

Solar Energy Conversion Devices and Plants

Prof. Sophia Haussener

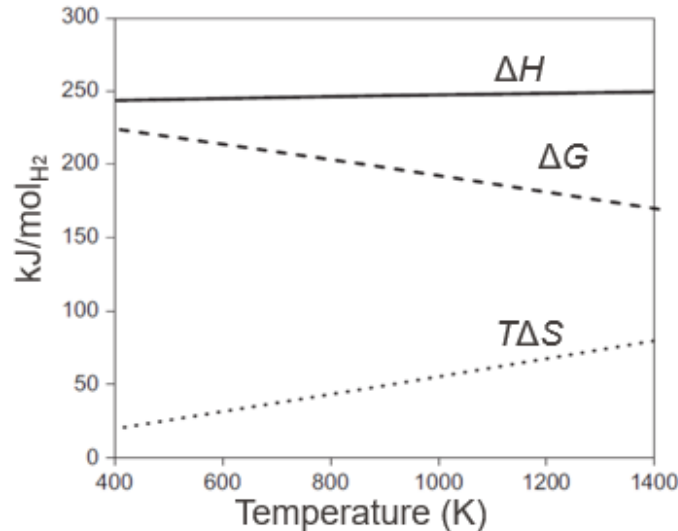
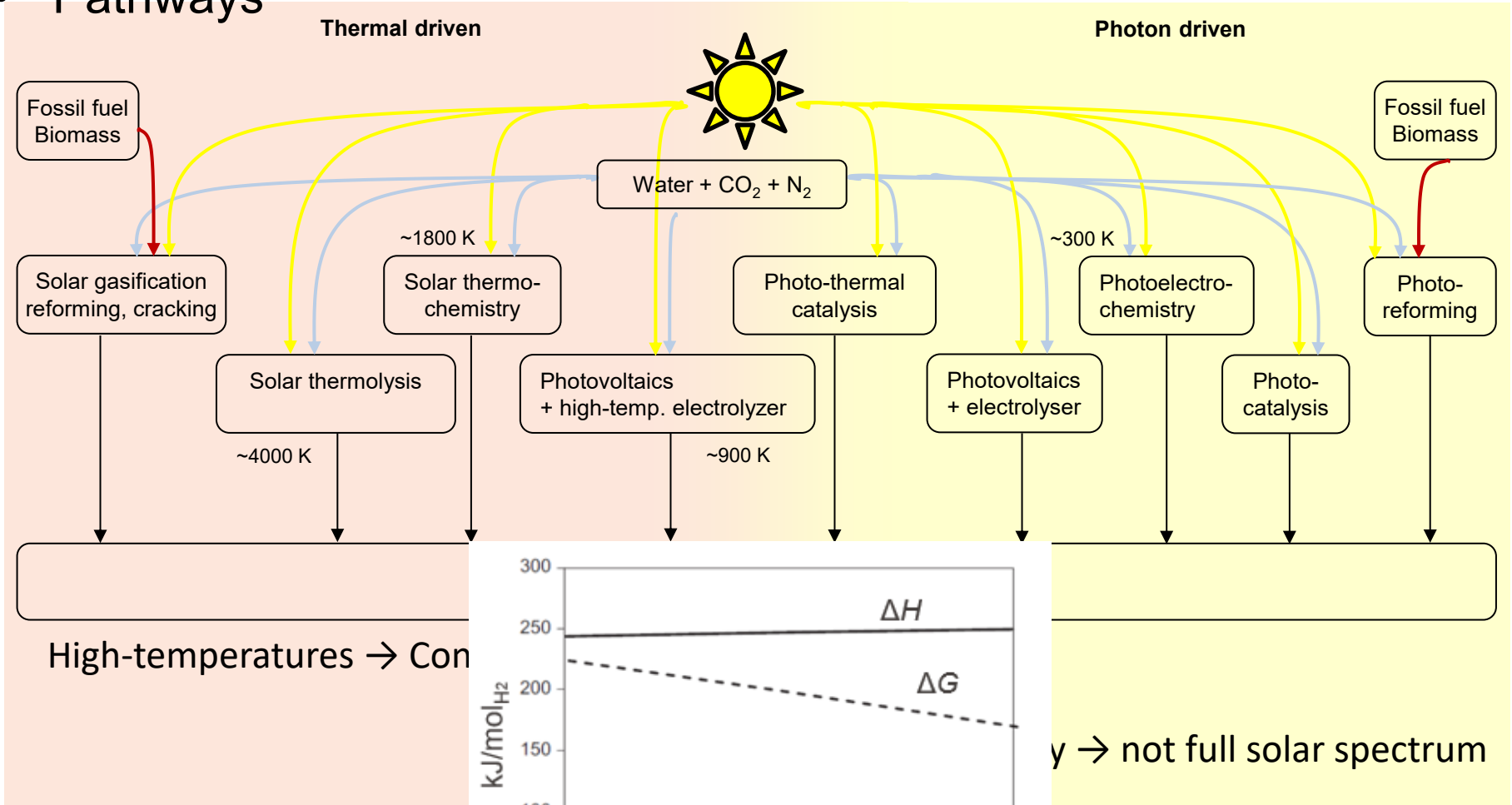
Laboratory of Renewable Energy Science and Engineering

Outline

- Solar-driven thermochemistry
 - Solar thermolysis
 - Solar thermochemical redox cycles
 - Hybrid approaches:
 - Solar reforming
 - Solar cracking
 - Solar gasification

Solar Fuels

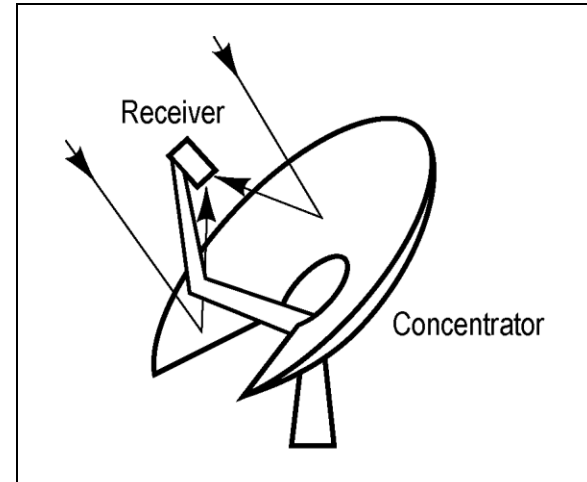
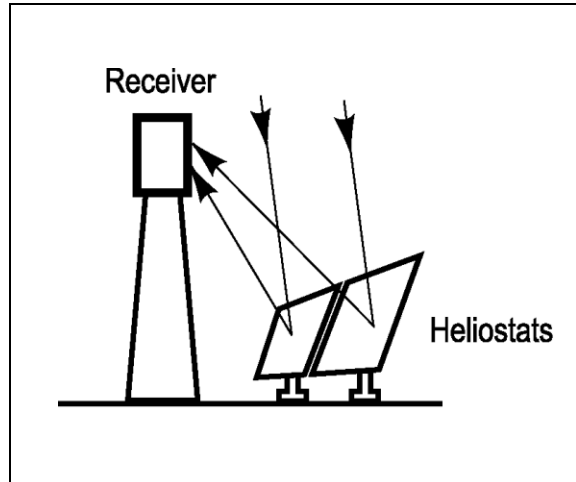
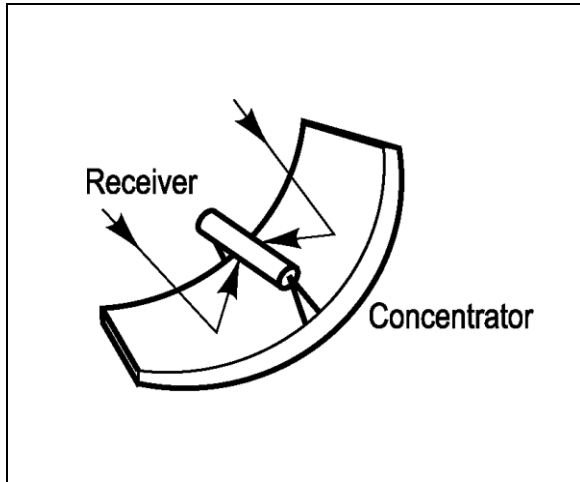
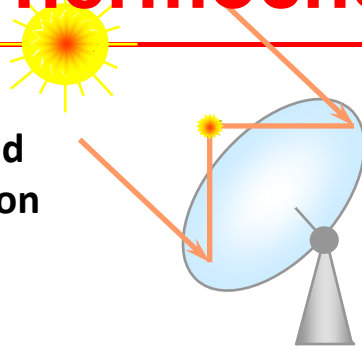
Pathways



