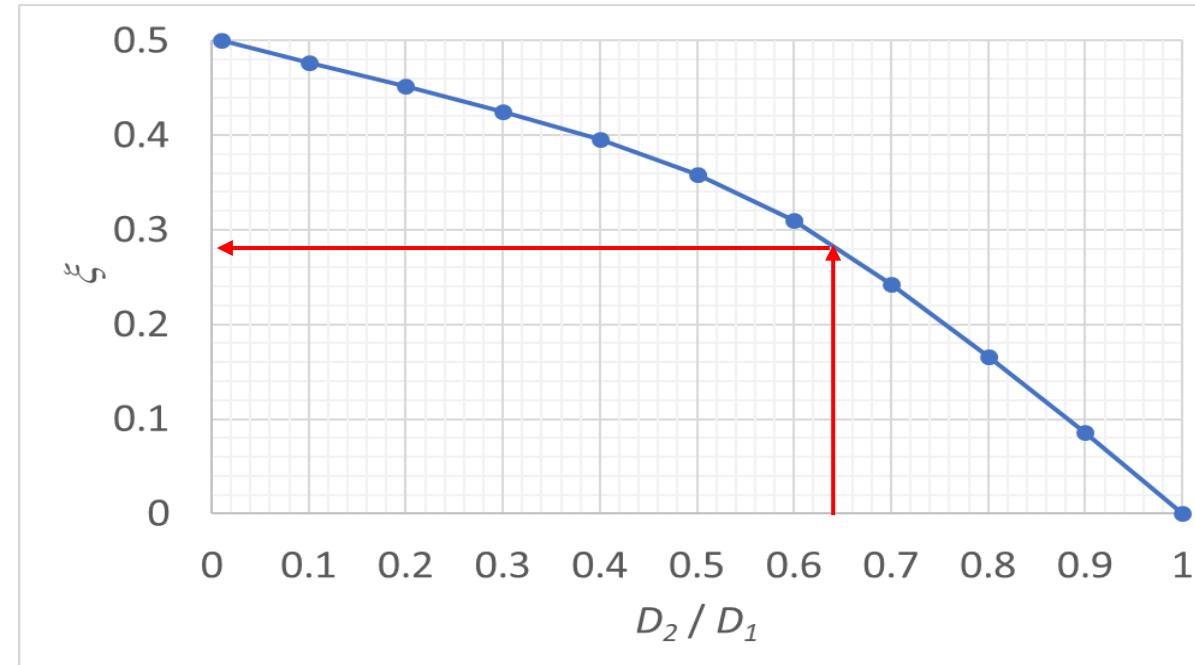
$$D_2/D_1 = 0.6383$$

By graphical evaluation

$$D_2/D_1 \approx 0.64$$

Table 1

D_2/D_1	ξ
0.01	0.5
0.1	0.477
0.2	0.452
0.3	0.425
0.4	0.396
0.5	0.358
0.6	0.31
0.7	0.243
0.8	0.166
0.9	0.086
1	0



By linear interpolation:

$$\xi = \xi \left(\inf \left(\frac{D_2}{D_1} \right) \right) + \frac{\xi \left(\sup \left(\frac{D_2}{D_1} \right) \right) - \xi \left(\inf \left(\frac{D_2}{D_1} \right) \right)}{\sup \left(\frac{D_2}{D_1} \right) - \inf \left(\frac{D_2}{D_1} \right)} \left(\frac{D_2}{D_1} - \inf \left(\frac{D_2}{D_1} \right) \right) = \frac{0.243 - 0.310}{0.7 - 0.6} (0.6383 - 0.6) + 0.31 = 0.284$$

Exercise 2. Hydraulic diagnostic problem - SOLUTION

$$z_A + \frac{p_A}{\gamma} + \frac{U_A^2}{2g} = z_B + \frac{p_B}{\gamma} + \frac{U_B^2}{2g} + \Delta H \quad \text{ENERGY BALANCE}$$

