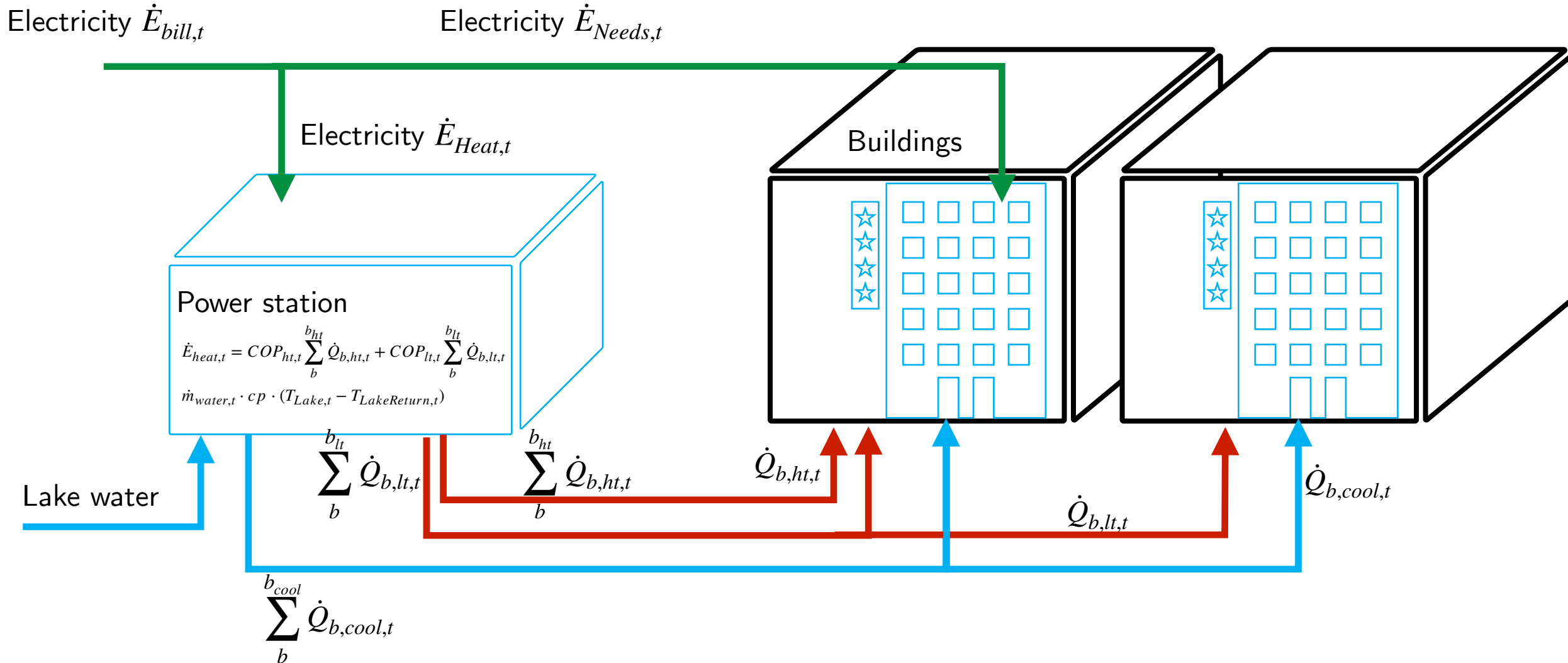
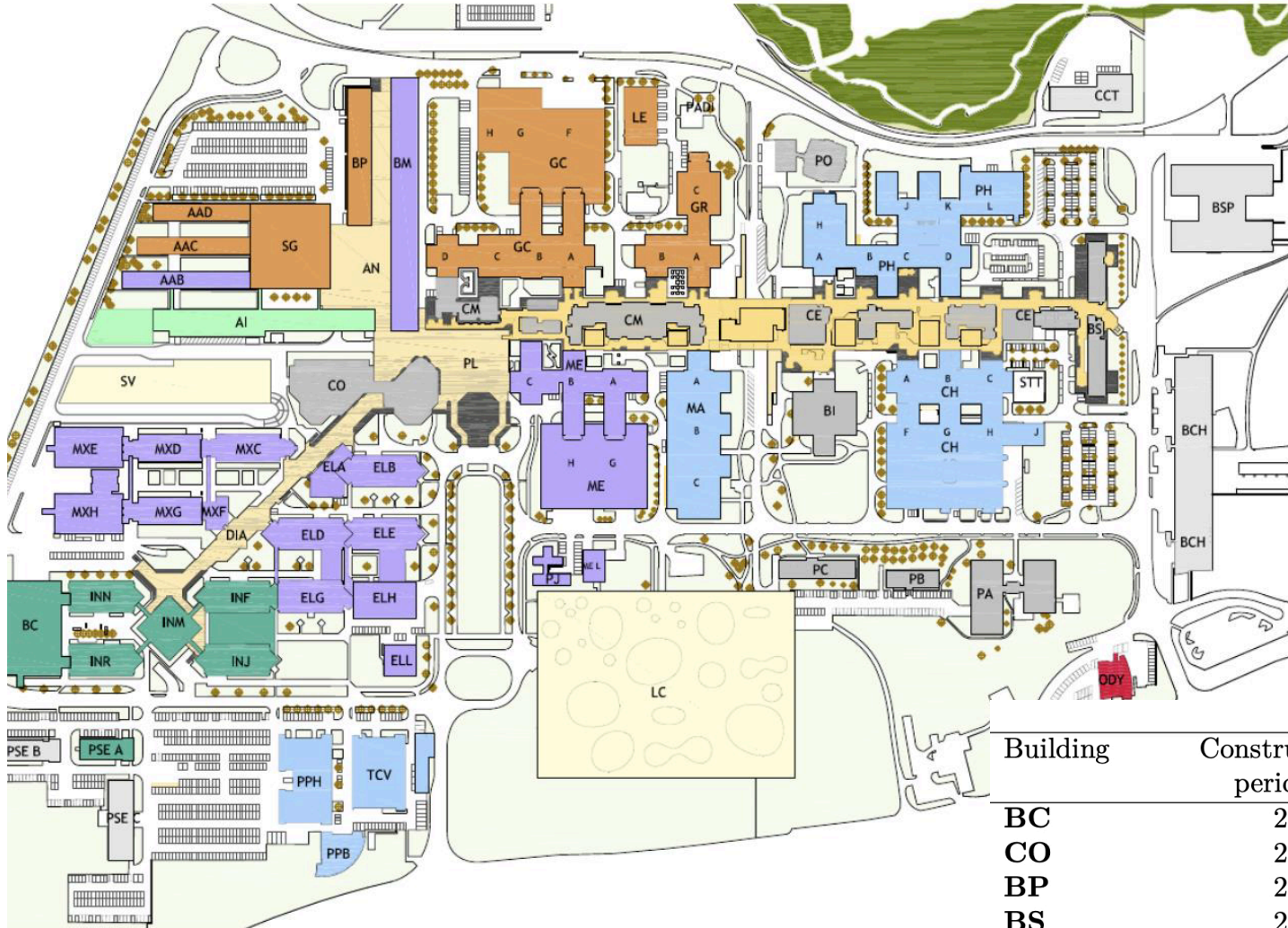