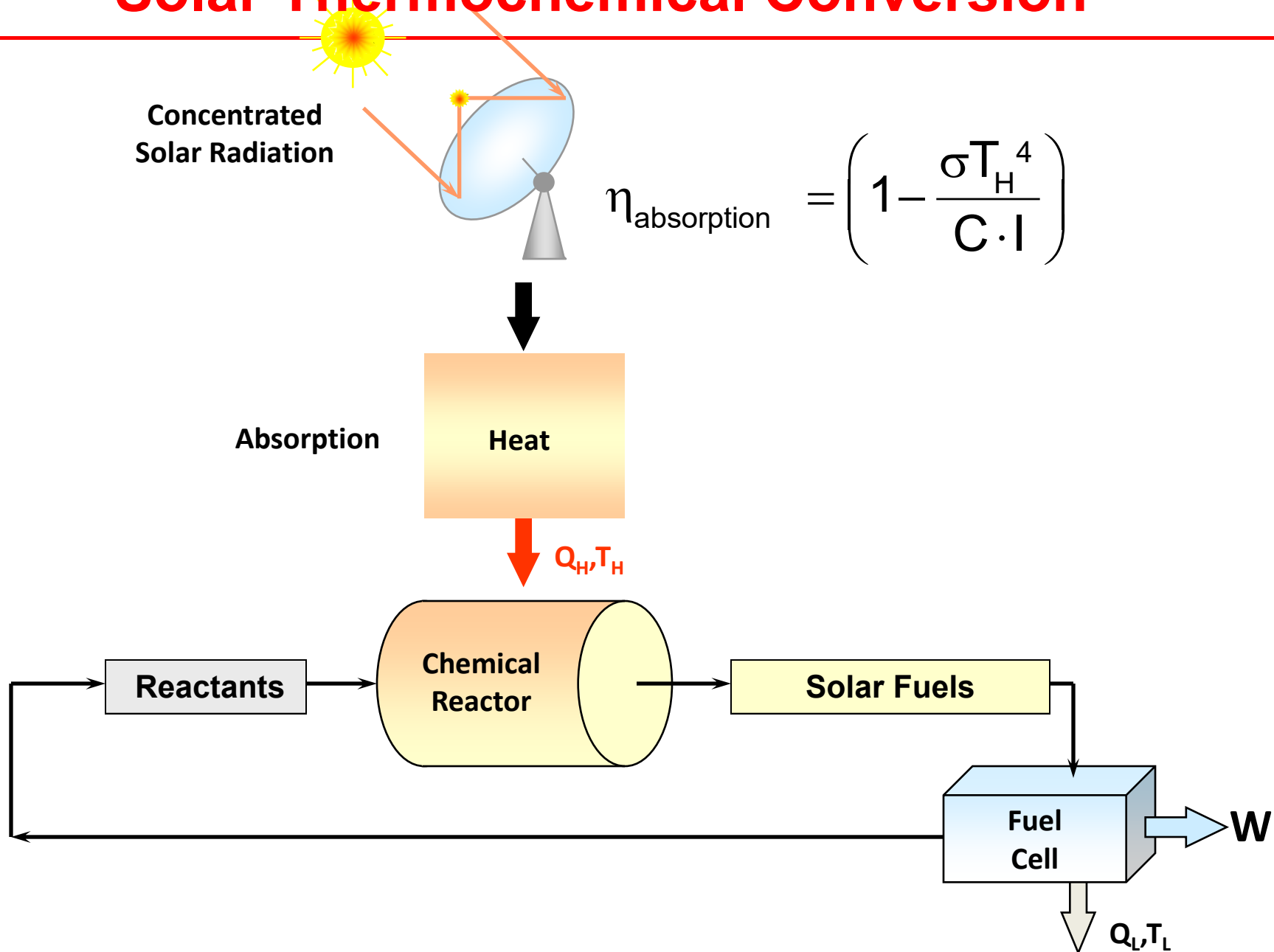
y → not full solar spectrum

Solar Thermochemical Conversion

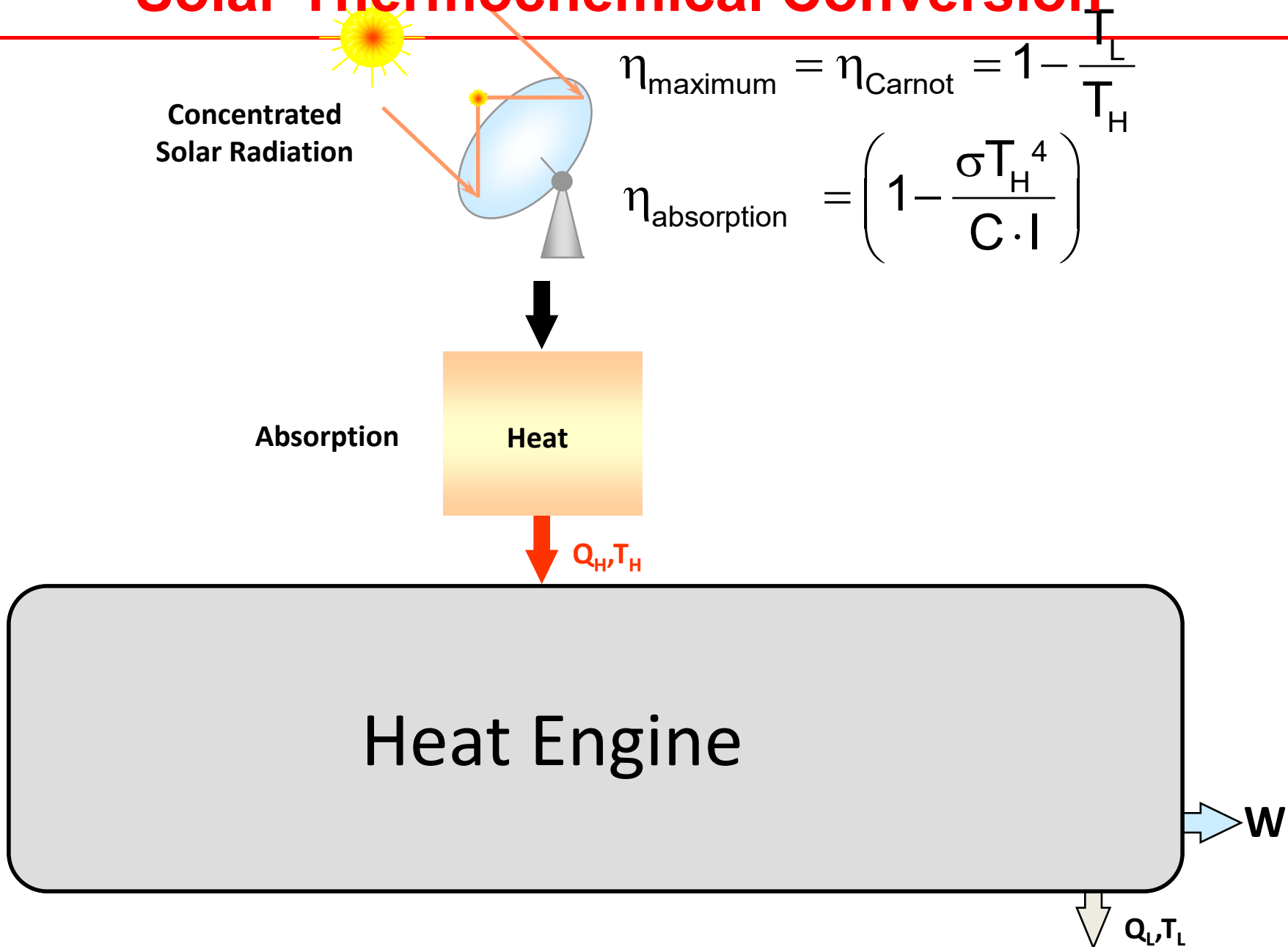
Concentrated
Solar Radiation



Solar Thermochemical Conversion

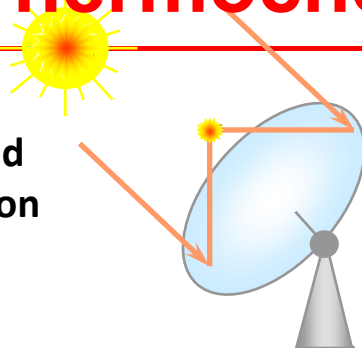


Solar Thermochemical Conversion



Solar Thermochemical Conversion

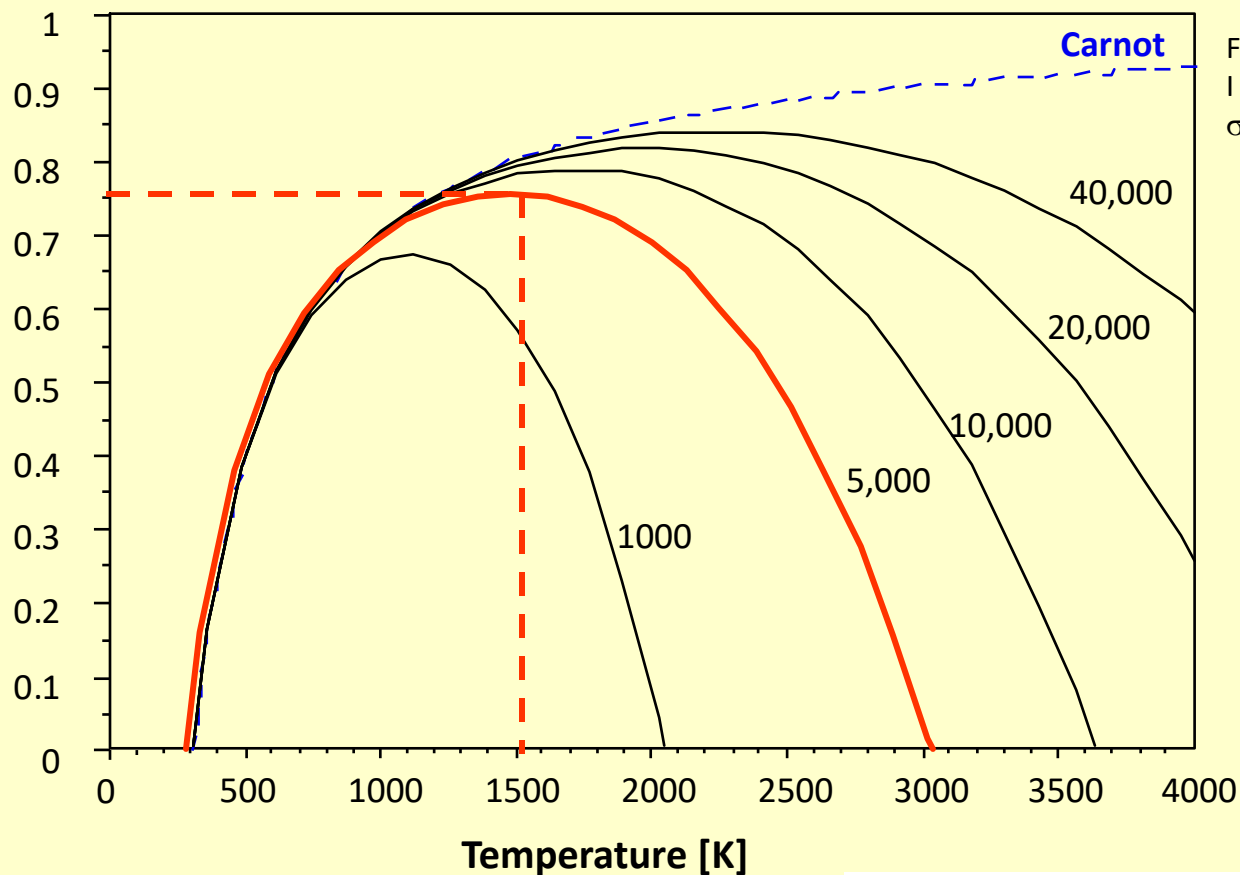
Concentrated
Solar Radiation



$$\eta_{\text{maximum}} = \eta_{\text{Carnot}} = 1 - \frac{T_L}{T_H}$$

$$\eta_{\text{absorption}} = \left(1 - \frac{\sigma T_H^4}{C \cdot I} \right)$$

$\eta_{\text{absorption}} \cdot \eta_{\text{Carnot}}$



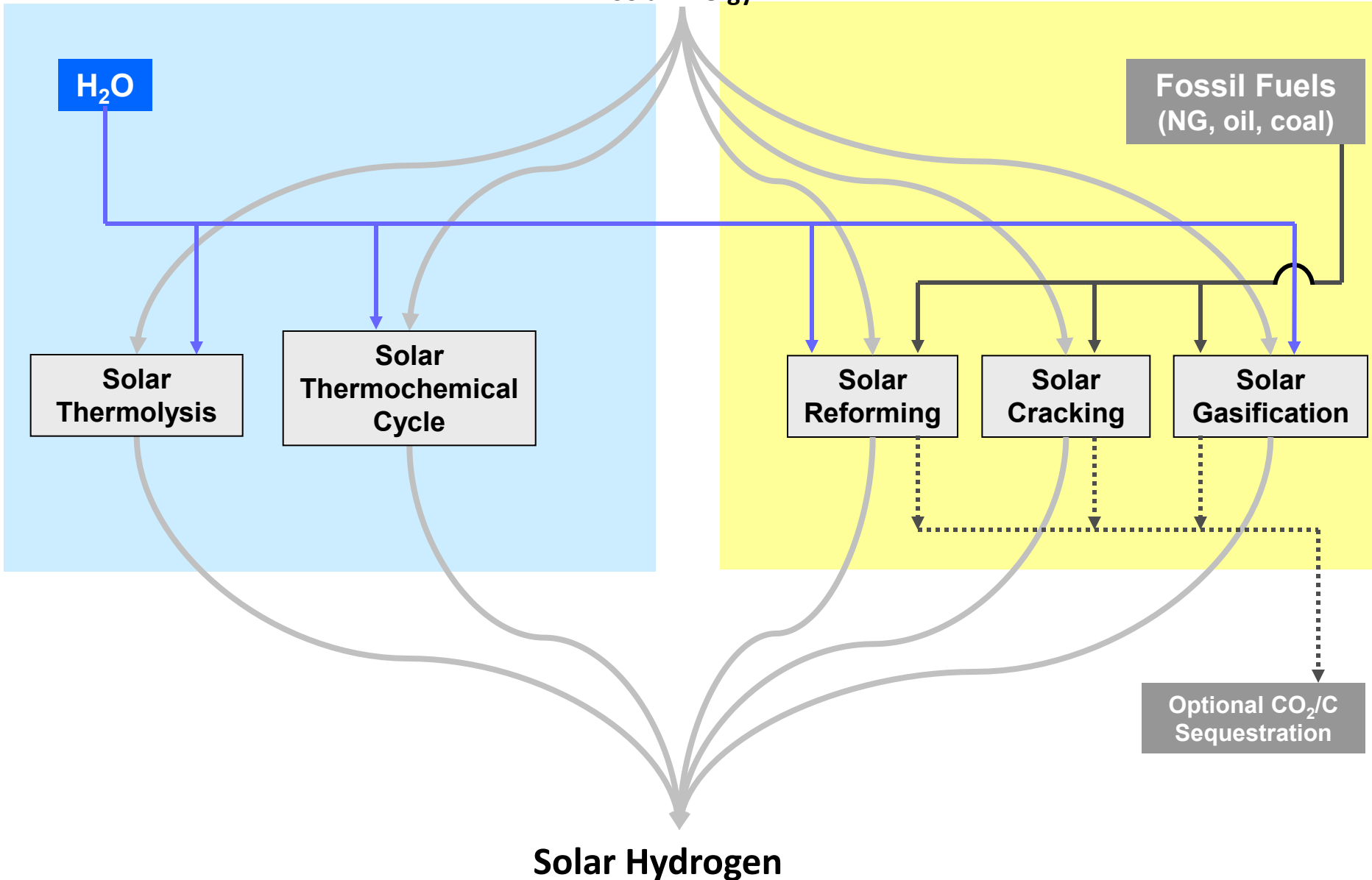
For:
 $I = 1 \text{ kW/m}^2$ (1 sun)
 $\sigma = 5.67 \cdot 10^{-8} \text{ W/m}^2\text{K}^2$

H₂O-splitting



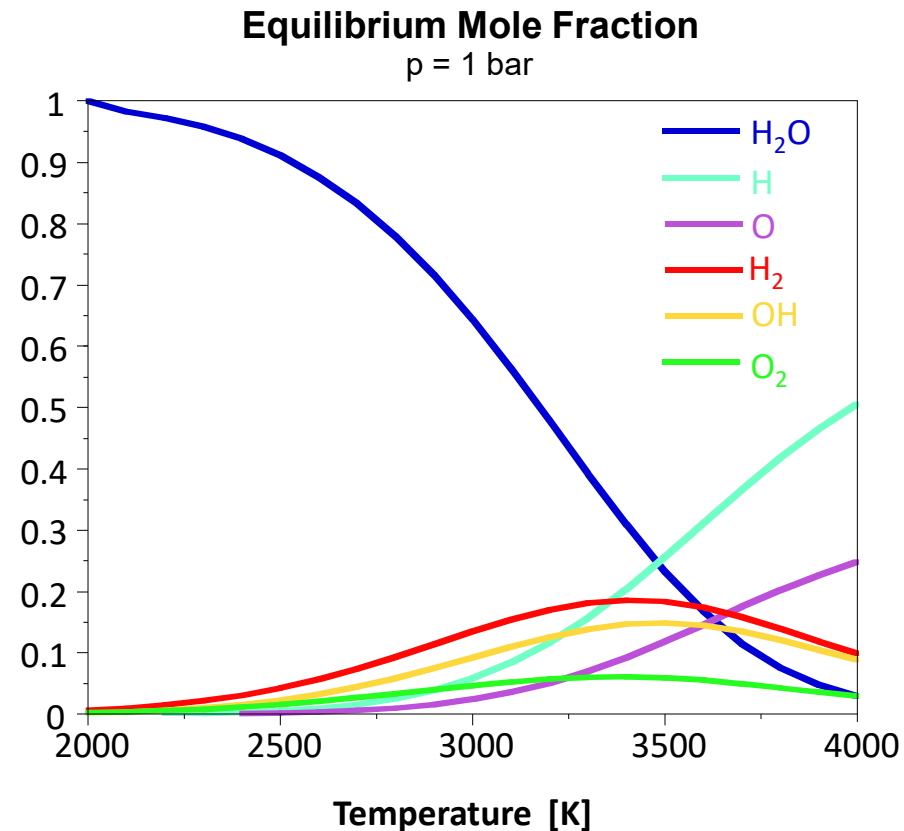
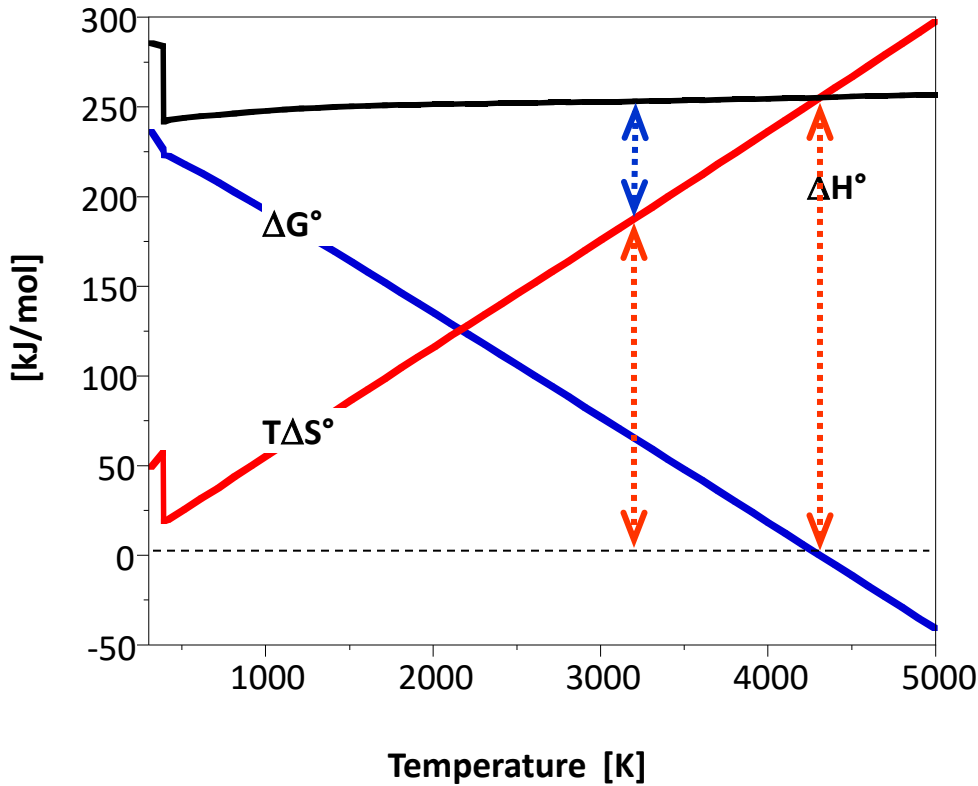
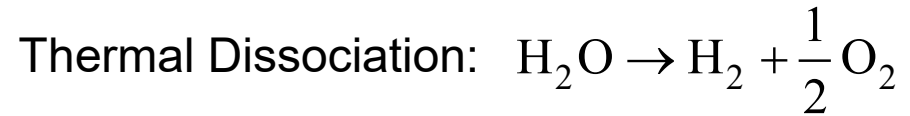
Concentrated Solar Energy

Decarbonization

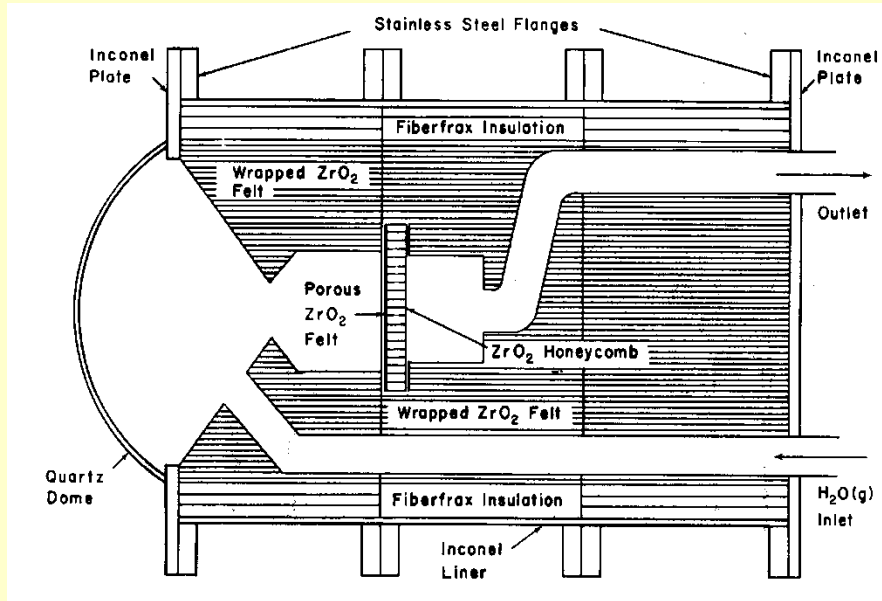


Solar Thermolysis

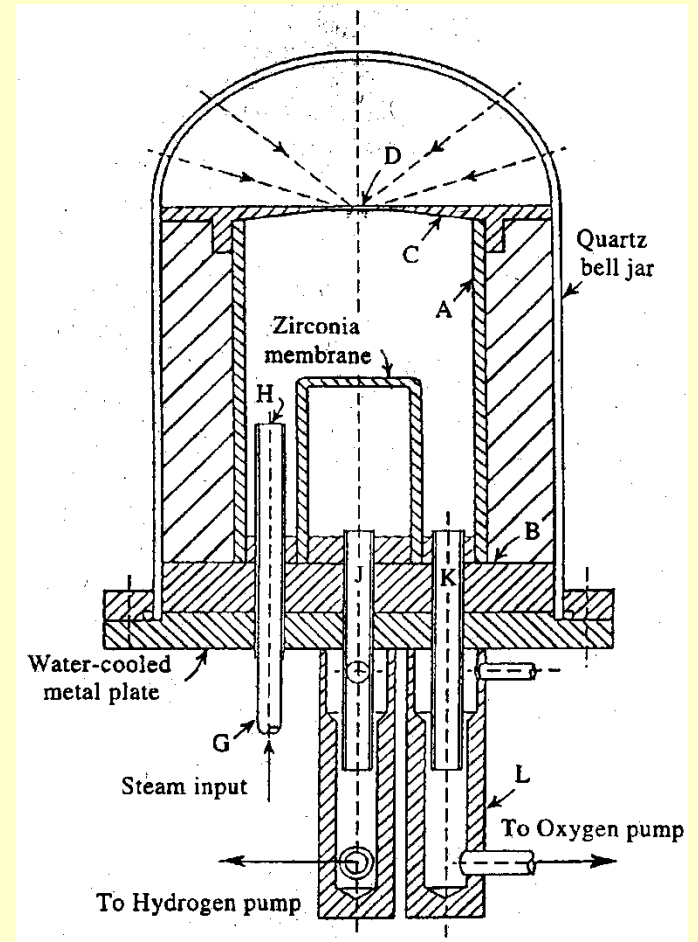
Solar Thermolysis



Solar Thermolysis

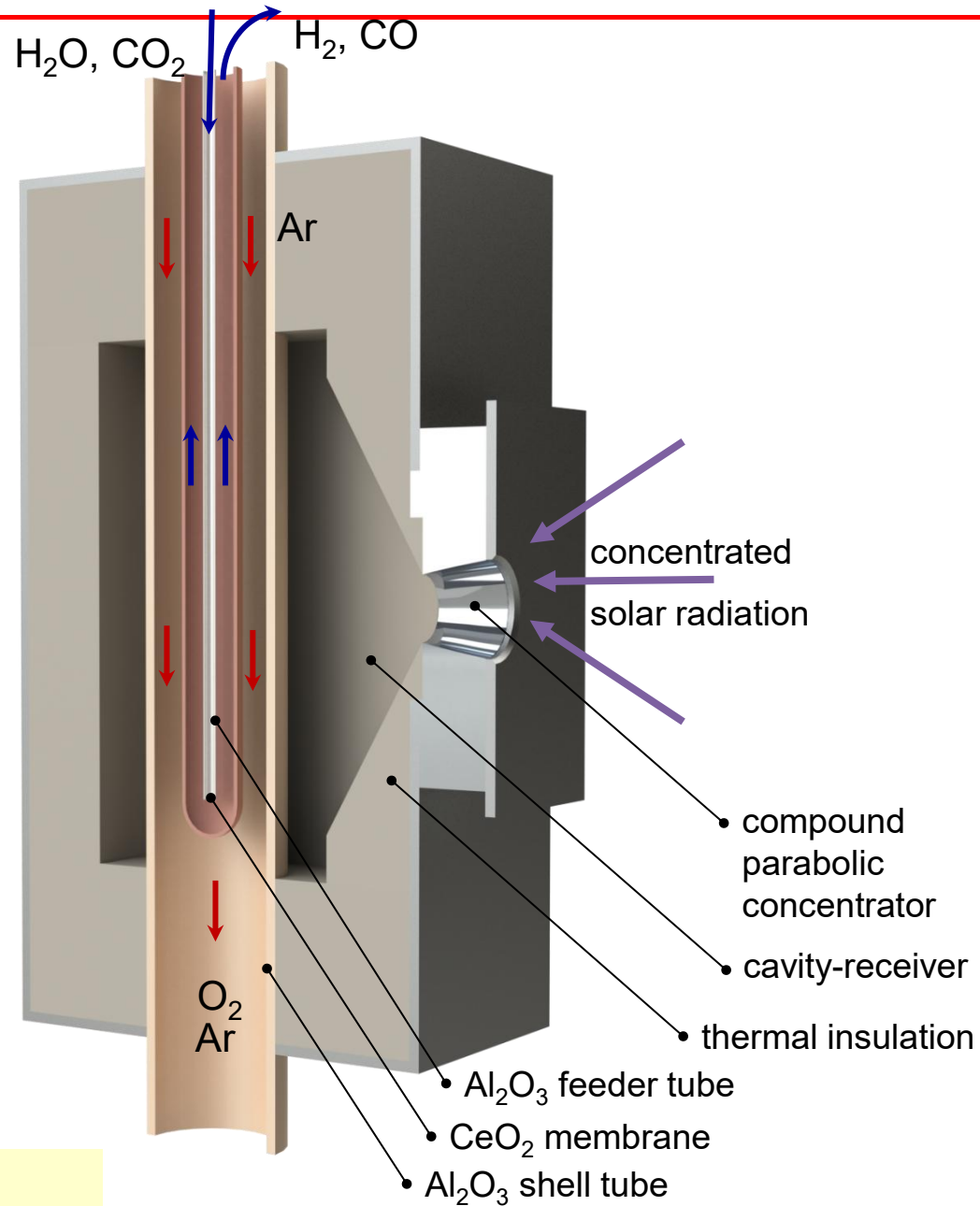
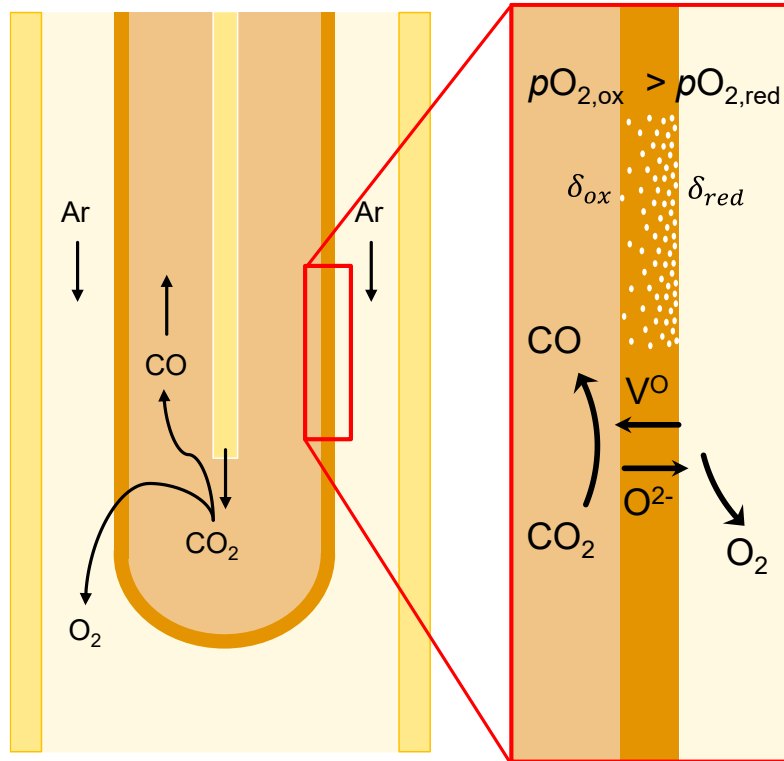


• Fletcher E., *J. Solar Energy Engineering* **123**, 63-74, 2001.



• Kogan et al., *Int. J. Hydrogen Energy* **23**, 89-98, 1998.

