
Heat exchanger network design

Pinch design method

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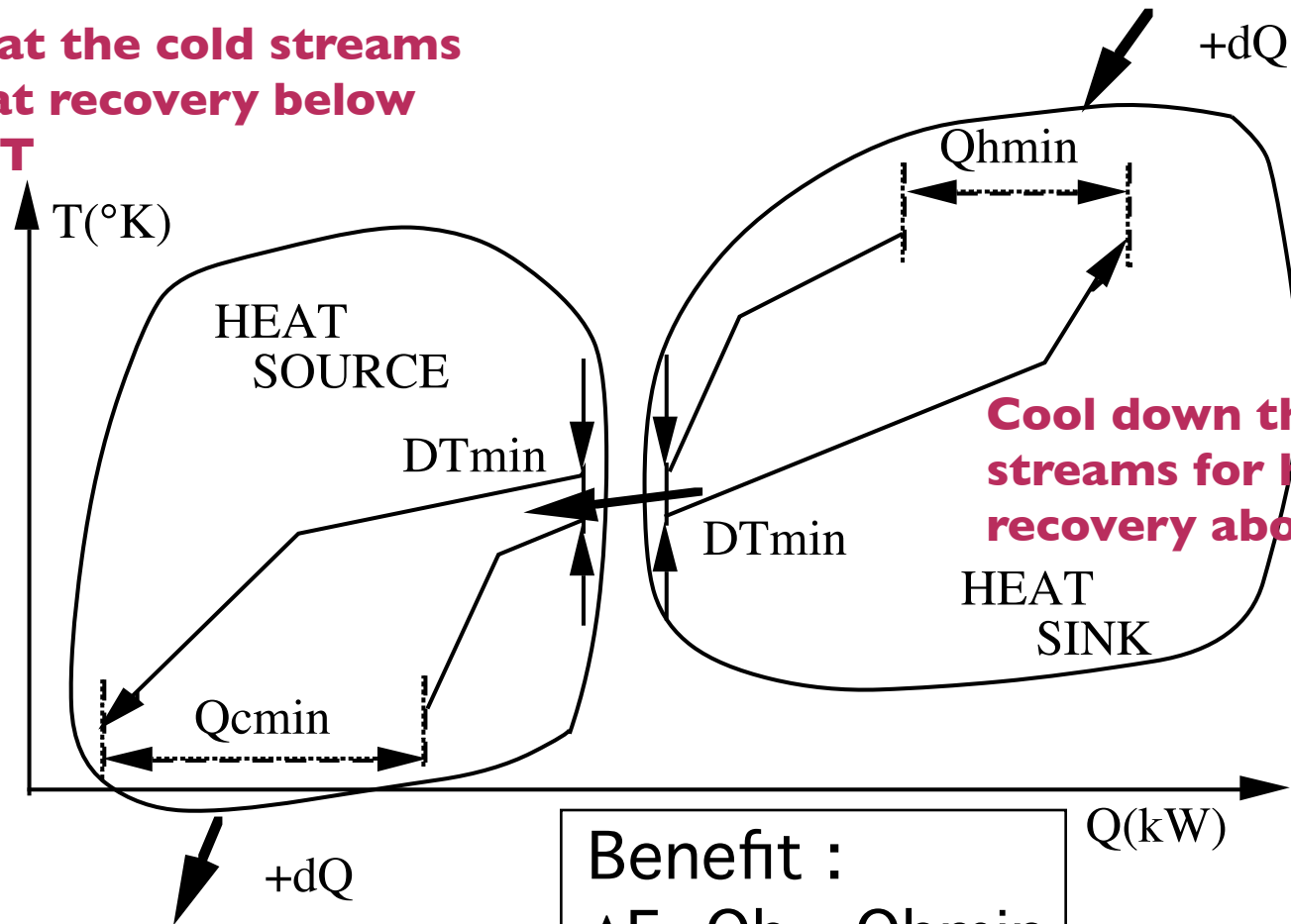
Conclusions of previous steps

- DTmin optimum
- Maximum heat recovery target
 - Utility heat load (hot, cold and refrigeration)
- Pinch point location
- Minimum number of heat exchangers
- Overall DTmin
- Non penalising heat exchangers
 - reduces the list of hot and cold streams to be considered

What is the heat exchanger network ?

The more in - the more out

Preheat the cold streams
by heat recovery below
pinch T



Cool down the hot
streams for heat
recovery above pinch T

Benefit :

$$\Delta E = Q_h - Q_{hmin}$$

$$\Delta E = Q_c - Q_{cmin}$$

$Q_H - Q_C = \text{Constant !}$

Minimum number of units

Pinch point = two independent sub-systems

Number of Independent sub-systems above the pinch point

Number of Independent sub-systems below the pinch point

$$U_{\min, MER} = (N_{above} - 1 - S_{above}) + (N_{below} - 1 - S_{below})$$

Number of streams above the pinch point

Number of streams below the pinch point

$$U_{\min, MER} = (N_{total} + N_{utility} - 1) + (N_{pinch} - 1) - (S_{above} + S_{below})$$

Total number of streams, including the utilities

Number of streams crossing the pinch point

Number of Independent sub-systems below and above the pinch point

Heat exchangers network synthesis

Find a heat exchangers network that satisfies:

- MER
- Minimum number of units
- Minimum investment
- Other criteria

- Which hot stream exchanges with which cold stream ?
- What is the heat exchanged ?
- What is the structure : serial or //, ...

