

## Thermodynamics and energetics I: Exercise 8, Solution

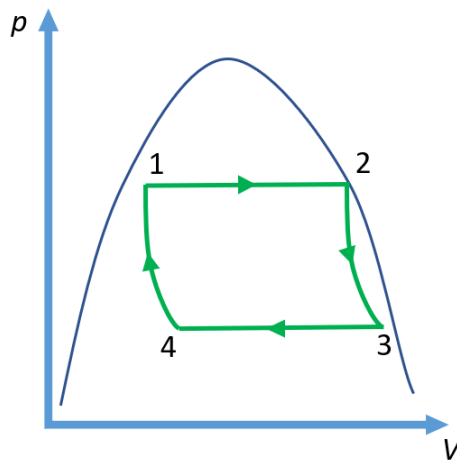
1. A Carnot power cycle is operated with steam/water as the working fluid. During the isothermal expansion, the water is heated from an initial state 1, with pressure  $p_1$ , temperature  $T_1$  and the quality 15 %, to saturated vapor state 2. The vapor then expands isentropically to a state 3 with temperature  $T_3$  and pressure  $p_3 < p_1$ . Isothermal compression then bring state 3 to state 4, and then back to state 1 with an isentropic compression.

Note the specific entropies at the saturate states satisfies  $s_g(p_3) < s_g(p_1) < s_f(p_1) < s_f(p_3)$

- (a) Sketch the states and the processes in the  $p$  $v$  diagram. (Don't be concerned about the specific shape of the isentropic curve)
- (b) Describe how you would obtain the specific internal energy and specific entropy for each of the 4 states in the Carnot cycle. Provide an analytical expression, not a numerical solution.
- (c) Determine the expressions for heat and work transfer for each process, assuming you know the specific internal energy and specific entropy for each of the 4 states in the Carnot cycle. Provide an analytical expression, not a numerical solution.
- (d) Provide an expression for the thermal efficiency.

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- (a) The Carnot cycle consists of the following processes:

- 1-2: Isothermal expansion
- 2-3: Adiabatic, reversible expansion (isentropic)
- 3-4: Isothermal compression
- 4-1: Adiabatic, reversible compression (isentropic)



(b)

- state 1

$$x_1 = 0.150$$

$$T_1 = T_{\text{sat}}(p_1)$$

$$u_1 = u_f + x_1(u_g - u_f)$$

$$s_1 = s_f + x_1(s_g - s_f)$$

- state 2

$$x_2 = 1$$

Process 1-2 is isothermal:  $T_2 = T_1$

In the two-phase region it holds that if  $T = \text{constant}$  also  $p = \text{constant}$ .  $p_2 = p_1$

$$u_2 = u_g(p_2)$$

$$s_2 = s_g(p_2)$$

- state 3

Process 2-3 is isentropic:  $s_3 = s_2$

$$x_3 = \frac{s_3 - s_f}{s_g - s_f}$$

$$T_3 = T_{\text{sat}}(p_3)$$

$$u_3 = u_f + x_3(u_g - u_f)$$

- state 4

Process 3-4 is isothermal:  $T_4 = T_3, p_4 = p_3$

Process 4-1 is isentropic:  $s_4 = s_1$

$$x_4 = \frac{s_4 - s_f}{s_g - s_f}$$

$$u_4 = u_f + x_4(u_g - u_f)$$

(c) First law of thermodynamics (closed system):  $\Delta U = Q - W$

- 1-2 (isobaric and isothermal)

$$W_{12} = m \int_1^2 p dv = mp_1(v_2 - v_1)$$

$$Q_{12} = m(u_2 - u_1) + W_{12}$$

or

$$Q_{12} = m \int_1^2 T ds = T_1 m(s_2 - s_1)$$

*Note:* Although 1-2 is an isothermal process,  $\Delta U \neq 0$  because it is not an ideal gas/liquid. In the last equation.

- 2-3 (adiabatic)

$$Q_{23} = 0$$

$$W_{23} = -U_{23} = -m(u_3 - u_2)$$

- 3-4 (isobaric and isothermal)

$$W_{34} = m \int_3^4 p dv = mp_3(v_4 - v_3)$$

$$Q_{34} = U_{34} + W_{34} = m(u_4 - u_3) + W_{34}$$

or

$$Q_{34} = m \int_3^4 T ds = T_3 m(s_4 - s_3)$$

- 4-1 (adiabatic)

$$Q_{41} = 0$$

$$W_{41} = -U_{41} = -m(u_1 - u_4)$$

(d)

$$\eta_{\text{th}} = \frac{W_{12} + W_{23} + W_{34} + W_{41}}{Q_{12}}$$

Or

$$\eta_{\text{Carnot}} = 1 - \frac{T_C}{T_H} = 1 - \frac{T_3}{T_1} = 1 - \frac{T_4}{T_2}$$