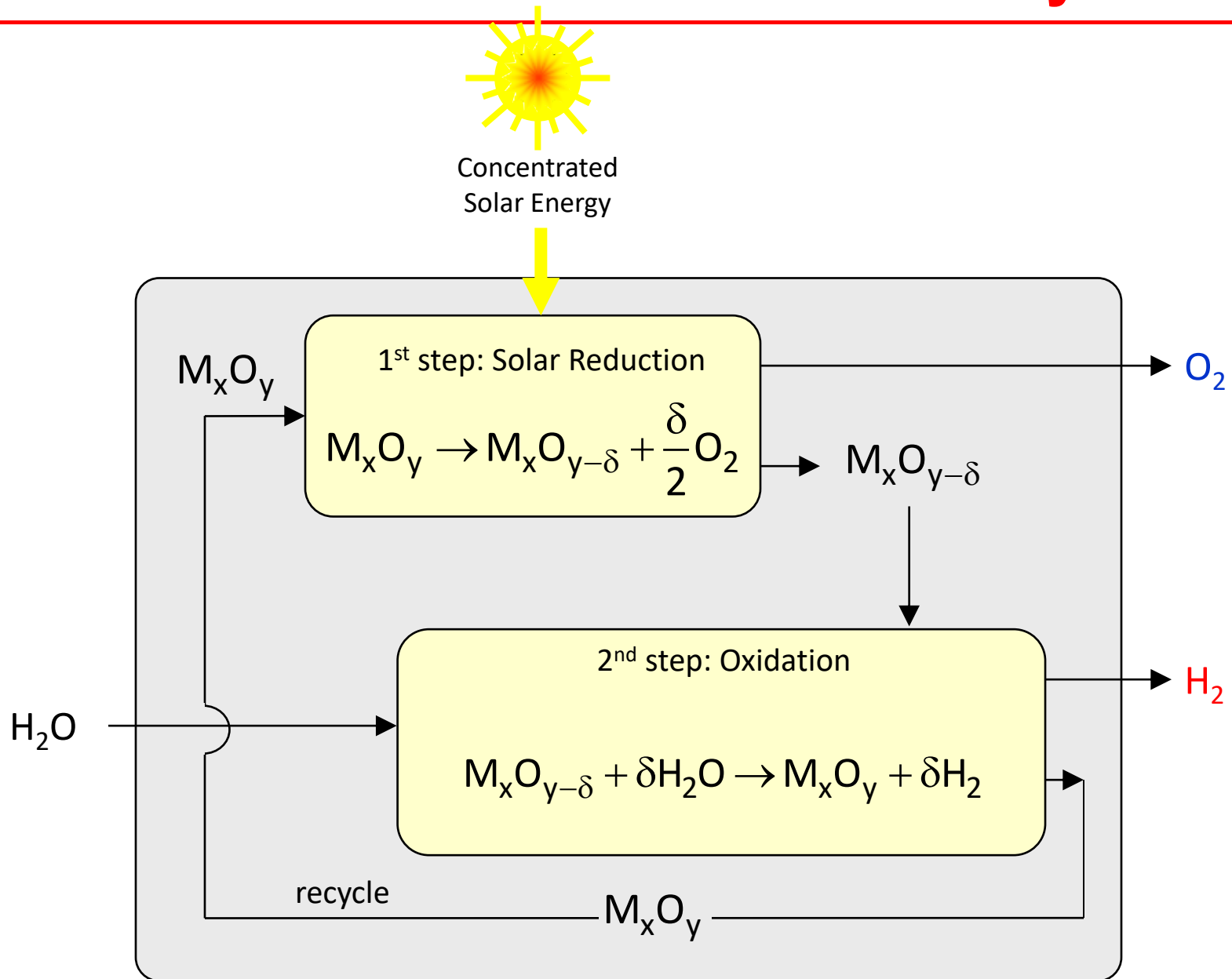
Solar Thermolysis



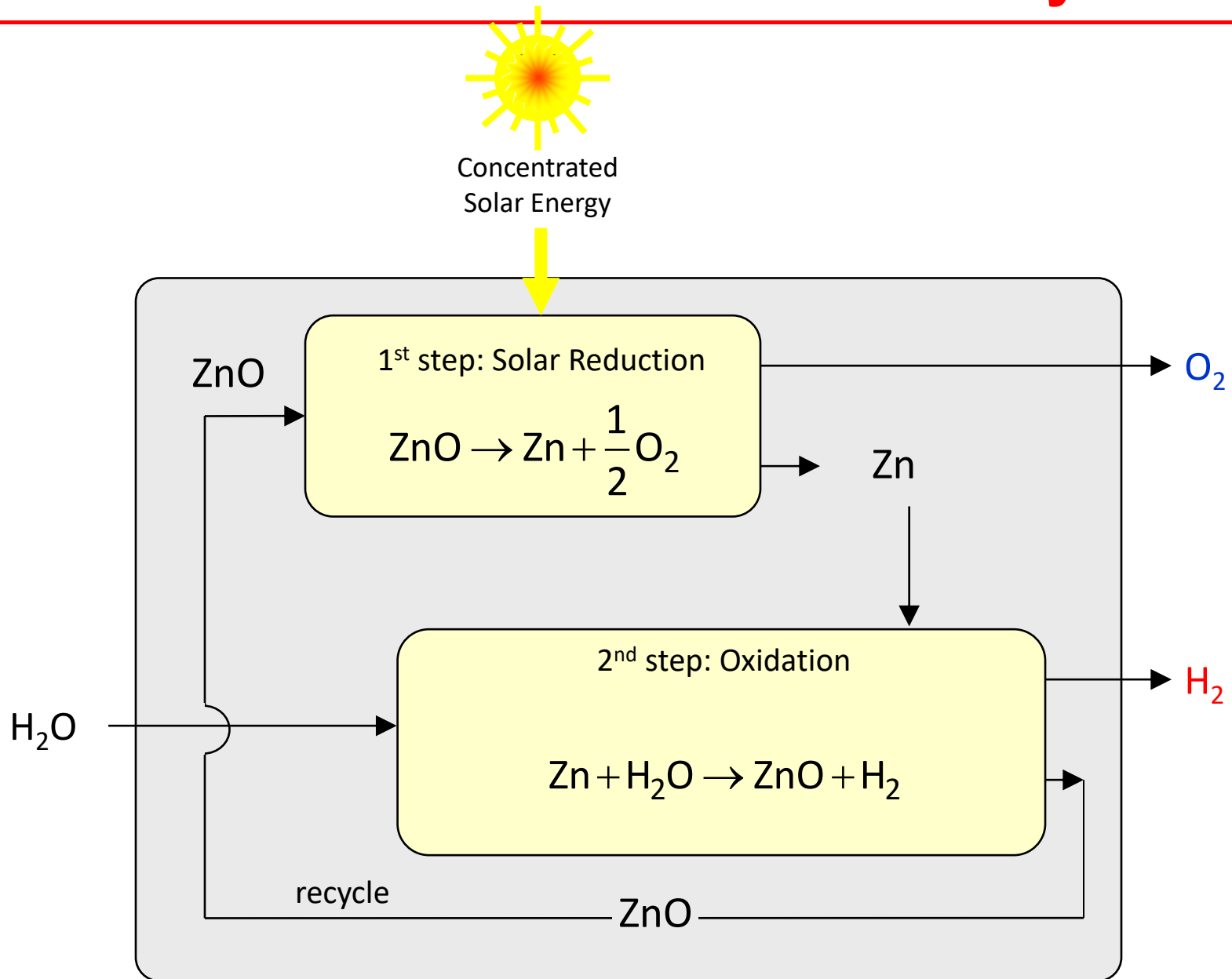
• *Joule*, Vol. 1, pp. 146-154, 2017
 • *Reaction Chemistry & Engineering*, Vol. 4, pp. 1431-1438, 2019

Solar Thermochemical Cycles

Solar Thermochemical Redox Cycle



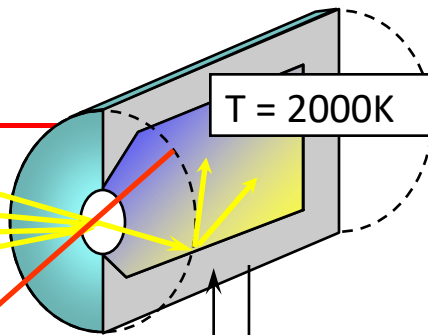
Solar Thermochemical Redox Cycle



$$I = 1 \text{ kW/m}^2$$

$$C = 5000$$

Concentrated
Solar
Power



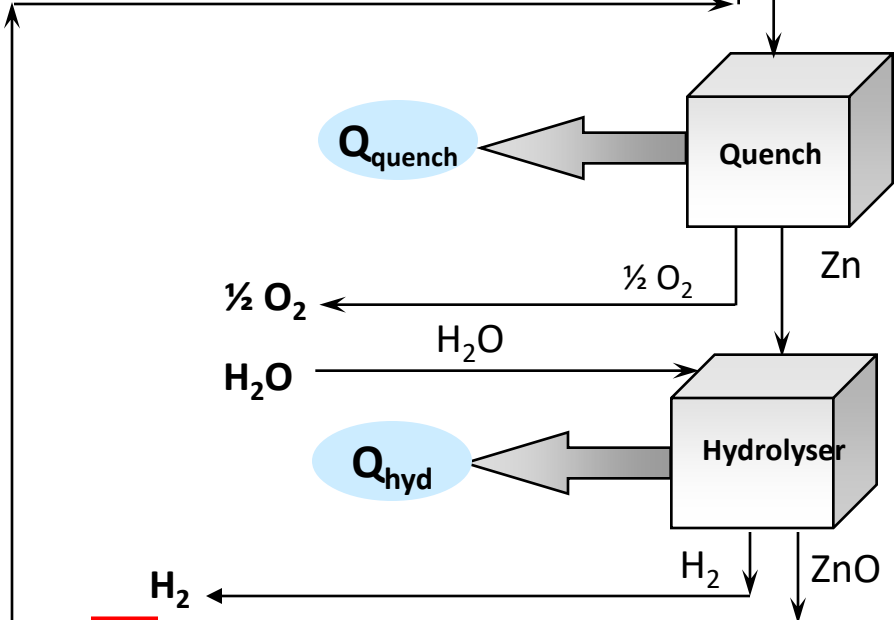
Q_{solar}

$T = 2000\text{K}$

Q_{rerad}

ZnO
@ 298 K

Zn + 1/2 O₂
@ 2000 K



Q_{quench}

Quench

1/2 O₂

1/2 O₂

Zn

H₂O

H₂O

Q_{hyd}

Hydrolyser

H₂

H₂

ZnO

$$\Delta H_{\text{ZnO @ 300K} \rightarrow \text{Zn} + \frac{1}{2}\text{O}_2 \text{ @ 2000K}} = 557 \text{ kJ/mol}$$

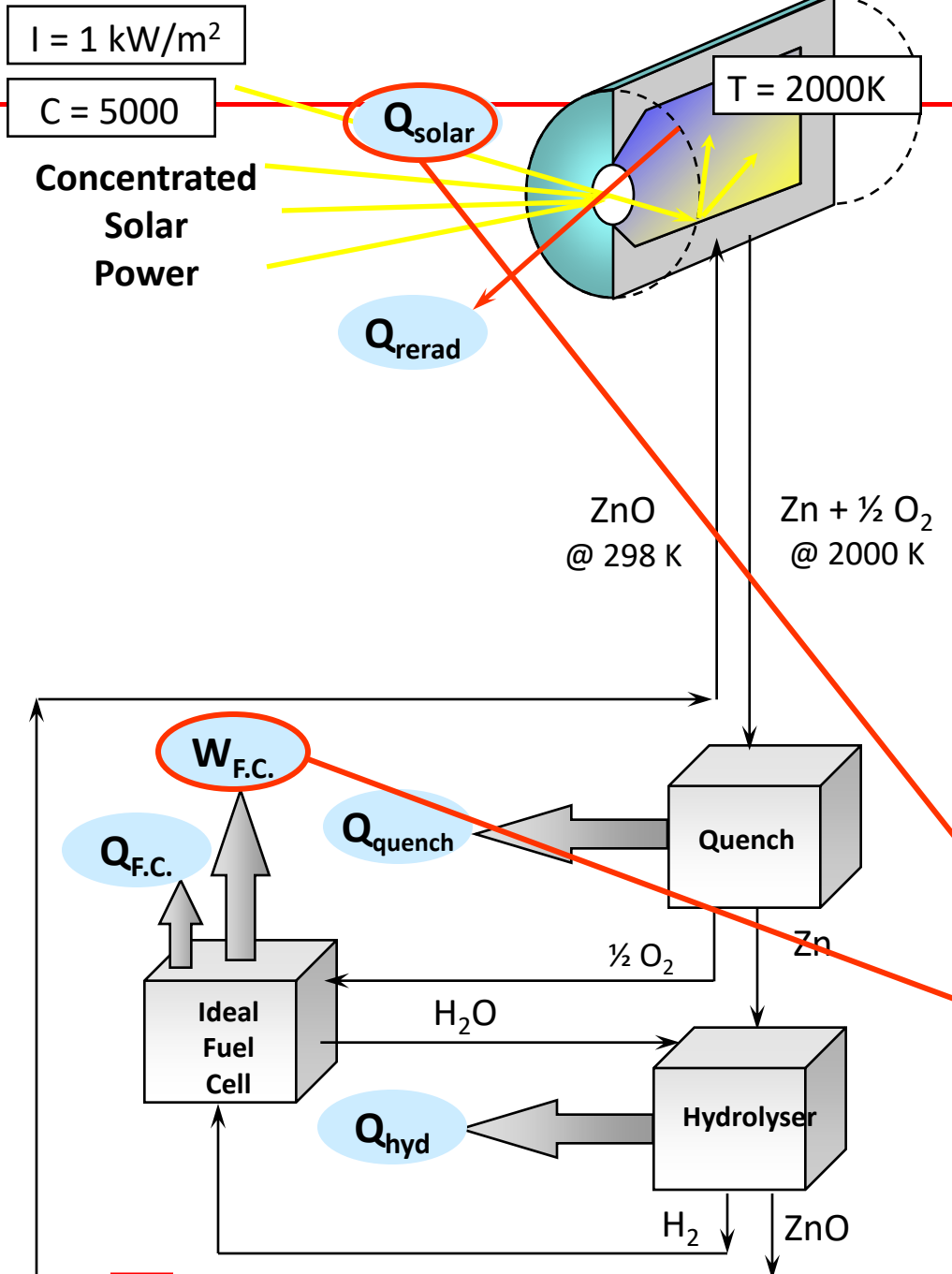
$$\eta_{\text{absorption}} = \frac{\Delta H_{\text{rxn}}}{Q_{\text{solar}}} = 1 - \frac{\sigma T^4}{I \times C} = 82\%$$

$$Q_{\text{solar}} = 680 \text{ kJ/mol}$$

$$Q_{\text{rerad}} = 123 \text{ kJ/mol}$$

$$Q_{\text{quench}} = \Delta H_{\text{Zn} + \frac{1}{2}\text{O}_2 \text{ @ 2000K} \rightarrow \text{Zn} + \frac{1}{2}\text{O}_2 \text{ @ 300K}} = -209 \text{ kJ/mol}$$

$$Q_{\text{hydrolyser}} = \Delta H_{\text{Zn} + \text{H}_2\text{O} \rightarrow \text{ZnO} + \text{H}_2} = -62 \text{ kJ/mol}$$



$$\Delta H_{ZnO @ 300K \rightarrow Zn + \frac{1}{2} O_2 @ 2000K} = 557 \text{ kJ/mol}$$

$$\eta_{\text{absorption}} = \frac{\Delta H_{\text{rxn}}}{Q_{\text{solar}}} = 1 - \frac{\sigma T^4}{I \times C} = 82\%$$

$$Q_{\text{solar}} = 680 \text{ kJ/mol}$$

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$$Q_{\text{quench}} = \Delta H_{Zn + \frac{1}{2} O_2 @ 2000K \rightarrow Zn + \frac{1}{2} O_2 @ 300K} = -209 \text{ kJ/mol}$$

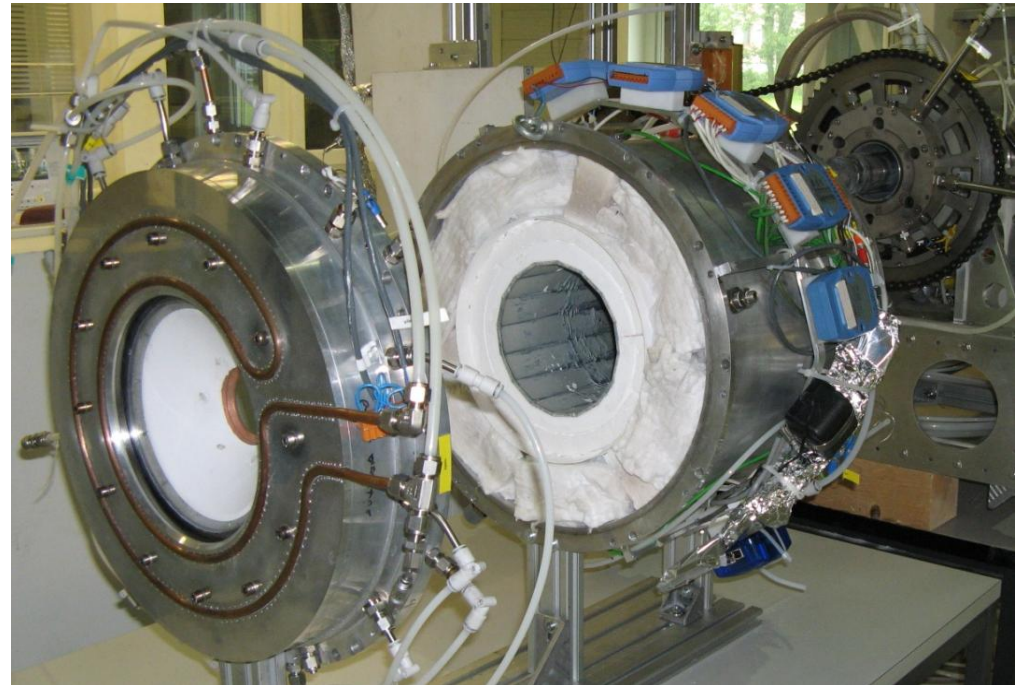
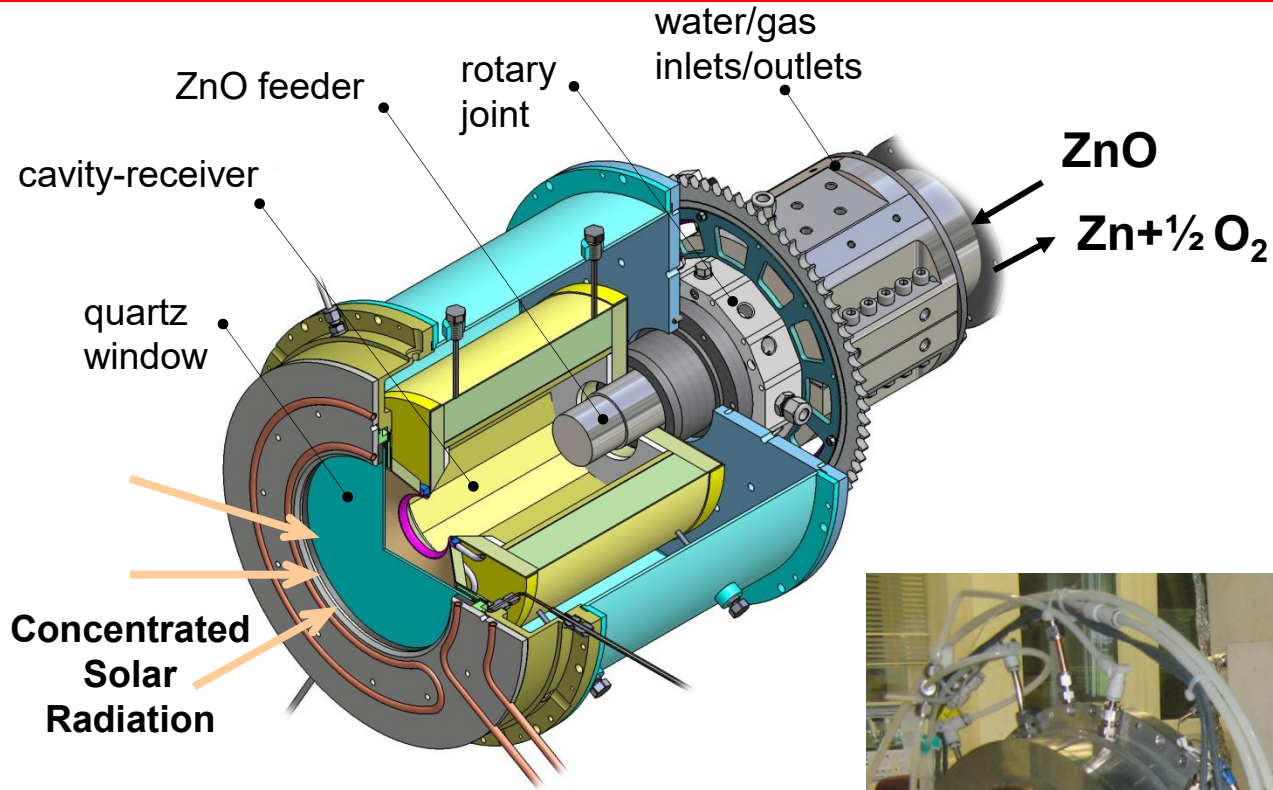
$$Q_{\text{hydrolyser}} = \Delta H_{Zn + H_2O \rightarrow ZnO + H_2} = -62 \text{ kJ/mol}$$

$$W_{\text{F.C.}} = -\Delta G_{H_2 + \frac{1}{2} O_2 \rightarrow H_2O @ 300K} = 237 \text{ kJ/mol}$$

$$Q_{\text{F.C.}} = (\Delta H - \Delta G) = -49 \text{ kJ/mol}$$

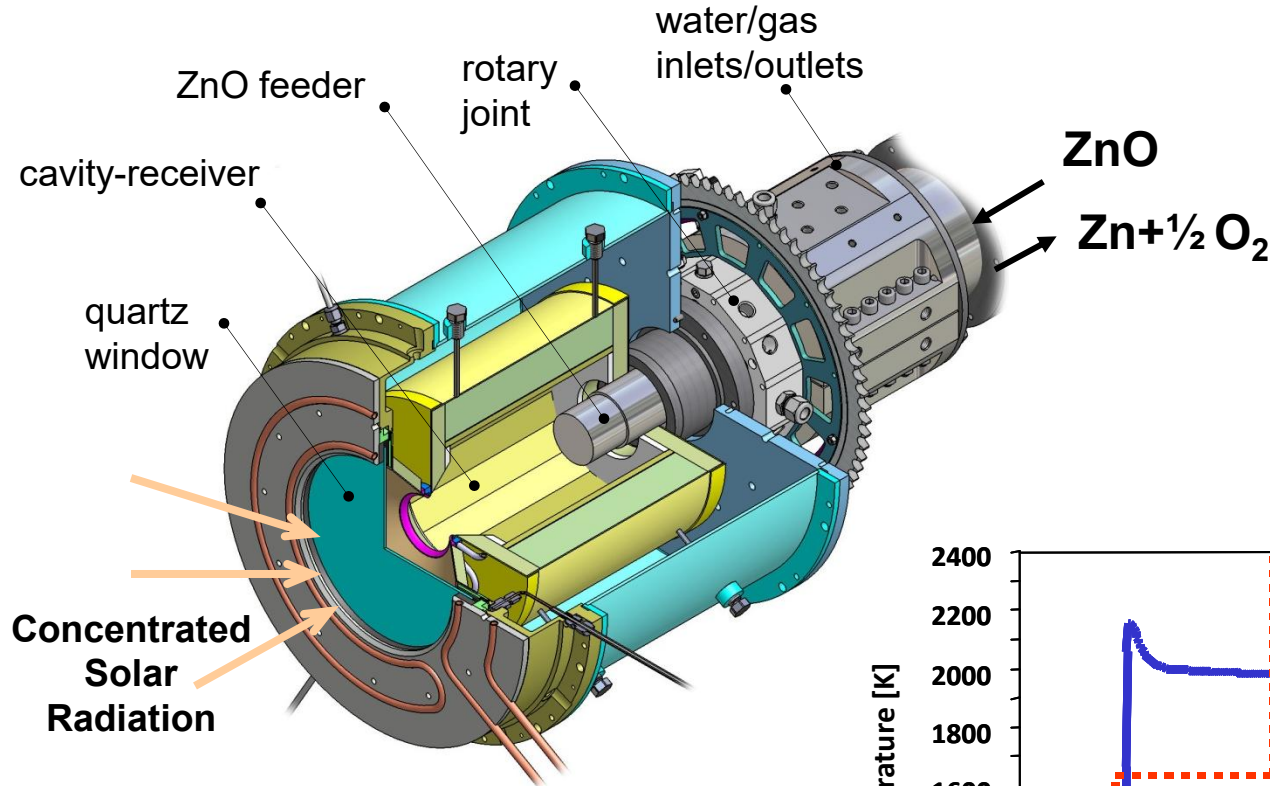
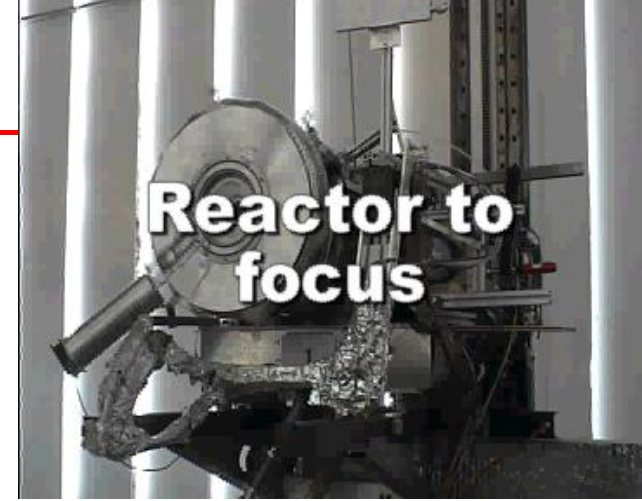
$$\eta = \frac{W_{\text{F.C.}}}{Q_{\text{solar}}} = \begin{cases} 35\% & \text{no h.r.} \\ 58\% & \text{with h.r.} \end{cases}$$