Above pinch point

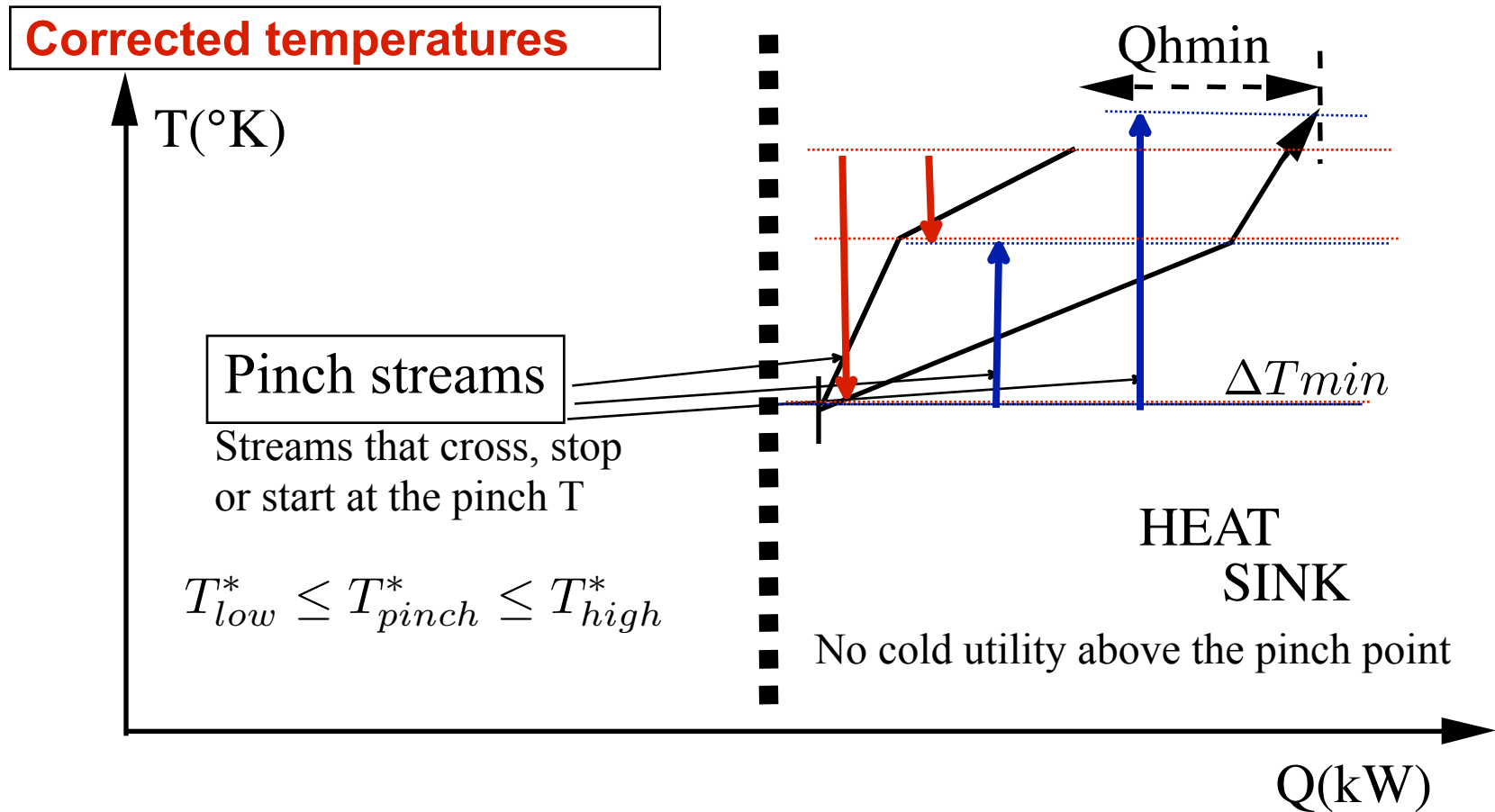
Drive hot streams to the pinch point or target temperature without cold utility

Below pinch point

Drive the cold streams to the pinch point or target temperature without hot utility