2.

$$M_{\text{air}} = 29 \text{ g/mol} \rightarrow R_{\text{air}} = \frac{\tilde{R}}{M_{\text{air}}} = 286.7 \text{ J/(kg K)}$$

(a)

$$T_1 = \frac{p_1 V_1}{m R_{\text{air}}} = 586.0 \text{ K} = 312.85 \text{ }^\circ\text{C} = T_2 = T_{\text{H}}$$

$$\eta_{\text{Carnot}} = 1 - \frac{T_{\text{C}}}{T_{\text{H}}}$$

$$T_{\text{C}} = (1 - \eta_{\text{Carnot}}) T_{\text{H}} = 234.4 \text{ K} = -38.77 \text{ }^\circ\text{C} = T_3 = T_4$$

(b) First law of thermodynamics (closed system):  $\Delta U = Q - W$

• 1-2 (isothermal)

Under the hypothesis of perfect gas,  $\Delta U_{12} = 0$

$$W_{12} = Q_{12} = 40 \text{ kJ}$$

$$pV = m R_{\text{air}} T_1 = p_1 V_1 \rightarrow p = p_1 \frac{V_1}{V}$$

$$W_{12} = \int_1^2 p dV = \int_1^2 p_1 \frac{V_1}{V} dV = p_1 V_1 \ln \left( \frac{V_2}{V_1} \right)$$

$$V_2 = V_1 \cdot \exp \left( \frac{W_{12}}{p_1 V_1} \right) = 0.3045 \text{ m}^3$$

(c)

$$p_2 = \frac{m R_{\text{air}} T_2}{V_2} = 5.517 \text{ bar}$$

Process 2-3 is isentropic:

$$pV^\gamma = \text{constant} \rightarrow \frac{m R_{\text{air}} T}{V} V^\gamma = \text{constant} \rightarrow T \cdot V^{(\gamma-1)} = \text{constant}$$

$$V_3 = \left( \frac{T_2}{T_3} V_2^{(\gamma-1)} \right)^{\frac{1}{\gamma-1}} = V_2 \left( \frac{T_2}{T_3} \right)^{\frac{1}{\gamma-1}} = 3.009 \text{ m}^3$$

Process 4-1 is isentropic:

$$V_4 = V_1 \left( \frac{T_1}{T_4} \right)^{\frac{1}{\gamma-1}} = 2.372 \text{ m}^3$$

$$p_4 = \frac{m R_{\text{air}} T_4}{V_4} = 0.2833 \text{ bar}$$

state	1	2	3	4
$p$ [bar]	7	5.517	0.2233	0.2833
$V$ [m <sup>3</sup> ]	0.240	0.3045	3.009	2.372
$T$ [°C]	312.8	312.8	-38.77	-38.77
$T$ [K]	586.0	586.0	234.4	234.4

(d) • 2-3 (isentropic)

$$Q_{23} = 0$$

$$pV^\gamma = \text{constant} \rightarrow p = p_2 \frac{V_2^\gamma}{V^\gamma}$$

$$W_{23} = \int_2^3 p dV = \int_2^3 p_2 \frac{V_2^\gamma}{V^\gamma} dV = \frac{p_2 V_2^\gamma}{1-\gamma} (V_3^{1-\gamma} - V_2^{1-\gamma}) = \frac{p_2 V_2 - p_3 V_3}{\gamma - 1} = 252.0 \text{ kJ}$$

• 3-4 (isothermal)

$$W_{34} = p_3 V_3 \ln \left( \frac{V_4}{V_3} \right) = -16 \text{ kJ}$$

$$\Delta U_{34} = 0 \rightarrow W_{34} = Q_{34} = -16 \text{ kJ}$$

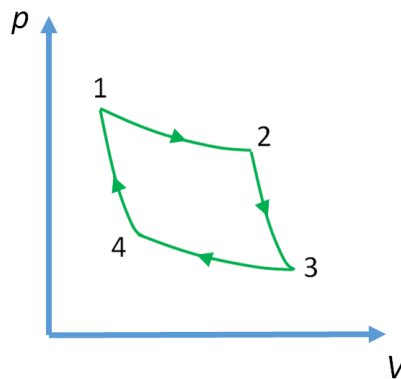
• 4-1 (isentropic)

$$Q_{41} = 0$$

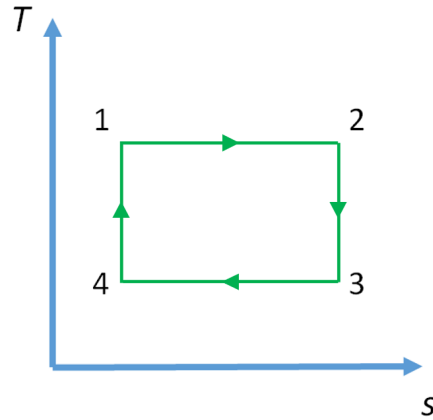
$$W_{41} = \int_4^1 p dV = \frac{p_1 V_1 - p_4 V_4}{1-\gamma} = -252.0 \text{ kJ}$$

	$W$ [kJ]	$Q$ [kJ]
1-2	40	40
2-3	252.0	0
3-4	-16	-16
4-1	-252.0	0

(e)



3. (a) *Note:* This is a Carnot cycle.



