

The background image is a composite of two scenes. On the left, a traditional wooden windmill stands on a grassy bank next to a body of water, with power lines and pylons visible in the distance. On the right, a large industrial power plant with a prominent cooling tower is situated near a body of water. A semi-transparent red rectangular box is overlaid on the right side of the image, containing the course title in white text.

ME-251: Thermodynamics and energetics I

First Law of Thermodynamics II

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Energy Transport Advances
Laboratory
EPFL Mechanical Engineering

2025 Fall Semester

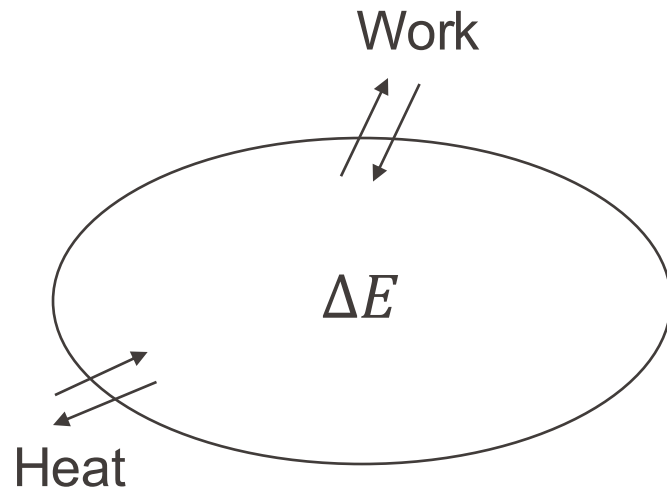
Photo Credit: Trougnouf

	Capacity	# of last week's participants
AAC137	80	16
SG 0 211	112	50
SG 0 213	80	71

- Explain key concepts in the first law of thermodynamics
 - Energy change
 - Work
 - Heat

- Apply energy balance to closed systems
- Analyze the energy balance of thermodynamic cycles
- Understand and interpret equation of state (p-T-v surface)

○ Reading materials: **Moran 2.1-2.4**



Can be intuitively understood as energy conservation

Energy change = Energy going in – Energy going out

Energy flows can take the form of heat, work, ...

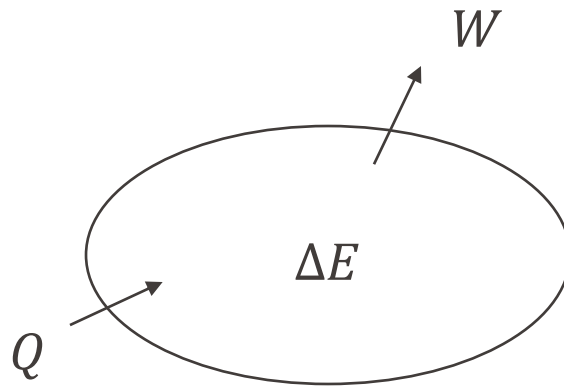
Change in the amount of energy contained within a system during some time interval

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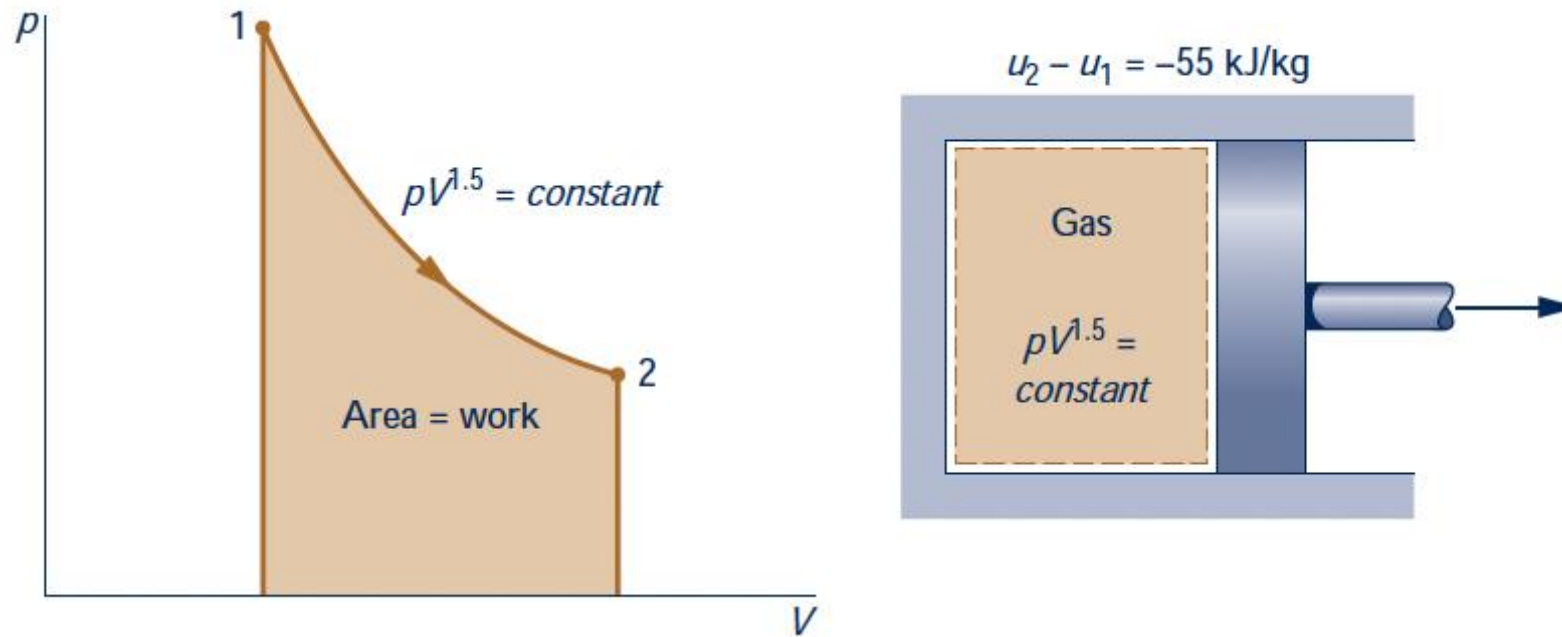
Net amount of energy transferred **into** the system by heat transfer during the time interval

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Net amount of energy transferred **out of** the system by work during the time interval



$$\Delta E = E_2 - E_1 = Q - W$$

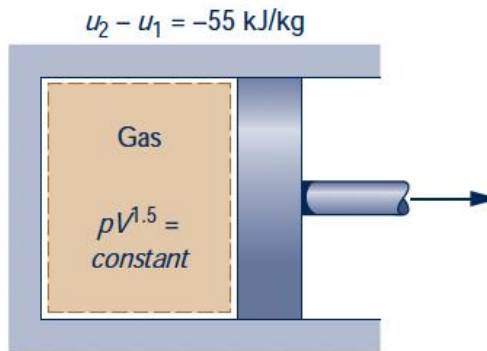
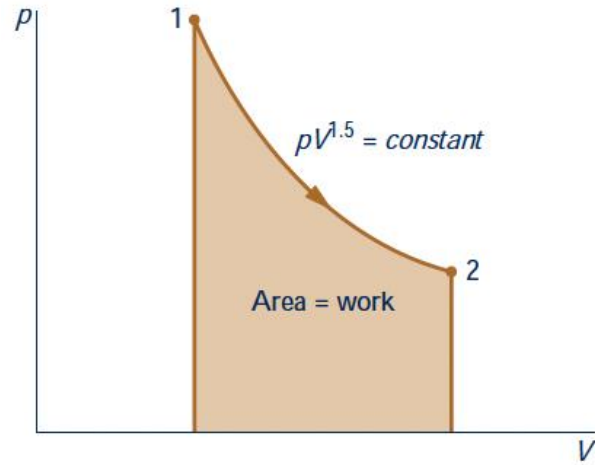