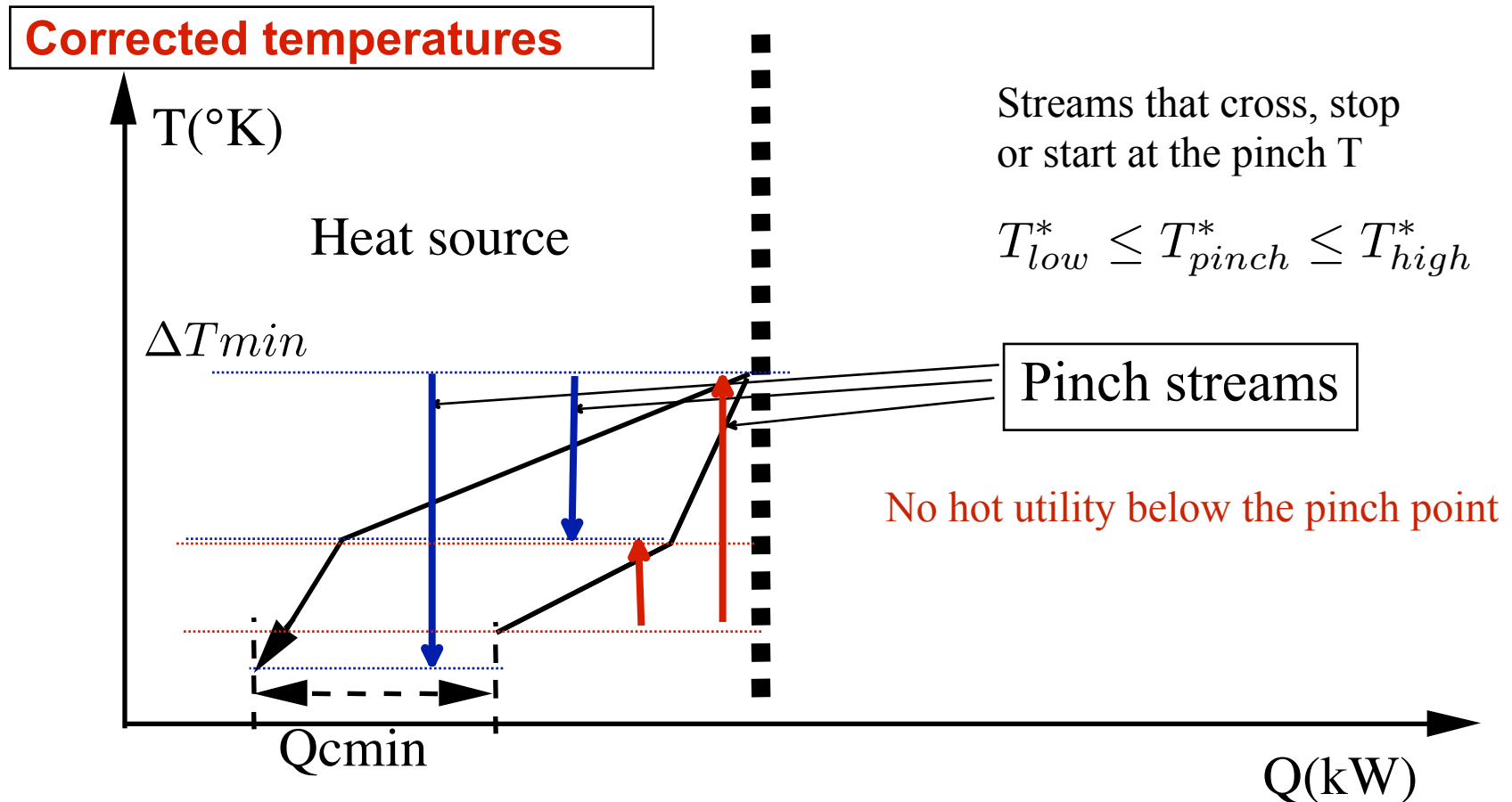
Above the Pinch point

The goal is to cool down **hot streams** to the pinch temperature or the target temperature without additional utility streams



