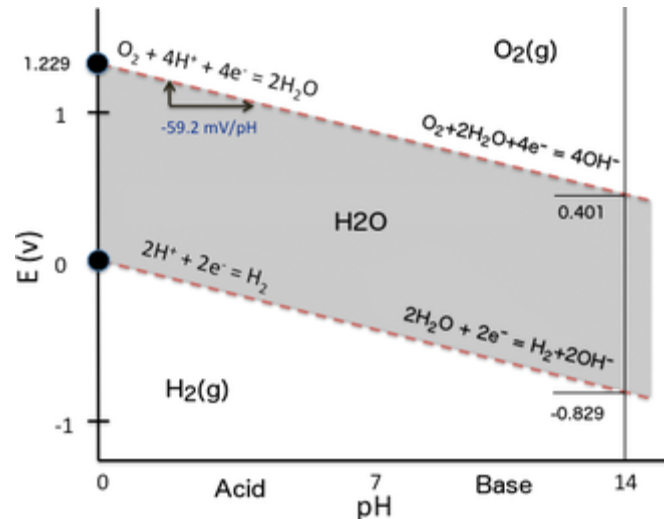


Electrolysers

1) A lab scale 1 kW alkaline water electrolyser operates at 70% HHV efficiency. The stack is operated at 60°C and is electrically connected in series, with each cell having a surface of 100 cm². The supporting electrolyte used is 1 M potassium hydroxide (pH=14), in conjunction with Zirfon Perl UTP 500µm thick diaphragm separator. The nominal current density of operation is 0.5 A cm⁻². The Pourbaix diagram for water electrolysis is given in the figure below.



Calculate:

- Reversible cell potential for hydrogen evolution ($E_{\text{rev,H}_2}$) and oxygen evolution ($E_{\text{rev,O}_2}$) reactions. (considering pH=14)
- The thermoneutral voltage (E_{tn}) at 25°C and at 60°C. (E_{tn} corresponds to $-\Delta H/nF$)
- The number of cells in the stack and the corresponding operating voltage of each cell.
- The water flowrate in L min⁻¹ necessary at the cathode to reach a conversion rate of 80%, assuming a Faradaic efficiency (=current efficiency) of 100%.

Further thinking:

- Is Faradaic efficiency of 100% a relevant assumption?
- How does the thermoneutral voltage change with the phase change of water to steam?

Hints:

HHV efficiency is defined as: $\eta_{\text{HHV}} = \frac{E_{\text{tn}}}{E_{\text{cell}}}$

for the reaction $\text{H}_2\text{O}(\text{l}) \rightarrow \text{H}_2(\text{g}) + \text{O}_2(\text{g})$ assume

$\Delta H_{25^\circ\text{C}} = 285.83 \text{ kJ mol}^{-1}$
$\Delta H_{60^\circ\text{C}} = 284.72 \text{ kJ mol}^{-1}$
$\text{HHV} = 141.88 \text{ MJ kg}^{-1}$
$\rho_{\text{H}_2} = 0.0813 \text{ g L}^{-1}$