ZnO/Zn Cycle

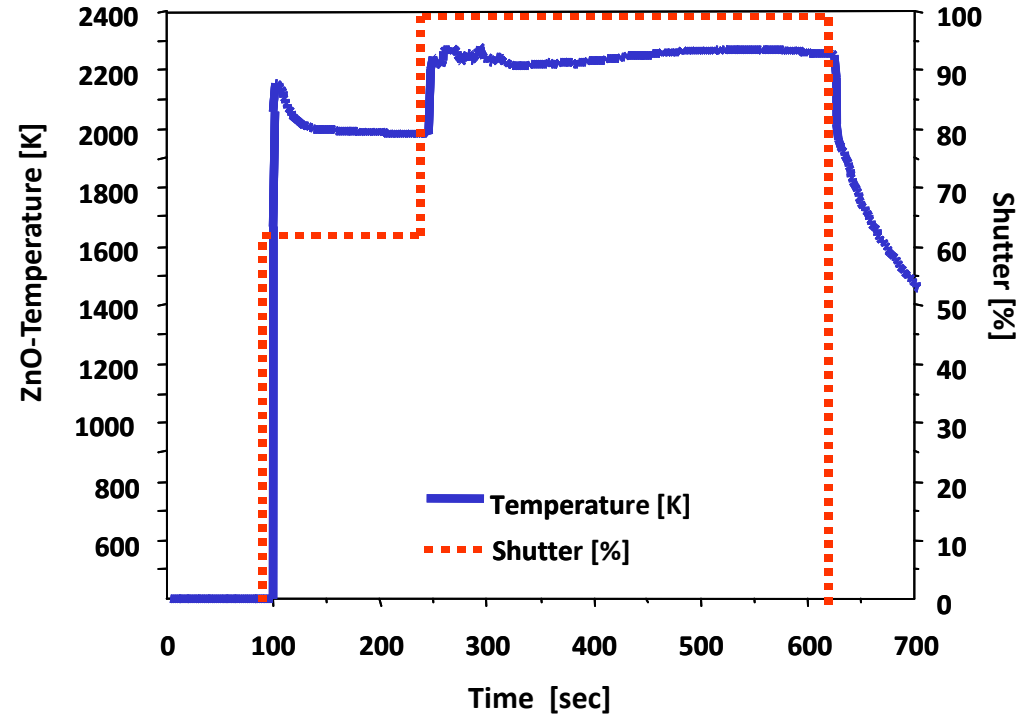


- *AIChE J.* 55, 1497-1504, 2009.
- *Chem. Eng. J.* 150, 502-508, 2009.
- *Int. J. Heat Mass Transfer* 52, 2444-2452, 2009.

ZnO/Zn Cycle

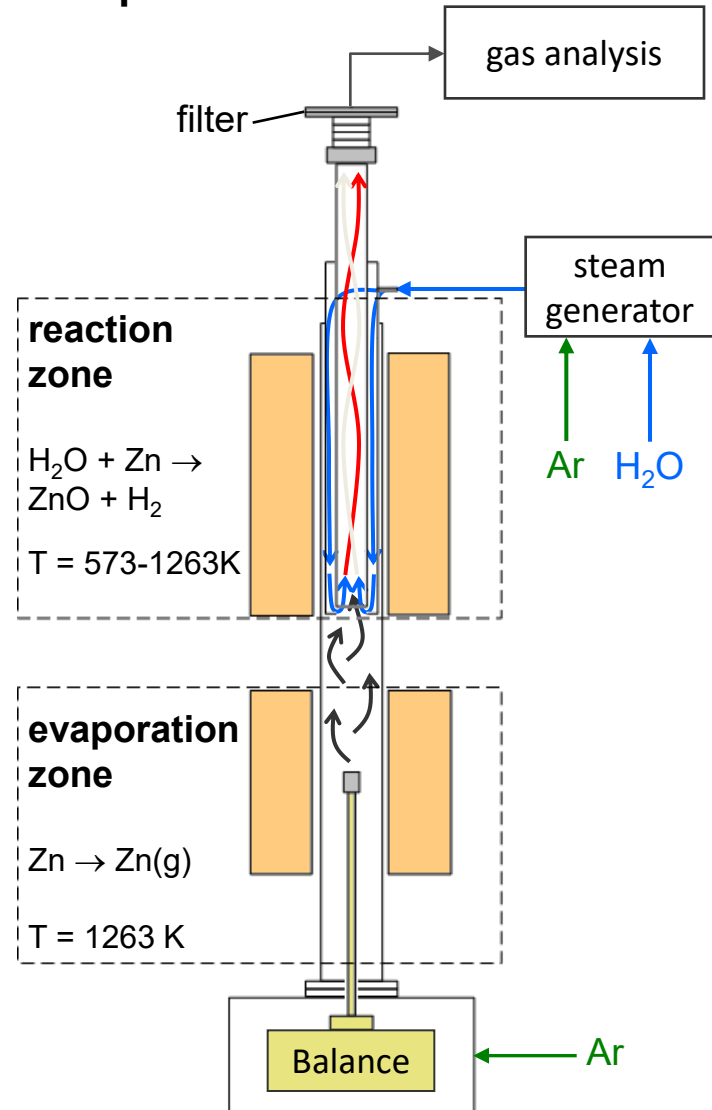


- $T_{\text{reactor}} = 2000 \text{ K}$
- $Q_{\text{solar}} = 10 \text{ kW}$
- $C_{\text{peak}} = 5880 \text{ suns}$
- $m_{\text{ZnO}} = 11 \text{ g/min}$
- Zn yield = 50 – 95 %

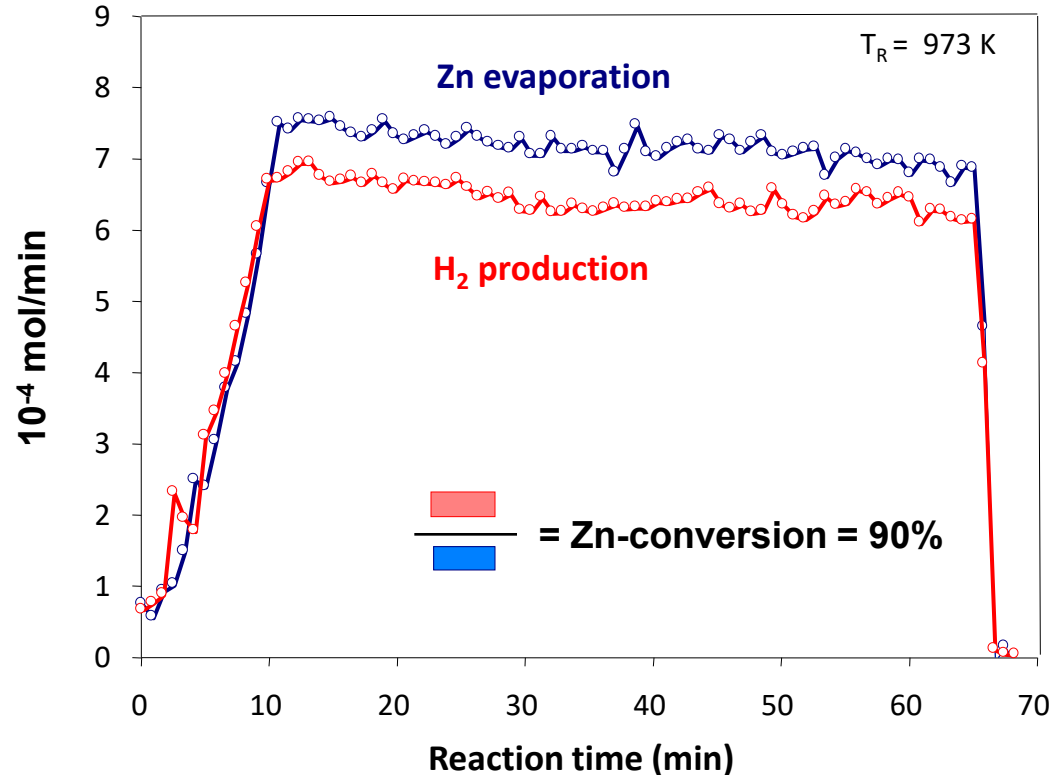
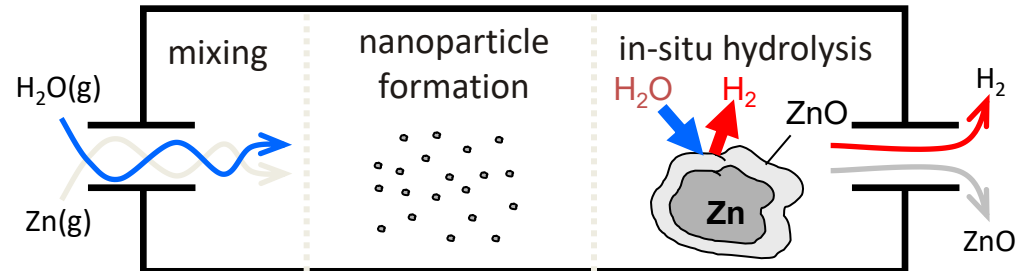


Zn Hydrolysis

Experimental Set-up

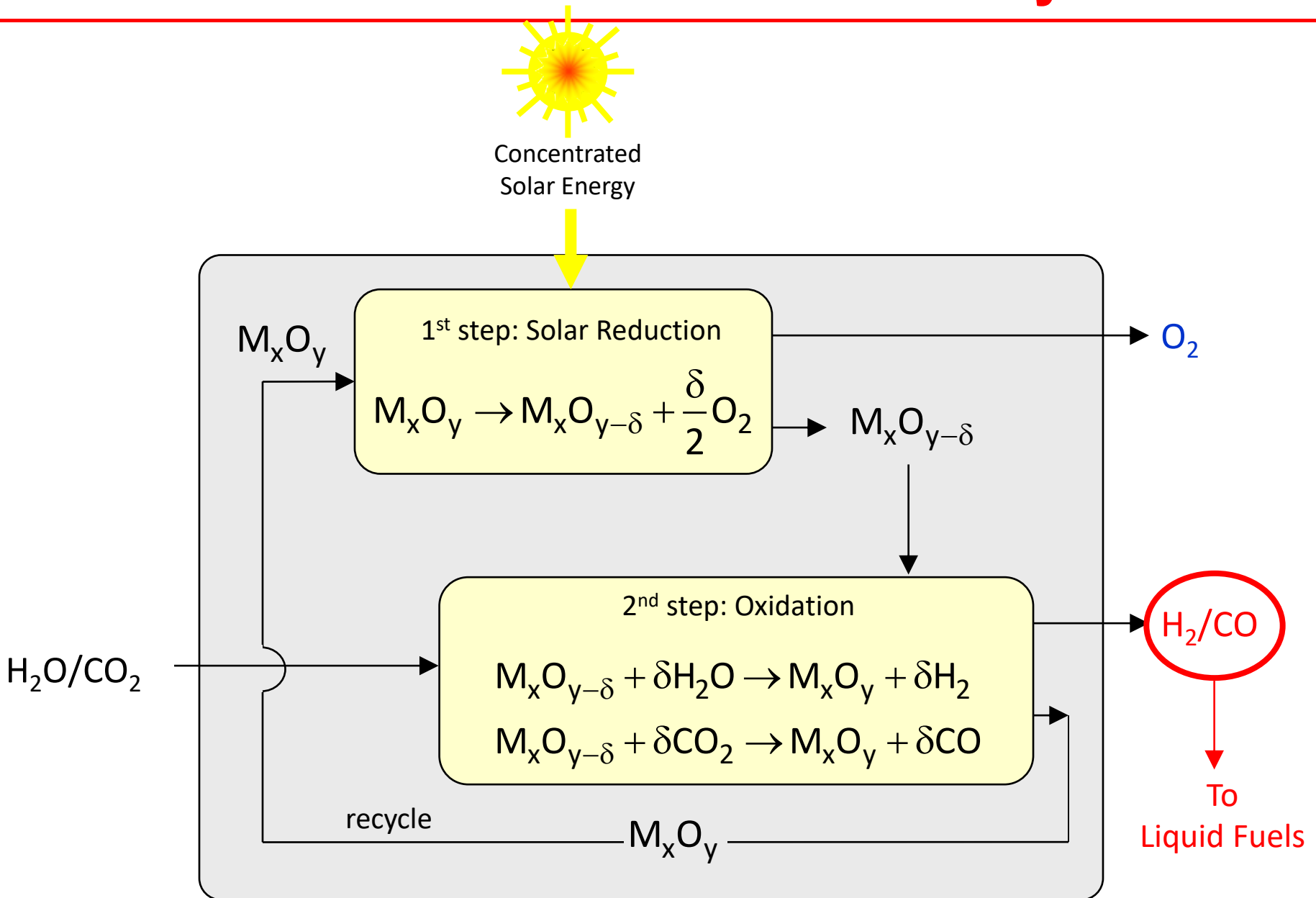


Aerosol reactor concept

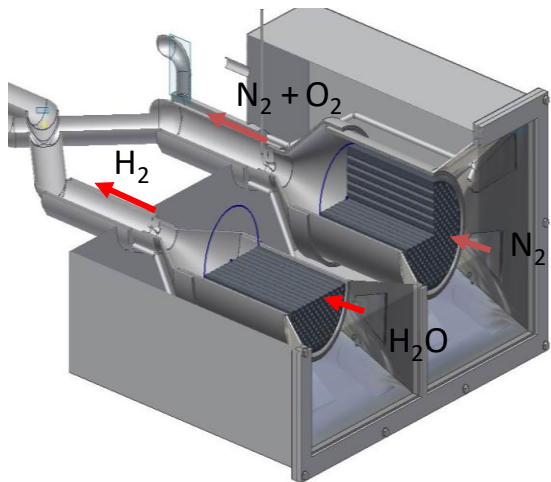
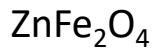


- *AIChE J.* 52, 3297-3303, 2006.
- *Chem. Eng. Sc.* 64, 1095-1101, 2009.

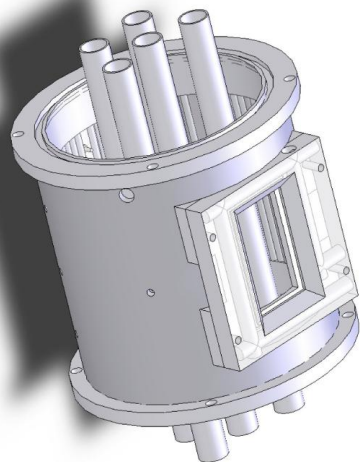
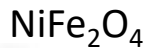
Solar Thermochemical Redox Cycle



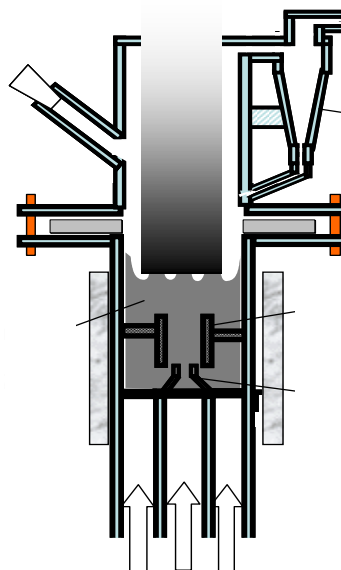
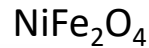
DLR, Germany



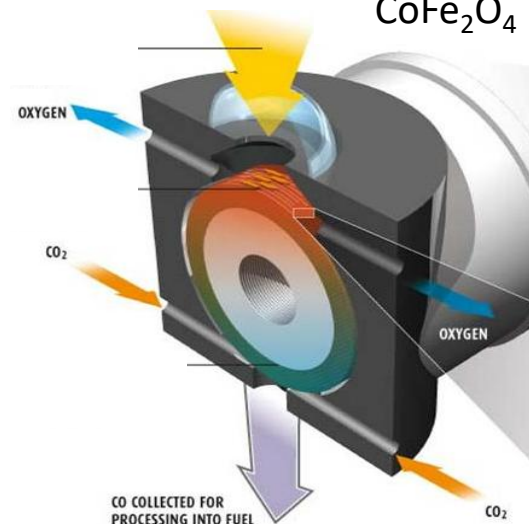
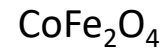
U. of CO, USA



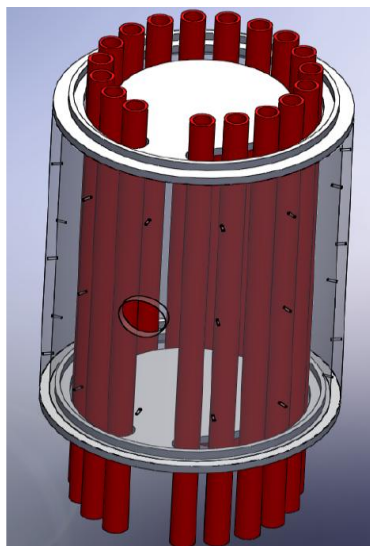
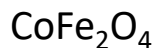
Niigata U., Japan



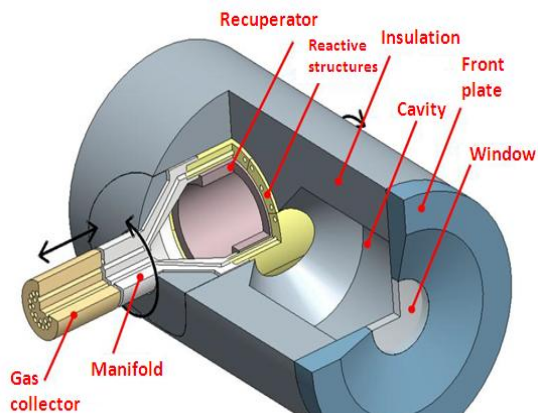
SNL, USA



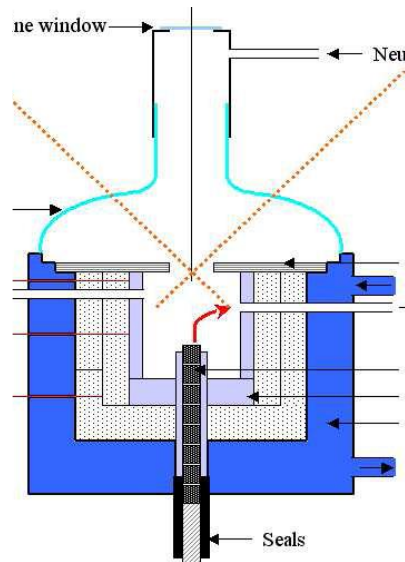
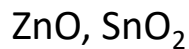
U. of FL, USA