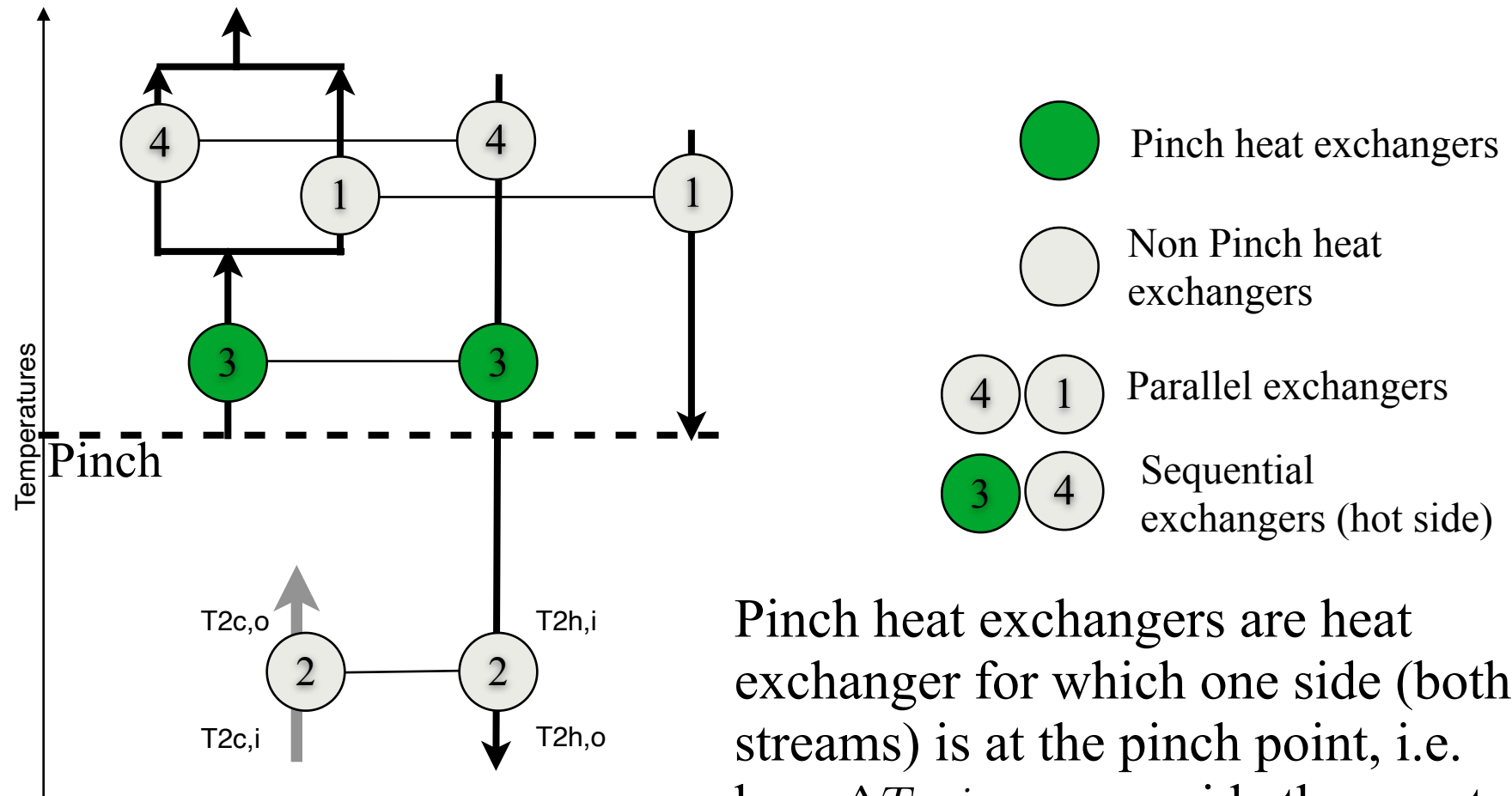
below the Pinch point

The goal is to heat up **cold streams** to the pinch temperature or the target without additional hot utility



Grid representation of HEN

Streams with inlet and outlet temperatures



Pinch heat exchangers are heat exchanger for which one side (both streams) is at the pinch point, i.e. have ΔT_{min} on one side the counter current heat exchanger