MILP formulation for energy supply and demand matching

Prof François Marechal



Buildings stock

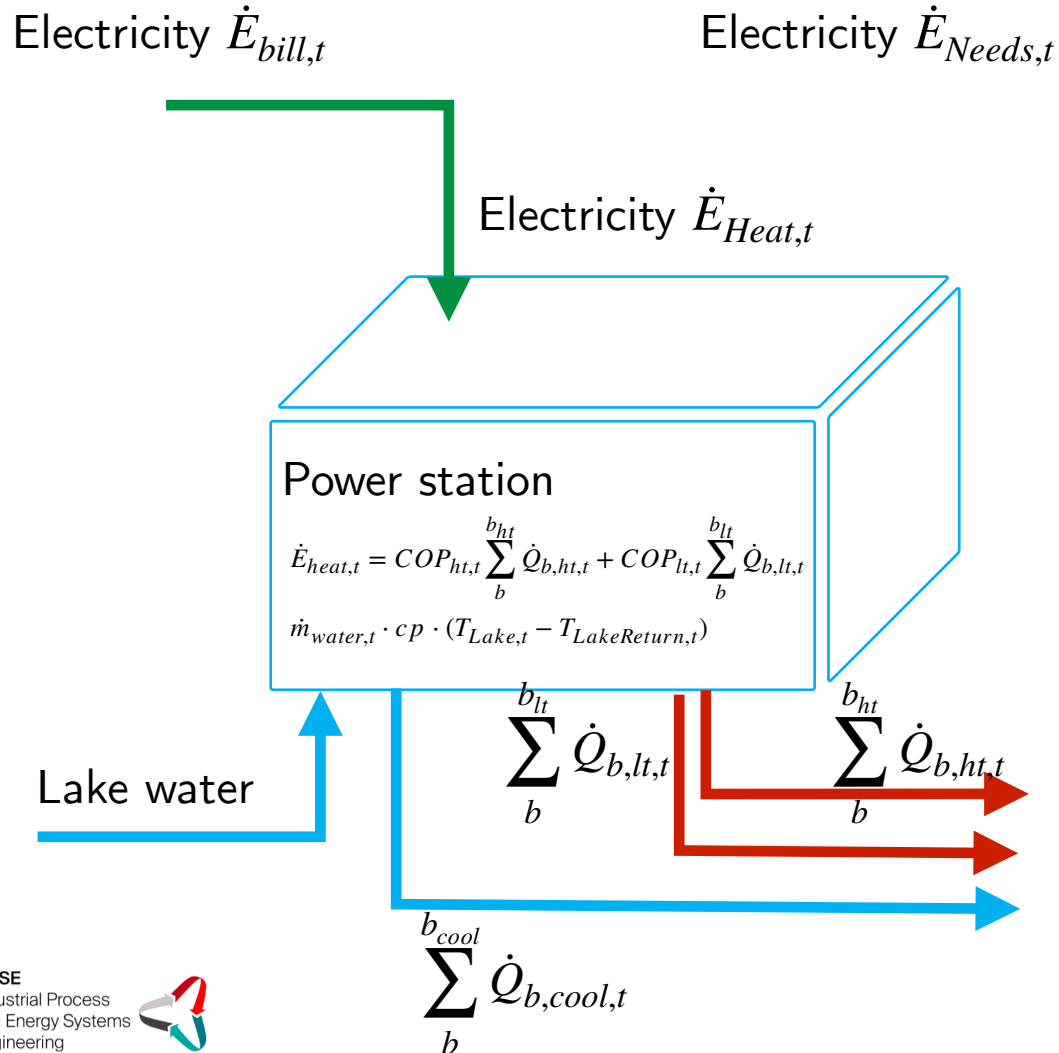


Measures

Table 1.1: EPFL Buildings

Building	Construction period ^a	Heated surface A_{th} [m ²]	Annual heat demand Q_{th} [kWh]	Annual electricity demand Q_{el} [kWh]
BC	2	17480	418,491	1,603,596
CO	2	11901	477,008	943,653
BP	2	10442	457,861	691,031
BS	2	10267	509,183	350,860
TCV	2	6095	318,209	2,067,675