Gas expansion: $V_1 = 0.1 \text{ m}^3$, $p_1 = 3 \text{ bar}$; $V_2 = 0.2 \text{ m}^3$; $pV^{1.5} = \text{const}$, $m = 0.4 \text{ kg}$

Change in specific internal energy: $u_2 - u_1 = -55 \text{ kJ/kg}$;
no significant change in kinetic/potential energy

Determine the net heat transfer between the gas and the surrounding

Example 2.2 in Moran



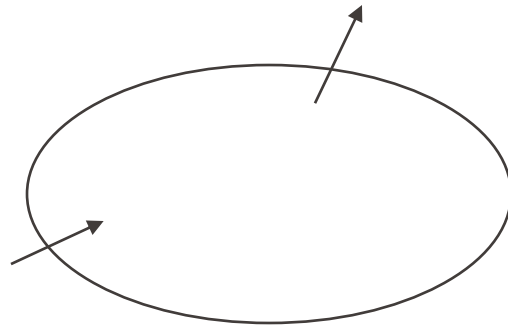
Time rate of change in the amount of energy contained within a system at time t

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Net rate at which energy is transferred into the system by heat transfer at time t

–

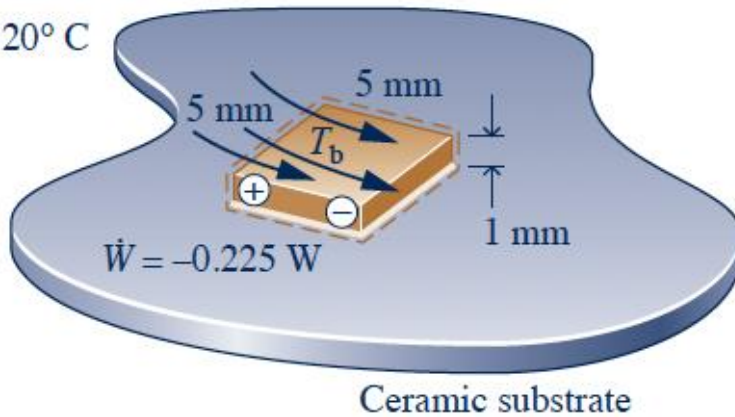
Net rate at which energy is transferred out of the system by work at time t



Coolant

$$h = 150 \text{ W/m}^2 \cdot \text{K}$$

$$T_f = 20^\circ \text{C}$$



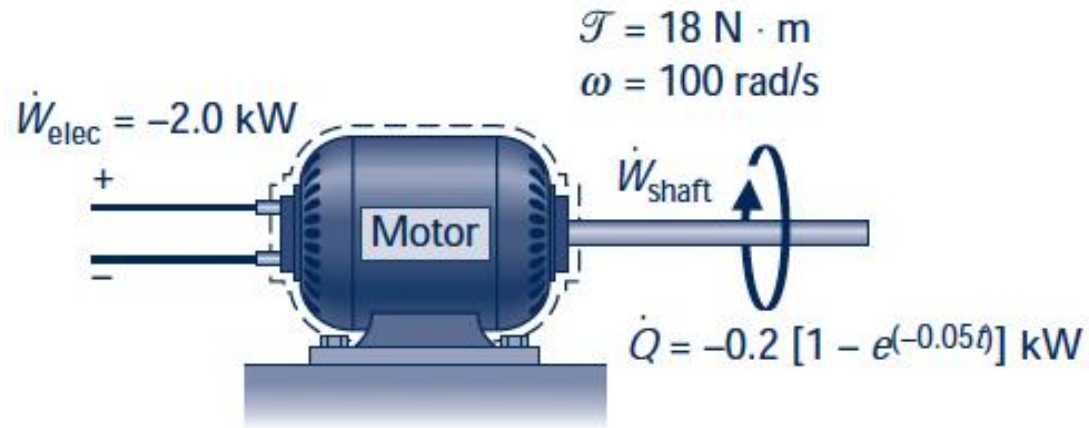
A silicon chip (5 mm x 5 mm x 1 mm) at a **steady state**

Electric power input is 0.225 W

Only the top surface is exchanging heat with the surrounding

$$\dot{Q}_{cool} = hA(T - T_f)$$

Determine the surface temperature of the silicon chip

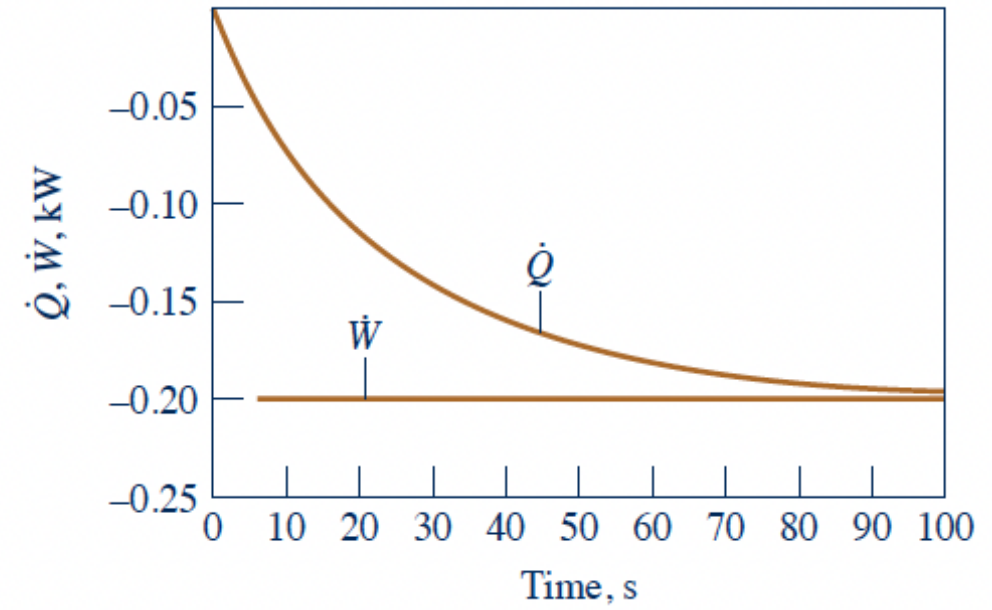
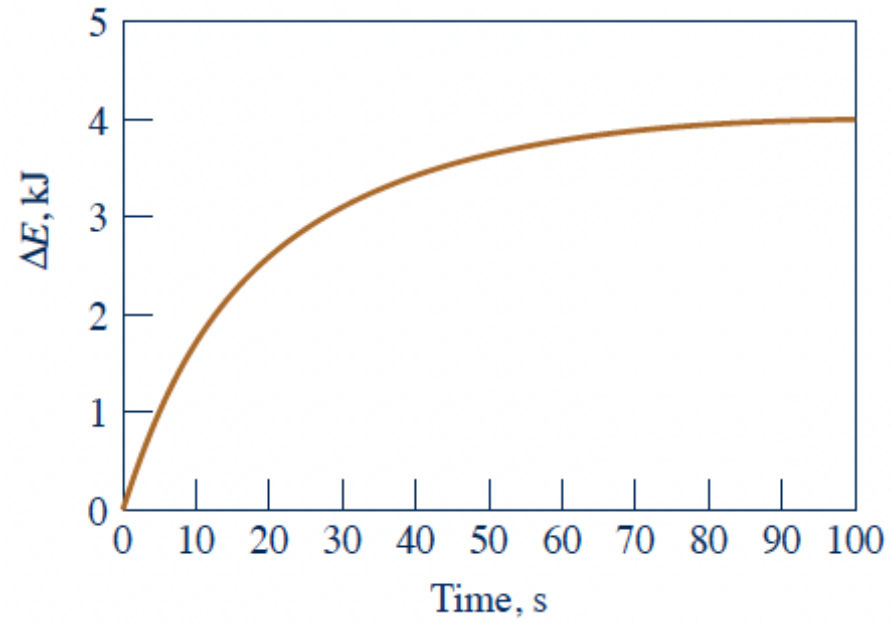