Feasibility rules for heat exchanger placement

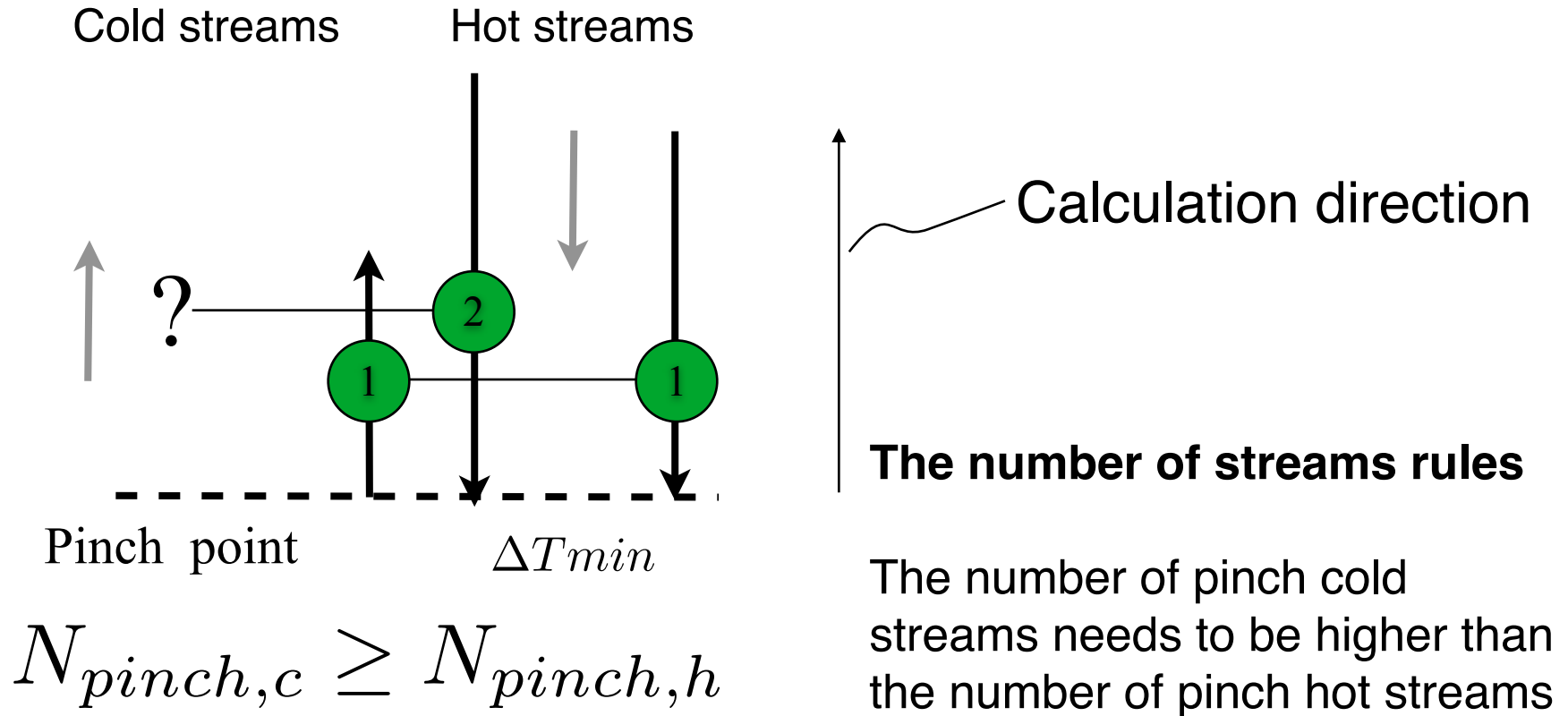
- For a pinch heat exchanger
 - Temperature difference on one side is known and is the DT_{min}
 - in reality $T_h^* - T_c^* = 0$
 - Goal :
 - above : cool down to pinch without cold utility
 - below : heat up to pinch without hot utility
- => Feasibility rules for pinch heat exchangers

Number of streams rule

Above the pinch :

Start from the pinch point and go towards increasing temperatures

The goal is to cool down **hot streams** to the pinch without cold utility



Direction of calculation : from the pinch to the highest temperatures

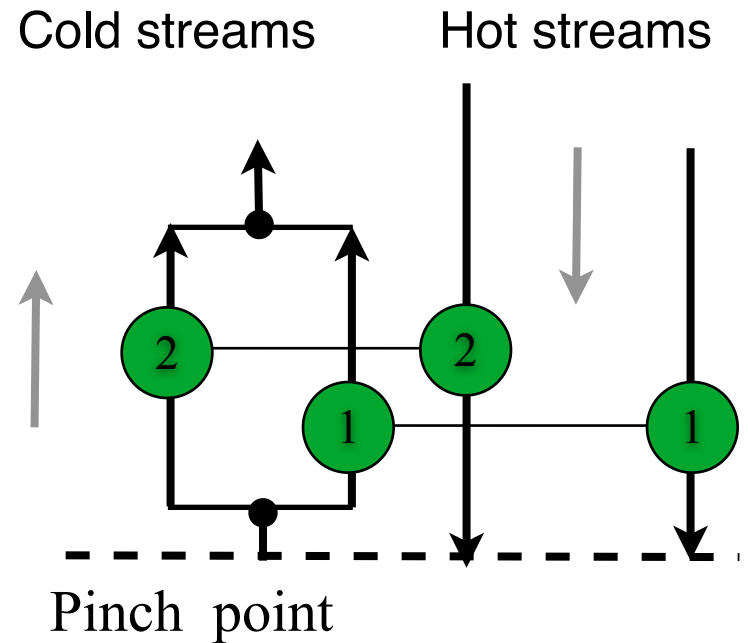
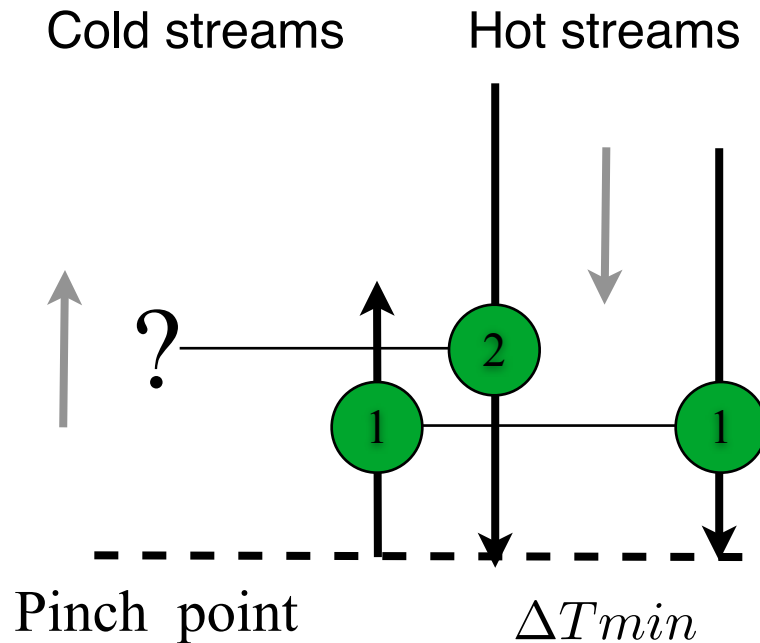
Note for the key streams (hot streams) we start from the target temperature , i.e. reach the pinch and go to highest temperatures, i.e. to the start temperature. the reverse for the cold streams, we start from the pinch or start temperature and go to the target (finishing with the hot utility).