- The president has first asked his colleagues to make some suggestions of the options :
 - Prof of Architecture : you have to refurbish the buildings
 - Prof of Heat exchangers : recover the heat of the data centers and the hot air in buildings
 - Prof of Compressor : use multi-level heat pumps, choose the right fluid
 - Prof of Photovoltaic : use PV panels
 - Prof of Fuel cells : use a solid oxide fuel cell
 - Prof of Bio-engineering : use biomethane
 - Prof of Geology : use deep geothermal sources
 - Prof of Water Treatment : use of the heat of the waste water
 - Prof of Energy system : look at the system integration
 - Prof of power systems : use my battery
 - Prof of Climate and economics : take into account the global warming
 - Vice-president finance : I do not have money for that
 - ETH board : demonstrate the sustainability



- For each distribution system d (e.g. ht)
 - Demand : $\dot{Q}_{d,t} = \sum_b^{n_b} \dot{Q}_{b,d,t} \quad \forall t \in lifetime$
- For each unit u (e.g. heat pump)
 - Supply by unit u : $\sum_{u=1}^{n_u} \dot{Q}_{u,d,t} = \dot{Q}_{d,t} \quad \forall t \in lifetime$
 - and $\dot{Q}_{u,t} = \sum_d^{n_d} \dot{Q}_{u,d,t}$
- Cost of the supply
 - Size of the conversion equipment :

$$\sum_{u=1}^{n_u} \max_{t \in lifetime} (\dot{Q}_{u,d,t}) = \max_{t \in lifetime} (\dot{Q}_{d,t})$$
 - $\dot{Q}_{u,max} = \max_{t \in lifetime} (\dot{Q}_{u,t})$
 - Buy the resources : $\sum_{r=1}^{n_{res}} \sum_u^{n_u} \left(\int_{t_0}^{lifetime} c_{r,t} \cdot m_{r,u,t} \cdot \dot{Q}_{u,t} \cdot dt \right)$

$$\sum_{r=1}^{n_{res}} \sum_u^{n_u} \left(\int_{t_0}^{lifetime} c_{r,t} \cdot m_{r,u,t} \cdot \dot{Q}_{u,t} \cdot dt \right) \quad [CHF/lifetime]$$

- $c_{r,t}$ $[CHF/unit_r]$ cost of one unit of resource r at time t
 - e.g. kg of water, kg of fuel, kJ of fuel or kWh of electricity
 - $c_{r,t} \leq 0$ for products (e.g. electricity production)
- $m_{r,u,t}$ $[unit_r/kJ_{th}]$ unit of resource r used to deliver one $[kJ_{th}]$ of heat by unit u at time t
- $\dot{Q}_{u,t}$ $[kW/unit_r]$ heat delivered by unit u at time t
- $lifetime$ $[s]$ expected lifetime of the project

- Operating EXpenditure (we assume a typical year of operation) :

$$\text{Cost of resources} \sum_{r=1}^{n_{res}} \sum_u^{n_u} \left(\int_{t_0}^{year} c_{r,t} \cdot m_{r,u,t} \cdot \dot{Q}_{u,t} \cdot dt \right) \quad [CHF/year]$$

with $m_{r,u,t}$ [kg/MJ] is the resource consumption per unit of heat $Q_{u,t}$

+ Maintenance [CHF/year]

+ Men Power [CHF/year]

+ Taxes [CHF/year] :

fixed : e.g. based on installed power

$$\text{proportional :} \sum_{r=1}^{n_{res}} \sum_u^{n_u} \left(\int_{t_0}^{year} t_{r,t} \cdot m_{r,u,t} \cdot \dot{Q}_{u,t} \cdot dt \right) \quad [CHF/year]$$