A motor operates with constant electric power input 2 kW, shaft speed ω , and applied torque \mathcal{T}

The heat transfer rate between the motor and the ambient follows

$$\dot{Q} = -0.2(1 - e^{-0.05t}) \quad \dot{Q} \text{ in [kW]}, t \text{ in [s]}$$

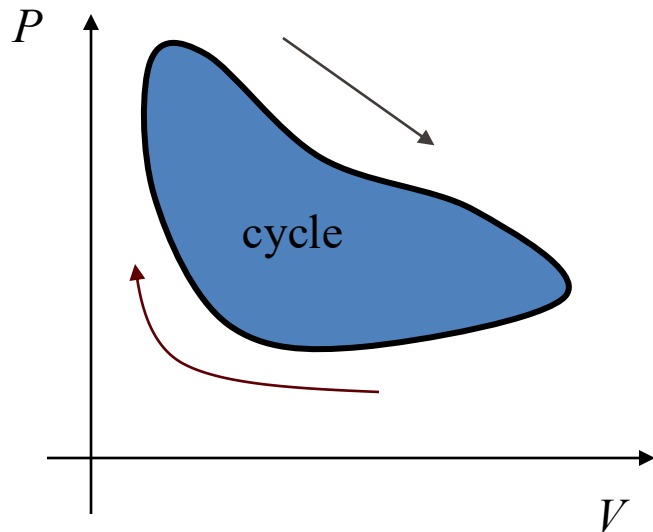
Plot the net heat transfer rate, the net power and the energy change of the motor system as a function of time

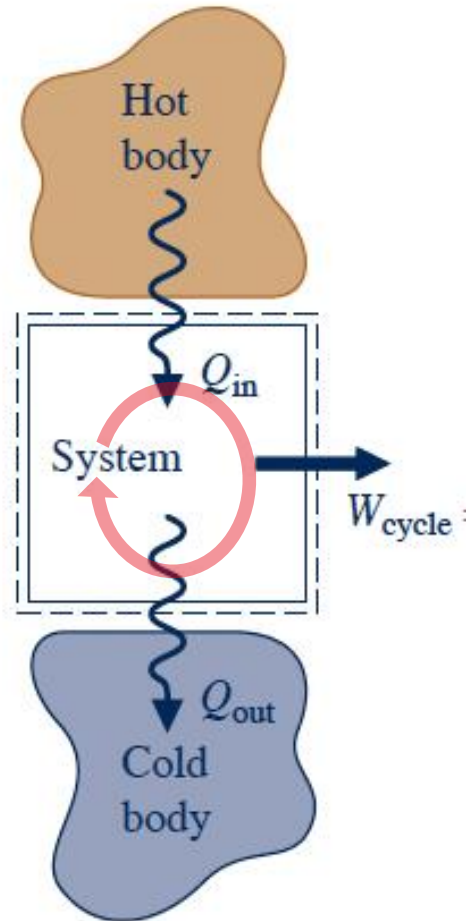


Thermodynamics

Cycles

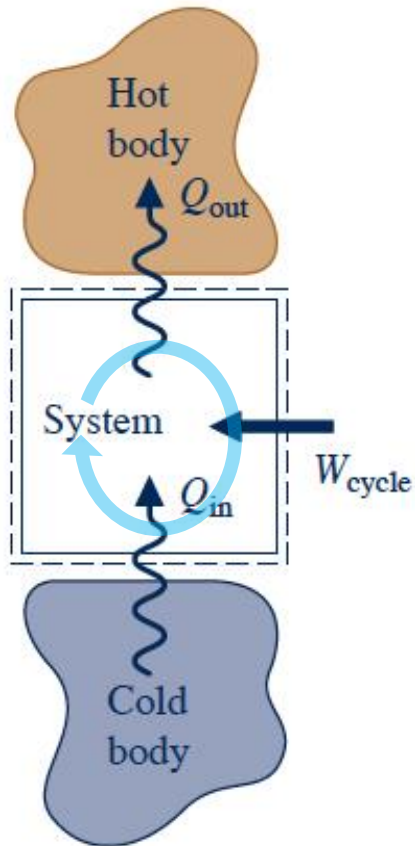
- A thermodynamic cycle is a sequence of processes that begins and ends at the same state.



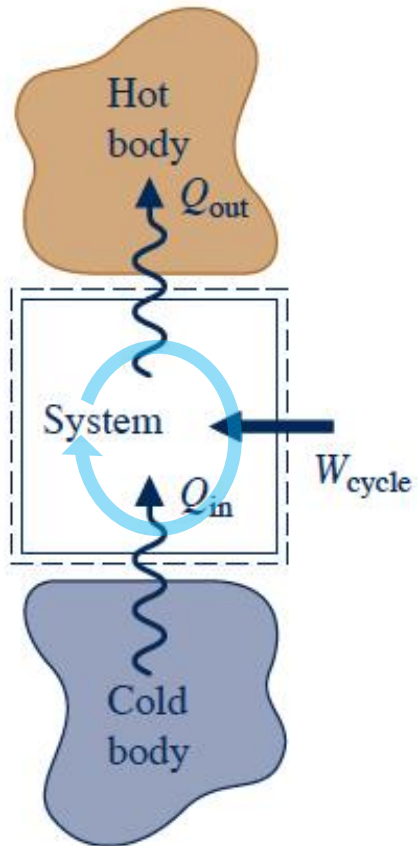


System undergoing a cycle to deliver a net work transfer to their surroundings

- Nuclear power plant: 0.32-0.34
- Fossil fuel power plant: 0.35-0.48
- Combustion engine: 0.35-0.42 (gasoline/diesel)



System undergoing a cycle to transfer heat from a cold body to a hot body



System undergoing a cycle to transfer heat from a cold body to a hot body

- Pure substance: uniform in chemical composition.
 - Pure water?
 - Ice-water mixture?
 - Air?
 - Aerosol?



- Homogeneous in both chemical composition and physical structure (solid, liquid, vapor/gas)

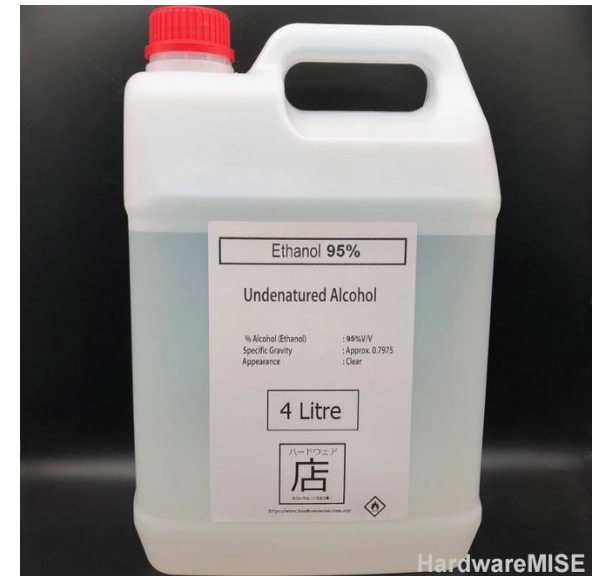
Ice-water mixture



Water-oil mixture



Ethanol diluted with water



System: salt (NaCl) solution + CO₂ bubbles



How many phases are there?

- A. 1
- B. 2
- C. 3
- D. 4

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luepfl

- Pressure
- Temperature
- Density
- Specific volume
- Specific internal energy
- ...