Number of streams solution : splitting cold streams

Above the pinch :

Start from the pinch point and go towards increasing temperatures

The goal is to cool down **hot streams** to the pinch without cold utility



$$N_{pinch,c} \geq N_{pinch,h} \quad \text{otherwise split 1 cold stream}$$

At the pinch we know that the temperature difference is the ΔT_{min} , it can therefore be used as the starting point for the calculation in order to calculate the other side of the counter current heat exchanger

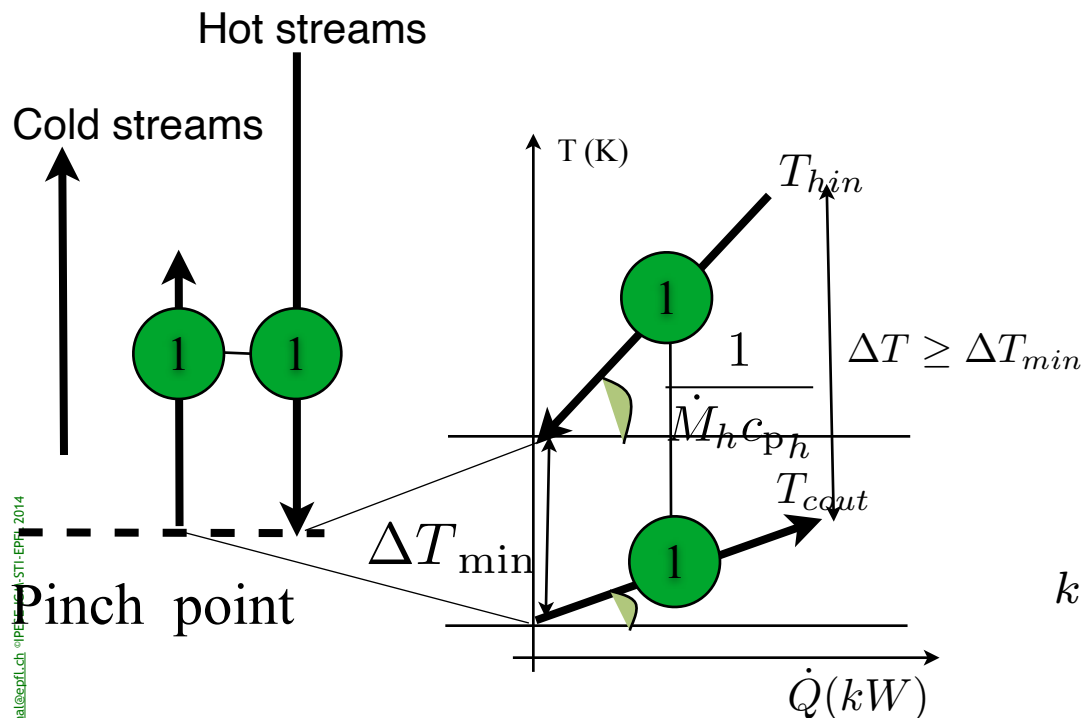
CP Rule : for pinch exchangers above the pinch

Above the pinch :