with $t_{r,t}$ [CHF/unit_r] tax per unit of r

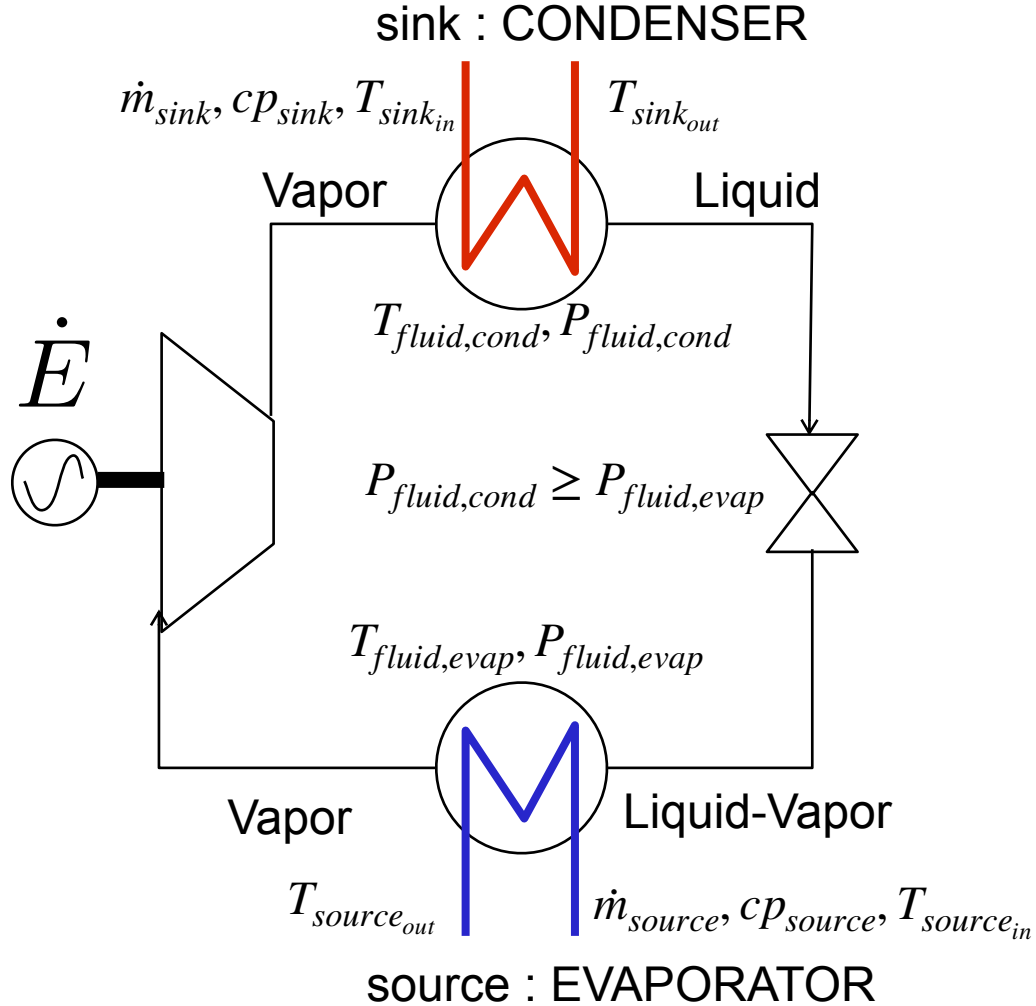
$$\text{e.g. } t_{r,t} = \tau_{CO_2} [CHF/kg_{CO_2}] \cdot m_{CO_2,r} [kg_{CO_2}/unit_r]$$

- resource use is calculated with a multiplication factor of a reference production $m_{r,u,t}$ [$unit_r/kJ_{th}$]

- Thermal efficiency : $\eta_{th,u} = \frac{\dot{Q}_{th,u}}{\dot{m}_{r,u}}$ [kJ_{th}/kJ_r] $\Rightarrow m_{r,u,t} = \frac{1}{\eta_{th,u}}$

- Electrical efficiency : $\eta_{e,u} = \frac{\dot{E}_u}{\dot{m}_{r,u}}$ [kJ_e/kJ_r] $\Rightarrow \dot{E}_{u,t} = \frac{\eta_{e,u}}{\eta_{th,u}} \cdot \dot{Q}_{u,t}$

-



$$\dot{Q}_{sink} = \dot{Q}_{u,t} = \dot{m}_{sink,t} \cdot c_{p,sink} \cdot (T_{sink_{out,t}} - T_{sink_{in,t}})$$

$$\dot{E}_{u,t} = \frac{1}{COP_{u,t}} \cdot \dot{Q}_{u,t}$$

$$COP_{u,t} = \eta_{COP} \cdot COP_{th,u,t}$$

$\eta_{COP} = 50\%$ or is a fitted curve

$$COP_{th,u,t} = \frac{\tilde{T}_{sink,t}}{\tilde{T}_{sink,t} - \tilde{T}_{source,t}}$$

$$\tilde{T}_{sink,t} = \frac{T_{sink_{out,t}} - T_{sink_{in,t}}}{\ln(T_{sink_{out,t}}) - \ln(T_{sink_{in,t}})}$$

$$\tilde{T}_{source,t} = \frac{T_{source_{out,t}} - T_{source_{in,t}}}{\ln(T_{source_{out,t}}) - \ln(T_{source_{in,t}})}$$

$$\dot{Q}_{source,t} = \dot{m}_{source,t} \cdot c_{p,source} \cdot (T_{source_{in,t}} - T_{source_{out,t}})$$

$$\dot{Q}_{source,t} = \dot{Q}_{u,t} - \dot{E}_{u,t}$$

- Level of use of unit u in time t:

$$\dot{Q}_{u,t} = f_{u,t} \cdot \dot{Q}_{ref,u,t}$$

with $\dot{Q}_{ref,u,t}$ [kW], the nominal flow of unit u in time t

$f_{u,t}$: the capacity factor or the level of usage of unit u in time t for the reference flow $\dot{Q}_{ref,u,t}$.