- **State principle:** for closed systems

$$\# \text{ of independent properties} = \# \text{ of relevant work exchange modes} + 1$$

- E.g., for gas in a piston-cylinder assembly, number of independent properties: 2 (**temperature** associated with heat transfer and **pressure** associated with compression/expansion work)
- **Simple system:** only one work exchange mode as the system undergoes quasiequilibrium processes (**two independent properties**).

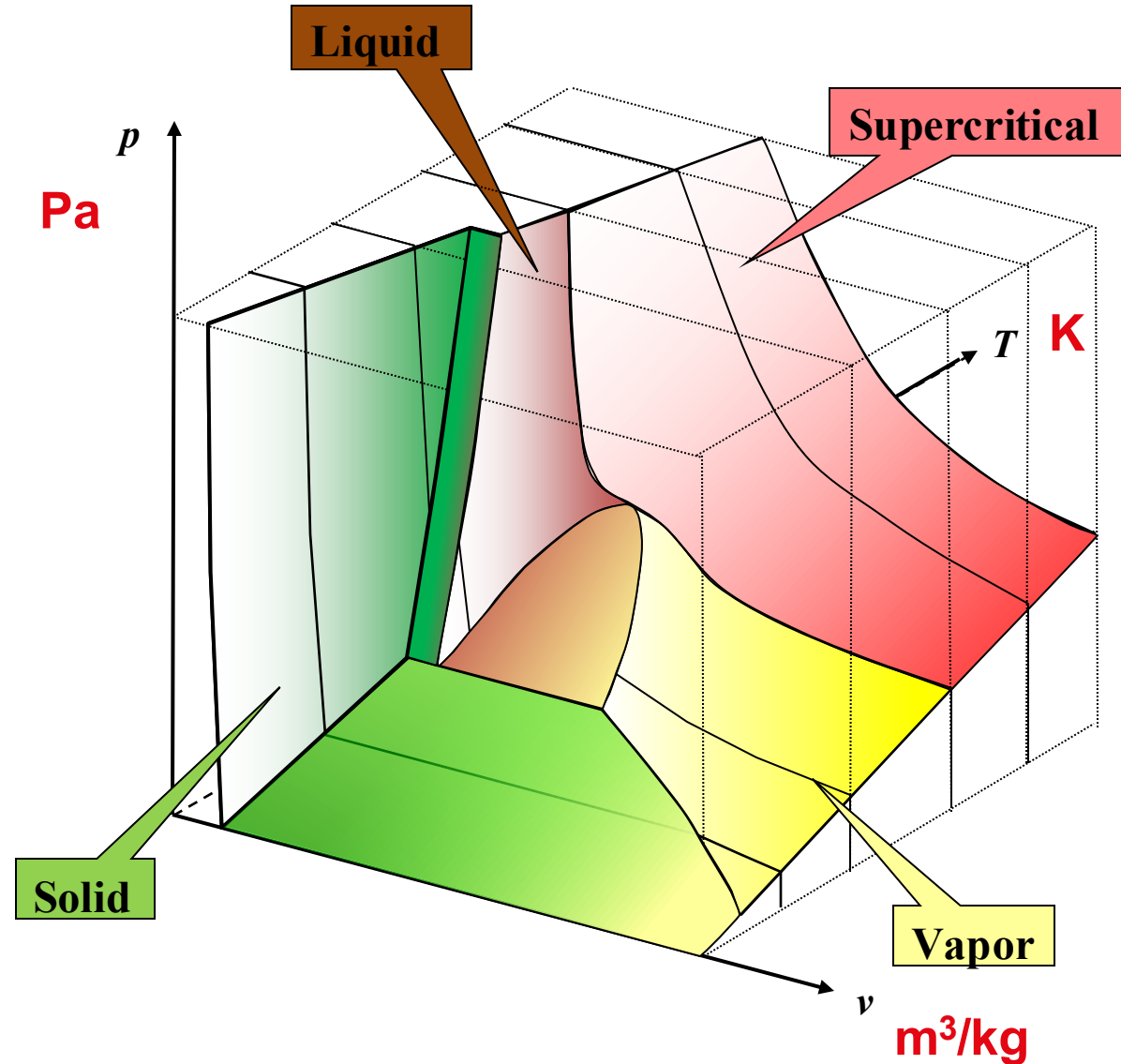
Pure Substance p-v-T Relation

Single phase regions:

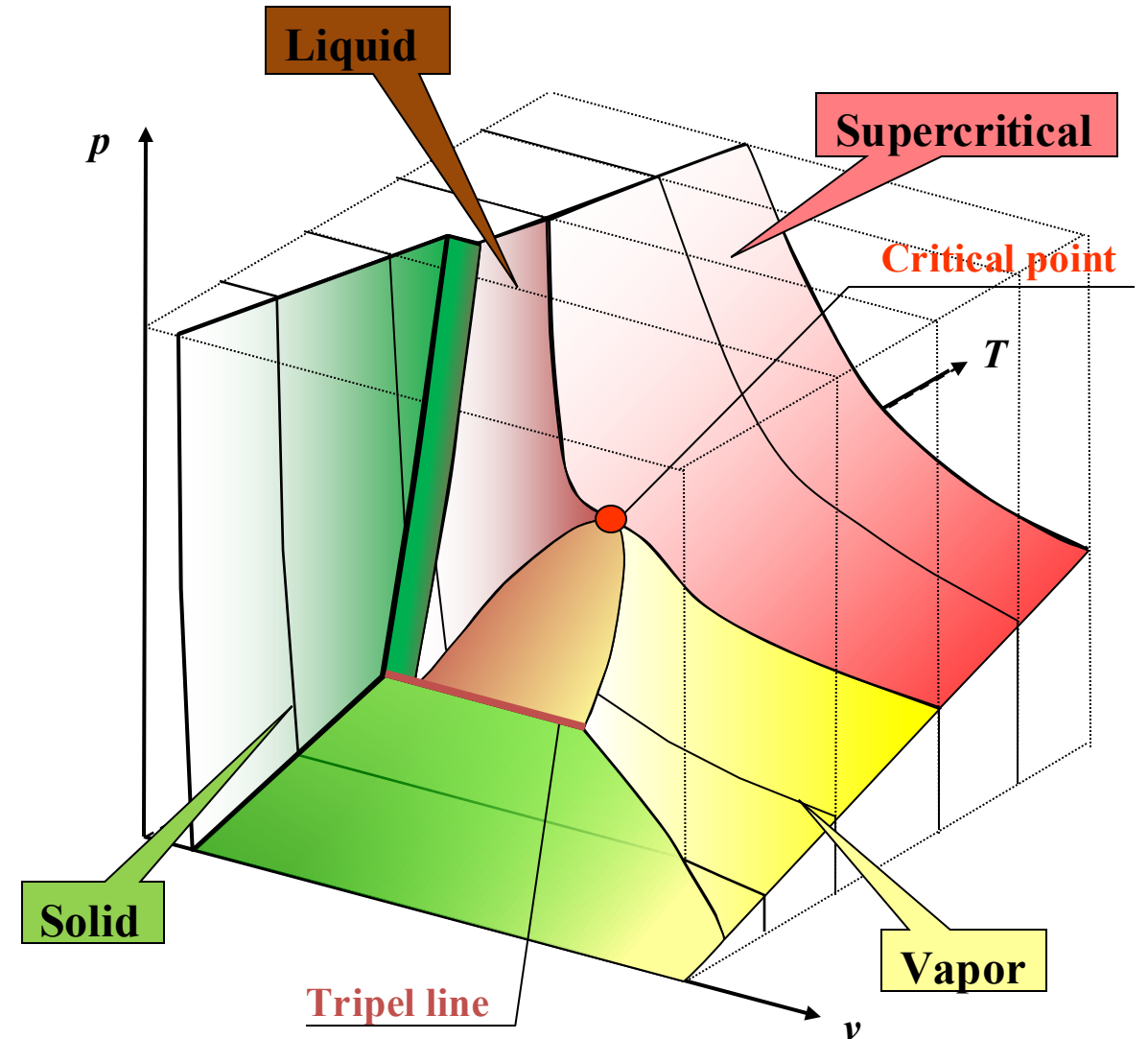
- **Solid**
- **Liquid**
- **Vapor**
- **Supercritical**