Start from the pinch point and go towards increasing temperatures

The goal is to cool down **hot streams** to the pinch without cold utility

Connexion feasibility between c and h



$$\dot{M}c_{p_h} \leq \dot{M}c_{p_c}$$

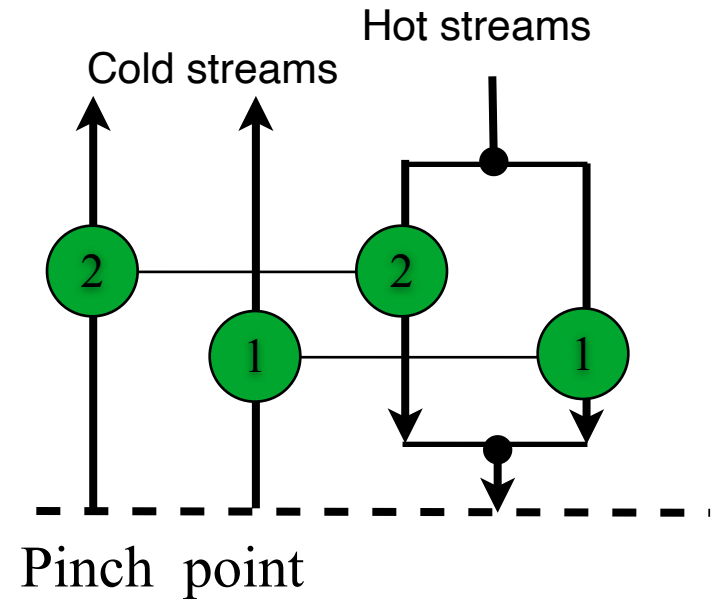
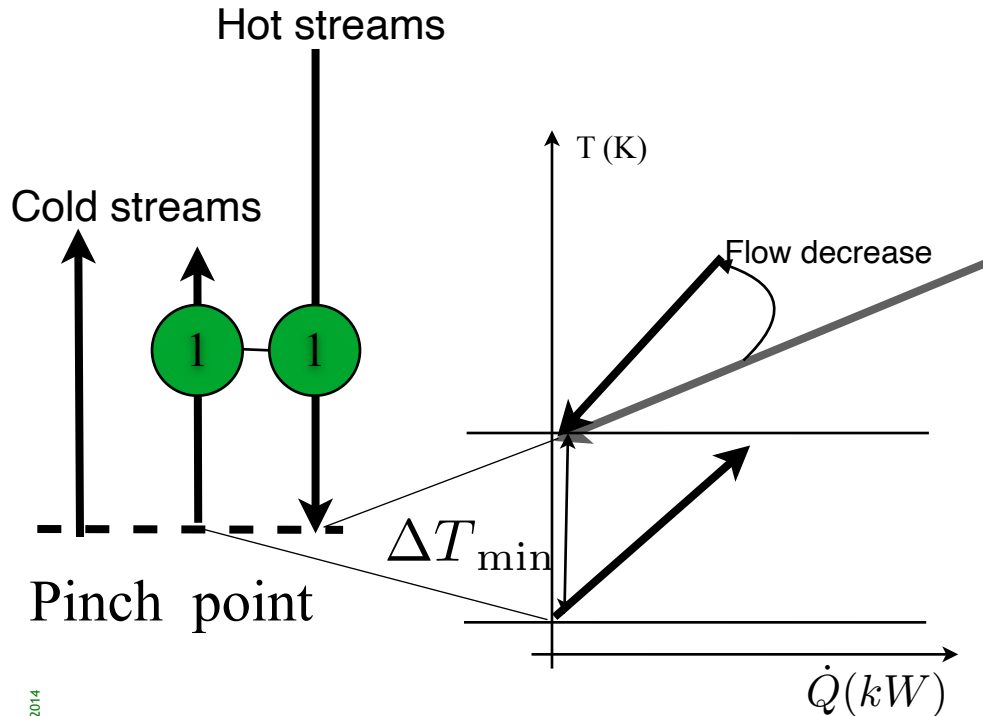
AND

$$\sum_{k=1, k \neq h}^{n_k} \dot{M}c_{p_k} \leq \sum_{j=1, j \neq c}^{n_{k-1}} \dot{M}c_{p_j}$$

At the pinch we know that the temperature difference is the ΔT_{min} , it can therefore be used as the starting point for the calculation in order to calculate the other side of the counter current heat exchanger

CP Rule : for pinch exchangers above the pinch

If Cp rule not satisfied split 1 hot stream



This is reducing the M_{cp} of hot stream in heat exchanger
CP rule is satisfied
Is Number of streams rule still valid ?