- TOTal EXpenditure :

$$TOTEX \text{ [CHF/year]} = OPEX \text{ [CHF/year]} + CAPEX \text{ [CHF/year]}$$

it assumes that the unit will be operated with the same power profile over the lifetime of the equipment

We assume a mean year and the associated costs as being representative of the lifetime of the project

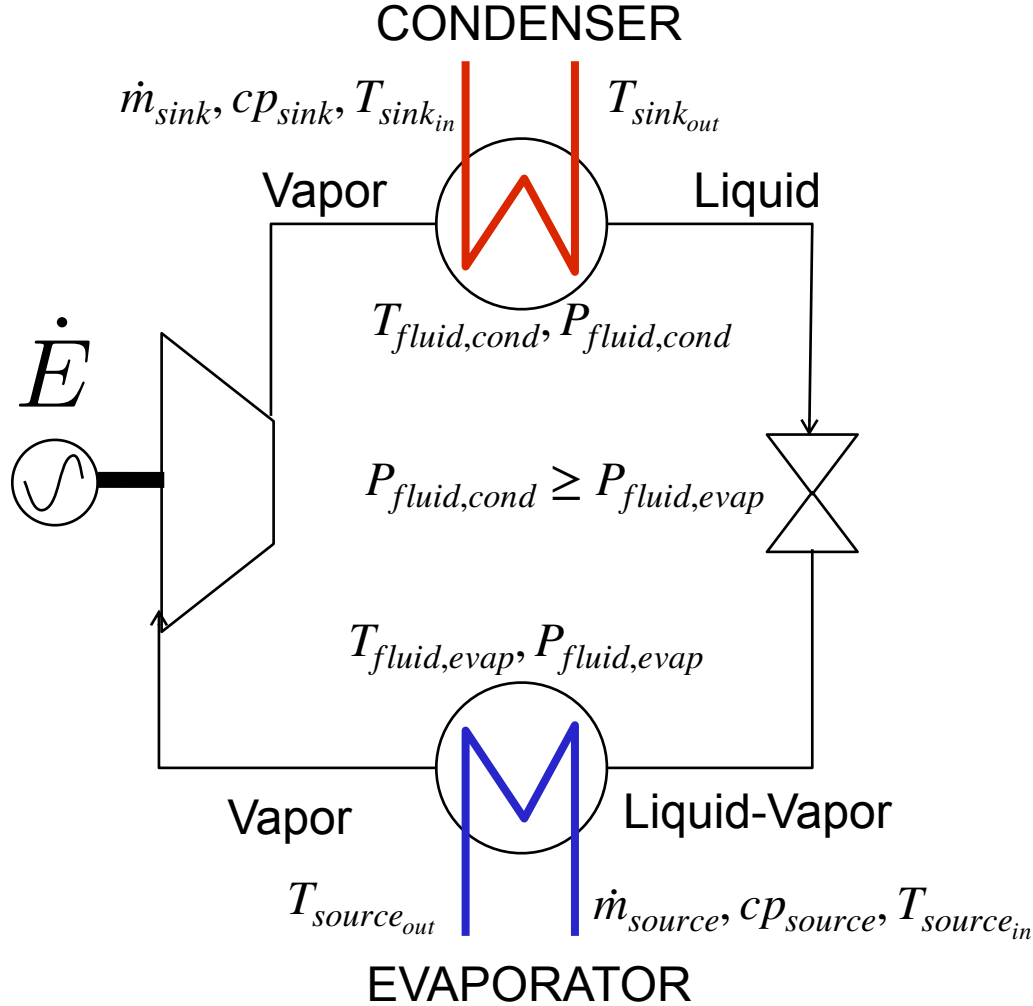
- $CAPEX$ [CHF/year] = $\sum_{u=1}^{n_u} \frac{1}{\tau_u} \cdot i_{u\dot{Q}_{u,max}} \cdot \dot{Q}_{u,max}$
 - $i_{u\dot{Q}_{u,max}}$ [CHF/kW] specific investment of unit u for installed capacity $\dot{Q}_{u,max}$
 - $\dot{Q}_{u,max} = \max_{t \in lifetime} (\dot{Q}_{u,t})$ [kW] size of unit u
 - $\frac{1}{\tau_u} = \frac{1}{\tau(i, lifetime_u)}$ [year⁻¹] : annualisation factor of unit u

- **linear constraints :**

level of usage: $\dot{Q}_{ref,u,t} \cdot f_{u,t} \leq \dot{Q}_{ref,u} \cdot f_u^{max} \quad \forall t, u$

existence: $f_{min_u} \cdot y_u \leq f_u^{max} \leq f_{max_u} \cdot y_u \quad y_u \in \{0,1\}, \forall t, u$

Sizing : condenser, evaporator & compressor



$$\dot{Q}_{u,t} = \dot{Q}_{sink,t} = \dot{m}_{sink,t} \cdot cp_{sink} \cdot (T_{sink_{out},t} - T_{sink_{in},t})$$

$$\dot{Q}_{sink,t} = \dot{m}_{fluid,t} \cdot (h(T_{fluid,cond_{in},t}, P_{fluid,cond_{in},t}) - h(T_{fluid,cond_{out},t}, P_{fluid,cond_{out},t}))$$

$$A_{condenser} = \max_{t \in lifetime} \left(\left(\frac{1}{u_{sink}} + \frac{1}{u_{fluid,cond}} \right) \frac{\dot{Q}_{sink,t}}{\frac{(T_{fluid,cond,t} - T_{sink_{in},t}) - (T_{fluid,cond,t} - T_{sink_{out},t})}{\ln(T_{fluid,cond,t} - T_{sink_{in},t}) - \ln(T_{fluid,cond,t} - T_{sink_{out},t})}} \right)$$

$$A_{evaporator} = \max_{t \in lifetime} \left(\left(\frac{1}{u_{source}} + \frac{1}{u_{fluid,evap}} \right) \frac{\dot{Q}_{source,t}}{\frac{(T_{source_{out},t} - T_{fluid,evap,t}) - (T_{source_{in},t} - T_{fluid,evap,t})}{\ln(T_{source_{out},t} - T_{fluid,evap,t}) - \ln(T_{source_{in},t} - T_{fluid,evap,t})}} \right)$$

$$\dot{E}_{max} = \max_{t \in lifetime} \left(\frac{\dot{Q}_{u,t}}{COP_{u,t}} \right)$$

$$\dot{Q}_{source,t} = \dot{m}_{source,t} \cdot cp_{source} \cdot (T_{source_{in},t} - T_{source_{out},t})$$