U. of MN, USA



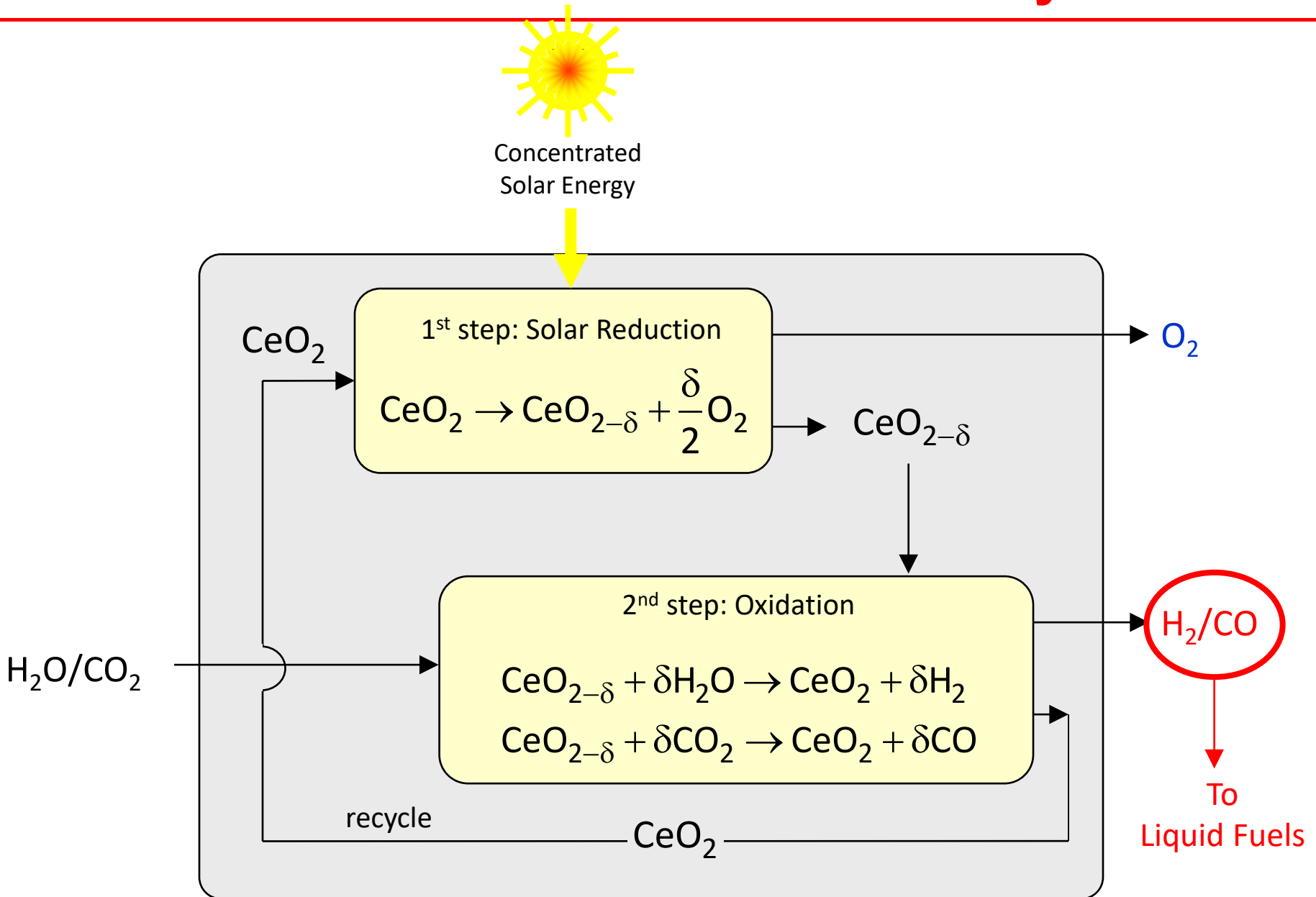
CNRS, France



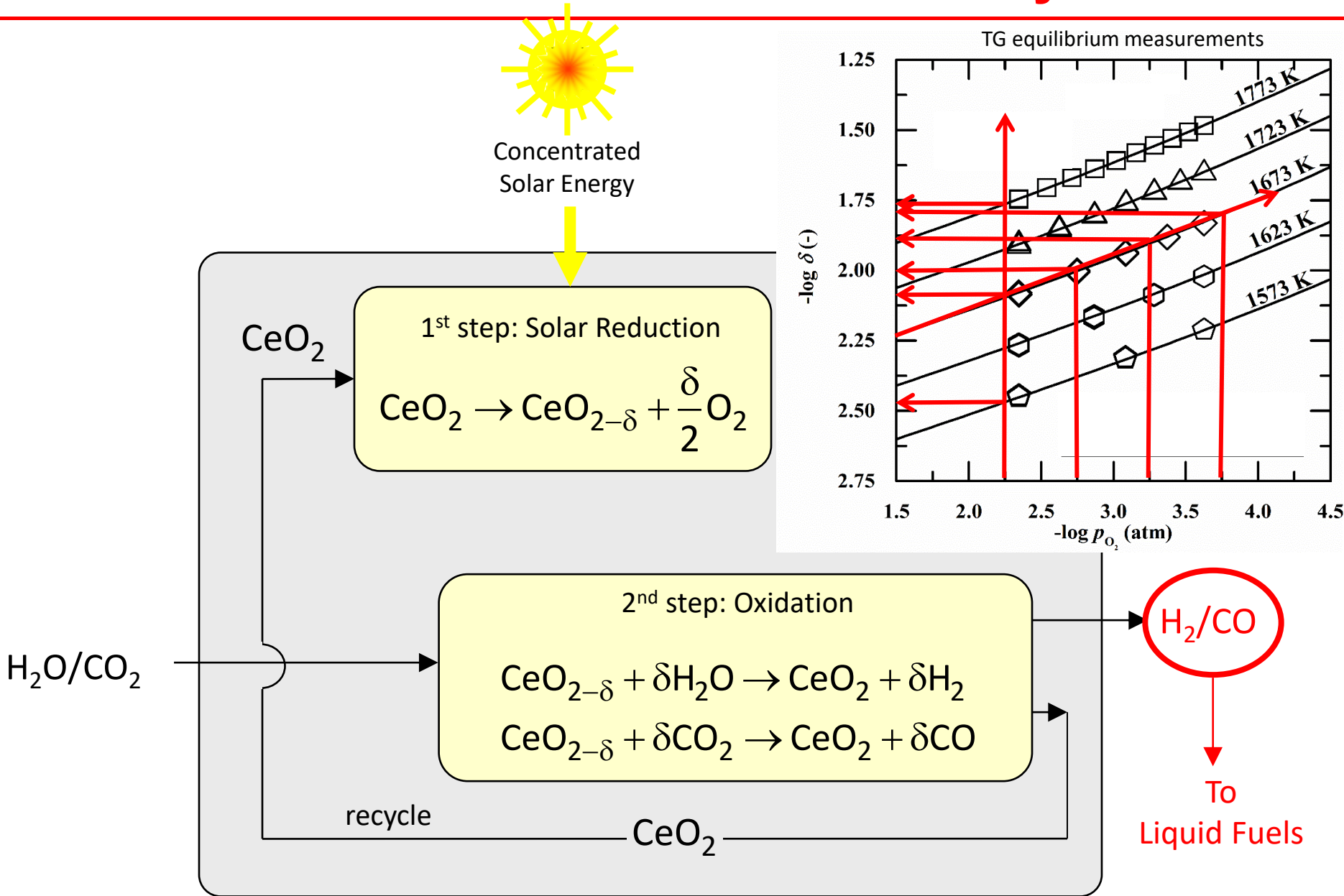
SNL, USA



Solar Thermochemical Redox Cycle

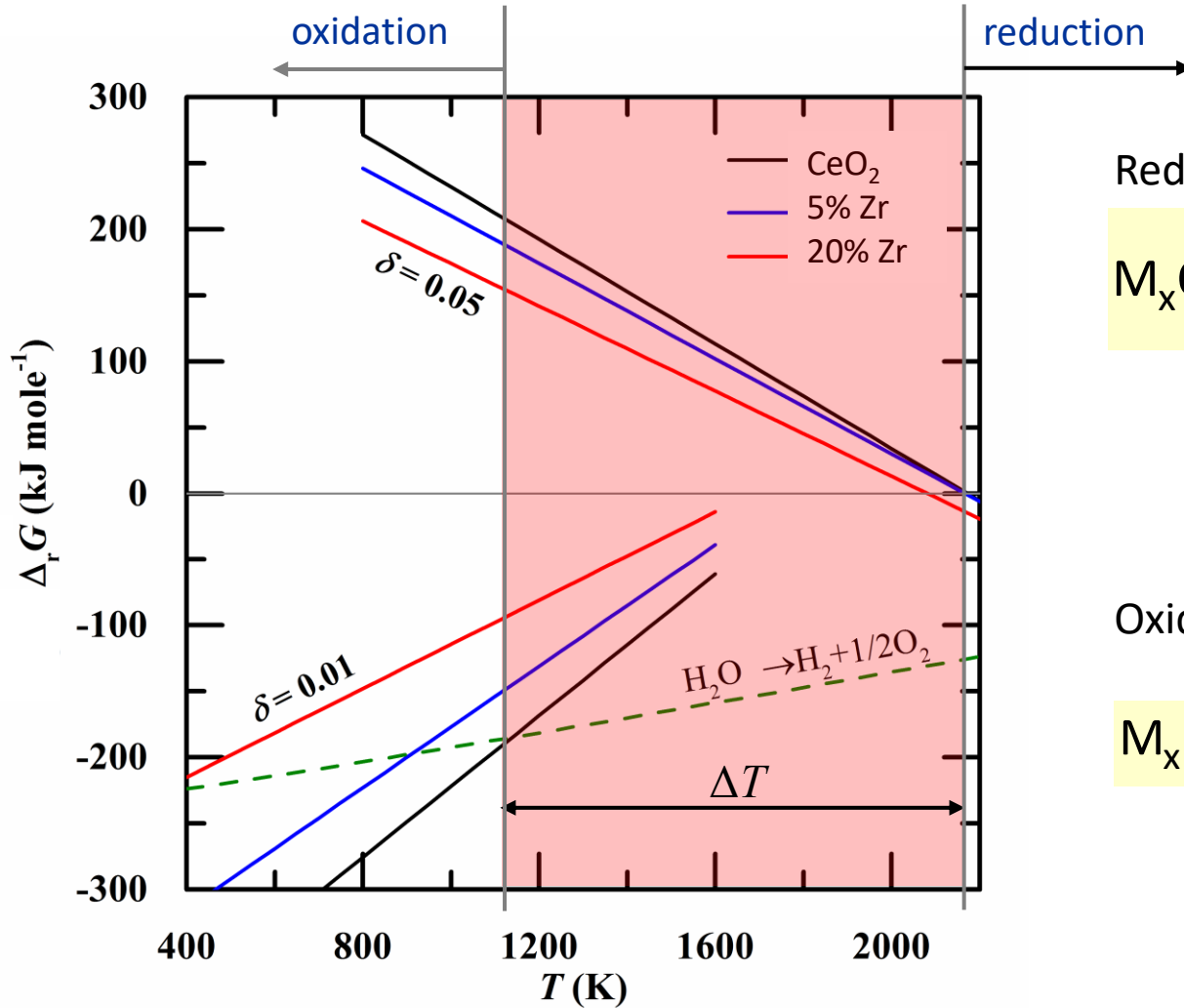


Solar Thermochemical Redox Cycle

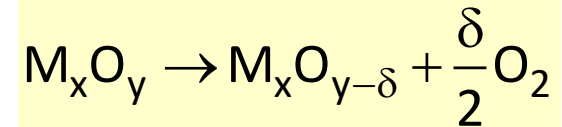


Redox Material

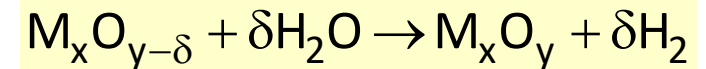
- Ellingham Diagrams



Reduction



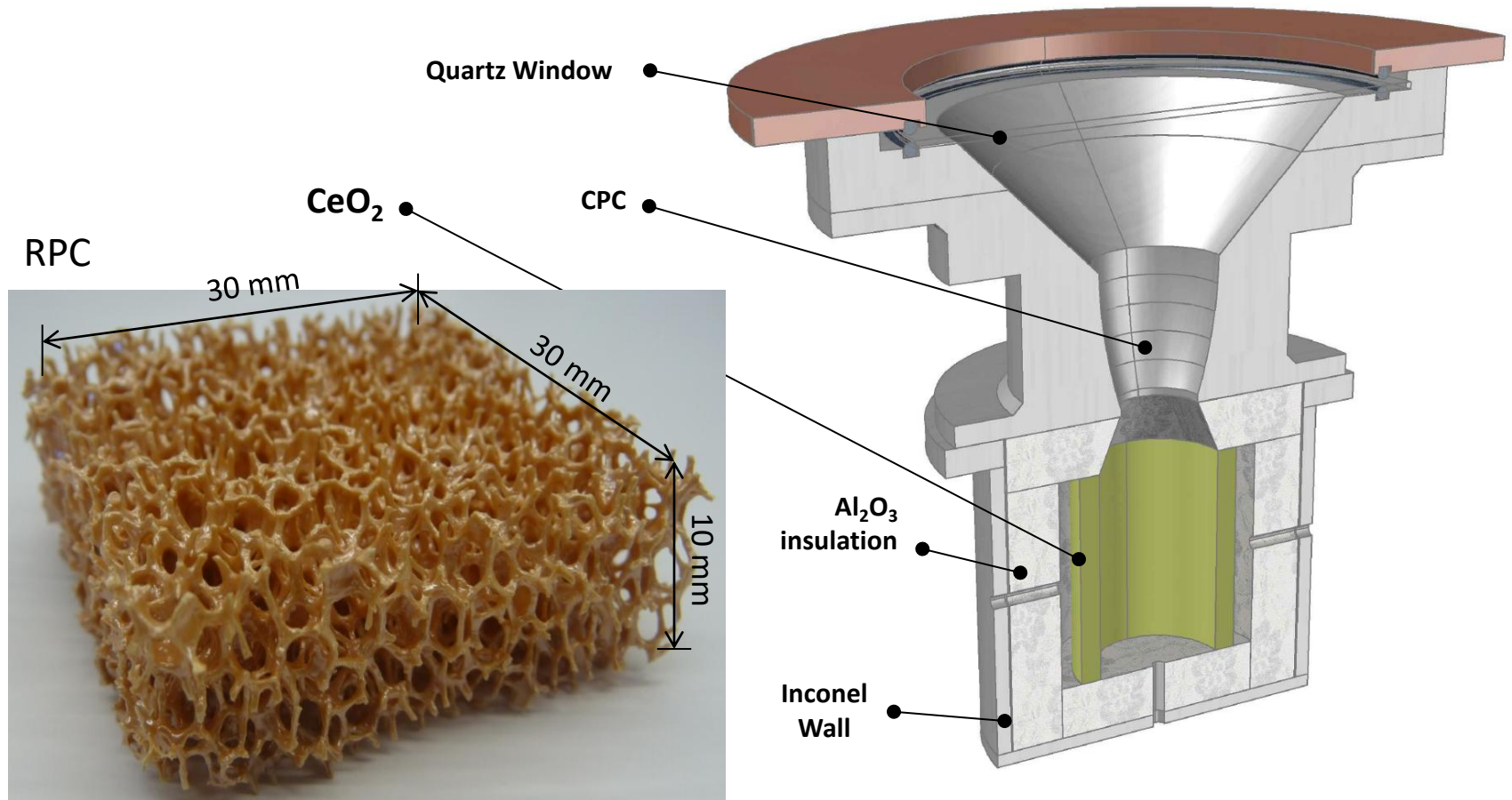
Oxidation



• Phys Chem Chem Physics 17, 7813-7822, 2015.

• Acta Materialia 103, pp. 700-710, 2016.

Solar Reactor Technology

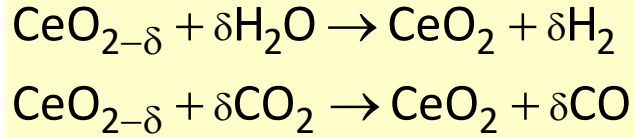


- Science 330, 1797-1801, 2010.
- Energy & Env. Science 5, 6098-6103, 2012.
- Energy & Fuels 26, 7051-7059, 2012.

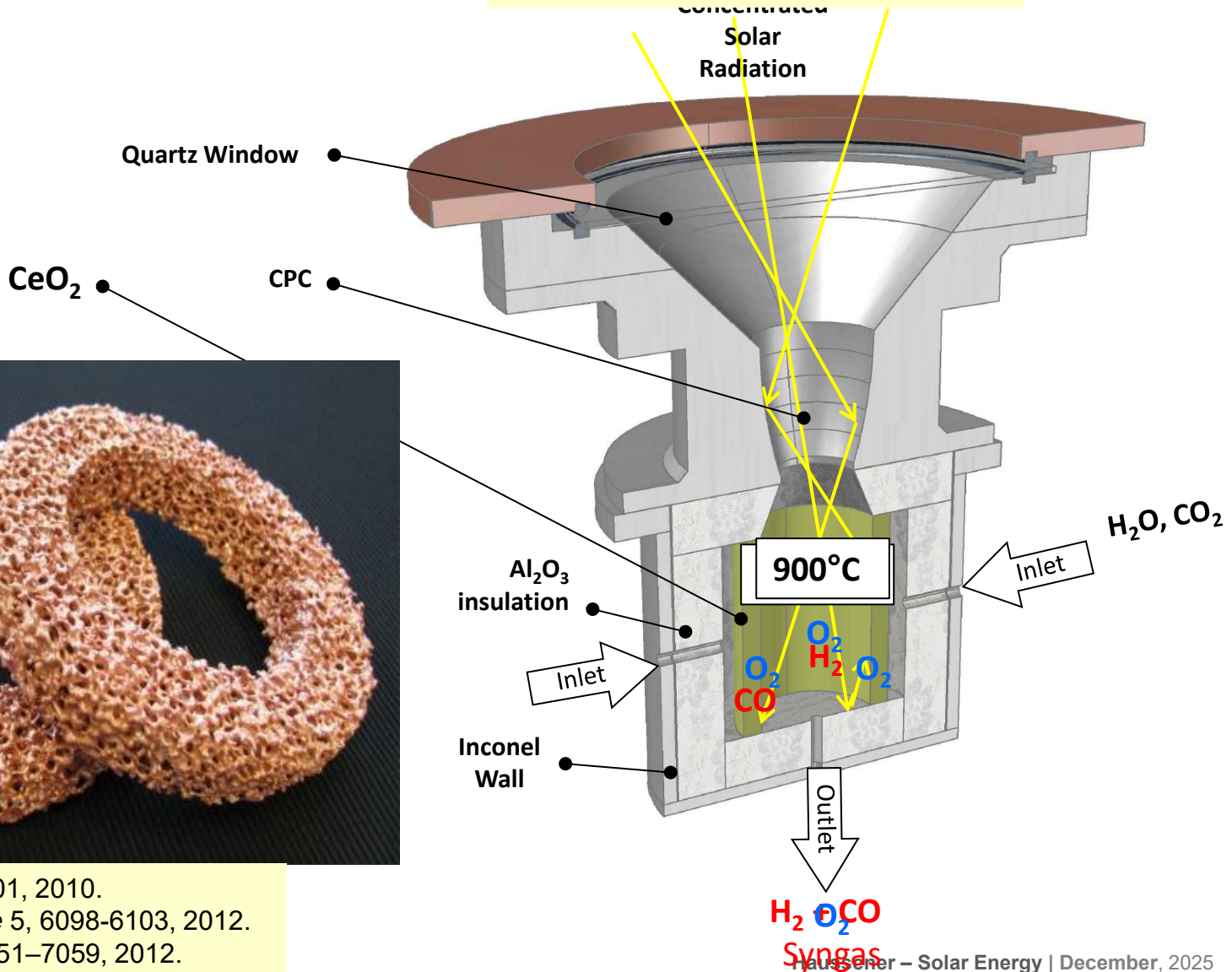
Solar Reactor Technology



2nd step: Oxidation



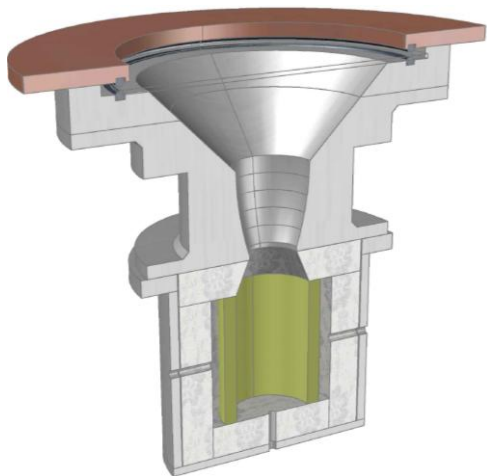
RPC



- Science 330, 1797-1801, 2010.
- Energy & Env. Science 5, 6098-6103, 2012.
- Energy & Fuels 26, 7051-7059, 2012.