- (b)

$$M_{\text{air}} = 29 \text{ g/mol} \rightarrow R_{\text{air}} = 286.7 \frac{\text{J}}{\text{kg K}}$$

$$\text{For perfect gas: } c_v = \frac{1}{\gamma - 1} R_{\text{air}} = 716.8 \frac{\text{J}}{\text{kg K}}$$

$$V_1 = \frac{m R_{\text{air}} T_1}{p_1} = 0.014 \text{ m}^3$$

$$V_2 = \frac{m R_{\text{air}} T_2}{p_2} = 0.072 \text{ m}^3$$

$$\text{Process 2-3 is isentropic (see 3c): } V_3 = V_2 \left( \frac{T_2}{T_3} \right)^{\frac{1}{\gamma-1}} = 0.125 \text{ m}^3$$

$$p_3 = \frac{m R_{\text{air}} T_3}{V_3} = 4.579 \text{ bar}$$

$$\text{Process 4-1 is isentropic: } V_4 = V_1 \left( \frac{T_1}{T_4} \right)^{\frac{1}{\gamma-1}} = 0.025 \text{ m}^3$$

$$p_4 = \frac{m R_{\text{air}} T_4}{V_4} = 22.90 \text{ bar}$$

	$p$ [bar]	$V$ [m <sup>3</sup> ]	$T$ [K]
1	50	0.014	500
2	10	0.072	500
3	4.579	0.125	400
4	22.90	0.025	400

- (c) • 1-2 (isothermal)

$$W_{12} = p_1 V_1 \ln \left( \frac{V_2}{V_1} \right) = 115.4 \text{ kJ}$$

$$\Delta U_{12} = 0, \text{ therefore: } Q_{12} = W_{12} = 115.4 \text{ kJ}$$

- 2-3 (isentropic)

$$Q_{23} = 0$$

$$W_{23} = -\Delta U_{23} = 35.84 \text{ kJ}$$

- 3-4 (isothermal)

$$W_{34} = p_3 V_3 \ln \left( \frac{V_4}{V_3} \right) = -92.29 \text{ kJ}$$

$$\Delta U_{34} = 0, \text{ therefore: } Q_{34} = W_{34} = -92.29 \text{ kJ}$$

- 4-1 (isentropic)

$$Q_{41} = 0$$

$$W_{41} = -\Delta U_{41} = -35.84 \text{ kJ}$$

	$W$ [kJ]	$Q$ [kJ]	$\Delta U$ [kJ]
1-2	115.4	115.4	0
2-3	35.84	0	-35.84
3-4	-92.29	-92.29	0
4-1	-35.84	0	35.84

- (d)

$$Q_{\text{net}} = Q_{12} + Q_{34} = 23.07 \text{ kJ}$$

$$W_{\text{net}} = W_{12} + W_{23} + W_{34} + W_{41} = 23.07 \text{ kJ}$$

- (e)

$$\eta_{\text{th}} = \frac{W_{12} + W_{23} + W_{34} + W_{41}}{Q_{12}} = 0.2$$

$$\text{Note: } \eta_{\text{Carnot}} = 1 - \frac{T_4}{T_2} = 0.2$$

(f) Each process is internally reversible, therefore it is possible to write:

$$dS = \left( \frac{\delta Q}{T} \right)_{\text{int rev}} \rightarrow \Delta S = \int \frac{\delta Q}{T}$$

$$\Delta S_{12} = \int_1^2 \frac{\delta Q}{T} = \frac{Q_{12}}{T_1} = \frac{115.4}{500} = 0.23 \frac{\text{kJ}}{\text{K}}$$

$$\Delta S_{23} = \int_2^3 \frac{\delta Q}{T} = 0$$

$$\Delta S_{34} = \int_3^4 \frac{\delta Q}{T} = \frac{Q_{34}}{T_3} = \frac{-98.29}{400} = -0.23 \frac{\text{kJ}}{\text{K}}$$

$$\Delta S_{41} = \int_4^1 \frac{\delta Q}{T} = 0$$

$$\Delta S_{\text{cycle}} = \oint \frac{\delta Q}{T} = \Delta S_{12} + \Delta S_{23} + \Delta S_{34} + \Delta S_{41} = 0$$

*Note:* The entropy variation in adiabatic and internally reversible processes is zero (isentropic processes). Being a state property, in every cycle (either reversible or irreversible) the total variation of entropy is zero.