A: water surface in the tank $\rightarrow p_A = 0$

B: outlet of pipe 2 $\rightarrow p_B = 0$

A: water surface in the tank $\rightarrow z_A = z_1 ; p_A = 0 ; Q_A = 0$

B: outlet of pipe 2 $\rightarrow z_B = z_2 ; p_B = 0 ; Q_B = Q$

We express all the terms as a function of the flowing discharge, Q

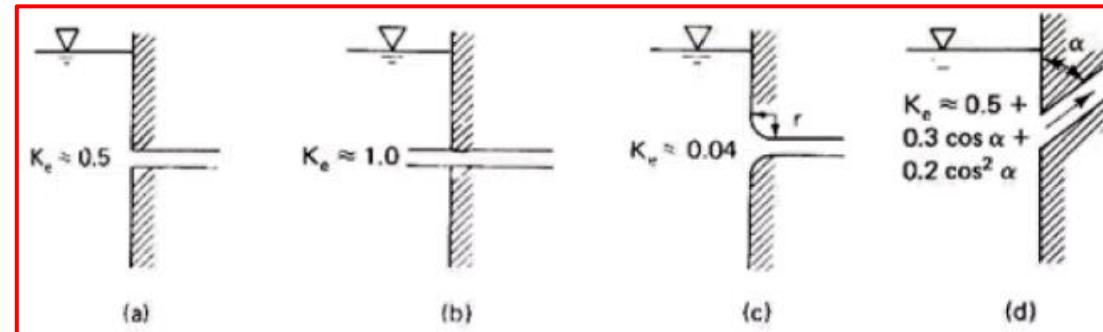
1) The major loss in the pipe 1 $\rightarrow \beta_1 = 2 \left(0.00164 + \frac{0.000042}{D_1} \right) = 0.00346 \rightarrow \Delta H_1 = \beta_1 \frac{Q^2}{D_1^5} L_1$

2) The major loss in the pipe 2 $\rightarrow \beta_2 = 2 \left(0.00164 + \frac{0.000042}{D_2} \right) = 0.00356 \rightarrow \Delta H_2 = \beta_2 \frac{Q^2}{D_2^5} L_2$

3) The minor loss at the pipe inlet $\rightarrow \Delta H_1^c = \frac{U_1^2}{2g} = \frac{Q^2}{2g \Omega_1^2}$

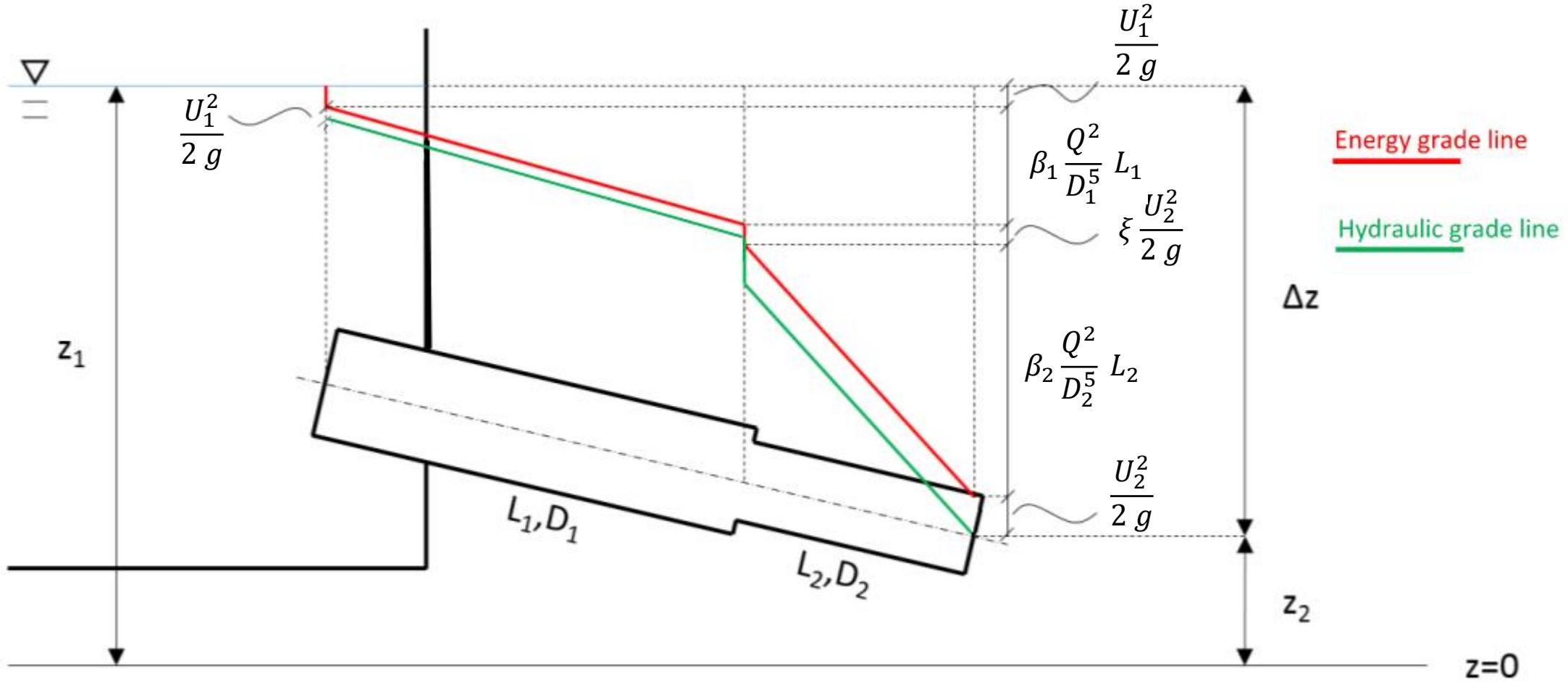
4) The minor loss at the pipe restriction $\rightarrow \Delta H_{12}^c = \xi \frac{U_2^2}{2g} = \xi \frac{Q^2}{2g \Omega_2^2}$