Two phase regions exist between the single-phase regions (co-existence of two phases in equilibrium)

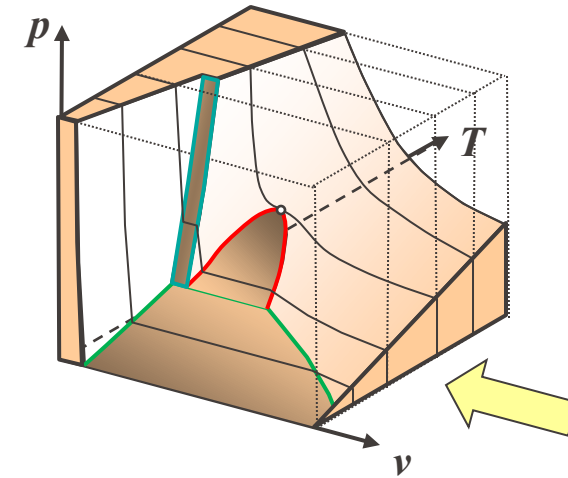
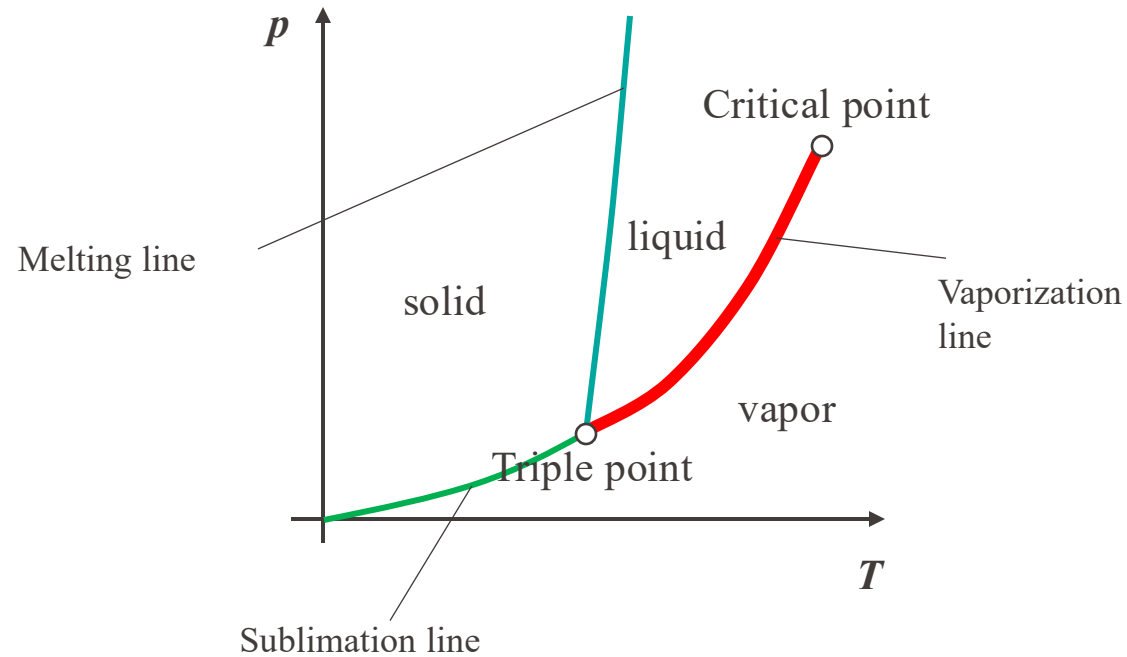
- **Solid-vapor**
- **Liquid-vapor**
- **Solid-liquid**



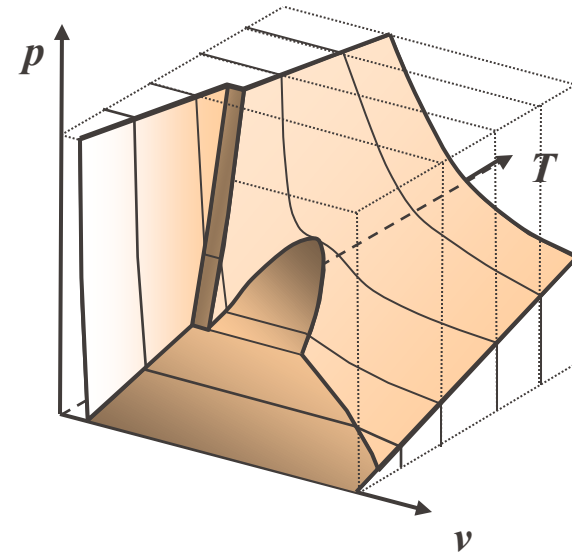
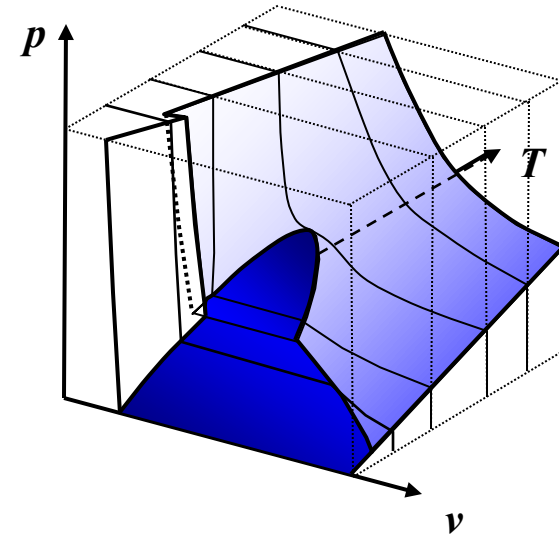
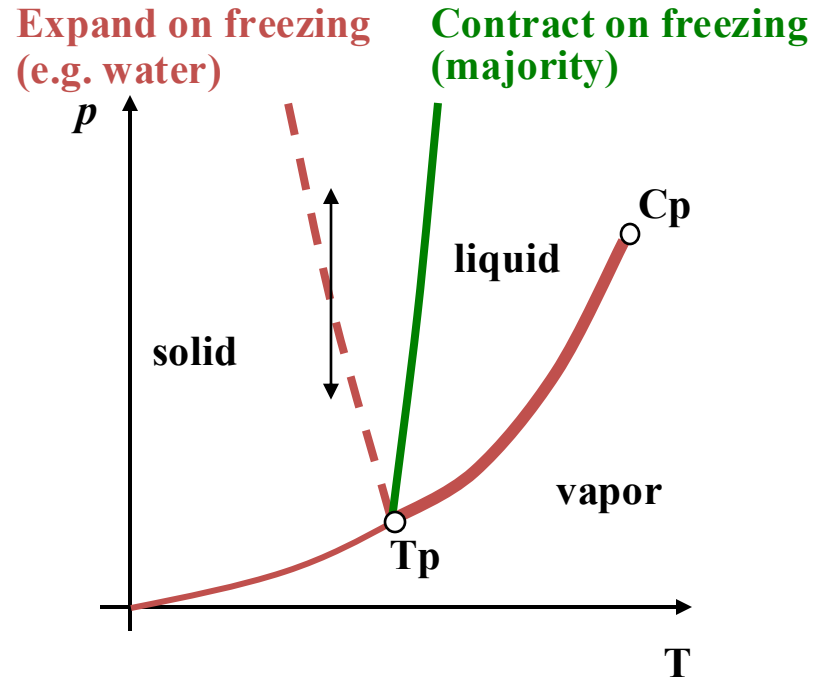
- In two-phase regions p and T are not independent! Need v to determine state.
- State where phase change begins or ends is called **saturation state**.
- Meeting point of the saturated liquid and saturated vapor lines is called **critical point**. Maximum p and T at which liquid and vapor can co-exist.
- **Triple line** separates liquid-vapor and solid-vapor two-phase regions. Three phases co-exist along it.