Feasibility rules for heat exchanger placement

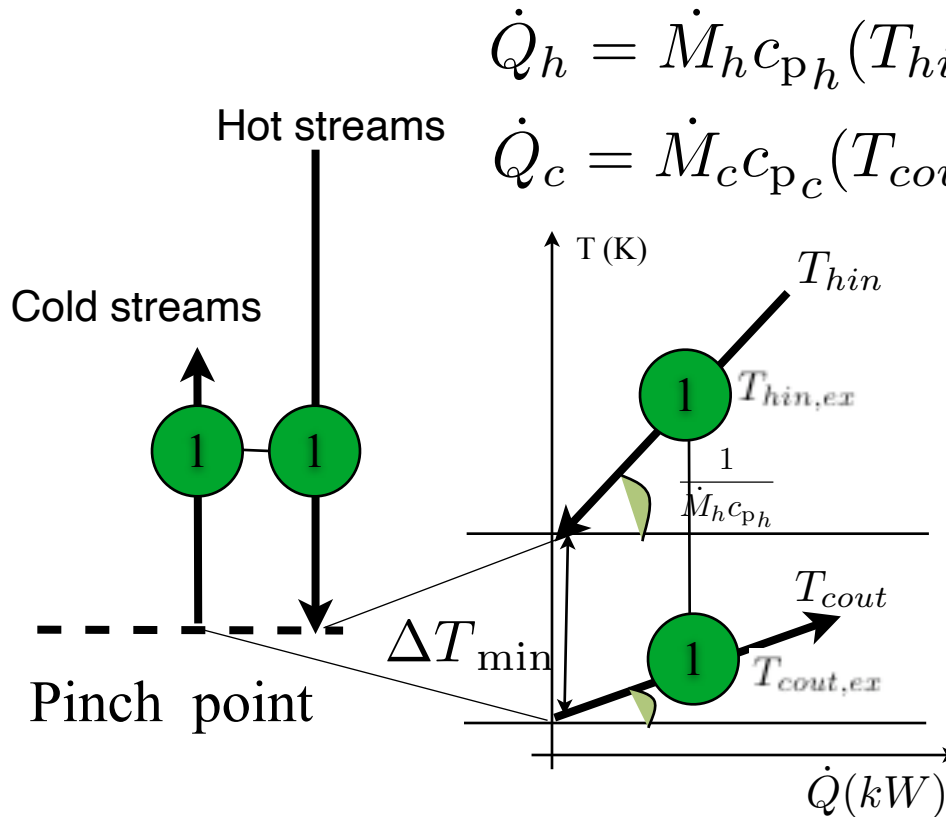
- At the pinch point : i.e. for pinch streams
 - Temperature difference is known : ΔT_{min}
 - Above (or Below) the goal is known
 - above : cool down to pinch without cold utility
 - below : heat up to pinch without hot utility
- => **Feasibility rules for pinch heat exchangers**
 - Number of streams
 - Cp rule

“this allows to select in the list of streams the one that could be potentially connected”

- What is the heat load ?

Tick off rule : satisfy the heat load of one stream

In order to satisfy the minimum number of units rule



$$\dot{Q}_h = \dot{M}_h c_{ph} (T_{hin} - (T_p^* + \Delta T_{min}/2))$$

$$\dot{Q}_c = \dot{M}_c c_{pc} (T_{cout} - (T_p^* - \Delta T_{min}/2))$$

Above the pinch

Calculation starts from the pinch and goes to higher temperatures

Both side !!!

We calculate the inlet conditions of the hot stream and the outlet conditions of the cold stream

$$\dot{Q} = \min(\dot{M}_c c_{pc} (T_{cout} - (T_p^* - \Delta T_{min}/2)), \dot{M}_h c_{ph} (T_{hin} - (T_p^* + \Delta T_{min}/2)))$$

$$\Rightarrow T_{hin,ex}, T_{cout,ex}$$

$$T_{hin,ex} = T_p^* + \Delta T_{min}/2 + \frac{\dot{Q}}{\dot{M}_h c_{ph}}$$

$$T_{cout,ex} = T_p^* - \Delta T_{min}/2 + \frac{\dot{Q}}{\dot{M}_c c_{pc}}$$

Heuristic rules

1 - Order the streams by decreasing C_p

Goals :

Above the pinch point: cool down the hot streams without cold utilities.

Below the pinch point : heat up the cold streams without hot utilities.

Start with pinch exchangers

2 - verify feasibility rules and split if no connection found

3 - The heat load is calculated to satisfy the heat load of one of the two stream involved : “tick-off”

- work from the pinch

4 - Place the utilities at the end of the streams (control purposes)

Remaining problem analysis

Initial problem

Hot stream

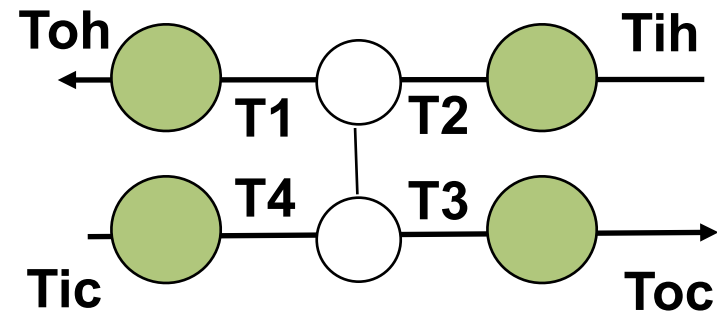
T_{ih} -> T_{oh}

Cold stream

T_{ic} -> T_{oc}

=> calculate heat cascade => $\dot{Q}^{+0}$

Place a heat exchanger



Remaining problem

New Hot streams:

T_{ih} -> T₂

T₁ -> T_{oh}

New Cold streams:

T_{ic} -> T₄

T₃ -> T_{oc}

=> calculate heat cascade $\dot{Q}^{+r}$

if $\dot{Q}^{+r} = \dot{Q}^{+0}$

=> Exchanger is well placed

When placing a heat exchanger, the remaining problem analysis consist of calculating the heat recovery with and without the heat exchanger in place (if it is in place the hot and cold streams in the heat exchanger are not anymore considered in the heat cascade). If the minimum energy requirement to close the heat cascade is not changed, the heat exchanger is well placed because it not create an energy penalty in the heat recovery

The synthesis of the HEN synthesis algorithm