$$\Delta H = \sum_i \Delta H_i = Q^2 \left(\beta_1 \frac{L_1}{D_1^5} + \beta_2 \frac{L_2}{D_2^5} + \frac{8}{g \pi^2 D_1^4} + \frac{8 \xi}{g \pi^2 D_2^4} \right)$$



ENERGY BALANCE $z_1 = z_2 + \frac{Q^2}{2g \Omega_2^2} + \Delta H \Rightarrow Q = \sqrt{\frac{1}{D_1^4} \left(\frac{8}{g \pi^2} + \beta_1 \frac{L_1}{D_1} \right) + \frac{1}{D_2^4} \left(\frac{8}{g \pi^2} (1 + \xi) + \beta_2 \frac{L_2}{D_2} \right)} = 0.293 \text{ m}^3/\text{s}$

Exercise 2. Hydraulic diagnostic problem - SOLUTION



Exercise 3. Pipes in series and parallel

The system of long pipes shown in the figure below is made of new steel pipes.

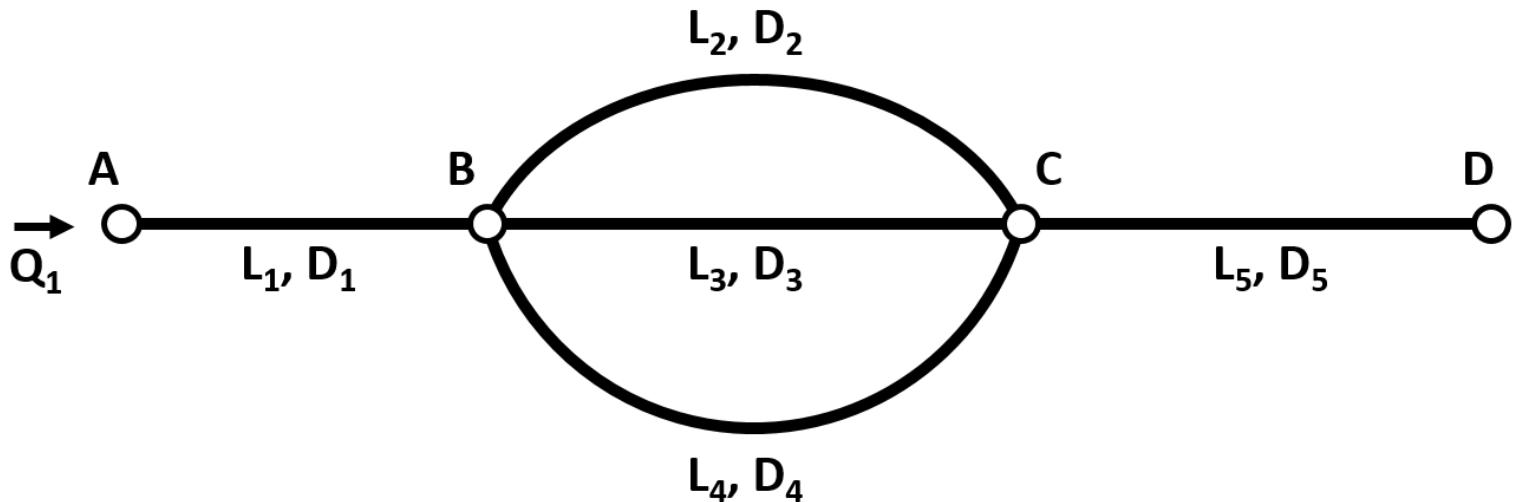
In this case, the major losses can be computed using the formula: $\Delta H_i = 0.0012 Q_i^2 D_i^{-5.26} L_i$