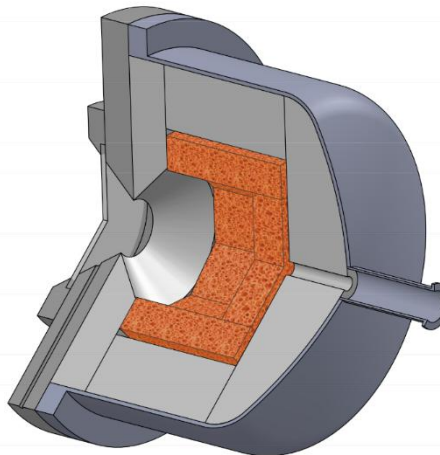
Solar Reactor Technology

Generation 0
2 kW Lab-scale
Monoliths



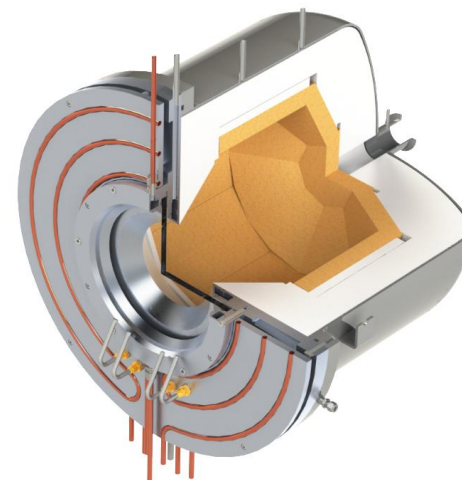
• Science 330, 1797-1801, 2010.

Generation 1
4 kW Lab-scale
RPC



• Energy & Env. Science 10;1142-1149, 2017.

Generation 2
50 kW Pilot-scale
RPC

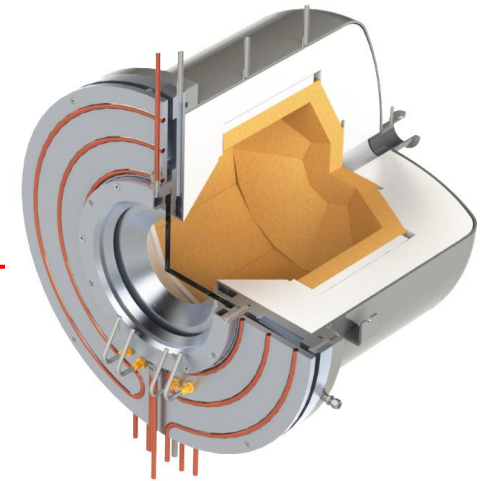


Solar Reactor Technology

EU Sun-to-Liquid Project

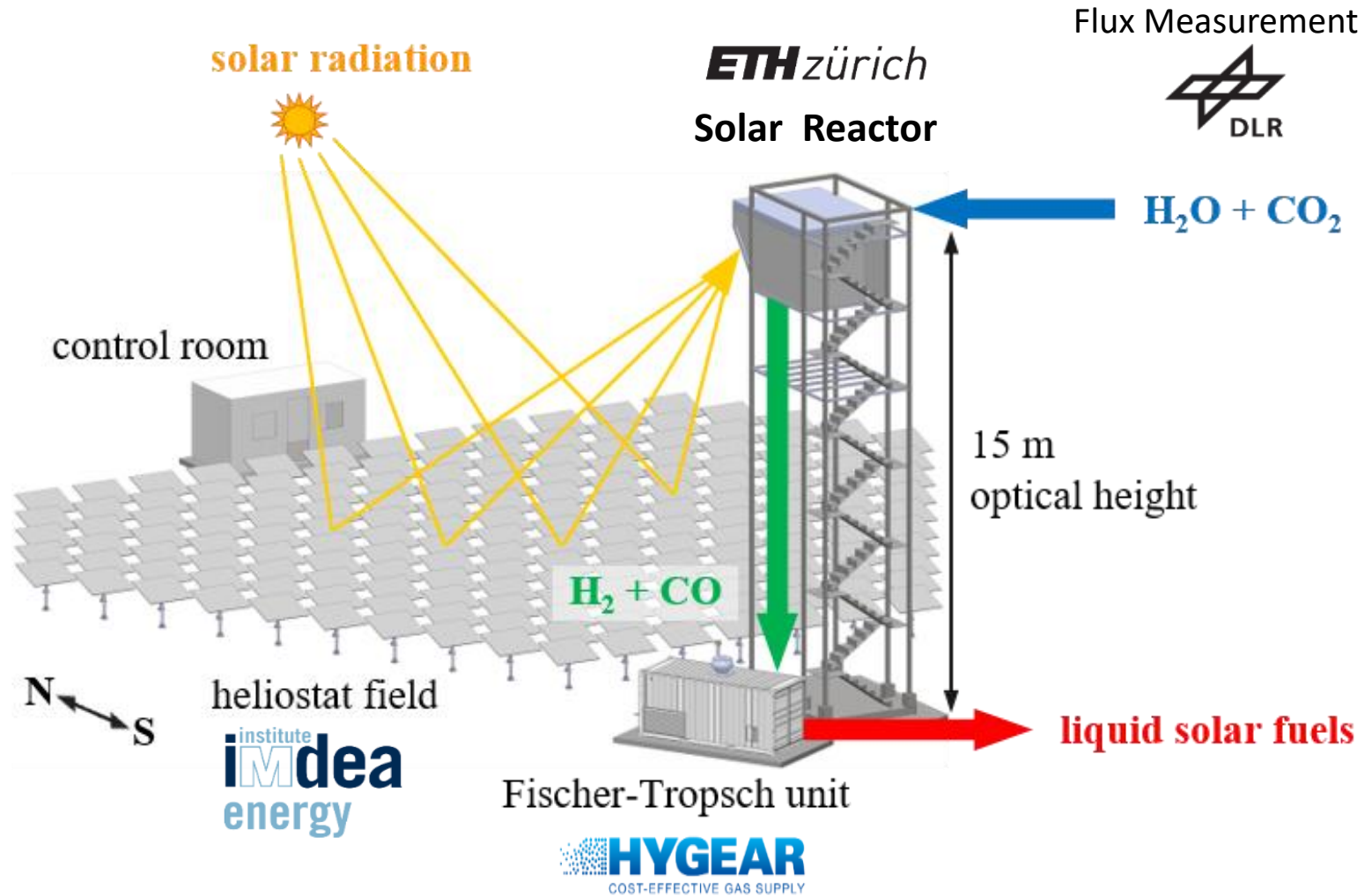


Generation 2
50 kW Pilot-scale
RPC



www.sun-to-liquid.eu

EU Sun-to-Liquid Project



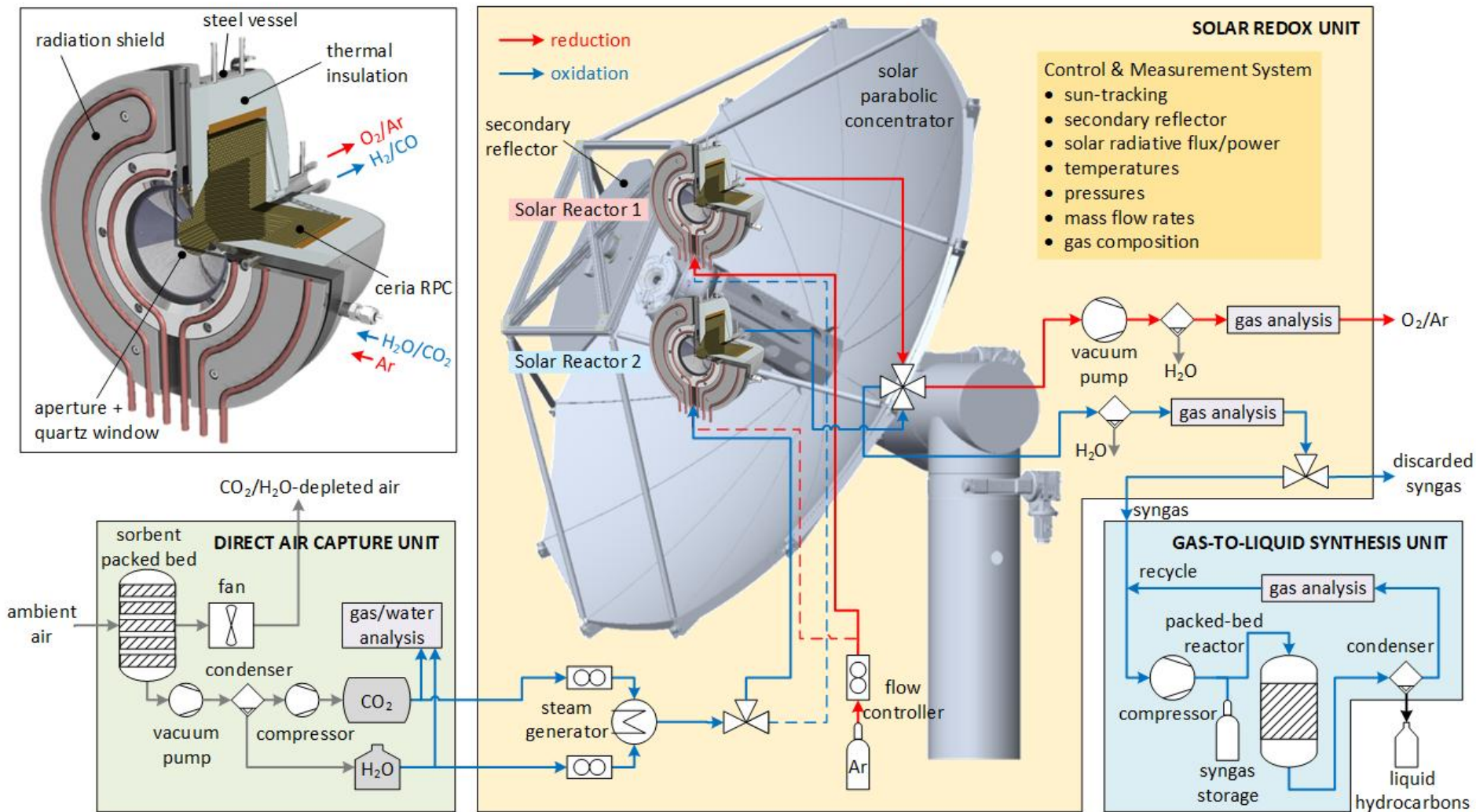
Fuels from Sunlight and Air

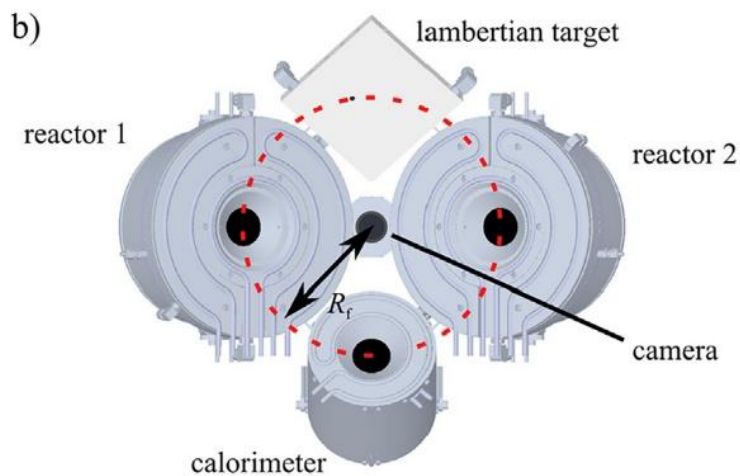
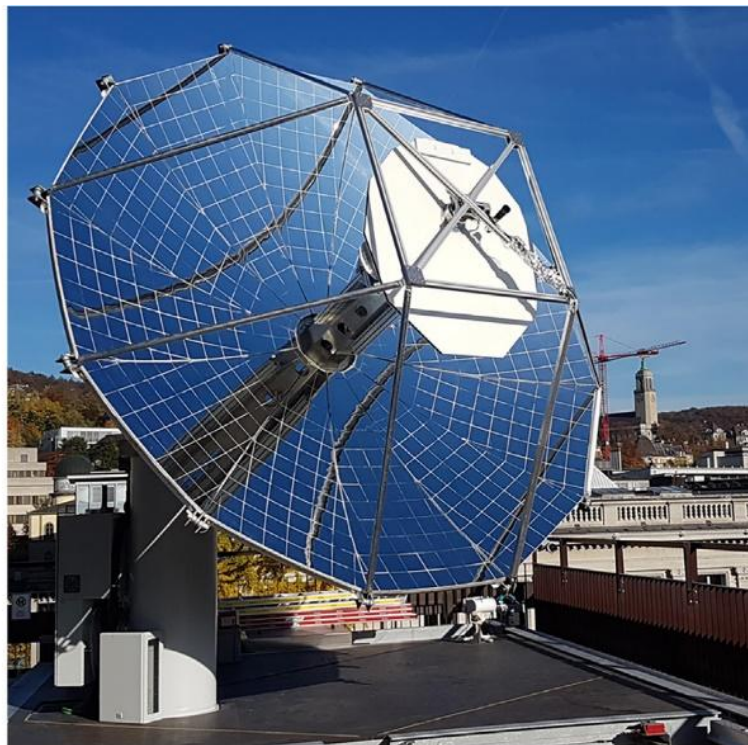
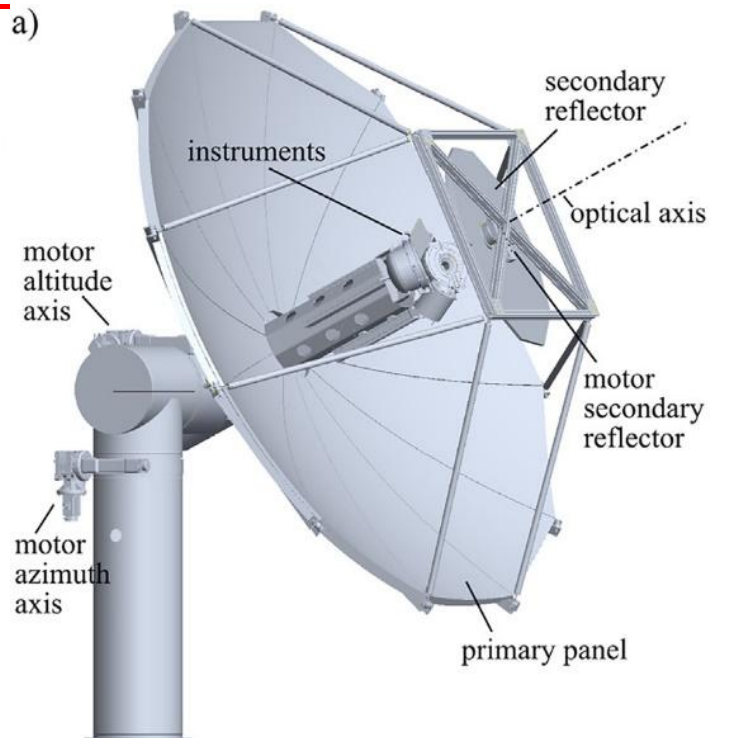
1st-ever production of carbon-neutral hydrocarbon fuels from sunlight and air

13-6-2019



Solar Mini-Refinery @ ETH

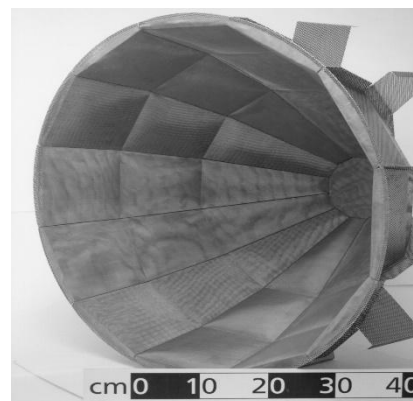
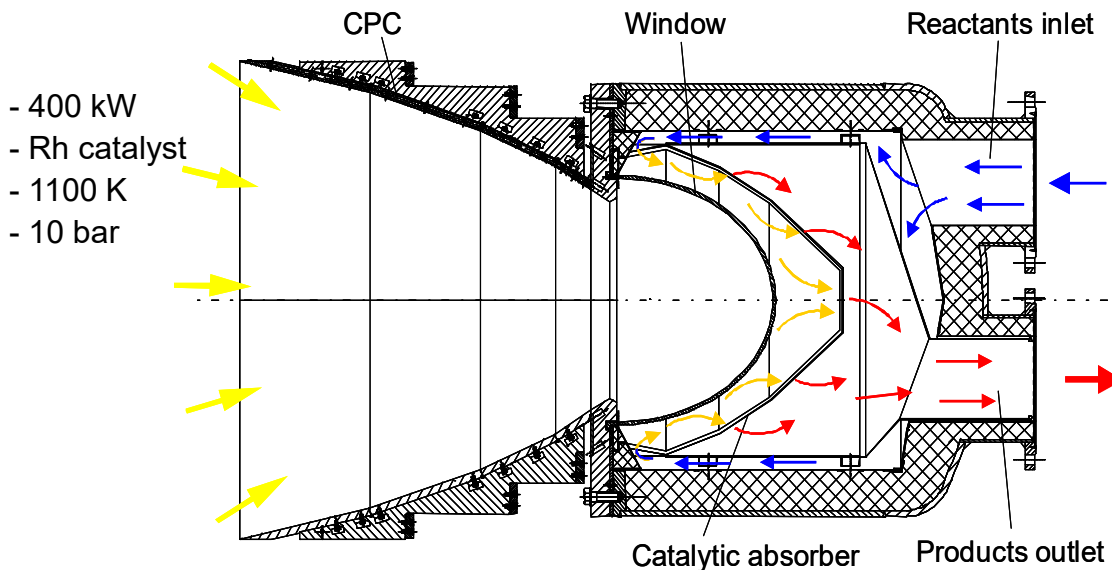
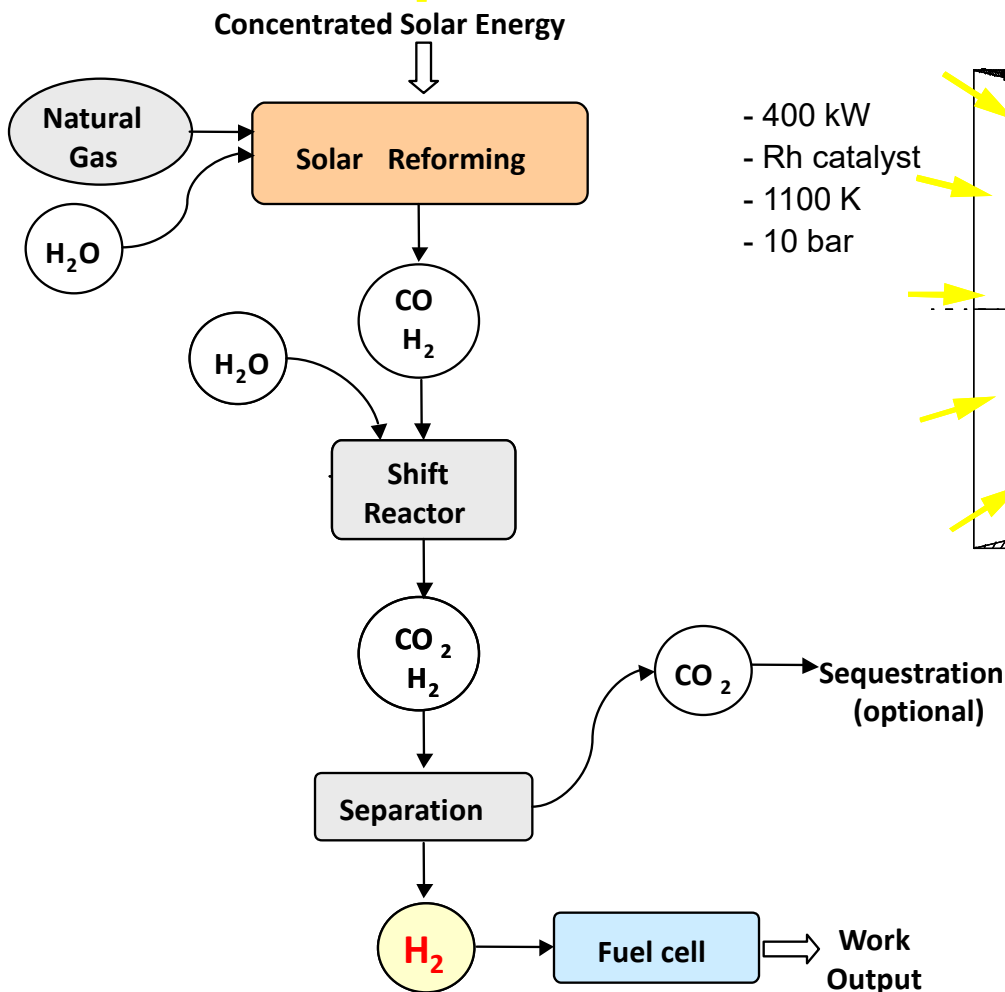
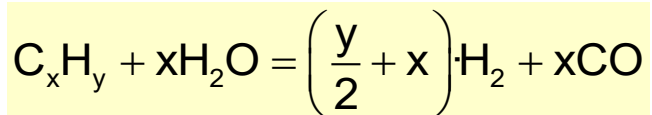
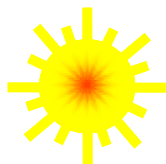