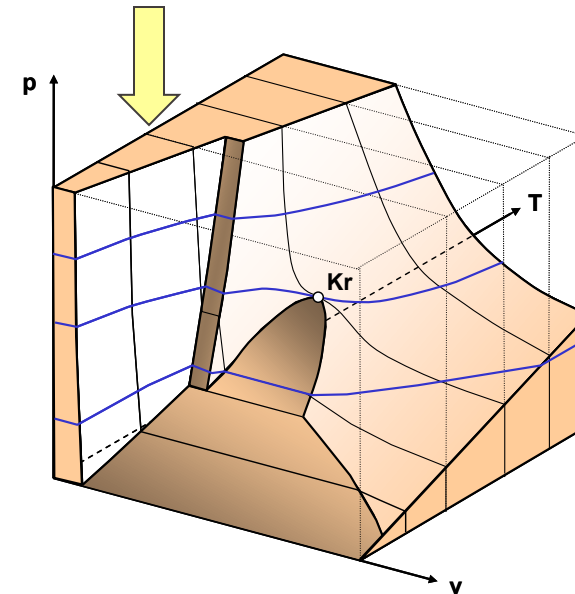
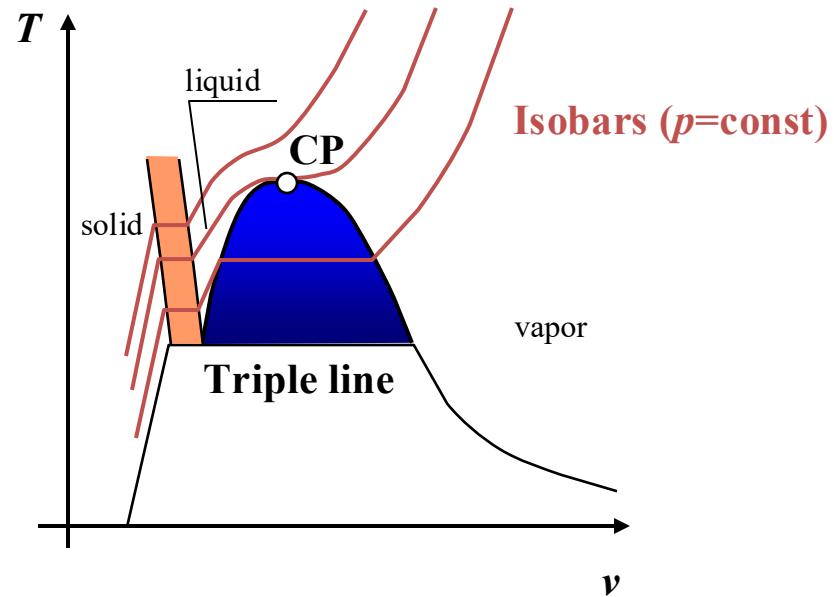
- Projection to p-T plane



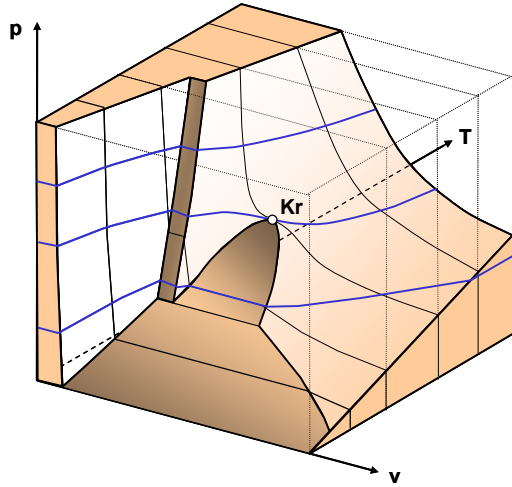
p-T diagram



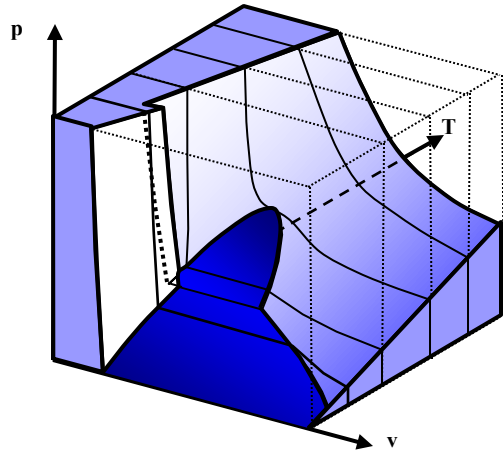
- Projection to T-v plane



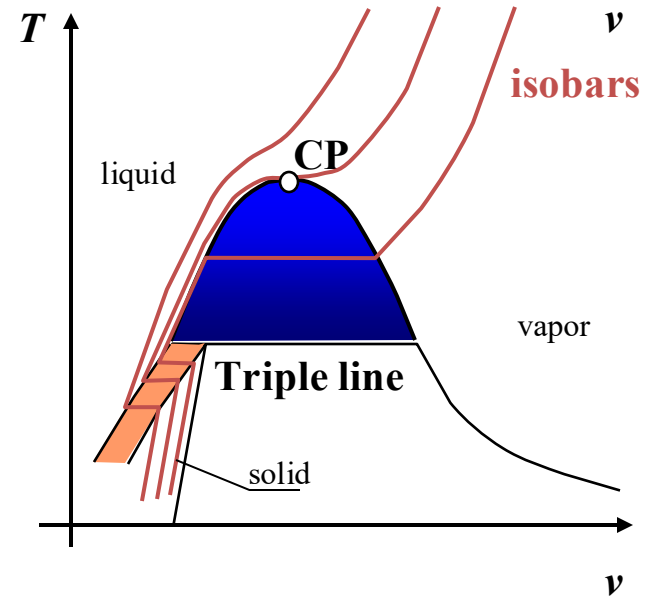
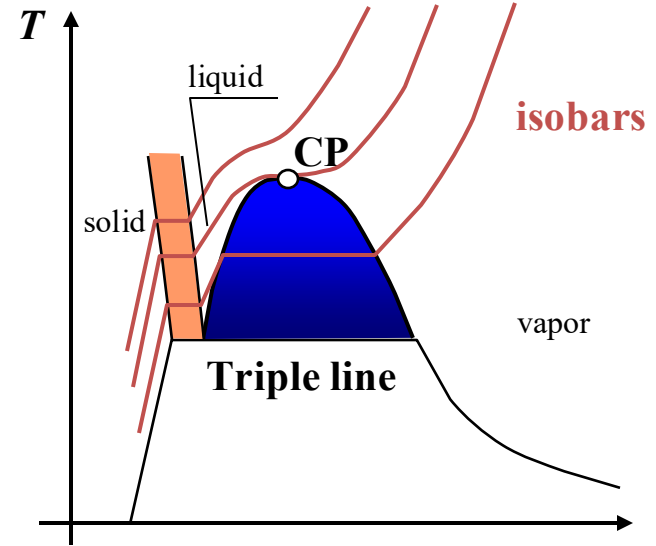
- At very low pressures: phase change from solid to vapor directly
- At moderate pressure (below critical pressure): solid to liquid, and then to vapor. Temperature is constant during isobaric phase change.
- For high pressures, no distinct phase transition between liquid and vapor