We can neglect the minor losses at the junctions.

In the future, the three pipes in parallel (2,3 and 4) are going to be replaced by a single pipe of length L_3 .

DATA

- Diameter of pipe 1 $\rightarrow D_1 = 600 \text{ mm}$
- Diameter of pipe 2 $\rightarrow D_2 = 350 \text{ mm}$
- Diameter of pipe 3 $\rightarrow D_3 = 300 \text{ mm}$
- Diameter of pipe 4 $\rightarrow D_4 = 400 \text{ mm}$
- Diameter of pipe 5 $\rightarrow D_5 = 500 \text{ mm}$
- Length of pipe 1 $\rightarrow L_1 = 1200 \text{ m}$
- Length of pipe 2 $\rightarrow L_2 = 800 \text{ m}$
- Length of pipe 3 $\rightarrow L_3 = 700 \text{ m}$
- Length of pipe 4 $\rightarrow L_4 = 900 \text{ m}$
- Length of pipe 5 $\rightarrow L_5 = 1500 \text{ m}$
- The flow rate in pipe 1 $\rightarrow Q_1 = 350 \text{ L/s}$



QUESTIONS

- The total loss ΔH between the points A and D, at the current state
- The diameter of the new pipe, assuming the same total head loss, ΔH , between the points A and D

Exercise 3. Pipes in series and parallel - SOLUTION

Mass continuity \rightarrow

$$Q_1 = Q_2 + Q_3 + Q_4 = Q_5$$

For flow in parallel, the head loss is the same $\rightarrow \Delta H_{BC} = \Delta H_2 = \Delta H_3 = \Delta H_4$

Head loss in pipes 2,3 and 4 $\rightarrow \Delta H_2 = 0.0012 Q_2^2 D_2^{-5.26} L_2 \quad \Delta H_3 = 0.0012 Q_3^2 D_3^{-5.26} L_3 \quad \Delta H_4 = 0.0012 Q_4^2 D_4^{-5.26} L_4$

Reverting $\rightarrow Q_2 = \sqrt{\frac{\Delta H_2 D_2^{5.26}}{0.0012 L_2}} \quad Q_3 = \sqrt{\frac{\Delta H_3 D_3^{5.26}}{0.0012 L_3}} \quad Q_4 = \sqrt{\frac{\Delta H_4 D_4^{5.26}}{0.0012 L_4}}$

And plugging into mass continuity eq. $\rightarrow Q_1 = Q_2 + Q_3 + Q_4 \Rightarrow Q_1 = \sqrt{\frac{\Delta H_2 D_2^{5.26}}{0.0012 L_2}} + \sqrt{\frac{\Delta H_3 D_3^{5.26}}{0.0012 L_3}} + \sqrt{\frac{\Delta H_4 D_4^{5.26}}{0.0012 L_4}}$

Considering $\Delta H_2 = \Delta H_3 = \Delta H_4 = \Delta H_{BC}$ and reverting $\rightarrow \Delta H_{BC} = 0.0012 Q_1^2 \left(\sqrt{\frac{D_2^{5.26}}{L_2}} + \sqrt{\frac{D_3^{5.26}}{L_3}} + \sqrt{\frac{D_4^{5.26}}{L_4}} \right)^{-2} = 3.16 \text{ m}$