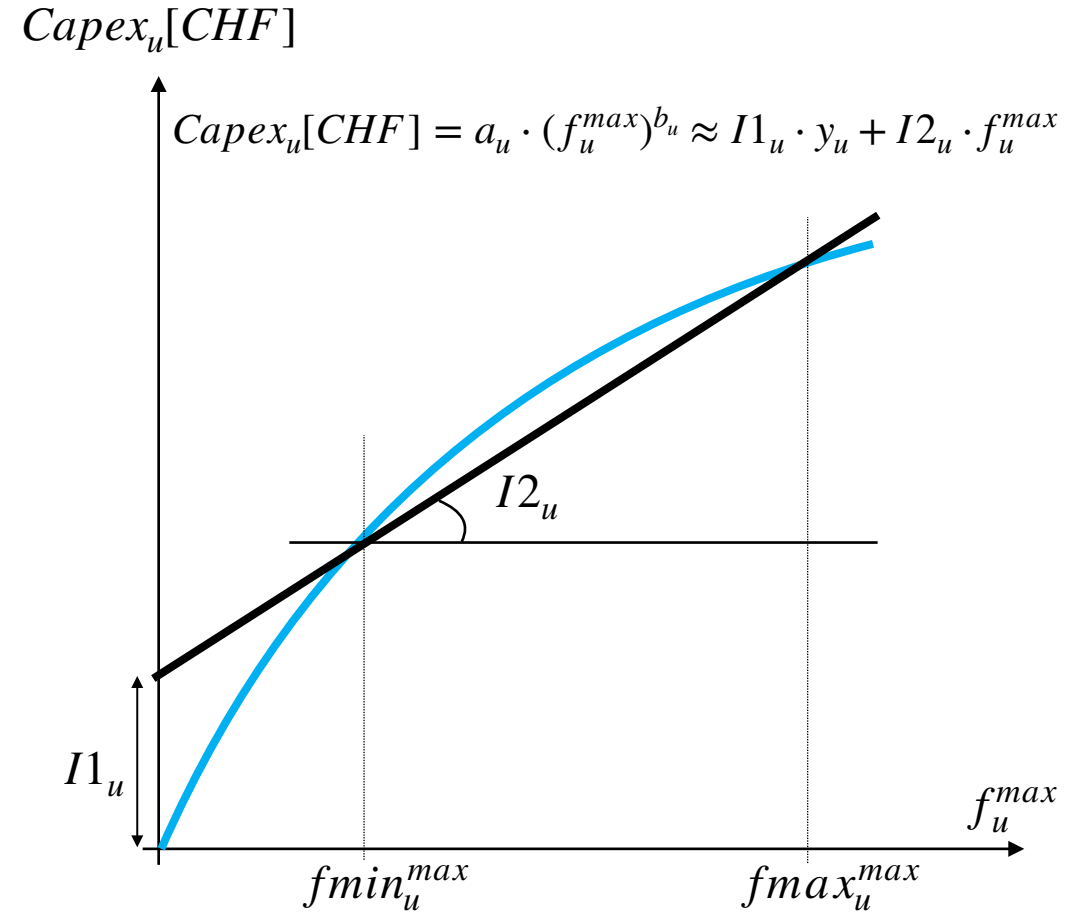
$$\dot{Q}_{source,t} = \dot{m}_{fluid,t} \cdot (h(T_{fluid,evap_{out},t}, P_{fluid,evap_{out},t}) - h(T_{fluid,evap_{in},t}, P_{fluid,evap_{in},t}))$$

$$\dot{Q}_{source,t} = \dot{Q}_{sink,t} - \dot{E}_{u,t}$$

$$CAPEX_u = \frac{1}{\tau} (I_{HTX}(A_{condenser}) + I_{HTX}(A_{Evaporator}) + I_{compressor}(\dot{E}_{max}))$$

$$CAPEX[CHF/year] = \sum_{u=1}^{n_u} \frac{1}{\tau(n_{y,u}, i)} (I1_u y_u + I2_u f_u^{max})$$

$\frac{1}{\tau(n_{y,u}, i)}$	$[\frac{1}{year}]$	annualisation factor of unit u
$n_{y,u}$	$[year]$	expected life time of unit u
$I1_u$	$[CHF]$	fixed investment of unit u
y_u	$[-]$	existence unit u
$I2_u$	$[CHF]$	proportional investment cost of unit u
f_u^{max}	$[-]$	size of unit u



$$f_{min_u}^{max} \cdot y_u \leq f_u^{max} \leq f_{max_u}^{max} \cdot y_u$$

$$f_{u,t} \leq f_u^{max} \quad \forall t \in periods$$

Objective function

The objective is to minimize the **total annualized cost** function:

$$TOTEX = OPEX + CAPEX + ENVEX \quad [CHF/year] \quad (1)$$

where:

- **Annual operating cost:**

$$OPEX = \int_0^{t^{op}} \sum_r c_r(t) \dot{m}_r(t) dt + \sum_u c_u S_u + \int_0^{t^{op}} c_e^+(t) \dot{E}^+(t) dt - \int_0^{t^{op}} c_e^-(t) \dot{E}^-(t) dt \quad (2)$$

Define the flows from the values of the flows =>

$$\approx \sum_t \sum_r c_{r,t} \dot{m}_{r,t} \Delta t + \sum_u c_u^{mt} S_u + \sum_t c_{e,t}^+ \dot{E}_t^+ \Delta t - \sum_t c_{e,t}^- \dot{E}_t^- \Delta t \quad [CHF/year] \quad (3)$$

- **Annualized investment cost:**

$$CAPEX = \frac{1}{\tau} \sum_u I(s_u) \approx \frac{1}{\tau} \sum_u (c_u^{inv1} y_u + c_u^{inv2} s_u) \quad [CHF/year] \quad (4)$$

Define the sizes =>

- **Annual cost related to emissions:**

$$ENVEX = c_{CO_2} \sum_t [\dot{m}_{CO_2,t} \Delta t + k_{CO_2,t} (\dot{E}_t^+ - \dot{E}_t^-) \Delta t] \quad [CHF/year] \quad (5)$$

Energy and mass balances

- **Heat distribution** $\forall t \in \mathbf{T}, \forall d \in \mathbf{D}$ with $T_{d+1,t} \geq T_{d,t}$

$$\sum_u^{\mathbf{U}} \dot{q}_{u,d} f_{u,t} - \dot{Q}_{d,t} = \emptyset \quad (13)$$

Balance demand and supply \Rightarrow

$$\dot{Q}_{d+1,t}^{\text{res}} + \dot{Q}_{d,t} - \sum_b^{\mathbf{B}} \dot{Q}_{b,d,t} = \dot{Q}_{d-1,t}^{\text{res}} \quad (14)$$

$$\dot{Q}_{d,t} = \dot{m}_{d,t} c p_d (T_{d,t}^{\text{s}} - T_{d,t}^{\text{r}}) \quad (15)$$

$$\dot{Q}_{0,t}^{\text{res}} = \emptyset, \quad \dot{Q}_{n_{d+1},t}^{\text{res}} = \emptyset \quad (16)$$

$$\dot{Q}_{d,t}^{\text{res}} \geq \emptyset \quad (17)$$

- **Inequality constraints** $\forall t \in \mathbf{T}, \forall u \in \mathbf{U}$

Choosing the option =>

$$f_u^{\min} y_u \leq f_u \leq f_u^{\max} y_u \quad (6)$$

$$f_u^{\min} y_{u,t} \leq f_{u,t} \leq f_u^{\max} y_{u,t} \quad (7)$$

$$f_{u,t} \leq f_u \quad f_{u,t}, f_u \in \{0,1\} \quad (8)$$

- **Modeling equations**

example: heat pump

$u = \text{heat pump}$

$$\dot{e}_u^+ = \frac{\dot{q}_u^-}{\text{COP}} \quad (9)$$

$$\text{COP} = \left(\frac{\tilde{T}^{\text{sink}}}{\tilde{T}^{\text{sink}} - \tilde{T}^{\text{source}}} \right) \eta_{\text{carnot}} \quad (10)$$

η_{Carnot} : fitted curve $\eta_{\text{Carnot}}(T_t^{\text{sink}}, T_t^{\text{source}}, \dot{Q}_t)$

The heat pump COP can be calculated as a function of the temperature at each time step t and distribution system d considered:

$u = \text{heat pump}, \forall t \in \mathbf{T}, \forall d \in \mathbf{D}$

$$\dot{e}_{u,d,t}^+ = \frac{\dot{q}_{u,d,t}^-}{\text{COP}} \quad (11)$$

Constant for the optimisation =>

$$\text{COP}_{d,t} = \left(\frac{\tilde{T}_{d,t}^{\text{sink}}}{\tilde{T}_{d,t}^{\text{sink}} - \tilde{T}_{d,t}^{\text{source}}} \right) \eta_{\text{carnot}} \quad (12)$$

- **Electricity balance** $\forall t \in \mathbf{T}$

Flows of resources =>

$$\dot{E}_t^+ - \dot{E}_t^- + \sum_u^{\mathbf{U}} f_{u,t} \dot{e}_u^- - \sum_u^{\mathbf{U}} f_{u,t} \dot{e}_u^+ - \sum_b^{\mathbf{B}} \dot{E}_{b,t} = \emptyset \quad (18)$$

- **Resource and material balance** $\forall t \in \mathbf{T}, \forall r \in \mathbf{R}$

Flows of resources =>

$$\dot{m}_{r,t} = \sum_u^{\mathbf{U}} f_{u,t} \dot{m}_{r,u} \quad (19)$$

example: emissions of CO₂ $\forall t \in \mathbf{T}, r = \text{CO}_2$

Flows of emissions =>

$$\dot{m}_{\text{CO}_2,t}^- = \sum_u^{\mathbf{U}} f_{u,t} \dot{m}_{\text{CO}_2,u} \quad (20)$$

The goal is to calculate the set of variables $f_{u,t}, y_{u,t}, f_u, y_u, \dot{E}_t^-, \dot{E}_t^+, \dot{m}_{r,t}, \dot{Q}_{d,t}, \dot{Q}_{d,t}^{\text{res}}$ that minimizes the objective TOTEX.