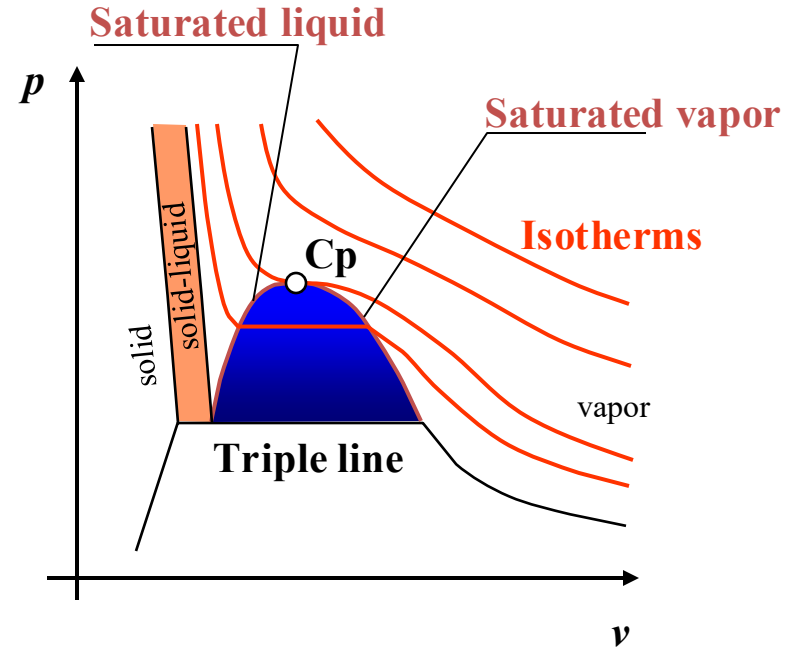
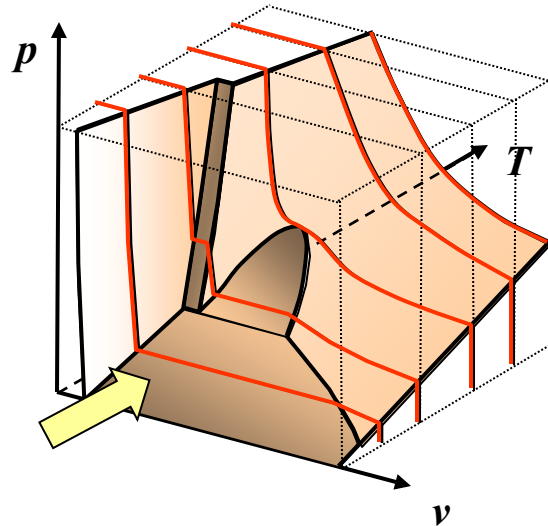


Contract on freezing



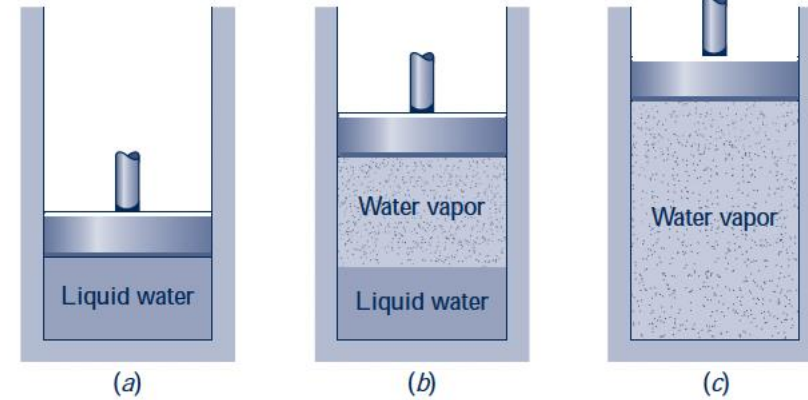
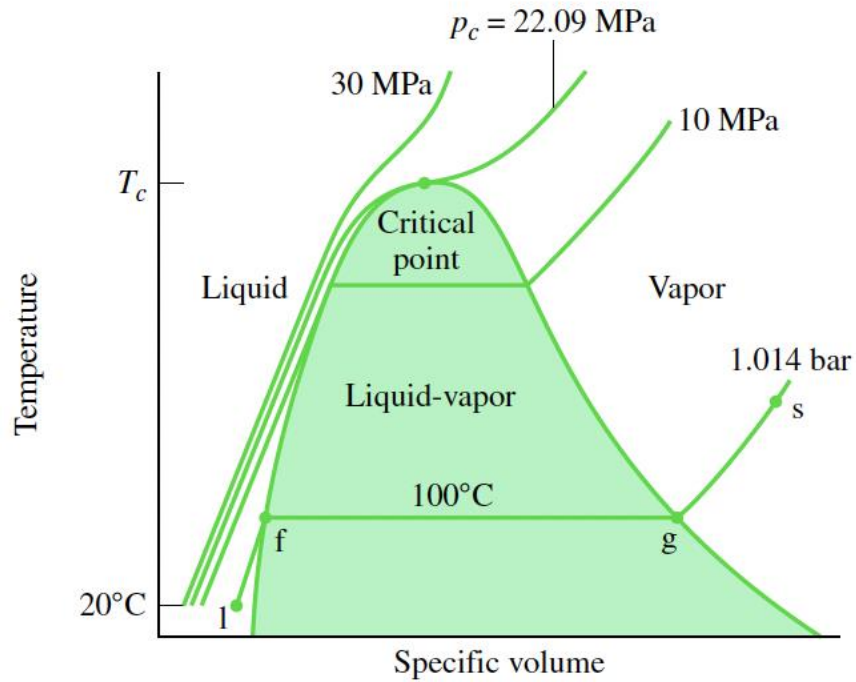
Expand on freezing