Head loss in pipes 1 and 5 $\rightarrow \Delta H_1 = 0.0012 Q_1^2 D_1^{-5.26} L_1 = 2.59 \text{ m} \quad \Delta H_5 = 0.0012 Q_5^2 D_5^{-5.26} L_5 = 8.45 \text{ m}$

Total head loss

$$\rightarrow \Delta H = \Delta H_1 + \Delta H_{BC} + \Delta H_5 = 14.20 \text{ m}$$

Exercise 3. Pipes in series and parallel - SOLUTION

Mass continuity →

$$Q_1 = Q_3 = Q_5$$

After replacement, the head loss → $\Delta H_{3,\text{future}} = \Delta H_{BC} = 0.0012 Q_3^2 D_{3,\text{future}}^{-5.26} L_3$

Considering mass continuity eq. and reverting → $D_{3,\text{future}} = \left(0.0012 \frac{Q_1^2}{\Delta H_{BC}} L_3 \right)^{\frac{1}{5.26}} = 0.522 \text{ m}$

Exercise 4. Pumping system

A pipeline is installed to deliver water from a reservoir to an upper tank, through a pump with known characteristics.

The pipe geometry and the static lift (difference between water levels in the reservoir and in the tank) are given.

DATA

- Diameter of the pipe $\rightarrow D = 0.15 \text{ m}$
- Length of the pipeline $\rightarrow L = 250 \text{ m}$
- Pipe roughness $\rightarrow k_s = 0.3 \text{ mm}$
- Static lift $\rightarrow \Delta z = 10 \text{ m}$
- Pump characteristics in Table 1

QUESTIONS

- Graphically estimate the pump efficiency η at the functioning point
- Graphically estimate the power requirement P_{pump} at the functioning point
- Comment on the suitability of this pump and pipeline combination, and eventually propose what could be changed (and how) to increase the efficiency at the new functioning point
- Graphically estimate the pump efficiency η^* and power P^*_{pump} at the new functioning point

Table 1

Flow rate $Q [\text{m}^3/\text{s}]$	Pump head $H_{\text{pump}} [\text{m}]$	Efficiency $\eta [\%]$
0	26.25	0
0.01	24	28
0.02	21.75	51
0.03	19.5	68
0.04	17.5	80
0.05	15	85
0.06	11.75	80
0.07	6.75	64

Exercise 4. Pumping system - SOLUTION

CURRENT STATE

D [m]	0.15	Q [m^3/s]	H_{pump} [m]	η [%]	U [m/s]	Re [-]	λ [-]	$\lambda(\text{CW})$ [-]	ΔH [m]	$\Delta H + \Delta z$ [m]	P_{hyd} [W]	P_{pump} [W]		
L [m]	250	0	26.25	0	0	0			0	10	0	0		
Δz [m]	10	0.01	24	28	0.566	84883	0.025359	0.025359	0.690	10.69	2354	8409		
k_s	0.0003	0.02	21.75	51	1.132	169765	0.024442	0.024442	2.660	12.66	4267	8367		
		0.03	19.5	68	1.698	254648	0.024112	0.024112	5.903	15.90	5739	8439		
		0.04	17.5	80	2.264	339531	0.023941	0.023941	10.420	20.42	6867	8584		
		0.05	15	85	2.829	424413	0.023837	0.023837	16.210	26.21	7358	8656		
		0.06	11.75	80	3.395	509296	0.023766	0.023766	23.274	33.27	6916	8645		
		0.07	6.75	64	3.961	594178	0.023715	0.023715	31.611	41.61	4635	7243		