EPFL Variables (to be calculated) and parameters (fixed)

Index and set	Description
$t \in \mathbf{T}$	Time $\mathbf{T} = \{t_1 \dots t_{n_t}\}$
$u \in \mathbf{U}$	Utility $\mathbf{U} = \{\text{boiler, heat pump, refrigeration, ...}\}$
$r \in \mathbf{R}$	Resource $\mathbf{R} = \{\text{hydrogen, natural gas, chocolate, ...}\}$
$d \in \mathbf{D}$	Distribution system $\mathbf{D} = \{d_1 \dots d_{n_d}\}$
$b \in \mathbf{B}$	Building $\mathbf{B} = \{b_1 \dots b_{n_b}\}$
Parameter	Description
t^{op}	Total operating time per year [h/year]
Δt_t	Duration of time interval t [h]
$c_{r,t}$	Specific cost of resource r at time t [CHF/kg]
$c_{e,t}^+$	Price for purchased electricity at time t [CHF/kWh]
$c_{e,t}^-$	Price for sold electricity at time t [CHF/kWh]
$c_u^{\text{inv}1}$	Fixed investment cost of utility u [CHF]
$c_u^{\text{inv}2}$	Variable investment cost of utility u [CHF/size]
c_u^{mt}	Maintenance specific cost of utility per year u [CHF/size/year]
$\frac{1}{T}$	Annualization factor of investment [1/year]
f_u^{min}	Minimum sizing factor of utility u [-]
f_u^{max}	Maximum sizing factor of utility u [-]
$k_{\text{CO}_2,t}$	CO ₂ equivalent emissions of the grid at time t [ton _{CO2} /kWh]
$\dot{m}_{r,u}$	Reference mass flow of resource r in utility u [kg/s]
\dot{q}_u^-	Reference heat load produced by utility u [kW]
\dot{q}_u^+	Reference heat load consumed by utility u [kW]
\dot{e}_u^-	Reference electrical power produced by utility u [kW]
\dot{e}_u^+	Reference electrical power consumed by utility u [kW]
$T_{d,t}$	Logarithmic mean temperature of the distribution system d at time t [K]
$T_{d,t}^s$	Supply temperature of the distribution system d at time t [K]
$T_{d,t}^r$	Return temperature of the distribution system d at time t [K]
$\dot{m}_{d,t}$	Mass flow in the distribution system d [kg/s]
cp_d	Heat capacity of the fluid in the distribution system d [kJ/K/kg]
$\dot{q}_{u,d}$	Reference heat load of utility u fed in the distribution system d [kW]
$\dot{Q}_{b,d,t}$	Heat load demand of building b at time t in the distribution system d [kW]
$\dot{E}_{b,t}$	Electricity consumption of building b at time t [kW]
COP	Coefficient Of Performance of the heat pump [-]
\tilde{T}_{sink}	Logarithmic mean temperature of the heat sink of the heat pump [K]
$\tilde{T}_{\text{source}}$	Logarithmic mean temperature of the heat source of the heat pump [K]
η_{carnot}	Carnot efficiency [-]

<= SETS : are groups of the same type and scopes in the problem

Variables => min and max bounds

Variable	Description
f_u	Sizing factor of utility u [-]
$f_{u,t}$	Sizing factor of utility u at time t [-]
y_u	Binary variable to use or not utility u [-]
$y_{u,t}$	Binary variable to use or not utility u at time t [-]
\dot{E}_t^+	Purchased electrical power at time t [kW]
\dot{E}_t^-	Sold electrical power at time t [kW]
$\dot{m}_{r,t}$	Mass flow of resource r at time t [kg/s]
$\dot{Q}_{d,t}^{\text{res}}$	Total utility heat load at time t in the distribution system d [kW]
$\dot{Q}_{d,t}$	Heat load cascaded from distribution system d to $d + 1$ at time t [kW]

<= Parameters calculated before solving the MILP problem

- The building b has n_{o_b} options to supply the heat (e.g. air heat recovery)

- Heat load of the building on distribution system d

$$\dot{Q}_{b,d,t} = \sum_{o_b}^{n_{o,b}} y_{o_b} \cdot \dot{Q}_{o_b,d,t}$$

- Choosing the option

$$\sum_{o_b}^{n_{o,b}} y_{o_b} = 1$$

- Electricity consumption

$$\dot{E}_b = \sum_{o_b}^{n_{o,b}} y_{o_b} \cdot \dot{E}_{o_b,t}$$

- Capital cost

$$CAPEX_b = \sum_{o_b}^{n_{o,b}} CAPEX_{o_b} \cdot y_{o_b}$$

- Heat supplied by u on distribution level d :

$$\dot{Q}_{u,d,t} = f_{u,d,t} \cdot \dot{Q}_{u,d,hp,t}$$

- Electricity in the compressor of u :

$$\dot{E}_{u,t} = \sum_d^{n_{d,u}} f_{u,d,t} \cdot \dot{Q}_{u,d,t} \cdot \frac{1}{COP_{u,d,t}}$$

- Size of the unit u : $\dot{E}_u^{max} \geq \dot{E}_{u,t} \quad \forall t$

- CAPEX of unit u :

$$CAPEX_u = \frac{1}{\tau_u} \cdot (I1_u \cdot y_u + I2_u \cdot \dot{E}_u^{max})$$