Solar Reforming

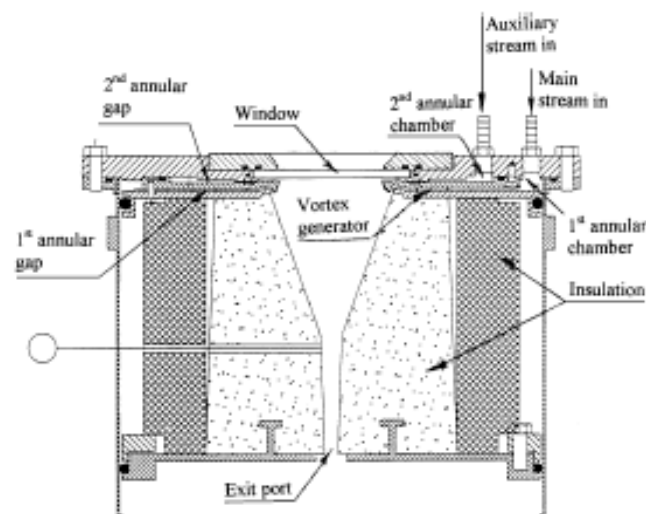
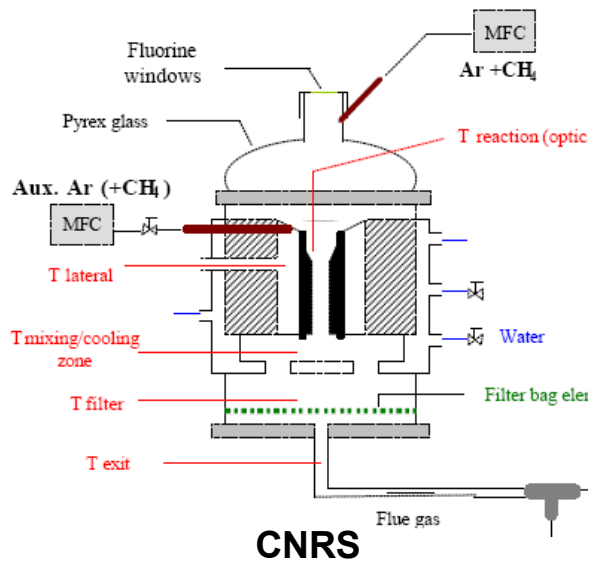
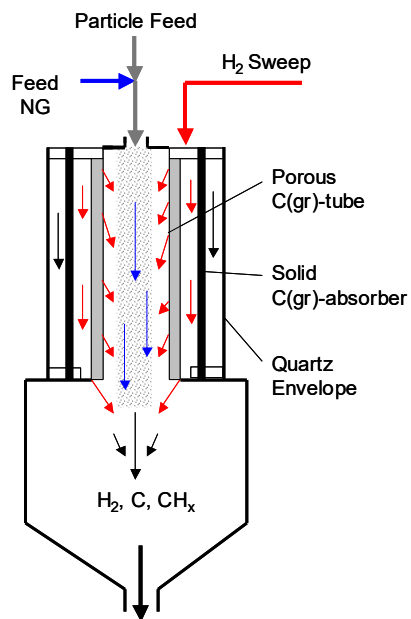
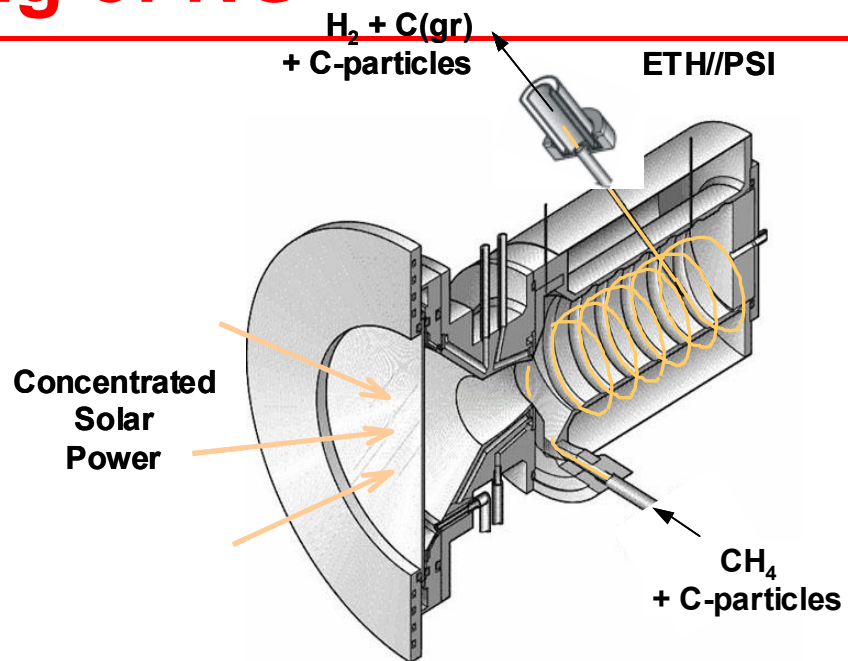
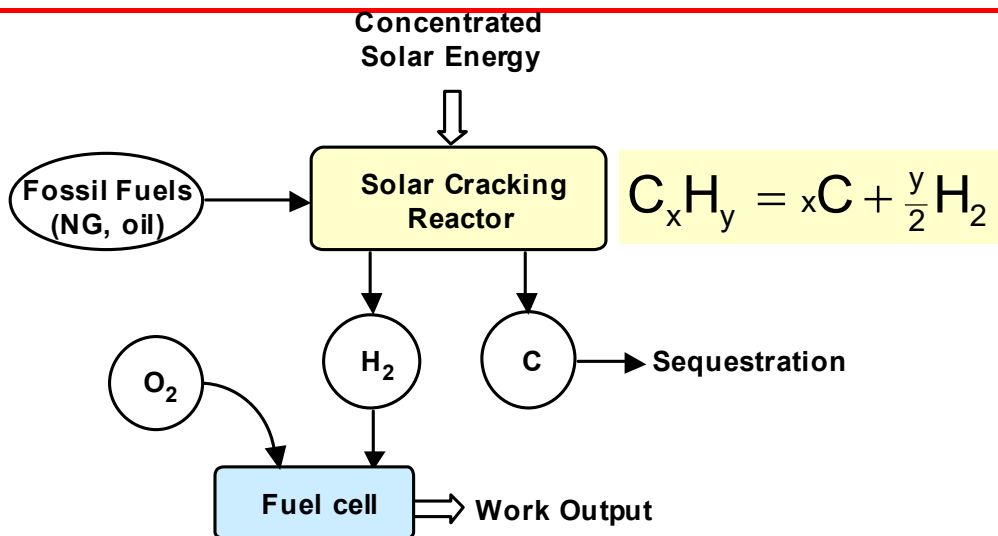
Solar Reforming

EU-Project SOLREF: DLR (D), WIS (IL), Hexion (NE), JM (UK), CERTH (GR), ESCO (I), ETH/PSI (CH)



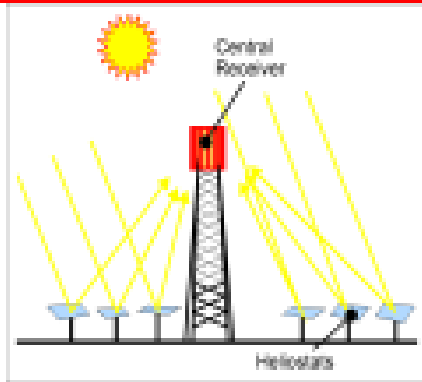
Solar Cracking

Solar Cracking of NG

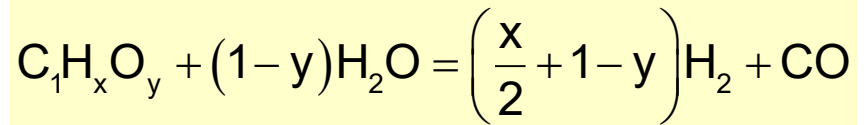
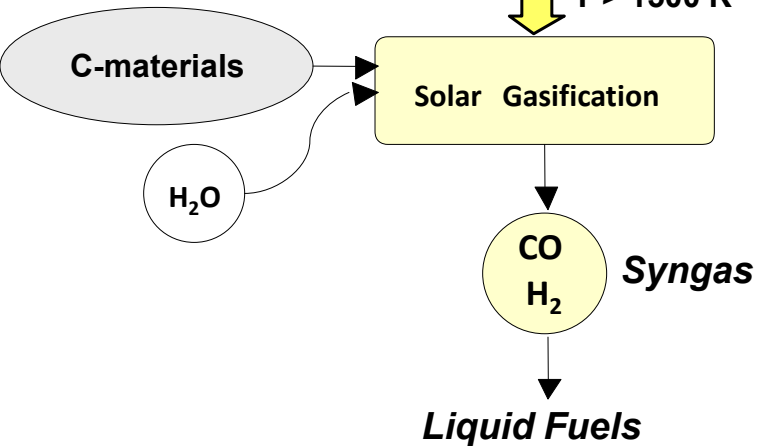


Solar Gasification

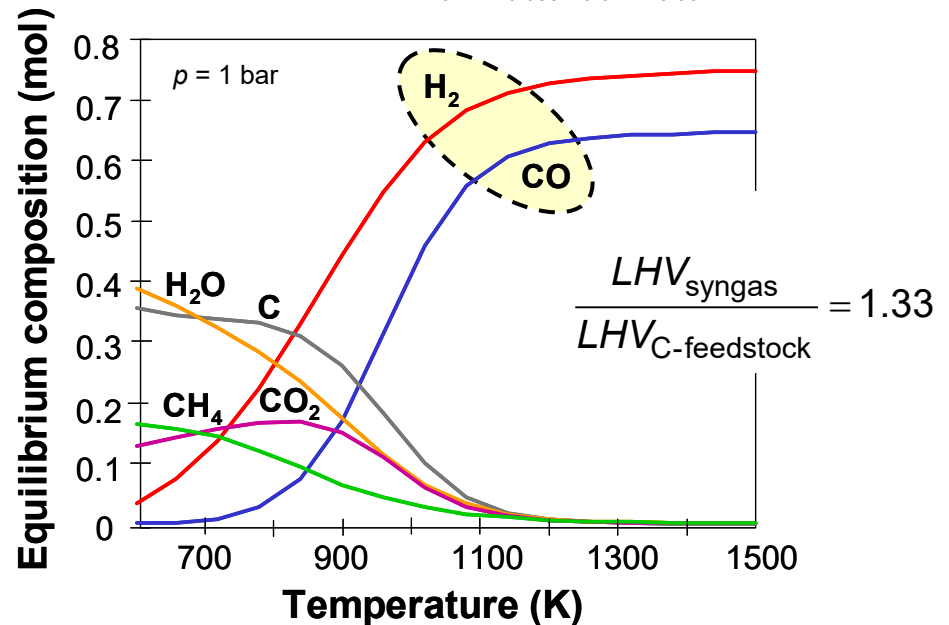
Solar Gasification



Concentrated Solar Radiation
 $T > 1500 \text{ K}$



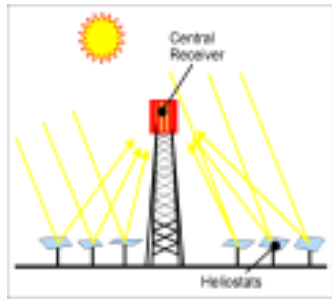
Beech charcoal $\text{C}_1\text{H}_{0.47}\text{O}_{0.055}\text{S}_{0.022}\text{N}_{0.004}$



Vis-à-vis autothermal:

- Syngas with higher calorific value and lower CO₂ intensity
- Higher syngas output per unit of feedstock
- Higher quality of the syngas produced
- Elimination of air-separation unit

Solar Gasification



Concentrated Solar Power

$$\eta = \frac{\text{Work Output}}{Q_{\text{solar}} + HV_{\text{coke}}}$$

Rankine

$\eta = 35\%$

$E = 3.5 \text{ kWh}_e/\text{kg}$

Coal

Solar Gasification

Syngas

CC

H_2

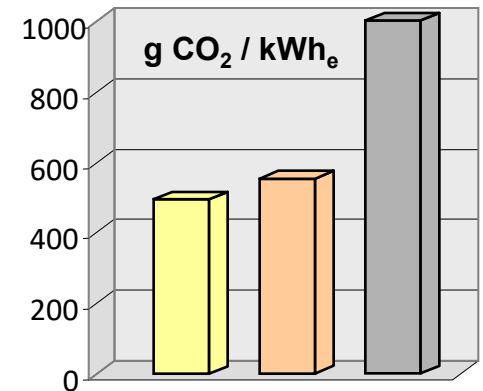
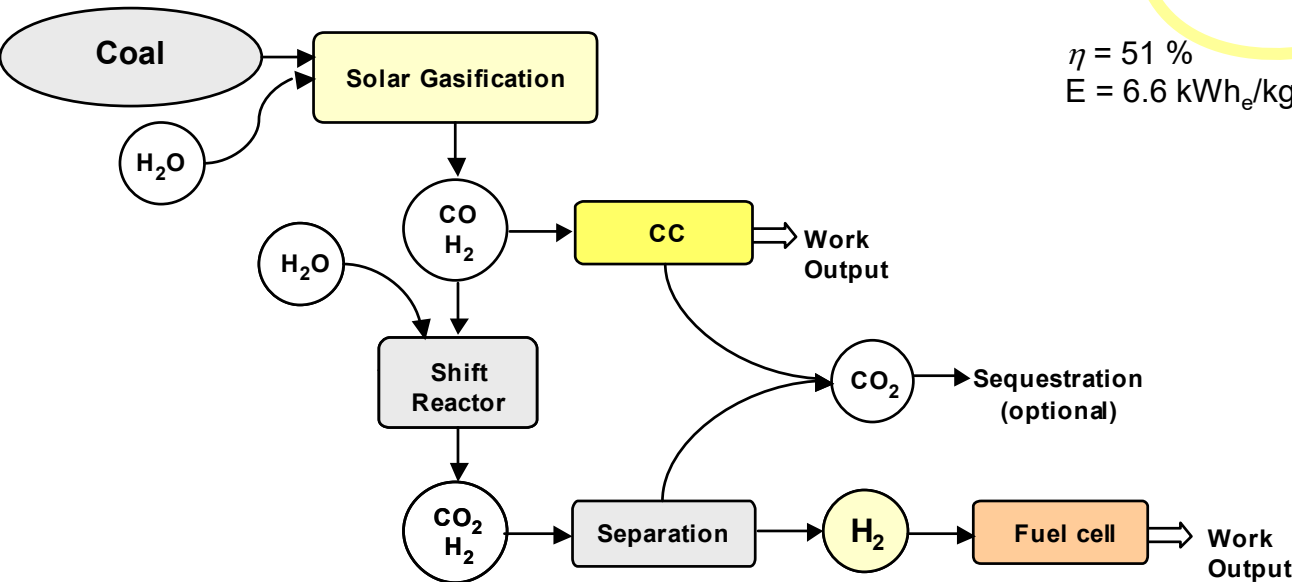
FC

$\eta = 51\%$

$E = 6.6 \text{ kWh}_e/\text{kg}$

$\eta = 46\%$

$E = 6.1 \text{ kWh}_e/\text{kg}$



■ Coal-gasification to syngas + 55%- η CC

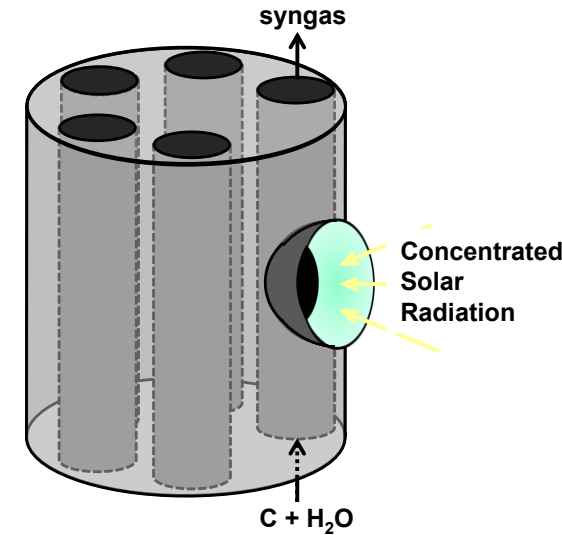
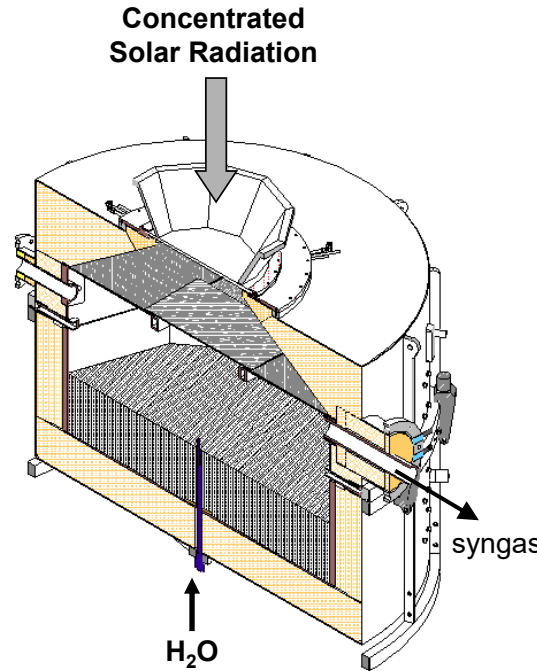
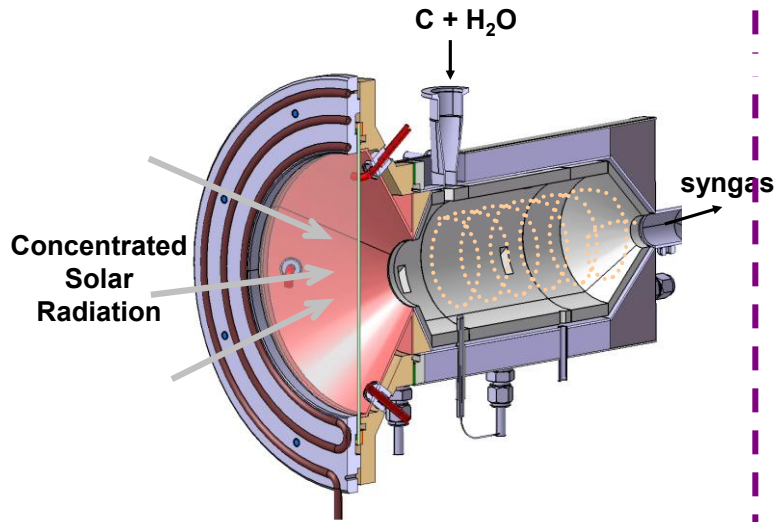
■ Coal-gasification to H₂ + 60%- η fuel cell





■ Coal-combustion + 35%- η Rankine cycle

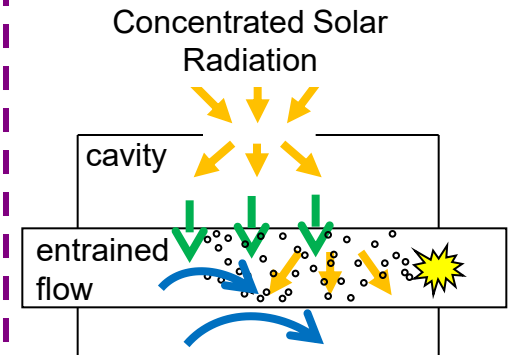
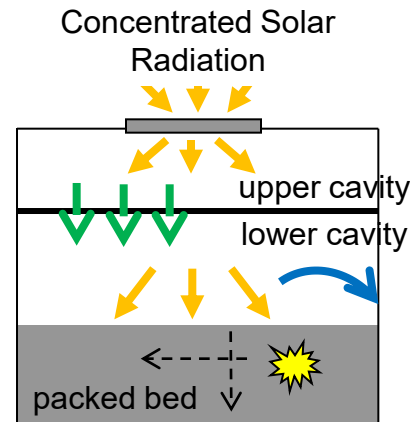
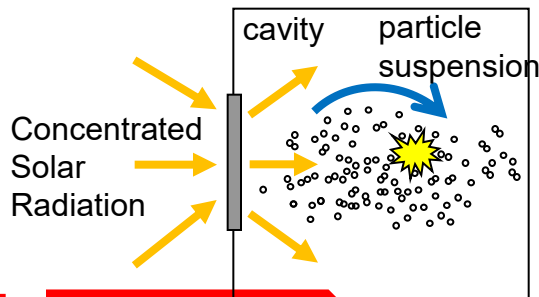
Solar Reactor Concepts