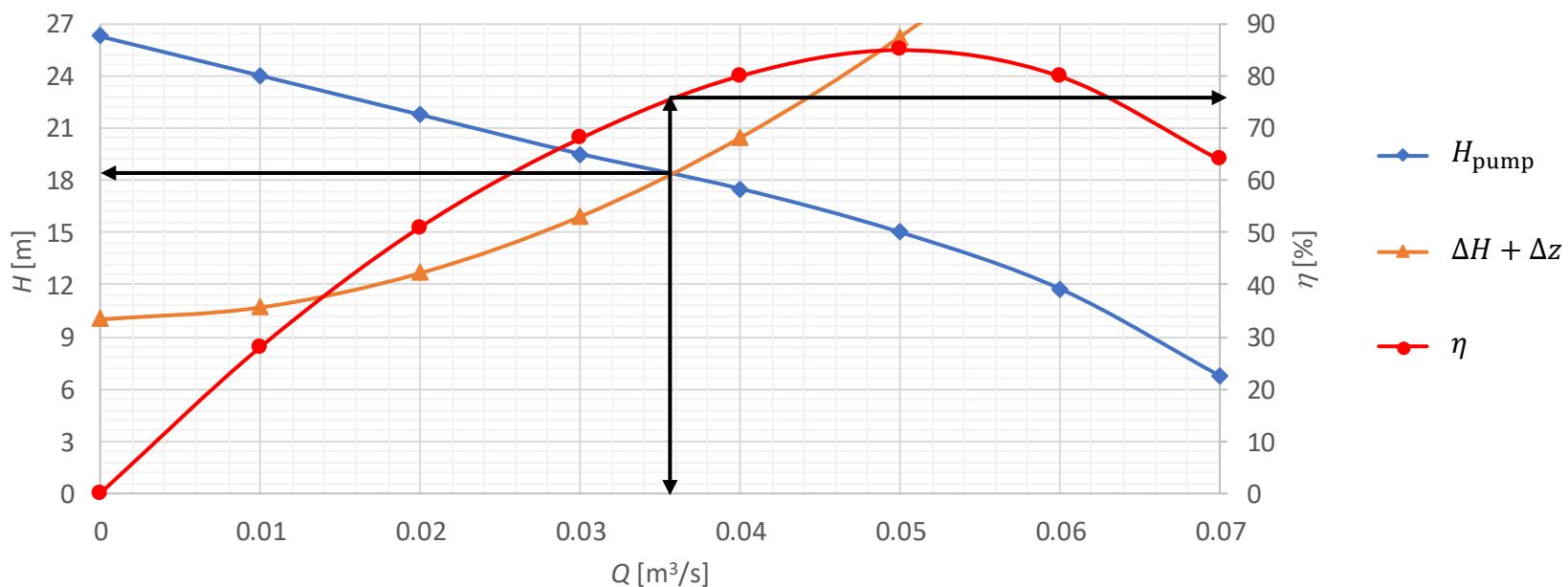
$Q \approx 0.036 \text{ m}^3/\text{s}$

$H \approx 18.6 \text{ m}$

$\eta \approx 76 \%$

$P_{\text{hyd}} \approx 6570 \text{ W}$

$P_{\text{pump}} \approx 8640 \text{ W}$



Exercise 4. Pumping system - SOLUTION

POSSIBLE IMPROVEMENT → Increase pipe diameter to reduce head loss

D [m]	0.2	Q [m^3/s]	H_{pump} [m]	η [%]	U [m/s]	Re [-]	λ [-]	$\lambda(\text{CW})$ [-]	ΔH [m]	$\Delta H + \Delta z$ [m]	P_{hyd} [W]	P_{pump} [W]		
L [m]	250	0	26.25	0	0	0			0	10	0	0		
Δz [m]	10	0.01	24	28	0.318	63662	0.024667	0.024667	0.159	10.16	2354	8409		
k_s	0.0003	0.02	21.75	51	0.637	127324	0.023337	0.023337	0.603	10.60	4267	8367		
		0.03	19.5	68	0.955	190986	0.022837	0.022837	1.327	11.33	5739	8439		
		0.04	17.5	80	1.273	254648	0.022572	0.022572	2.331	12.33	6867	8584		
		0.05	15	85	1.592	318310	0.022409	0.022409	3.616	13.62	7358	8656		
		0.06	11.75	80	1.910	381972	0.022298	0.022298	5.182	15.18	6916	8645		
		0.07	6.75	64	2.228	445634	0.022217	0.022217	7.027	17.03	4635	7243		

$$Q^* \approx 0.0525 \text{ m}^3/\text{s}$$

$$H^* \approx 14.4 \text{ m}$$

$$\eta^* \approx 84 \%$$

$$P_{\text{hyd}}^* \approx 7420 \text{ W}$$

$$P_{\text{pump}}^* \approx 8830 \text{ W}$$