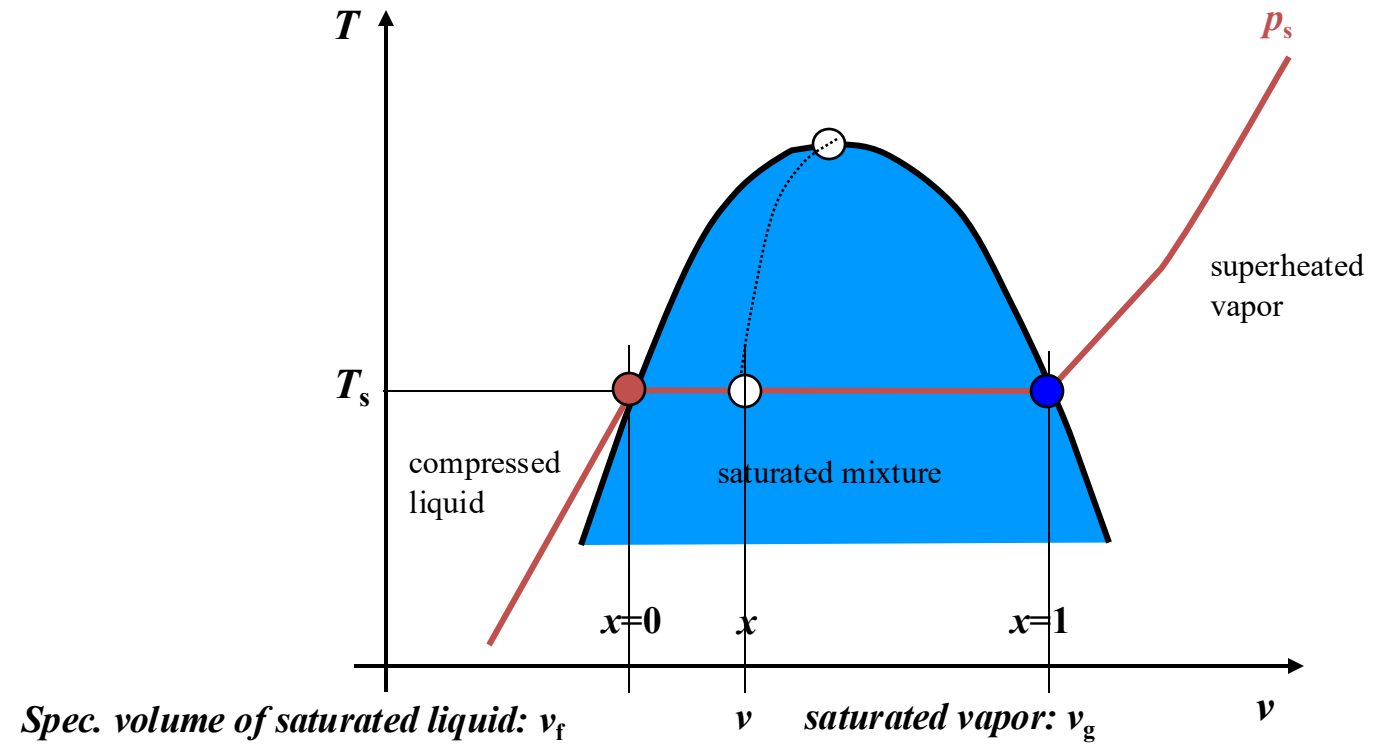


- At low temperatures, phase change from solid to vapor directly
- At moderate temperatures (below C_p): solid to liquid, and then to vapor. Pressure is constant during isobaric phase change (between saturated liquid and saturated vapor)
- At high temperatures, no distinct transition between liquid and vapor

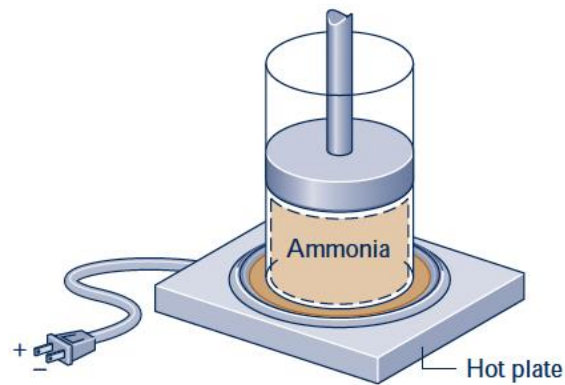
Two-Phase Liquid-Vapor Mixture



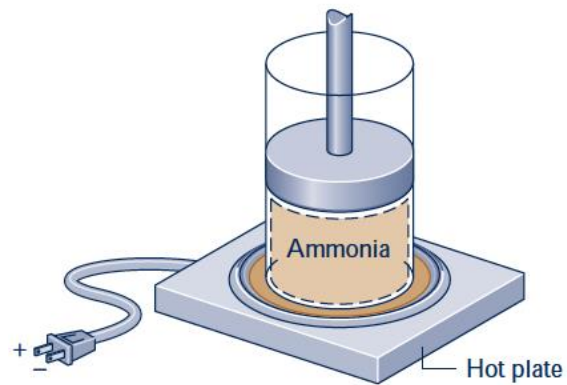
Saturation temperature is only defined after specifying pressure
water: 99.97 °C at 1.014 bar



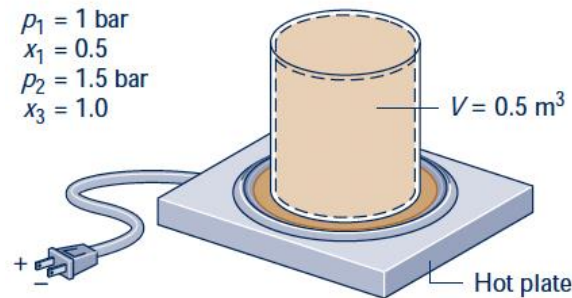
- A vertical piston-cylinder assembly contains ammonia, initially a saturated vapor, and is placed on a hot plate. The pressure of the ammonia is **1.5 bar**.
- Heating occurs slowly and the ammonia expands at constant pressure until the final temperature is **25°C**.
- **Show the initial and final state in p - v - and T - v -diagrams**



- A vertical piston-cylinder assembly contains ammonia, initially a saturated vapor, and is placed on a hot plate. The pressure of the ammonia is **1.5 bar**.
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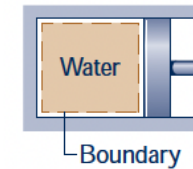


- A closed, rigid container of fixed volume is placed on a hot plate. Initially, at state 1, the container holds a two-phase mixture of saturated liquid water and saturated water vapor at $p_1 = 1 \text{ bar}$ with a **quality of 0.5**.
- After heating, at state 2, the pressure in the container is $p_2 = 1.5 \text{ bar}$. Finally, with further heating, at state 3, the container only contains **saturated vapor**.
- **Indicate states 1-3 on a T-v diagram**



- Water contained in a piston–cylinder assembly undergoes two processes in series from an initial state where the pressure is 10 bar and the temperature is 400 °C.
 - Process 1–2: The water is cooled as it is compressed at a constant pressure of 10 bar to the saturated vapor state.
 - Process 2–3: The water is cooled at constant volume to 150 °C.

Sketch both processes on T–v and p–v diagrams.



- How to determine properties?
- Using property tables, for:
 - Compressed liquid (e.g., Table-A5)
 - Superheated vapor (e.g., Table-A2, A3)
 - Saturated liquid-vapor mixture (e.g., Table-A4)

Properties of Compressed Liquid Water

T °C	$v \times 10^3$ m ³ /kg	u kJ/kg	h kJ/kg	s kJ/kg · K	$v \times 10^3$ m ³ /kg	u kJ/kg	h kJ/kg	s kJ/kg · K
$p = 25 \text{ bar} = 2.5 \text{ MPa}$ ($T_{\text{sat}} = 223.99^\circ\text{C}$)					$p = 50 \text{ bar} = 5.0 \text{ MPa}$ ($T_{\text{sat}} = 263.99^\circ\text{C}$)			
20	1.0006	83.80	86.30	.2961	.9995	83.65	88.65	.2956
40	1.0067	167.25	169.77	.5715	1.0056	166.95	171.97	.5705
80	1.0280	334.29	336.86	1.0737	1.0268	333.72	338.85	1.0720
100	1.0423	418.24	420.85	1.3050	1.0410	417.52	422.72	1.3030
140	1.0784	587.82	590.52	1.7369	1.0768	586.76	592.15	1.7343
180	1.1261	761.16	763.97	2.1375	1.1240	759.63	765.25	2.1341
200	1.1555	849.9	852.8	2.3294	1.1530	848.1	853.9	2.3255
220	1.1898	940.7	943.7	2.5174	1.1866	938.4	944.4	2.5128
Sat.	1.1973	959.1	962.1	2.5546	1.2859	1147.8	1154.2	2.9202

- How to determine properties from tables:
 - Linear interpolation of desired property (u, v, s, h, \dots) for desired temperature, pressure, ... (z):

$$f(z) = \frac{f(z_2) - f(z_1)}{z_2 - z_1} (z - z_1) + f(z_1)$$

Moran 3.8.1

- **Instead of tables, we can also use databases online, e.g.:**
 - <http://www.coolprop.org/>



- <https://colab.research.google.com/drive/1x1MU3CXz5fMMe7nZgiKsZopjYz2jvvQ1?usp=sharing>

- Read the manual before using the package

<http://www.coolprop.org/coolprop/HighLevelAPI.html#propssi-function>