Direct-irradiation

Indirect-irradiation



-  convective heat transfer
-  conductive heat transfer
-  radiative heat transfer
-  chemical reaction

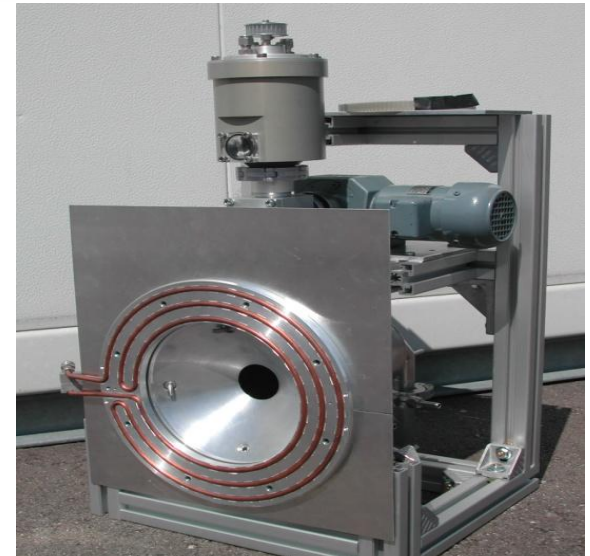
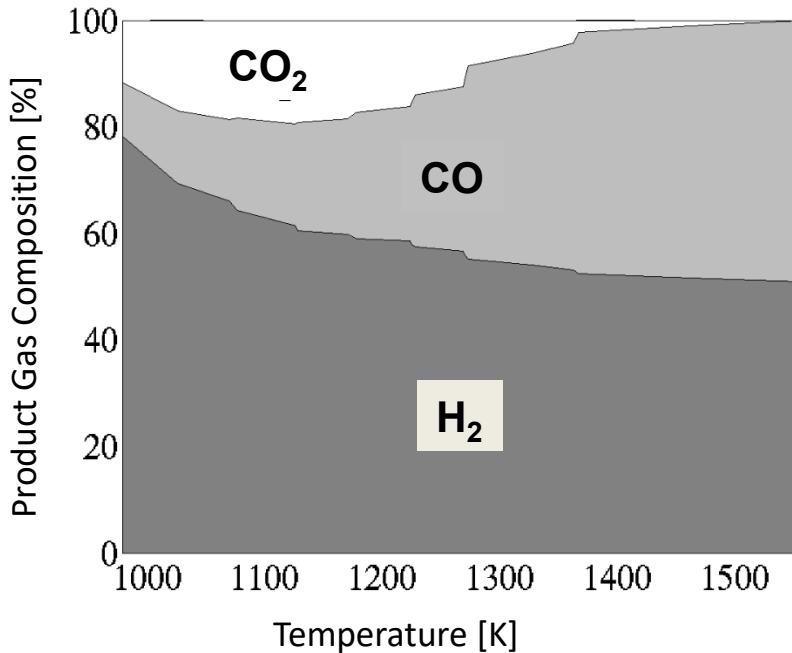
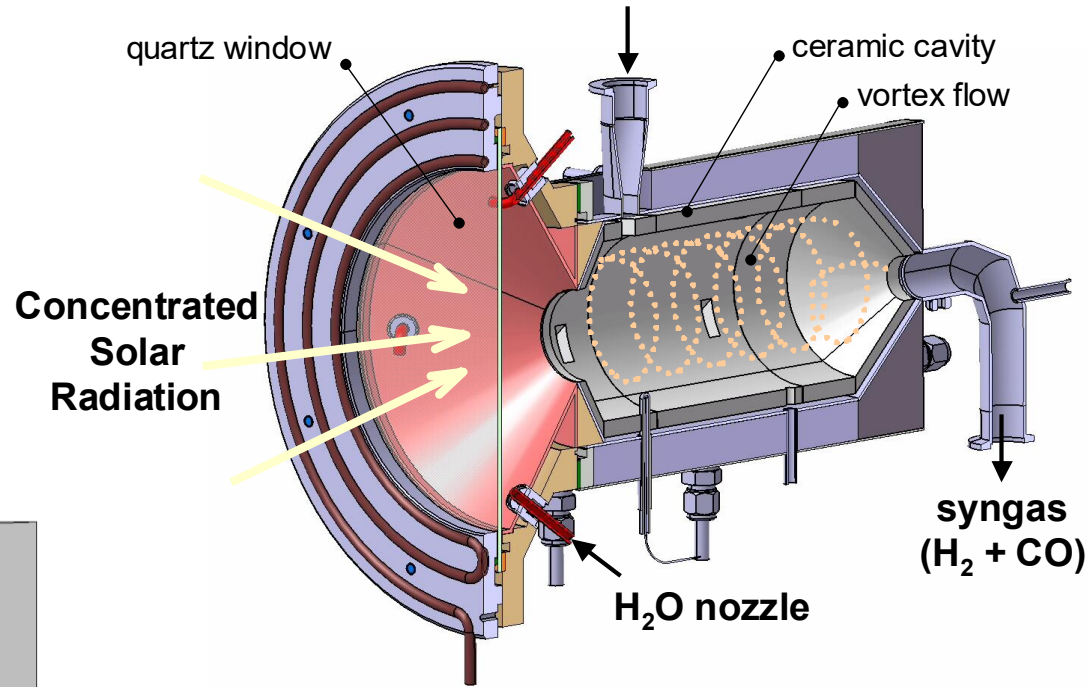


Solar Vortex Reactor

Petcoke + H₂O slurry



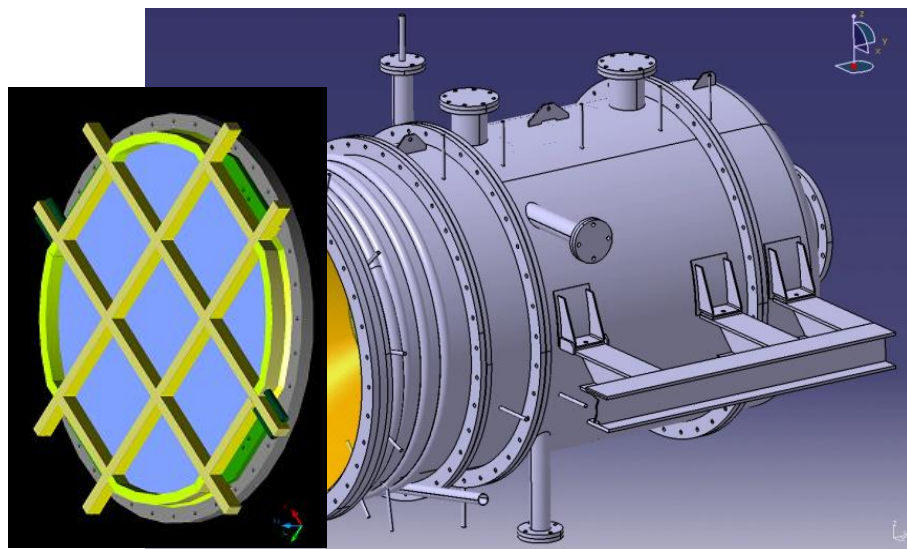
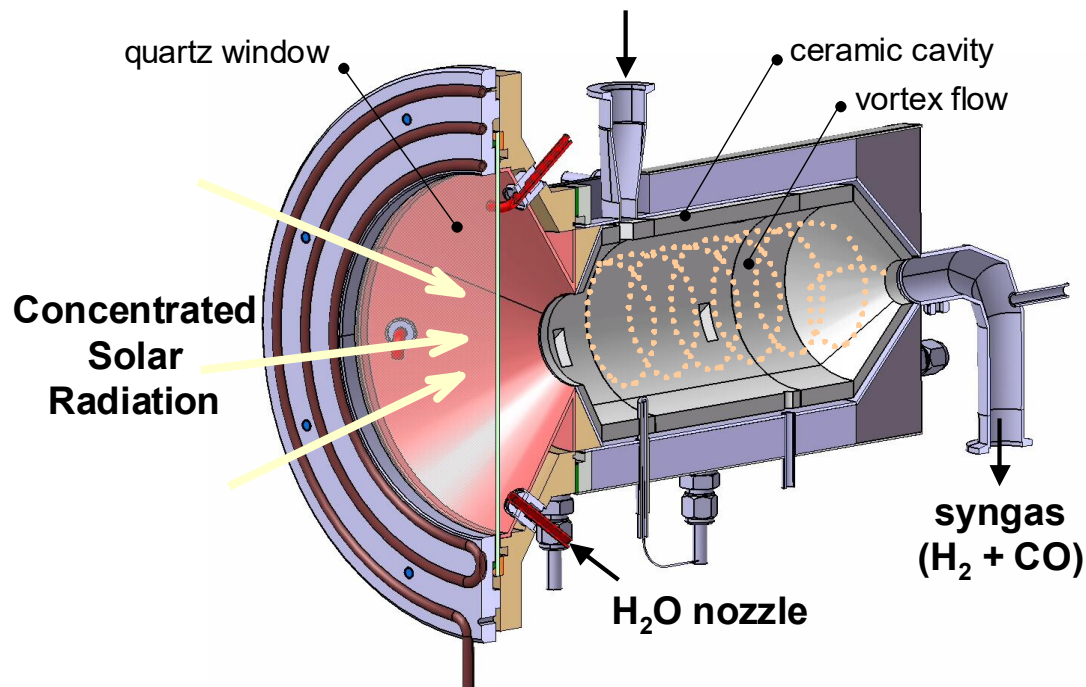
- $Q_{solar} = 5 \text{ kW}$
- $C = 3000 \text{ suns}$
- $m_C = 4 \text{ g/min}$
- $T_{reactor} = 1600 \text{ K}$
- $x_C = 87 \%$
- $\eta_{thermal} = 19 \%$



Solar Vortex Reactor – 500 kW

Petcoke + H₂O slurry

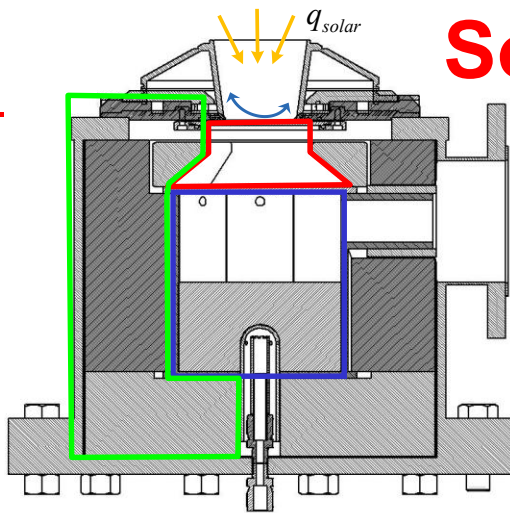
- Reaction temperature:
 - T = 1400-1700 K
- Material flows:
 - $m_{\text{petcoke}} = 30\text{-}50 \text{ kg/h}$
 - $m_{\text{water}} = 60\text{-}100 \text{ kg/h}$
- Syngas production:
 - $m_{\text{syngas}} = 100\text{-}180 \text{ Nm}^3/\text{h}$



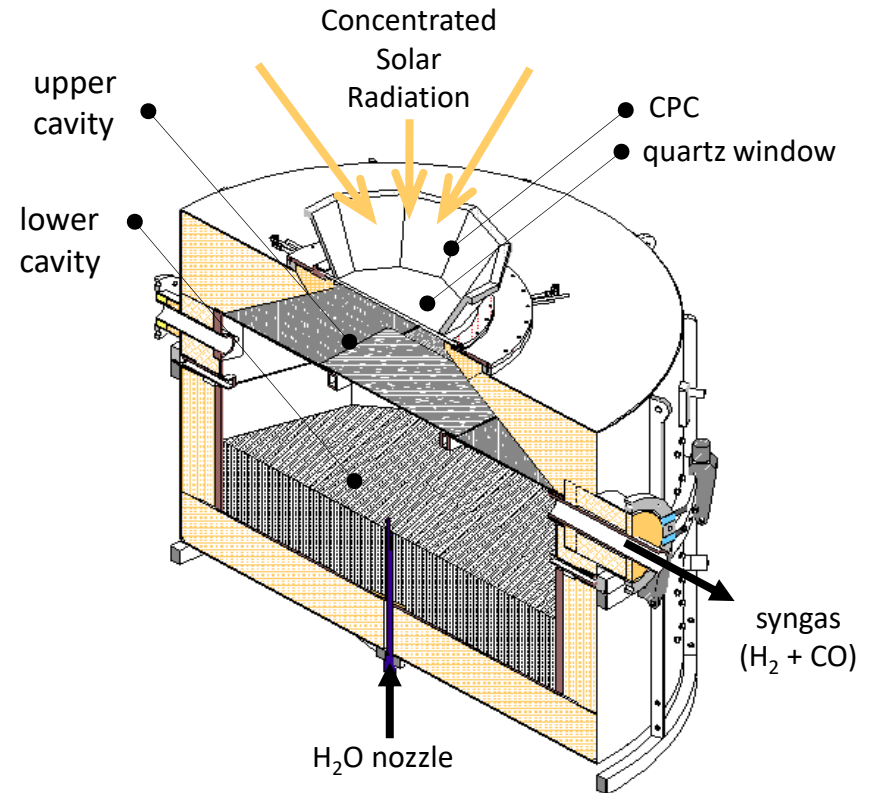
PSA



Solar Two-Cavity Reactor

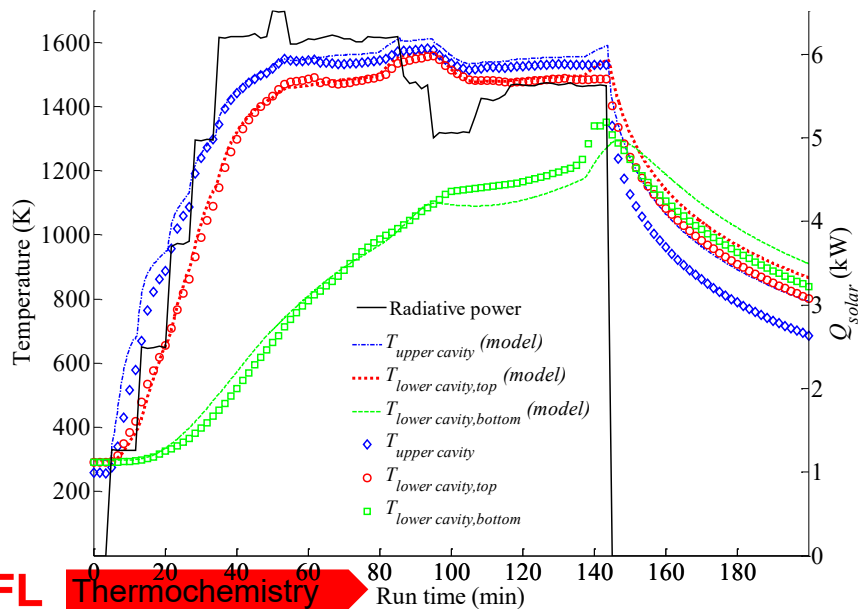


Solar Reactor Technology



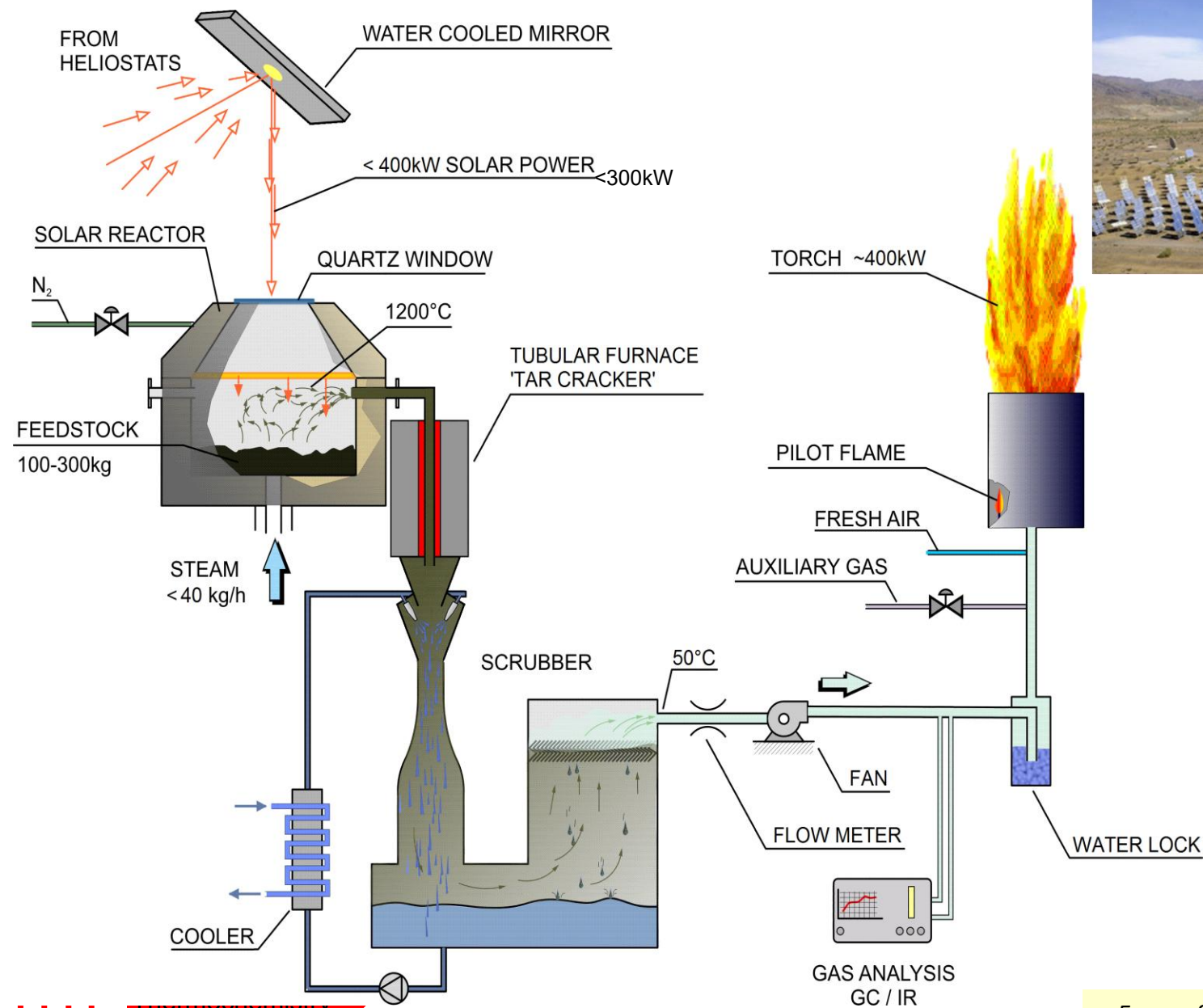
$$\rho c_p \frac{\partial T}{\partial t} = \underbrace{\nabla(k_{\text{eff}} \nabla T)}_{\text{heat transfer}} - \underbrace{k_0 e^{-\frac{E_A}{RT}} \cdot \Delta H_r(T)}_{\text{chemistry}}$$

Beech charcoal



- Fuel 89, 1133–1140, 2010.
- AIChE Journal 57, 3522–3533, 2011.

Solar Two-Cavity Reactor – 250 kW



Solar Gasification Pilot Plant



Holcim



Beech charcoal



Low Rank Coal



Tire chips



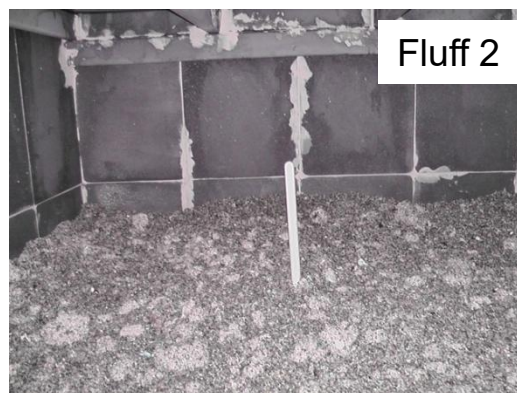
Fluff 1



Industrial sludge 1



Dried sewage sludge



Fluff 2



Industrial sludge 2



Bagasse

Solar Gasification Pilot Plant

U, η

Performance indicators

$$U = \frac{m_{\text{syngas}} \cdot LHV_{\text{syngas}}}{m_{\text{feedstock}} \cdot LHV_{\text{feedstock}}}$$

$$\eta_{\text{solar-to-fuel}} = \frac{m_{\text{syngas}} \cdot LHV_{\text{syngas}}}{Q_{\text{solar}} + m_{\text{feedstock}} \cdot LHV_{\text{feedstock}}}$$

